



California Energy Commission Staff Workshop Present and Future Central Station Renewable Plant Costs April 16, 2009





Input for Levelized Cost of Generation Model

California Energy Commission Contract Number 500-06-014 KEMA Inc, Oakland, CA Workshop Presentation

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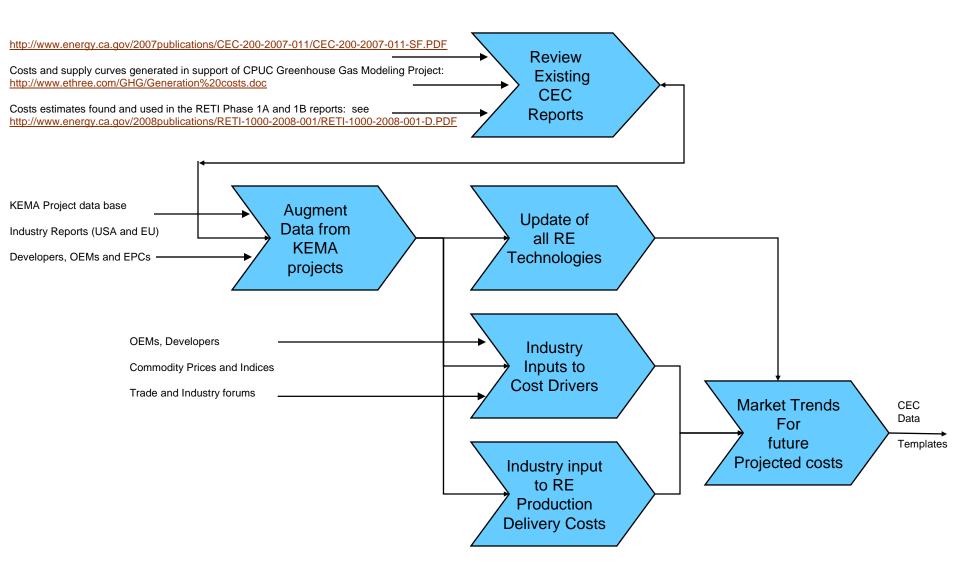
Approach and Methodology

The research team undertook the following approach:

- Conducted a technical and analytical critique of reference documents, including:
- Comparative Costs of California Central Station Electricity Generation Technologies. California Energy Commission Final Staff Report. December 2007. CEC-200-2007-011-SF.
- Costs and supply curves generated in support of CPUC Greenhouse Gas Modeling Project: http://www.ethree.com/GHG/Generation%20costs.doc
- Costs estimates found and used in the RETI Phase 1A and 1B reports: see
 http://www.energy.ca.gov/2008publications/RETI-1000-2008-001/RETI-1000-2008-001-D.PDF
- Recommended utility-scale RE technologies for cost analysis with technical and market justification.
 Utility-scale RE technologies are generally defined as those over 20MW.
- Identified the primary existing commercial embodiment of each utility-scale technology in California.
- Identified the expected primary commercial embodiment in the year 2018.
- Note that the research team will revisit Task 1 for the community and building-scale technologies in the second phase of the project and include findings in the Final Project Report.



Approach & Methodology – Tasks 1 to 4



Technology Selection Criteria

The research team used selection criteria similar to the following:

Example Sample criteria:

- is the technology commercially available and is anyone using it?
- how many projects worldwide are initiated?
- is the technology commercial somewhere, not necessarily in CA.
- what is the industrial capacity that would apply to CA?
- are there any things that make it difficult to make it viable in CA?
- what's going on in the world, what's commercial, what's being purchased,
- what's viable in CA and what could become viable, and what would it take to make it viable?
- political climate (for nuclear, off shore wind, etc)



Renewable Energy Technologies - Central Station

Technology List	Gross Capacity (MW)	Data Start Date
Biomass		
Biomass Combustion - Fluidized Bed Boiler	28	Current
Biomass Combustion - Stoker Boiler	38	Current
Biomass Cofiring	20	Current
Biomass Co-Gasification IGCC	30	2018
Geothermal		
Geothermal – Binary	50	Current
Geothermal - Flash	50	Current
Hydropower		
Hydro - Small Scale (developed sites without power)	15	Current
Hydro - Capacity upgrade for developed sites with power	80	Current
Solar		
Solar - Parabolic Trough	250	Current
Solar - Photovoltaic (Single Axis)	25	Current
Wind		
Onshore Wind - Class 5	50	Current
Onshore Wind - Class 3/4	50	Current
Offshore Wind - Class 5	350	2018
Wave		
Ocean Wave	40	2018
IGCC without carbon capture - Current commercial scale: single or multiple 300 MW trains	300	Current
Nuclear		
Nuclear: WESTINGHOUSE - AP1000	1100	Current



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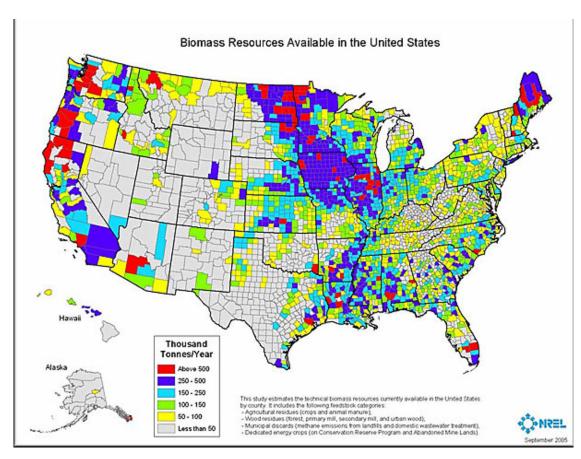


Biomass – Technologies / US Resource Map

California has significant biomass potential – in both northern and southern geographies.

Biomass Technologies Selected:

- □Biomass Combustion Stoker Boiler
- □ Biomass Combustion Fluidized Bed Boiler
- **□**Biomass Cofiring
- ☐Biomass Co-Gasification IGCC





Biomass – Stocker Boiler Technology Selection Criteria

Biomass combusted using Stocker boiler technology in ~40MW unit size was selected based on reference plants in operation

Technology
Reference
Material and
Key
Assumptions

Biomass Combustion with Stoker Boiler

Stoker boilers have been a standard technology option for biomass as well as coal for many years. A stoker boiler is an excellent combustor of cellulose waste such as wood, garbage, bagasse, industrial residue, peanut shells and shredded tires. Most of these fuels can be burned without auxiliary fuel given proper attention to moisture content.

In a stoker boiler, biomass is added in a thin layer on a grate near the bottom of the boiler. This provides a more even distribution of feed material.

Mature, most commonly used technology. Incremental improvements being made to increase steam temperature and pressure

Reference Material: see "Task 1- Central Plant Technologies.xls"

Biomass – Stoker Boiler Selected Technology Description

Biomass combusted using Stoker boiler technology in ~40MW unit size was selected based on reference plants in operation

Typical Plant



Burney Plant CHP, woody Biomass Stoker Boiler 1 x 28.4MW

Description

In a **stoker boiler**, biomass is added in a thin layer on a grate near the bottom of the boiler. This provides a more even distribution of feed material.

Mature, most commonly used technology. Incremental improvements being made to increase steam temperature and pressure

Biomass – Stoker Boiler Cost Drivers

Stoker Boiler Technology is well established and a simple BTU extraction process

Cost Drivers

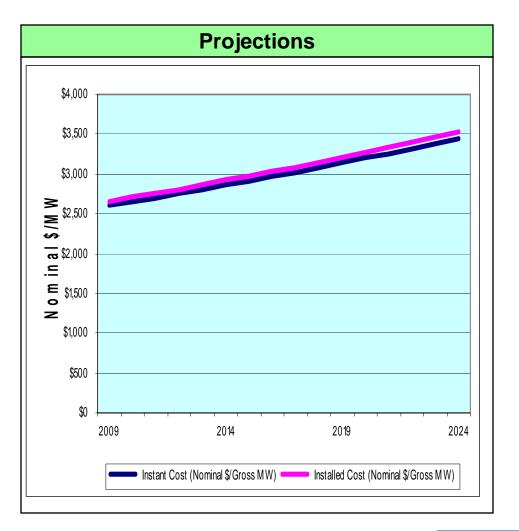
Key Cost Drivers

- Type of Biomass used
- •Fuel (Biomass) transport and handling equipment
- The boiler island cost
- Type and cost of emission control equipment (SCR/SNCR).
- Greenfield or retrofit of existing plant

Plant Configuration Data Overview PLANT DATA Average High Low Gross Capacity (MVV) 38 38 25 2.40% Station Service (%) 2.40% 2.40% 37.09 24.40 Net Capacity (MVV) 37.09 276 309 160 Net Energy (GVVh) Transformer Losses 0.50% 0.50% 0.50% Tranmission losses 1.49% 1.49% 1.49% Load Center Delivered Capacity (MW) 36.35 36.35 23.92 Net Capacity Factor (NCF) 85.00% 95.00% 75.00% Planned Percent of Year Operational 85.43% 97.57% 75.47% Average Percent Output 100.0% 100.0% 100.0% Net Energy Delivered to Load Center (GVVh) 270.68 302.53 157.13 Forced Outage Rate (FOR) 0.50% 1.50% 0.25% Scheduled Outage Factor (SOF) 0.77% 1.15% 0.38% Curtailment (Hours) 60 120 0 Degradation Factors Capacity Degradation (%/Year) 0.10% 0.20% 0.00% Heat Rate Degradation (%/Year) 0.15% 0.20% 0.10% Emission Factors NOX (lbs/MWh) 0.075 0.075 0.075 0.012 VOC/ROG (Lbs/M/Vh) 0.012 0.012 CO (Lbs/MWh) 0.105 0.105 0.105 CO2 (lbs/MVVh) 0.000 0.000 0.000 SOX (lbs/MV/h) 0.034 0.034 0.034 PM10 (lbs/MV/h) 0.100 0.200 0.025

Biomass – Stoker Boiler Current Cost and Cost Trajectory

Current Costs			
PLANT COST DATA	Start Y	еаг	2009
Average			
Instant Cost (Nominal \$/Gro	ss MVV)		\$2,600
Installed Cost (Nominal \$/Gr	oss MVV)		\$2,658
% Cost of last year of cons	struction		80%
% Cost next to last year of	construction	on	20%
% Cost of previous year of	constructi	on	
High			
Instant Cost (Nominal \$/Gro	ss MVV)		\$3,250
Installed Cost (Nominal \$/Gr			\$3,323
% Cost first year of constru			50%
% Cost second year of cor			40%
% Cost third year of constr			10%
Low			
Instant Cost (Nominal \$/Gro	ss MVV)		\$1,750
Installed Cost (Nominal \$/Gr			\$1,789
% Cost first year of constru			90%
% Cost second year of cor			10%
% Cost third year of constr			
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$MW-Year)	\$16.01	\$20.00	\$10.78
Variable Cost (\$/M/Vh)	\$6.98	\$8.73	\$4.70



Biomass – Fluidized Bed Boiler Technology Selection Criteria

Biomass combusted using Fluidized Bed boiler technology in ~30MW unit size was selected based on reference plants in operation

Biomass Combustion with Fluidized Bed Boiler

Technology
Reference
Material and
Key
Assumptions

Circulating fluidized bed (CFB) technology is used for combustion of solid fuels. It was first used due to its ability to handle low quality, high sulphur coals. One of the main advantages of the CFB technology is that it allows the owner to optimize profitability by selecting a wide range of fuels (bituminous coal, bituminous gob or high-ash waste coal, subbituminous coal, lignite and brown coal, anthracite culm, coal cleaning tailings and petroleum coke). Other fuels such as wood, shredded tires, and sludge are fuel candidates depending on their heat input, moisture content and emissions requirements. This type of boiler provides economy and flexibility.

In a fluidized-bed boiler, combustors burn biomass fuel in a bed of hot granular material. Air is injected at a high-rate underneath the bed to create the appearance of a boiling liquid. This helps to evenly distribute the fuel.

Relatively mature technology - fluidized bed combustors are becoming the systems of choice for biomass fuels, due to good fuel flexibility and good emissions characteristics

Reference Material: see "Task 1- Central Plant Technologies.xls"

Biomass – Fluidized Bed Boiler Selected Technology Description

Biomass combusted using Fluidized Bed boiler technology in ~30MW unit size was selected based on reference plants in operation

Typical Plant Fibrominn, Benson Plant, Turkey Litter Plant, MN

Description

Compared to a stoker boiler system a fluidized-bed boiler:

- Proven technology which optimizes combustion for a variety of fuels
- Achieves a higher carbon burn-out.
- Ensures more fuel flexibility due to the good mixing that occurs on the fluidized bed.
- The relatively low combustion temperature ensures reduced NOx emissions, and the CFB process allows for the addition of certain minerals into the bed to control SOx emissions.

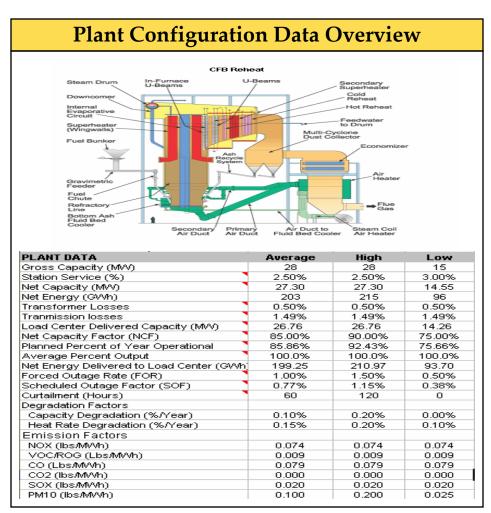
Biomass – Fluidized Bed Boiler Cost Drivers

Fluidized Bed Boiler Technology is well established, efficient BTU extraction process

Cost Drivers

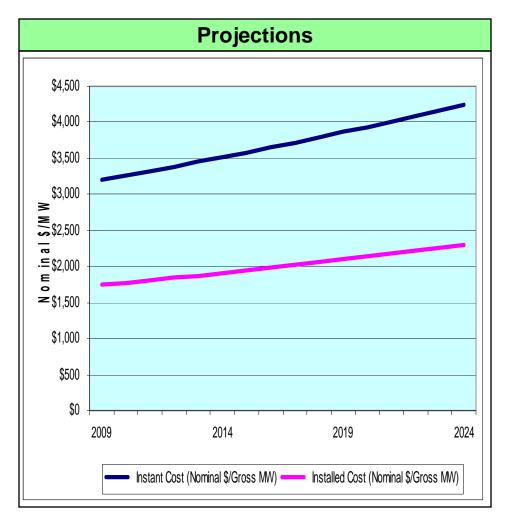
Key Cost Drivers

- Type of Biomass used
- •Fuel (Biomass) transport and handling equipment
- The boiler island cost
- Type and cost of emission control equipment (SCR/SNCR).
- Greenfield or retrofit of existing plant
- O&M costs



Biomass – Fluidized Bed Boiler Current Cost and Cost Trajectory

PLANT COST DATA Average Instant Cost (Nominal \$/Gross			
Instant Cost (Nominal \$/Gross			
	s MVV)		\$3,200
Installed Cost (Nominal \$/Gros	ss MVV)		\$1,740
% Cost of last year of constr	uction		80%
% Cost next to last year of co	onstruction		20%
% Cost of previous year of c	onstruction		
High			
Instant Cost (Nominal \$/Gross	s MVV)		\$4,800
Installed Cost (Nominal \$/Gros	ss MVV)		\$4,975
% Cost first year of construc	tion		60%
% Cost second year of const	truction		40%
% Cost third year of construc	tion		0%
Low			
Instant Cost (Nominal \$/Gross	s MVV)		\$1,600
Installed Cost (Nominal \$/Gros	ss MVV)		\$1,740
% Cost first year of construc	tion		100%
% Cost second year of const	truction		
% Cost third year of construc	tion		
Year=2009, Value & Dollars	Average	High	Low
ixed Cost (\$/KW-Year)	\$15.0	\$9.95	\$7.00
ariable Cost (\$/M/Vh)	\$10.00	\$4.47	\$3.00



Biomass – Cofiring Technology Selection Criteria

Cofiring Biomass combusted using an existing coal fired plant is an optimal use of existing assets to displace coal BTUs

Technology
Reference
Material and
Key
Assumptions

Cofiring Biomass in existing Coal Plant

Biomass co-fi ring at coal-burning power plants helps to reduce net carbon dioxide emissions, providing a necessary break for the environment. Co-firing is also economically attractive for electricity producers as many national governments provide tax benefits and other statutory and financial incentives to encourage the practice. Moreover, biomass co-fi ring is a good way for a power producer to demonstrate awareness of its corporate social responsibilities.

There is much more to co-fi ring than simply adding a secondary fuel to the coal. A power producer wishing to introduce a bio-fuel to the mix used at a plant must address numerous economic, logistic, technical and environmental considerations:

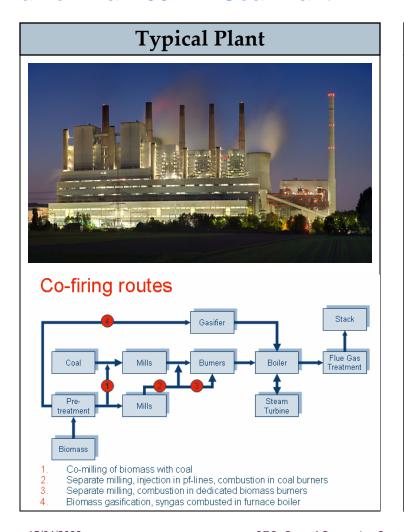
- Is the capital cost justified by the economic benefits of supplying green power or reducing CO2 emissions?
- How do we decide on the best ratio of biomass to coal?
- How will biomass co-fi ring influence the plant in the shorter and longer term?
- Will emissions from the plant still be within the legal limits? And will the ash produced still be saleable?

At a minimum, it is necessary to gain a clear picture of the risks involved and the options for managing them.

Reference Material: see "Task 1- Central Plant Technologies.xls"

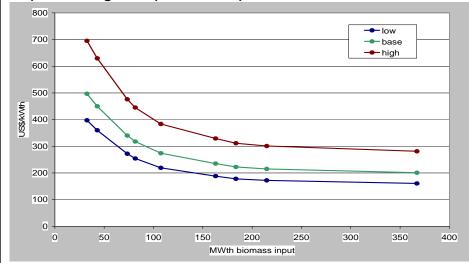
Biomass – Cofiring Selected Technology Description

Biomass can be cofired in any coal plant and from 5% to 30% ratio. We selected a nominal 100MW Coal Plant



Description

- Cofiring technology makes use of an existing coal fired power plant
- Experience has been gained in injection of Biomass in various points into the fuel feed or combustion point
- The analysis has selected low (10%), average (20%) and high (40%) cases where the cofiring percentages represent equivalent MWe





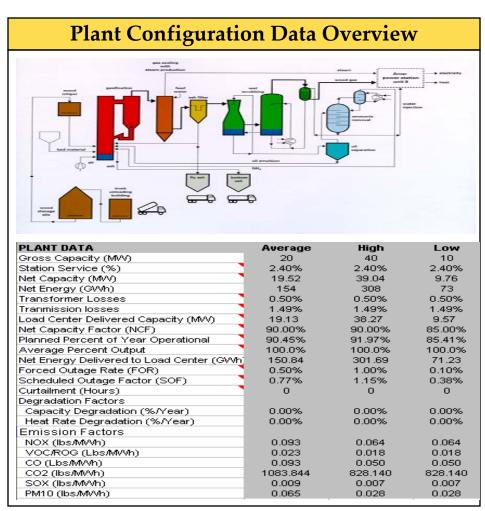
Biomass – Cofiring Cost Drivers

Cofiring Technology is well established and an optimal way to replace coal with renewable energy

Cost Drivers

Key Cost Drivers

- Type of Biomass used
- •Fuel (Biomass) transport and handling equipment
- Fuel feed modifications
- Type and cost of emission control equipment (SCR/SNCR).
- Percentage of cofiring deployed

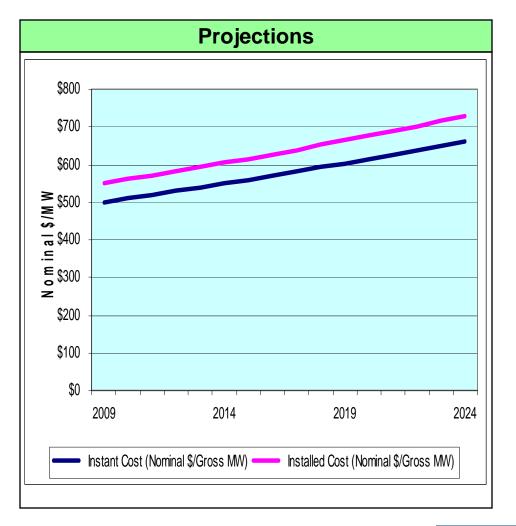




Biomass – Cofiring Current Cost and Cost Trajectory

Very attractive costs per MW!

Current Costs			
	Start Year	r 2	D09
PLANT COST DATA			
Average			
Instant Cost (Nominal \$/Gros			\$500
Installed Cost (Nominal \$/Gro	oss MVV)		\$550
% Cost of last year of const	ruction		100%
% Cost next to last year of d	construction		
% Cost of previous year of	construction		
High			
Instant Cost (Nominal \$/Gros	s MVV)		\$700
Installed Cost (Nominal \$/Gro			\$770
% Cost first year of constru			100%
% Cost second year of cons			
% Cost third year of constru			
Low			
Instant Cost (Nominal \$/Gros	s MVV)		\$400
Installed Cost (Nominal \$/Gro	•		\$440
% Cost first year of constru			100%
% Cost second year of cons			
% Cost third year of constru			
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$/k/V/-Year)	\$15.0	\$21.00	\$12.00
Variable Cost (\$/MV/h)	\$1.27	\$1.78	\$1.02



Biomass – Co-Gasification IGCC Technology Selection Criteria

Co Gasification of Biomass using IGCC

Technology
Reference
Material and
Key
Assumptions

Co Gasification using IGCC

This technology gives biomass access to the higher efficiencies of gas fired power generation and combined cycles

Key characteristics of the system is:

Direct (single stage and autothermal), pressurized, fluidized bed gasifier

Heat exchanger to 400C prior to hot gas filter for dust removal (tar removal is not necessary)

Cleaned gas is a combusted in a gas turbine, which also supplies the gasifier with pressurized air from the compressor Residual heat is used in a steam cycle

Commercial deployment of this technology can only be justified with a large plant and a sound biomass supply infrastructure.

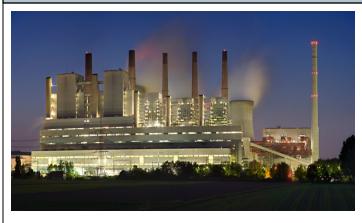
Demonstration plants have been built, mainly in Europe with many technology and reliability issues emerging

Reference Material: see "Task 1- Central Plant Technologies.xls"

Biomass – Co Gasification IGCC Selected Technology Description

Biomass can be gasified and the syngas used in a classical IGCC plant

Typical Plant



?

Description

- This technology gives biomass access to the higher efficiencies of gas fired power generation and combined cycles
- Key characteristics of the system we will profile
 - Direct (single stage and autothermal), pressurized, fluidized bed gasifier
 - Heat exchanger to 400C prior to hot gas filter for dust removal (tar removal is not necessary)
 - Cleaned gas is a combusted in a gas turbine, which also supplies the gasifier with pressurized air from the compressor
 - Residual heat is used in a steam cycle
- Commercial deployment of the technology has not occurred. One demonstration BIGCC unit has been built in Europe but it is no longer in operation.
 - Information on actual capital and operating costs is limited



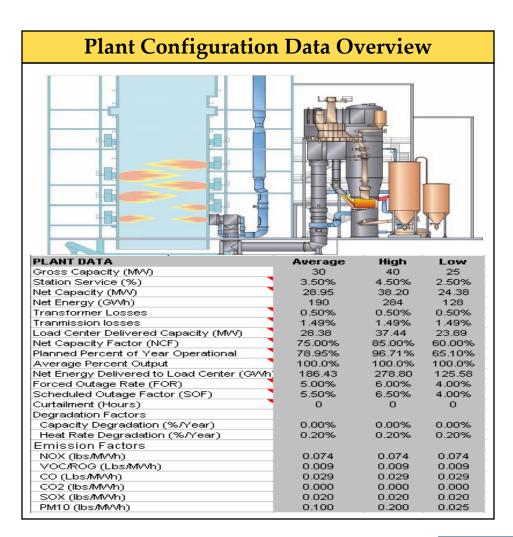
Biomass – Co Gasification IGCC Cost Drivers

Co Gasification with IGCC is an emerging technology

Cost Drivers

Key Cost Drivers

- Type of Biomass used
- •Fuel (Biomass) transport and handling equipment
- •Type of gasification used (i.e Shell, FB gasifier...)
- Type and cost of emission control equipment (SCR/SNCR).
- Type of cycle selected (CT CC or Direct into Boiler)





Biomass – Co Gasification IGCC Current Cost and Cost Trajectory

This technology is projected to be viable in 2018

Current Costs			
PLANT COST DATA	Start Year	20	909
Average			
Instant Cost (Nominal \$/Gross	MVV)		\$2,950
Installed Cost (Nominal \$/Gros	s MVV)		\$3,150
% Cost of last year of constru	iction		75%
% Cost next to last year of co	nstruction		25%
% Cost of previous year of co	nstruction		
High			
Instant Cost (Nominal \$/Gross	MVV)		\$3,688
Installed Cost (Nominal \$/Gros	s MVV)		\$3,938
% Cost first year of construct	ion		50%
% Cost second year of constr	uction		40%
% Cost third year of construct			10%
Low			
Instant Cost (Nominal \$/Gross	MVV)		\$2,655
Installed Cost (Nominal \$/Gros			\$2,835
% Cost first year of construct			100%
% Cost second year of constr			
% Cost third year of construct			
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$/kW-Year)	\$150.0	\$175.00	•
Variable Cost (\$MMVh)	\$4.00	\$4.50	\$3.00

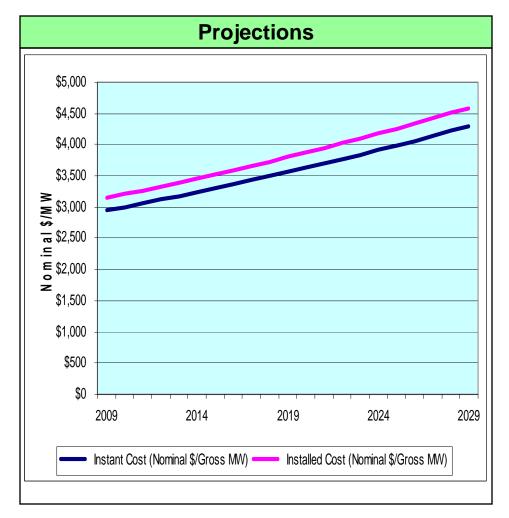


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Geothermal - Binary Technology Selection Criteria

Geothermal technology deploys the basic technology of the Steam Turbine Generator.

Technology
Reference
Material and
Key
Assumptions

Geothermal – Technologies

There are four commercial types of geothermal power plants:

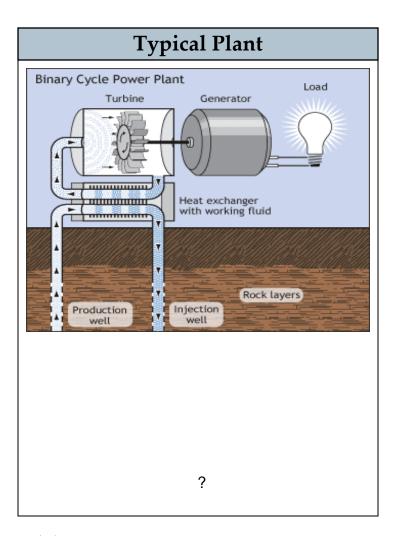
- (a) flash power plants,
- (b) dry steam power plants,
- (c) binary power plants, and
- (d) flash/binary combined power plants

The analysis focuses on Fash and Binary geothermal power plants

Reference Material: see "Task 1- Central Plant Technologies.xls"

Geothermal - Binary Selected Technology Description

Geothermal – Binary technology



Description

Binary Power Plant: Recent advances in geothermal technology have made possible the economic production of electricity from geothermal resources lower than 150°C (302°F). Known as binary geothermal plants, the facilities that make this possible reduce geothermal energy's already low emission rate to zero. Binary plants typically use an Organic Rankine Cycle system. The geothermal water (called "geothermal fluid" in the accompanying image) heats another liquid, such as isobutane or other organic fluids such as pentafluoropropane. which boils at a lower temperature than water. The two liquids are kept completely separate through the use of a heat exchanger, which transfers the heat energy from the geothermal water to the working fluid. The secondary fluid expands into gaseous vapor. The force of the expanding vapor, like steam, turns the turbines that power the generators. All of the produced geothermal water is injected back into the reservoir.

Geothermal - Binary Cost Drivers

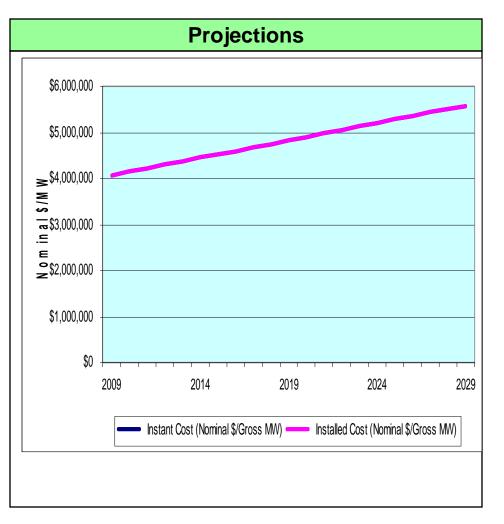
Geothermal Binary technology uses a heat exchanger to

Cost Drivers Key Cost Drivers Site geographies Turbine Island Exploration Confirmation Drilling Steam gathering Royalties **M**&0

Plant Configuration Data Overview			
PLANT DATA	Average	High	Low
Gross Capacity (MVV)	50	50	50
Station Service (%)	0.50%	0.50%	0.50%
Net Capacity (MVV)	49.75	49.75	49.75
Net Energy (GWh)	405	405	405
Transformer Losses	0.50%	0.50%	0.50%
Tranmission losses	1.49%	1.49%	1.49%
Load Center Delivered Capacity (MVV)	48.76	48.76	48.76
Net Capacity Factor (NCF)	93%	93%	93%
Planned Percent of Year Operational	100.0%	100.0%	100.0%
Average Percent Output	93.84%	93.84%	93.84%
Net Energy Delivered to Load Center (GWh)	397	397	397
Forced Outage Rate (FOR)	0.6%	0.6%	0.6%
Scheduled Outage Factor (SOF)	0.30%	0.30%	0.30%
Curtailment (Hours)	0.0	0.0	0.0
Degradation Factors			
Capacity Degradation (%/Year)	4.00%	4.00%	4.00%
Heat Rate Degradation (%/Year)	N/A	N/A	N/A
Emission Factors			
NOX (lbs/M/Vh)	N/A	N/A	N/A
VOC/ROG (Lbs/M/Vh)	N/A	N/A	N/A
CO (Lbs/M/Vh)	N/A	N/A	N/A
CO2 (lbs/M/Vh)	N/A	N/A	N/A
SOX (lbs/M/Vh)	N/A	N/A	N/A
PM10 (lbs/M/Vh)	N/A	N/A	N/A

Geothermal - Binary Current Cost and Cost Trajectory

Current C	osts		
PLANT COST DATA	Start Ye	аг	2009
Average			
Instant Cost (Nominal \$/Gross MVV)		\$4	,070,000
Installed Cost (Nominal \$/Gross MVV)		\$4	,070,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MVV)		\$4	,070,000
Installed Cost (Nominal \$/Gross M/V)		\$4	,070,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross M/V)		\$4	,070,000
Installed Cost (Nominal \$/Gross M/V)		\$4	,070,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
V 2000 V-I 0 D-II		II:_L	
Year=2009, Value & Dollars Fixed Cost (\$AWV-Year)	Average \$47,44	High 647,44	Low \$47.44
, ,	•	\$4.40	\$4.40
Variable Cost (\$M/Vh)	Φ4.4U	Φ4.4U	⊅4.40



Geothermal - Flash Technology Selection Criteria

Geothermal – Flash

Technology
Reference
Material and
Key
Assumptions

Geothermal – Flash

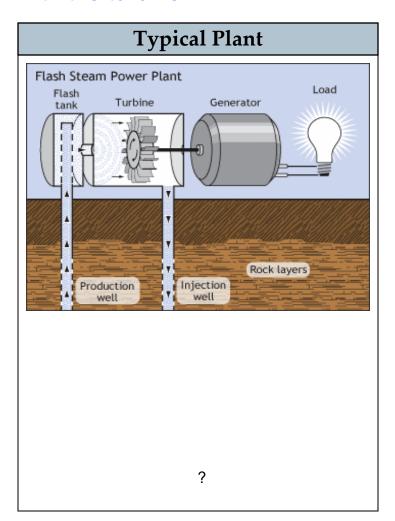
Flash Power Plant: Geothermally heated water under pressure is separated in a surface vessel (called a steam separator) into steam and hot water (called "brine" in the accompanying image). The steam is delivered to the turbine, and the turbine powers a generator. The liquid is injected back into the reservoir.

Other configurations employ both Flash and Binary in a Combined Cycle: This type of plant, which uses a combination of flash and binary technology, has been used effectively to take advantage of the benefits of both technologies. In this type of plant, the portion of the geothermal water which "flashes" to steam under reduced pressure is first converted to electricity with a backpressure steam turbine and the low-pressure steam exiting the backpressure turbine is condensed in a binary system.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Geothermal - Flash Selected Technology Description

Geothermal – Flash technology results in direct geo steam coming into contact with the turbine



Description

Flash Power Plant: Geothermally heated water under pressure is separated in a surface vessel (called a steam separator) into steam and hot water (called "brine" in the accompanying image). The steam is delivered to the turbine, and the turbine powers a generator. The liquid is injected back into the reservoir..

Geothermal - Flash Cost Drivers

Geothermal Binary emerging technology

Cost Drivers

Key Cost Drivers

- Site geographies
- Turbine Island
- Exploration
- Confirmation Drilling
- Steam gathering
- Royalties
- **M**&0

Plant Configuration Data Overview			
PLANT DATA	Average	High	Low
Gross Capacity (MW)	50	50	50
Station Service (%)	0.50%	0.50%	0.50%
Net Capacity (MW)	49.75	49.75	49.75
Net Energy (GWh)	392	392	392
Transformer Losses	0.50%	0.50%	0.50%
Tranmission losses	1.49%	1.49%	1.49%
Load Center Delivered Capacity (MW)	48.76	48.76	48.76
Net Capacity Factor (NCF)	90%	90%	90%
Planned Percent of Year Operational	100.0%	100.0%	100.0%
Average Percent Output	90.82%	90.82%	90.82%
Net Energy Delivered to Load Center (GWh)	384	384	384
Forced Outage Rate (FOR)	0.6%	0.6%	0.6%
Scheduled Outage Factor (SOF)	0.30%	0.30%	0.30%
Curtailment (Hours)	0.0	0.0	0.0
Degradation Factors			
Capacity Degradation (%/Year)	4.00%	4.00%	4.00%
Heat Rate Degradation (%/Year)	N/A	N/A	N/A
Emission Factors			
NOX (lbs/MVVh)	0.191	0.191	0.191
VOC/ROG (Lbs/MWh)	0.011	0.011	0.011
CO (Lbs/MWh)	0.058	0.058	0.058
CO2 (lbs/MVVh)	N/A	N/A	N/A
SOX (lbs/MWh)	0.026	0.026	0.026
PM10 (lbs/MWh)	N/A	N/A	N/A

Geothermal - Flash Current Cost and Cost Trajectory

Current Costs			
PLANT COST DATA	Start	Year	2009
Average			
Instant Cost (Nominal \$/Gross MW)	1		\$3,675,000
Installed Cost (Nominal \$/Gross MV	V)		\$3,675,000
% Cost first year of construction			100%
% Cost second year of construction	ı		
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MW))		\$3,675,000
Installed Cost (Nominal \$/Gross MV	V)		\$3,675,000
% Cost first year of construction			100%
% Cost second year of construction	ı		
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross MVV)	1		\$3,675,000
Installed Cost (Nominal \$/Gross MV	V)		\$3,675,000
% Cost first year of construction			100%
% Cost second year of construction	1		
% Cost third year of construction			
Year=2009, Value & Dollars	Average	High	ı Low
Fixed Cost (\$/kW-Year)	\$54.38	\$54.30	8 \$54.38
Variable Cost (\$/MWh)	\$5.28	\$5.28	\$5.28

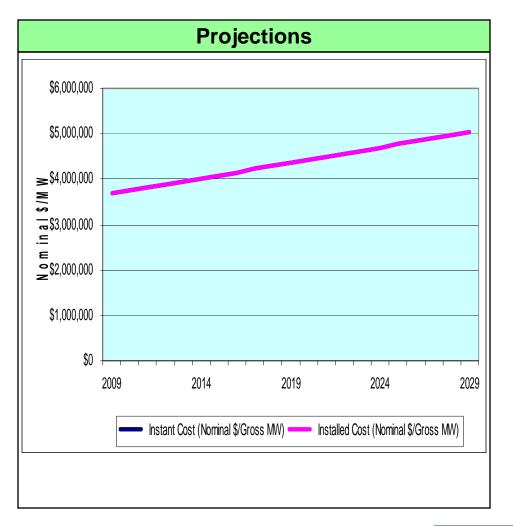


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Wave
IGCC
Nuclear
Reference to IEPR 2007 data



Hydro Technology Selection Criteria

Hydro Generation - General

Technology
Reference
Material and
Key
Assumptions

Hydro:

Hydroelectric power is generated by capturing the kinetic energy of water as it moves from a higher elevation to a lower elevation by passing it through a turbine. The amount of kinetic energy captured by a turbine is dependent on the head (vertical height the water is falling) and the flow rate of the water. Often, the water is raised to a higher potential energy by blocking its natural flow with a dam. If a dam is not feasible, it is possible to divert water out of the natural waterway, through a penstock, and back to the waterway. Such applications allow for hydroelectric generation without the impact of damming the waterway. There are three main types of hydropower facilities:

Impoundment Hydropower - utilizes a dam to store water in a reservoir. Water can be released from the reservoir to generate electricity.

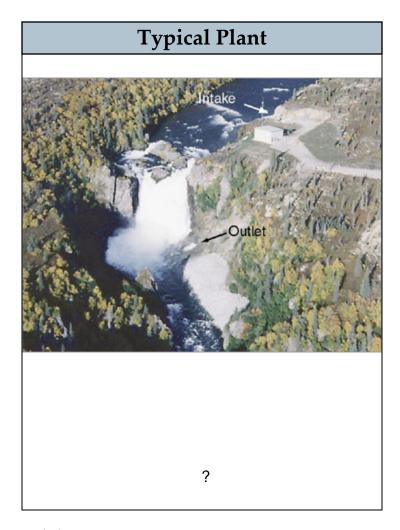
Run-of-River - utilizes the flow of water within a river, requiring very little or no impoundment. Run-of-River hydropower is typically designed for large flows with low head or small flows with high head.

Diversion Hydropower – diverts a portion of river flows through a canal or penstock to generate electricity.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Hydro – Small Scale Selected Technology Description

Small Scale Hydro



Description

The most common type of hydroelectric power plant is an impoundment facility. An impoundment facility, typically a large hydropower system, uses a dam to store river water in a reservoir. Water released from the reservoir flows through a turbine, spinning it, which in turn activates a generator to produce electricity. The water may be released either to meet changing electricity needs or to maintain a constant reservoir level.

In-Conduit Hydropower: Developed within man-made conduits instead of natural rivers, streams or creeks. Key advantages include no impact on wildlife, reduced O&M due to the cleanliness of the water, more streamlined permitting processes, and often less civil works. "Man-made conduits" include pipelines, aqueducts, irrigation ditches and canals.

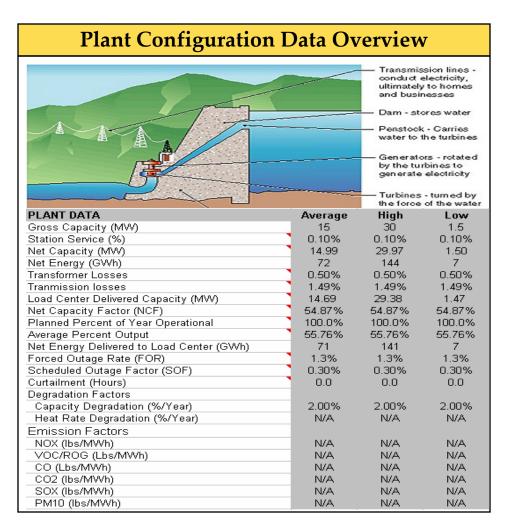
Hydro – Small Scale Cost Drivers

Small Scale Hydro selected in ranges from 1.5MW, 15MW and 30MW

Cost Drivers

Key Cost Drivers

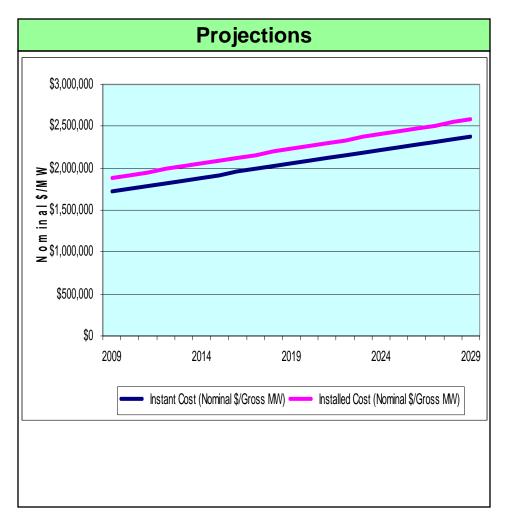
- Site geographies
- Licensing
- Environmental mitigation
- Fixed and variable O&M
- FERC annual Charge





Hydro – Small Scale Current Cost and Cost Trajectory

Current Costs			
PLANT COST DATA	Start Year	2009	
Average			
Instant Cost (Nominal \$/Gross MVV)	•	\$1,730,000	
Installed Cost (Nominal \$/Gross MW)	•	\$1,882,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MVV)		\$1,503,000	
Installed Cost (Nominal \$/Gross MW)		\$1,628,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross MVV)		\$2,770,000	
Installed Cost (Nominal \$/Gross MW)		\$3,046,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
Year=2009, Value & Dollars Av	verage Hig	h Low	
Fixed Cost (\$/kW-Year)	17.57 \$15.2	26 \$31.57	
Variable Cost (\$/MWh)	\$3.48 \$3.00	2 \$5.54	



Hydro – Capacity Upgrades Technology Selection Criteria

Technology
Reference
Material and
Key
Assumptions

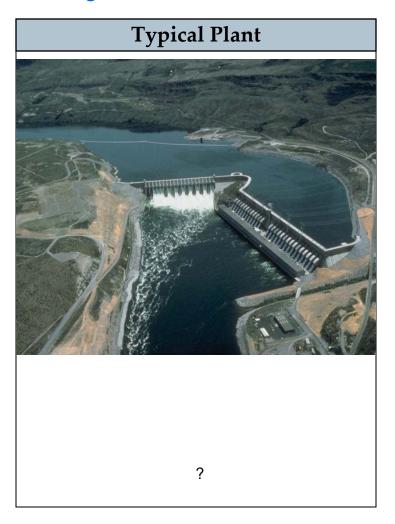
<u> Hydro – Capacity Upgrades</u>

Hydro - Capacity upgrade for developed sites with power:
Some existing hydroelectric facilities in California and the surrounding states are developed with power generation in place, but with potential to increase generation output. This can be accomplished through increasing reservoir size, upgrading total turbine capacity, increasing the number of turbines, or any combination thereof.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Hydro – Capacity Upgrades Selected Technology Description

Hrdro Capacity Upgrades build off current assets and create new MW's from an existing head of water



Description

- Hydroelectric power is a well established technology. The United States hydroelectric plant population is comprised of 2,388 licensed plants (not including pumped storage plants) according to the 1998 version Federal Energy Regulatory Commission's Hydroelectric Resource Assessment (HPRA) database (FERC 1998). These plants range in capacity from less than 100 kW to over 6,000 MW and have a total capacity of 74,872 MW. The plants are owned by 1,134 owners which include owners in the public and private sectors
- Upgrades to existing facilities can result in new MW capacities from 2MW, 80MW and up to 600MW

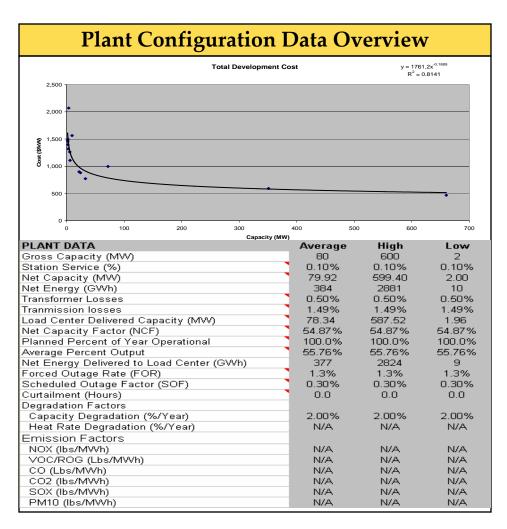
Hydro – Capacity Upgrades Cost Drivers

Capacity Upgrades Hydro

Cost Drivers

Key Cost Drivers

- Site geographies
- Licensing
- Environmental mitigation
- Fixed and variable O&M
- FERC annual Charge





Hydro – Capacity Upgrades Current Cost and Cost Trajectory

DI ANT COCT DATA	Start Year	2009
PLANT COST DATA		ı
Average		#774 000
Instant Cost (Nominal \$/Gross MVV)		\$771,000
Installed Cost (Nominal \$/Gross MW)		\$932,000
% Cost first year of construction		100%
% Cost second year of construction		
% Cost third year of construction		
High		
Instant Cost (Nominal \$/Gross MW)		\$514,000
Installed Cost (Nominal \$/Gross MVV)		\$637,000
% Cost first year of construction		100%
% Cost second year of construction		
% Cost third year of construction		
Low		
Instant Cost (Nominal \$/Gross MW)		\$1,638,000
Installed Cost (Nominal \$/Gross MW)		\$1,871,000
% Cost first year of construction		100%
% Cost second year of construction		
% Cost third year of construction		
,		
U 0000 U I 0 7 11		
<u>. </u>	werage Hig	
(,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	\$12.59 \$8.7	•
/ariable Cost (\$/MWh)	\$2.39 \$1.8	60 \$5.00

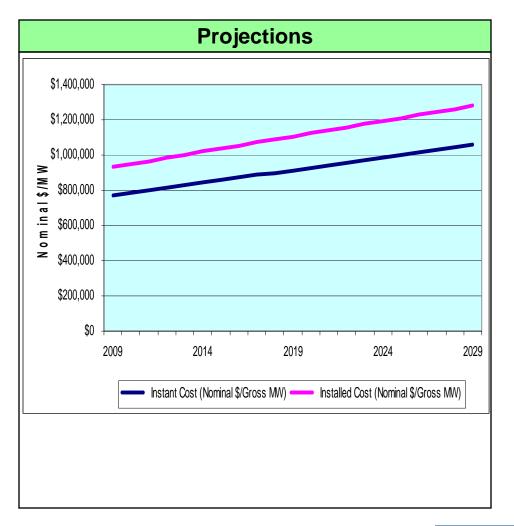




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Solar – Parabolic Trough Technology Selection Criteria

Technology Reference Material and Key Assumptions

Solar Parabolic Trough

The research team selected parabolic trough technology because it is commercially available. Installations are producing electricity with a capacity of 354 MW since 1990. With Andasol 1 -3 one parabolic trough system with 50 MW is commercially running in Spain and two additional 50 MW plants are under construction. Storage technology (molten salt) for 7 full load hours is included in the Andasol project. Storage or combined operation with gas leads to extended operation hours per day. Additional projects in Greece and Spain are under planning.

Primary commercial embodiment in California – need information here on the applications that have been filed for California.

In the year 2018, the research team expects that the primary commercial embodiment will tend towards larger systems. The current primary worldwide commercial embodiment today is in Spain, where feed-in tariffs have encouraged solar development, but system sizes are less than 50 MW due to restrictions in the feed-in tariff system. Solar Millennium has announced a 250 MW parabolic trough power station in Nevada. 1 An engineer at Solar Millennium told our research team that the system will consist of one 250 MW steam turbine (not 50 MW modules). According to the engineer at Solar Millennium, the company believes 250 MW and expects to be the optimal size for parabolic trough systems and expects future systems to range from 200 to 300 MW. For smaller systems the turbine is too small (and therefore too expensive) and for bigger systems the losses in the solar collector field would be too high. Solar Millenium Corporate News. April 3, 2009. Nevada Energy, Solar Millennium and MAN

Ferrostaal cooperate in the development of projects

Reference Material: see "Task 1- Central Plant Technologies.xls"

Solar – Parabolic Trough Selected Technology Description

Solar Parabolic Tough systems act as collectors of heat to create a boiler, steam and drive a TG set

Typical Plant

Description

For 2009, the Spanish Government has announced a change in the feed-in tariff. This will reduce the amount of new registered projects in Spain.

Nevada Energy, Solar Millenium and MAN Ferrostaal have announced a solar thermal power plant with a capacity of 250 MW and thermal storage capacity.

Abengoa Solar has signed an agreement with Arizona Public Service (APS) to build and operate what will be the largest solar power plant in the world. The plant will be installed about 100 kilometers southwest of Phoenix, near Gila Bend. Solana, with 280 MWe of power output capacity, is based on parabolic trough technology and thermal storage using molten salts. It uses a single steam turbine.

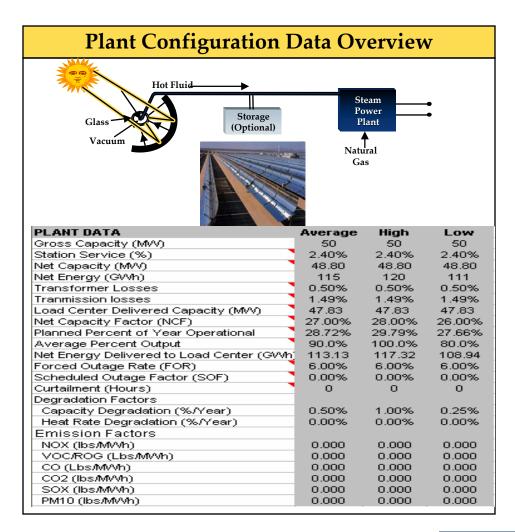
Solar – Parabolic Trough Cost Drivers

Parabolic can be integrated into existing steam cycle

Cost Drivers

Key Cost Drivers

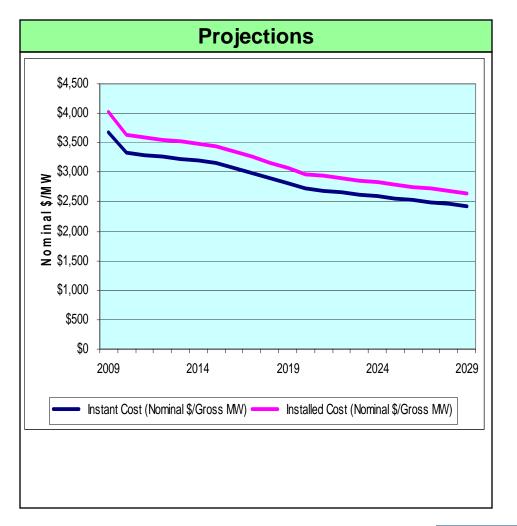
- Steam system
- Parabolic apparatus
- Land acquisition
- Fixed and variable O&M





Solar – Parabolic Trough Current Cost and Cost Trajectory

Current Costs			
PLANT COST DATA	Start Y	еаг	2009
Average			
Instant Cost (Nominal \$/Gross	: M///)		\$3,687
Installed Cost (Nominal \$/Gros	s MVV)		\$4,019
% Cost of last year of constru	uction		100%
% Cost next to last year of co	nstructi	on	0%
% Cost of previous year of co	onstructi	ion	
High			
Instant Cost (Nominal \$/Gross	: MVV)		\$3,900
Installed Cost (Nominal \$/Gros	s MVV)		\$4,251
% Cost first year of construct	tion		100%
% Cost second year of const		0%	
% Cost third year of construc	tion		
Low			
Instant Cost (Nominal \$/Gross	: MVV)		\$3,408
Installed Cost (Nominal \$/Gros		\$3,715	
% Cost first year of construct	tion		100%
% Cost second year of const			
% Cost third year of construc			
·			
Year=2009, Value & Dollars	High	Low	
Fixed Cost (\$/k/V-Year)	\$68.0	\$92.00	\$60.00
Variable Cost (\$MWh)	\$0.00	\$0.00	\$0.00
Tanasa coo (viiii ii)	V 0.00	ψσ	40.00





Solar – Photovoltaic Technology Selection Criteria

Solar PV

Technology
Reference
Material and
Key
Assumptions

Solar PV

Flat-plate Photovoltaic (FPV) modules are commercially available worldwide. The solar electricity market is booming. By the end of 2007, the cumulative installed capacity of solar PV systems around the world had reached more than 9,200 MW. This compares with a figure of 1,200 MW at the end of 2000. Installations of PV cells and modules around the world have been growing at an average annual rate of more than 35% since 1998

There are almost 880 photovoltaic power plants (put into service in 2007 or earlier), each with peak power of 200 kWp or more, are listed. Cumulative power of all these photovoltaic power plants is about 955 MWp and average plant power output is slightly more than 1.24 MWp. More than 390 large-scale photovoltaic plants are located in Germany, 225 in USA and more than 130 in Spain (source: pvresources).

The PV modules can be mounted on fixed tilt strucures or on one or two axis tracking devices. As of December 2007, the market share of fixed arrays was 73% of the total installed capacity in large-scale PV installations, only 27% were tracking systems (source: pvresources). However in situations with a high proportion of direct normal insolation, such as in California, the one-axis tracking system could increase the sunlight capture by up to 25% over traditional fixed-tilt systems, while significantly reducing land use requirements

Reference Material: see "Task 1- Central Plant Technologies.xls"

Solar – Photovoltaic Selected Technology Description

PV fixed axis installations.

Typical Plant



?

Description

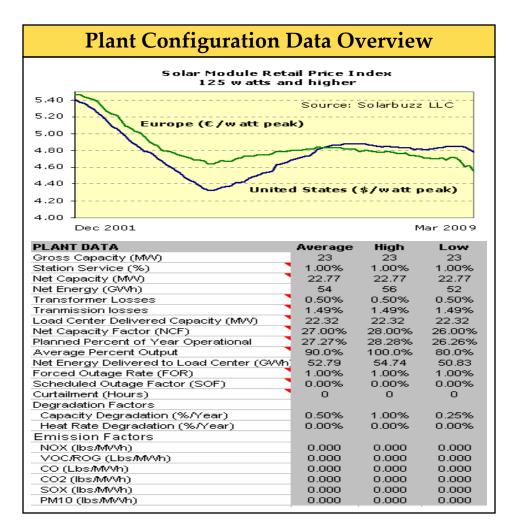
- Spain's PV market reached 2,600 MW in 2008

 (annual growth rate of more than 400%) and now accounts for 44% of the world market. Germany reached a moderate increase to 1,500 MW, while the United States increased by 220% to 500 MW. It became the world's third largest market even in front of Japan, once the world leader, which stayed stable at a level of 230 MW. (Source: BSW-Solar/EPIA/NNPVA)
- World Solar cell production doubled in comparison to 2007 (3,436 MW). Chinese manufacturers raised their share in 2008. Meanwhile, thin film production reached a remarkable market share (2007: 12%). (We expect actual market numbers for 2008 later in March from Solarbuzz).
- In 2008 an interesting trend could be observed in Spain: many large scaled PV installations have come into operation with capacities in the range of 20 to 60 MW (Source: Photon).

Solar – Photovoltaic Cost Drivers

PV increasing in capacity, driving costs down.

Cost Drivers Key Cost Drivers PV Module costs Silicon Production capacity New manufacturing Capacity Land acquisition Fixed O&M



Solar – Photovoltaic Current Cost and Cost Trajectory

Current Costs				
PLANT COST DATA	Start Y	еаг	2009	
Average				
Instant Cost (Nominal \$/Gross	: MVV)		\$4,550	
Installed Cost (Nominal \$/Gros	s MVV)		\$4,960	
% Cost of last year of constru	uction		100%	
% Cost next to last year of co	onstructi	on	0%	
% Cost of previous year of co	onstruct	ion		
High				
Instant Cost (Nominal \$/Gross	: MVV)		\$5,005	
Installed Cost (Nominal \$/Gros	s MVV)		\$5,455	
% Cost first year of construct	tion		100%	
% Cost second year of const	ruction		0%	
% Cost third year of construc	tion			
Low				
Instant Cost (Nominal \$/Gross	: MVV)		\$4,095	
Installed Cost (Nominal \$/Gros		\$4,464		
% Cost first year of construct	tion		100%	
% Cost second year of const	ruction			
% Cost third year of construc	tion			
Year=2009, Value & Dollars	-	High	Low	
Fixed Cost (\$MW-Year)	\$68.0	\$92.00	\$60.00	
Variable Cost (\$/M/Vh)	\$0.00	\$0.00	\$0.00	

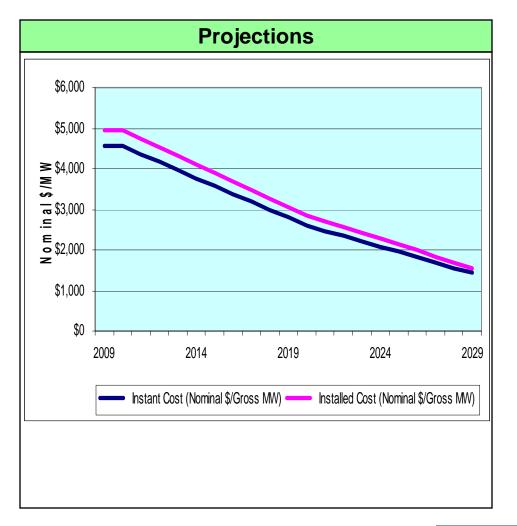




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Wind – Onshore Technology Selection Criteria

Onshore Wind.....

Technology
Reference
Material and
Key
Assumptions

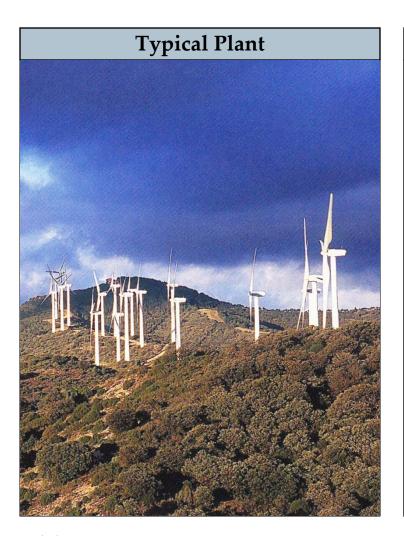
Wind - Onshore

Essentially wind turbine concepts are as follows: the rotor blades drive the main shaft which rotational movement is speeded up in a gearbox and drives the generator. The electricity is converted to high voltage by a transformer in the wind turbine. Gearbox, generator and transformer are all located in the nacelle. Some wind turbines use direct drive generators so one doesn't need a gearbox being a critical component from a maintenance perspective.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Wind - Onshore Selected Technology Description

Wind farms located in areas with Wind Energy Category 3 or 4

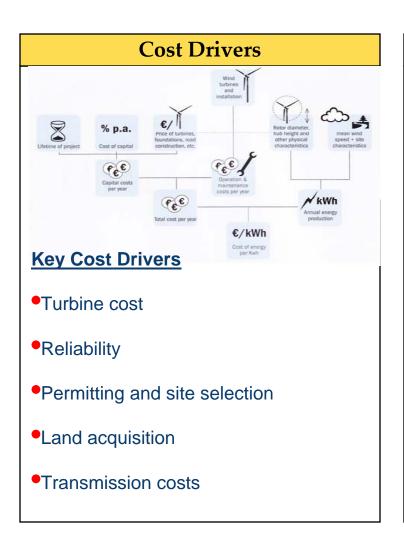


Description

- A 50 MW wind development consisting of multiple wind turbines atop steel towers. Typical facilities today consist of 1.5 to 2.5 MW turbines atop 80m towers.
- In the future, wind farms are likely to see a continued evolution towards larger rotors, turbine sizes, and tower heights.
- Since installed costs and performance vary with turbine size, tower height and site conditions. NCI assumes some typical turbine sizes, tower heights, and site conditions to develop the cost estimates, recognizing that actual wind farm configurations will see a wider range.
- The expected or typical wind regime is uncertain as new wind developments are likely to be in poorer wind regimes, but re-powering at existing good wind sites like Altamont and Tehachapi is also likely.

Wind - Onshore Cost Drivers

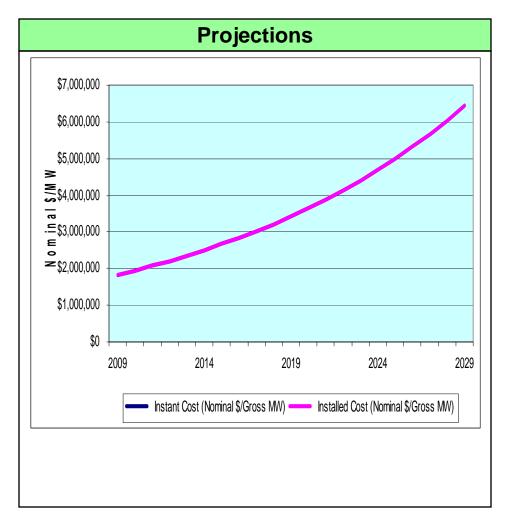
Onshore Wind classes 3, 4 and 5



Plant Configuration Data Overview				
Year=2009, Value & Dollars	Class 3/4	Class 5		
PLANT DATA	Average	Average		
Gross Capacity (MVV)	50	50		
Station Service (%)	0.10%	0.10%		
Net Capacity (MW)	49.95	49.95		
Net Energy (GWh)	79	96		
Transformer Losses	0.50%	0.50%		
Tranmission losses	1.49%	1.49%		
Load Center Delivered Capacity (MVV)	48.96	48.96		
Net Capacity Factor (NCF)	18%	22%		
Planned Percent of Year Operational	100.0%	100.0%		
Average Percent Output	18.29%	22.36%		
Net Energy Delivered to Load Center (GWh)	77	94		
Forced Outage Rate (FOR)	1.3%	1.3%		
Scheduled Outage Factor (SOF)	0.30%	0.30%		
Curtailment (Hours)	0.0	0.0		
Degradation Factors				
Capacity Degradation (%/Year)	1.00%	1.00%		
Heat Rate Degradation (%/Year)	N/A	N/A		
Emission Factors				
NOX (lbs/MWh)	N/A	N/A		
VOC/ROG (Lbs/MWh)	N/A	N/A		
CO (Lbs/MWh)	N/A	N/A		
CO2 (lbs/MWh)	N/A	N/A		
SOX (lbs/MWh)	N/A	N/A		
PM10 (lbs/MWh)	N/A	N/A		

Wind - Onshore Current Cost and Cost Trajectory

Current Costs			
	Start Year	. 2	2009
PLANT COST DATA			
Average			
Instant Cost (Nominal \$/Gross MVV)			,825,000
Installed Cost (Nominal \$/Gross MV	V)	\$1	,825,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MVV)		\$1	,825,000
Installed Cost (Nominal \$/Gross MV	V)	\$1	,825,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross MVV)		\$1	,825,000
Installed Cost (Nominal \$/Gross MV	V)	\$1	,825,000
% Cost first year of construction			100%
% Cost second year of construction			
% Cost third year of construction			
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$/kW-Year)	\$0.00	\$0.00	\$0.00
Variable Cost (\$/MWh)	\$22.00 \$	22.00	\$22.00
	,		





Wind – Offshore Technology Selection Criteria

Offshore Wind has been analyzed in Wind Categories of 5 or greater...

Technology
Reference
Material and
Key
Assumptions

Wind – Offshore

One of the advantages of offshore wind is that it has the potential to produce more electricity than onshore wind farms.

Offshore wind projects can have high performance characteristics due to high Capacity Factors. This is a result of stronger, more constant wind and areas where the wind resource is classified as a 5 or greater

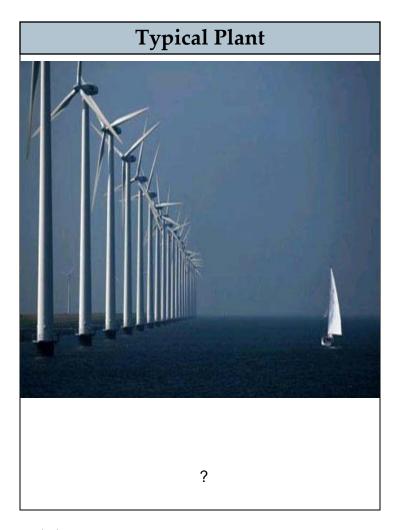
Analyzing Wind potential around the world has shown that at the height of a wind turbine, offshore wind is on average 90 percent stronger than onshore wind. That's because hills, trees, buildings and other structures don't get in the way of winds blowing over the ocean.

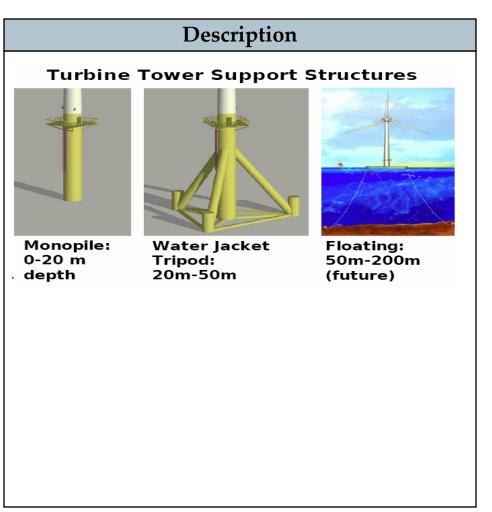
Reference Material: see "Task 1- Central Plant Technologies.xls"

Wind - Offshore

Selected Technology Description

Wind potential high offshore, but projects difficult to realize

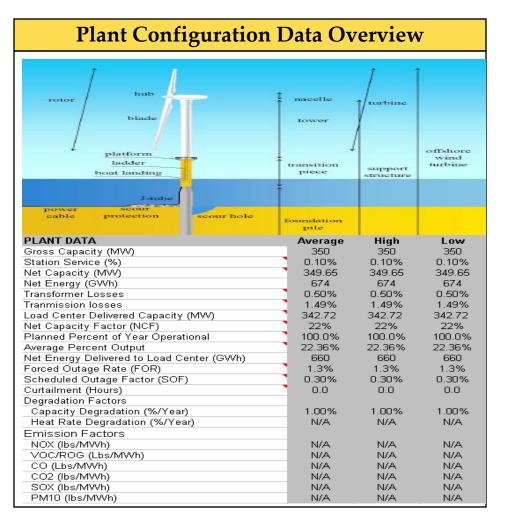




Wind - Offshore Cost Drivers

Offshore Wind costs are heavily influenced by location, sea depth and transmission distance

Cost Drivers Key Cost Drivers Foundations Turbine cost Reliability and maintenance Permitting and site selection Lease costs Transmission costs



Wind - Offshore Current Cost and Cost Trajectory

Current Costs			
	Start '	Year	2018
PLANT COST DATA			
Average			
Instant Cost (Nominal \$/Gross MVV)			\$6,433,382
Installed Cost (Nominal \$/Gross MV	V)		\$6,433,382
% Cost first year of construction			100%
% Cost second year of construction	l		
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MW)			\$6,433,382
Installed Cost (Nominal \$/Gross MV	V)		\$6,433,382
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross MW)	l		\$6,433,382
Installed Cost (Nominal \$/Gross MV	V)		\$6,433,382
% Cost first year of construction			100%
% Cost second year of construction	1		
% Cost third year of construction			
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$/kW-Year)	\$0.00	\$0.00	\$0.00
Variable Cost (\$/MWh)	\$44.00	\$44.00	\$44.00

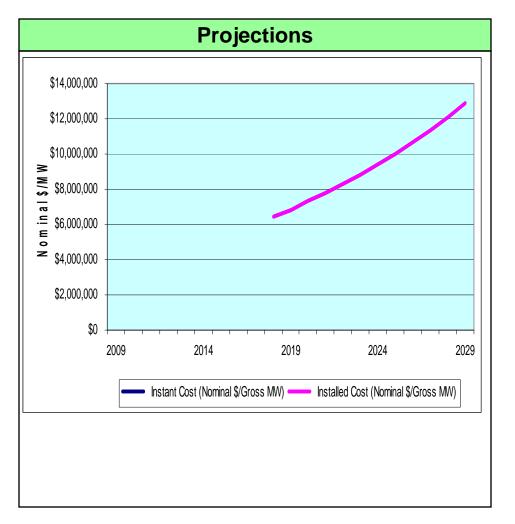




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Wave - Ocean Technology Selection Criteria

Wave energy extraction can be performed in a number of ways

Technology Reference Material and Key Assumptions

Wave-Ocean

Wave energy extraction is complex and many device designs have been proposed. For understanding the device technology, it is helpful introduce these in terms of their physical arrangements and energy conversion mechanisms.

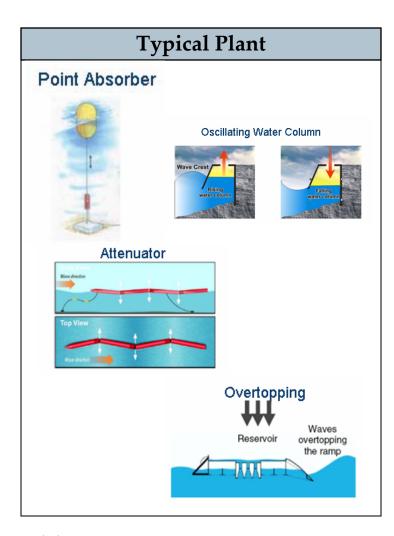
- Distance from shore Wave energy devices may convert wave power at the shoreline, near to the shore (defined as shallow water where the depth is less than one half of the wavelength) or offshore.
- Bottom mounted or floating Wave energy devices may be either bottom-mounted or floating.
- **Wave energy devices** can be classified by means of the type of displacement and reaction system employed. Various hydraulic or pneumatic power take off systems are used and in some cases the mechanical motion of the displacer is converted directly to electrical power (direct-drive) Four of the most well-known device concepts are:
- Symmetrical point absorber A bottom mounted or floating structure that absorbs energy. The power take-off system may take a number of forms, depending on the configuration of displacers/reactors.
 The key characteristic of a point absorber is that it can absorb more energy then available within the devices width if the device is tuned Oscillating Water Column (OWC) –Nearshore or offshore, this is a partially submerged chamber with air trapped above a column of water. As waves enter and exit the chamber, the water column moves up and down and acts like a piston on the air, pushing it back and forth. The air is forced through a turbine/generator to produce electricity.
- Overtopping terminator A floating reservoir structure with a ramp over which the waves topple and hydro turbines/generators through which the water returns to the sea.
- Attenuator One form of the attenuator principle is a long floating structure which is orientated parallel
 to the direction of the waves. The structure is composed of multiple sections which rotate in pitch and
 yaw relative to each other. That motion is then converted to electricity using an electro-hydraulic power
 conversion machine.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Wave - Ocean

Selected Technology Description

Wave multiple technologies



Description

Composite Estimates of cost of Wave Energy extraction.

Cost Factor	Current (\$2009)	CEC (\$2007)	CPUC (\$2008)	RETI (\$2008)
Capacity (MW)	40	0.75	NA	100
Total Overnight Installed				
Cost (\$/kW)	\$2,590	\$6,970	NA	\$2,800 - \$5,200
Transmission & Undersea Cables (\$/kW)	\$279	\$1,340	NA	
Equipment (\$/kW)	\$1,274	\$4,000	NA	
Facilities (\$/kW)	\$509	\$0	NA	
Installation (\$/kW)	\$346	\$990	NA	
Construction				
Management and				
Permitting (\$/kW)	\$181	\$640	NA	
Fixed O&M (\$/kW-yr)	\$36	\$30	NA	\$150-\$270
Variable O&M (\$/MWh)	\$12	\$25	NA	Inc. in FOM
Capacity Factor (%)	26%	15%	NA	25%-45%

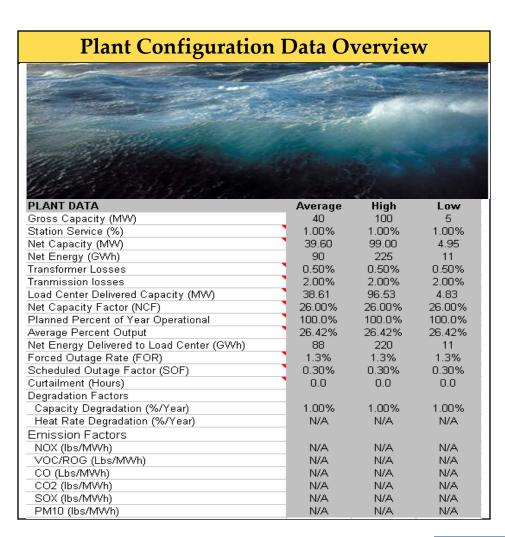
Wave - Ocean Cost Drivers

Wave energy extraction technology is projected to be viable in 2018.

Cost Drivers

Key Cost Drivers

- Turbine cost
- Reliability
- Permitting and site selection
- Licensing
- Transmission costs



Wave - Ocean

Current Cost and Cost Trajectory

As this technology matures and more experience is gained the best configuration will merge in 2018

Current Costs (2018)			
	Start Year	2018	
PLANT COST DATA			
Average			
Instant Cost (Nominal \$/Gross MW)		\$3,000,000	
Installed Cost (Nominal \$/Gross MW)		\$3,000,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
High			
Instant Cost (Nominal \$/Gross MW)		\$3,000,000	
Installed Cost (Nominal \$/Gross MW)		\$3,000,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
Low			
Instant Cost (Nominal \$/Gross MW)		\$3,000,000	
Installed Cost (Nominal \$/Gross MW)		\$3,000,000	
% Cost first year of construction		100%	
% Cost second year of construction			
% Cost third year of construction			
Year=2009, Value & Dollars A	lverage Hig	jh Low	
Fixed Cost (\$/kW-Year)	\$36.00 \$36.		
Variable Cost (\$/MWh)	\$12.00 \$12.	00 \$12.00	

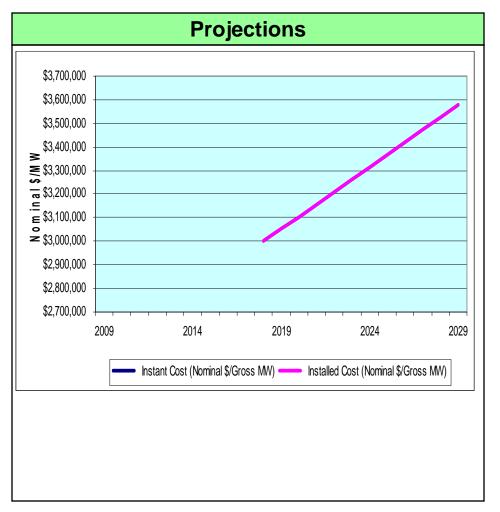




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Coal - IGCC Technology Selection Criteria

Clean Coal IGCC technology in 300MW unit size was selected based on reference plants in operation

Technology Reference Material and Key Assumptions

Integrated Gasification Combined Cycle (IGCC)

Therefore the selected IGCC technology for this study is based on the current worldwide practice for coal-fueled IGCC technology at a scale of 300 MW. This results in the selection of the oxygen-blown entrained flow gasifier process technology. The oxygen blown IGCC process:

A process schematic of a typical oxygen blown IGCC process is given in figure 1.2.1 Part of the air compressed in the gas turbine is fed to an elevated pressure ASU (air separation unit). The larger part from the air required air in the ASU is supplied by an independent compressor driven by an electric motor. In the ASU the air is split in oxygen and nitrogen.

In the gasification island coal (either supplied in slurry or in powder form) is gasified is the reactor into raw gas. Apart from the raw gas also flash and slag are formed. The raw gas contains:

- 1. combustible components CO and H2
- 2. incombustible harmless components H2O, N2, Ar
- 3. greenhouse gas CO2
- 4. traces of environmentally and/or technically harmful gaseous components: Sulphur: H2S and COS, Halogens: HCI and HF, Nitrogen: NH3, HCN, traces of alkali and heavy metals (such as mercury)

The raw gas is purified in the gas cleanup, that is stripped of the sulphur, halogen, nitrous compounds and alkali and heavy metals. During this process waste water and some tailgas is produced. The tail gas is recycled back into the gasification island while the waste water is cleaned in the waste water treatment plant. During this process clean distillate and residue are produced. The distillate is reused in the power plant.

The cleaned syngas is moisturized to achieve a lower heating value. This contributes to lower NOx-emisisons from the also. Also the heat rate is improved marginally. To improve the heat rate further the humid syngas is heated with feed water from the water steam circuit between gasification island and steam cycle. Subsequently the heated syngas is mixed with heated nitrogen from the ASU.

The diluted syngas is combusted under pressure in the gas turbine used ambient air pressurized by the gas turbine's compressor. The hot combustion gases drive the gas turbine's expander providing electric power to drive compressor and generator. The exhaust gases are lead into the steam cycle where steam is produced in the waste heat boiler and is expanded in the steam turbine installation, producing electricity.

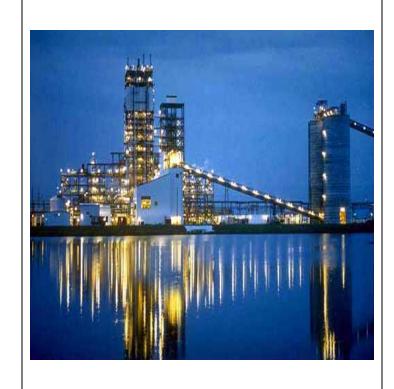
Reference Material: see "Task 1- Central Plant Technologies.xls"

Coal – IGCC

Selected Technology Description

Integrated Gasification Combined Cycle is a power plant using syngas (developed from coal) as a source of clean fuel.

Typical Plant



Tampa Electric Integrated
Gasification Combined Cycle Plant

Description

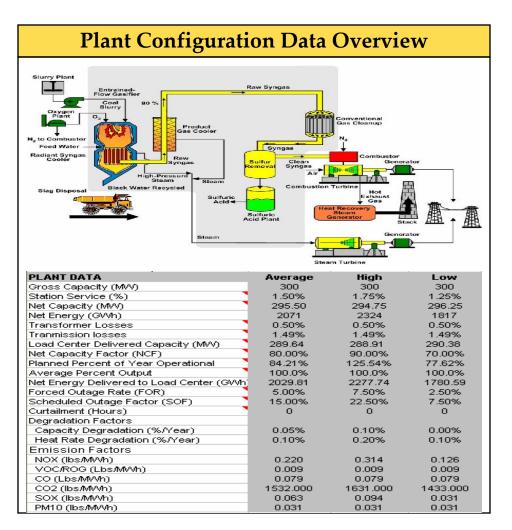
- Integrated Gasification Combined Cycle, or IGCC, is a power plant using synthetic gas (syngas) as a source of clean fuel. Syngas is produced in a gasification unit built for Combined Cycle purposes. Steam generated by waste heat boilers of the gasification process is utilized to help power steam turbines.
- Heavy petroleum residues, coal, and even biomass are possible feeds for gasification process.
- IGCC plants in units of 300MW is being analyzed since it may offer a low-cost long-term option for the reduction of carbon dioxide emissions (through capture and storage).
- The main inhibiting factor for IGCC is high capital cost, but new plants have been recently constructed which are demonstration reliability.



Coal – IGCC Cost Drivers

Fuel gasification process is a large part of the construction and operating costs

Cost Drivers			
Relative expressed cost drivers	Basis	%	
Equipment & Material	% TPC 2)	50	
Labour	% TPC ²⁾	20	
Engineering	% TPC 2)	15	
Owners cost	% TPC ²⁾	15	
Gas cleanup (primary Air Emission Controls)	% TPC 2)	10	
O&M integral (typically)	% CoE 3)	20	
Fuel cost (typically)	% CoE 3)	20	
Key Cost Drivers The construction cost of building the plant. Flue gas cleanup systems construction and maintenance.			



Clean Coal (IGCC) Current Cost and Cost Trajectory

Current Costs			
PLANT COST DATA	Start Yea	ır	2009
Average			
Instant Cost (Nominal \$/Gro	ss MVV)		\$2,250
Installed Cost (Nominal \$/Gr	oss MVV)		\$2,412
% Cost of last year of cons	truction		80%
% Cost next to last year of	construction		20%
% Cost of previous year of	construction		
High			
Instant Cost (Nominal \$/Gro	ss MVV)		\$2,800
Installed Cost (Nominal \$/Gr	oss MVV)		\$2,951
% Cost first year of constru	uction		60%
% Cost second year of construction			40%
% Cost third year of constru	uction		0%
Low			
Instant Cost (Nominal \$/Gro	ss MVV)		\$1,500
Installed Cost (Nominal \$/Gr	oss MVV)		\$1,608
% Cost first year of constru	uction		80%
% Cost second year of con	struction		20%
% Cost third year of constru	uction		
Year=2009, Value & Dollars	Average	High	Low
Fixed Cost (\$MW-Year)	\$41.7	\$52.00	\$31.67
Variable Cost (\$/M/Vh)	\$6.67	\$8.33	\$5.00

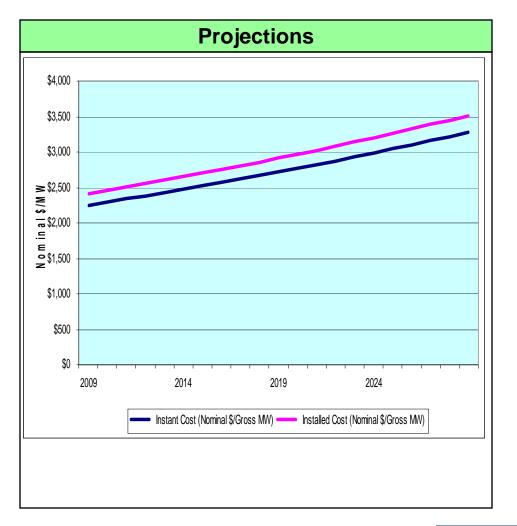




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Nuclear

Technology Selection Criteria

AP1000 PWR technology was selected based on proven technology, references and numerous license applications in process

Technology
Reference
Material and
Key
Assumptions

PWR nuclear technology was selected to supply new nuclear plants in China and other countries. Its' design of the AP-1000 system has been accepted on the world basis.

The most recent announcements from China regarding the plans to purchase 100 AP-1000 plants over the next 25 years is an indication of an international acceptance of this design.

Furthermore, the AP1000 has been identified as the technology of choice for no less than 12 new projected plants in the United States.

The AP1000 is ideally suited for the worldwide and the USA nuclear power marketplace based on the following assumptions.

The AP1000 is:

- -- The safest, most advanced, yet proven nuclear power plant currently available in the worldwide marketplace
- -- Based on standard Westinghouse pressurized water reactor (PWR) technology that has achieved more than 2,500 reactor years of highly successful operation
- -- An 1100MWe design that is ideal for providing baseload generating capacity
- -- Modular in design, promoting ready standardization and high construction quality
- -- Economical to construct and maintain (less concrete and steel and fewer components and systems mean there is less to install, inspect and maintain)
 - -- Designed to promote ease of operation (features most advanced instrumentation and control in the industry)

References:

http://www.ap1000.westinghousenuclear.com.

Reference Material: see "Task 1- Central Plant Technologies.xls"

Nuclear – AP1000

Technology Description

The AP100 is the most advanced US Nuclear Power technology based on the advanced NRC approval process.



- 1117 MWe, 2-loop PWR, 33% efficiency
- Evolutionary design, based on AP-600 designs
- 60 years design life
- Simplified design with less components
- Passive safety systems
- TCDF ~ 5xE-7/year
- In-vessel retention of molten core
- 1st GEN III+ design certified by the USNRC
- 4 units being built in China

Description

WESTINGHOUSE - AP1000 Synonyms: Advanced Passive 1000:

- Approximate Capacity (electric): 1117-1154 MWe, Reactor Type: Pressurized Water Reactor
- NRC Design Certification Status: Certified after December 2005, though amendments have since been proposed.
- Supporting Generating Companies (potential site): Duke Power (Cherokee County), Progress Energy (Harris), Southern Company (Vogtle), NuStart Energy-Tennessee Valley Authority (Bellefonte)
- The AP1000 design is favored for construction at five to six potential sites (ten to twelve reactors) in the United States. The AP1000 is an enlargement of the AP600, designed to almost double the reactor's target electricity output without proportionately increasing the total cost of building the reactor. Westinghouse anticipates that operating costs should be below the average of reactors now operating in the United States. While Westinghouse owns rights to several other designs, the AP1000 is the principal product that the company now promotes in the United States for near term deployment. The AP1000 includes innovative, passive safety features and a much simplified design intended to reduce the reactor's material and construction costs while improving operational safety. During 2007 or 2008 it is anticipated that the AP1000 will be the subject of combined license (COL) applications to build and operate new reactors in the United States. In early 2005 Westinghouse submitted a bid to build a version of the AP1000 to build as many as four AP1000s at two sites in China.
- Further Information: http://www.nrc.gov/reactors/new-licensing/design-cert/ap1000.html http://www.ap1000.westinghousenuclear.com/http://en.wikipedia.org/wiki/AP1000http://www.nei.org/doc.asp?docid=770



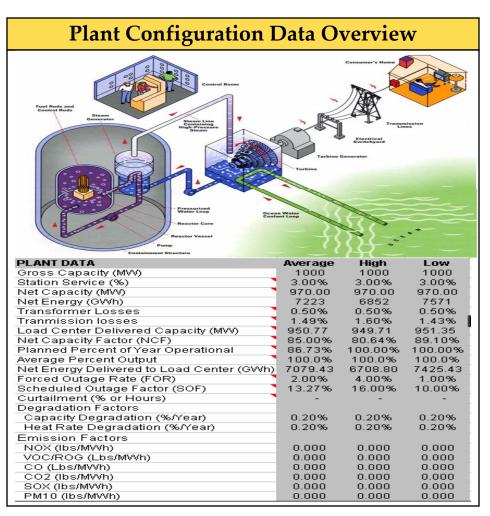
Nuclear Cost Drivers

Decommissioning costs are a significant component in the overall costs for Nuclear

Cost Drivers			
Cost Driver Header	Percentage Cost		
LICENSING OF THE NUCLEAR POWER PLANTS	1%		
PLANT CONSTRUCTION	65%		
O & M OPERATION AND MAINTENANCE	5%		
FUEL PRODUCTION	3%		
NUCLEAR WASTE - TRANSPORTATION	2%		
FUEL STORAGE AND DISPOSAL	4%		
PLANT DECOMMISSIONING	20%		

Key Cost Drivers

- •The construction cost of building the plant.
- The operating cost of running the plant and generating energy.
- The cost of waste disposal from the plant.
- The cost of decommissioning the plant.



Nuclear

Current Costs and Cost Trajectory

Decommission costs are built in as a reserve in the operation costs

Current Costs			
	Start Yo	еаг	2009
PLANT COST DATA			
Average			
Instant Cost (Nominal \$/Gross			\$3,081
Installed Cost (Nominal \$/Gros			\$3,921
% Year0 (Last Year of Contructi		_	6%
% Year1 (Next to Last Year of C		on)	17%
% Year2 (2 years Before Last Y		_	30%
% Year3 (3rd years Before Last		_	29%
% Year4 (4th Year before Last)			14%
% Year5 (First Year of Contructi	ion)		4%
High			
Instant Cost (Nominal \$/Gross			\$4,622
Installed Cost (Nominal \$/Gros			\$5,882
% Year0 (Last Year of Contructi			6%
% Year1 (Last Year of Contructi			17%
% Year2 (Last Year of Contructi			30%
% Year3 (Last Year of Contructi			29%
% Year4 (Last Year of Contruction)			14%
% Year5 (Last Year of Contruction)			4%
Low			
Instant Cost (Nominal \$/Gross			\$2,311
Installed Cost (Nominal \$/Gros			\$2,941
% Year0 (Last Year of Contructi			6%
% Year1 (Last Year of Contructi			17%
% Year2 (Last Year of Contructi			30%
% Year3 (Last Year of Contructi			29%
% Year4 (Last Year of Contructi	ion)		14%
% Year5 (Last Year of Contructi	ion)		4%
V 2000	A	Hink	Law
Year=2009		High	Low
Fixed Cost (\$/k/V-Year)	\$147.7	\$147.7	\$147.7
Variable Cost (\$/MWh)	\$5.27	\$5.27	\$5.27

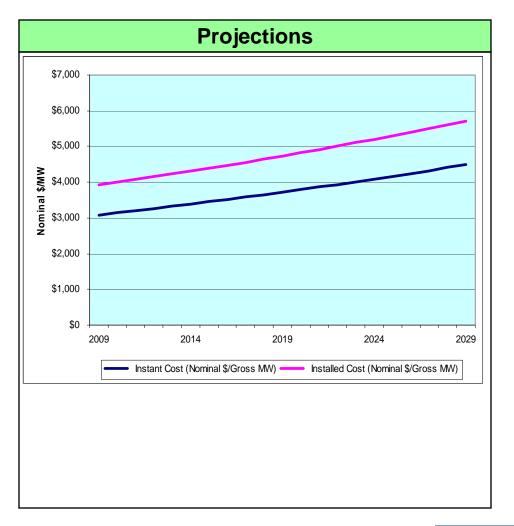


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Geothermal – Flash Analysis Comparison

Geothermal - Flash	2007 IEPR	2009 Update
	2006	2009
	2006	2009
Plant Capacity (MW)₁	50	50
Project Life (yrs)	20	30
Overnight Installed Cost (\$/kW)2	\$2,750	\$3,675
Fixed O&M (\$/kW-yr)3	\$80	\$54
Variable O&M (\$/MWh)₄	\$5	\$5
Typical Net Capacity Factor (%)	95%	90%
Fuel Cost (\$/MMBtu)	n/a	n/a
Heat Rate (HHV)	n/a	n/a
HHV Efficiency (%)	n/a	n/a
Annual Output Degradation (%/yr)	4%	4%



Reference to IEPR 2007 Data

Solar Parabolic Trough Analysis Comparison

Solar - Parabolic Trough		
	2007 IEPR	2009 Update
	2006	2009
Gross Plant Capacity (kW)1	63,500	50,000
Net Plant Capacity (kW)1	50,000	48,800
Annual Output Degradation (%/yr)2	0.20%	0.50%
Project Life (yrs)	30	20
Overnight Cost (\$/kWp)3	3,900	3,687
Fixed O&M (\$/kW-yr)4	60	68
Variable O&M (\$/MWh)	NA	NA
Development Time (months)	20	20
Construction Time (months)	12	12
Scheduled Outage Factor (%)1	NA	NA
Forced Outage Rate (%)1	6%	6%
Typical Net Capacity Factor		
(%)2	27%	27%
Fuel Cost (\$/MMBtu)	NA	NA
HHV Efficiency (%)	NA	NA

Reference to IEPR 2007 Data

Wind - Onshore Analysis Comparison

Onshore Wind		
	2007 IEPR	2009 Update
	2006	2009
Plant Capacity (MW)	50	50
Turbine Size (range) (MW)	2.0 (1.5-2.5)	2.0 (1.5-2.5)
Tower Height (range) (m)	80 (60 – 80)	80 (60 – 80)
Project Life (yrs)	30	30
Overnight Cost (\$/kW)	\$1,900	\$1,825
Fixed O&M (\$/kW-yr)	\$30	\$0
Variable O&M (\$/MWh)		22
Scheduled Outage Factor (%)	0.30%	0.30%
Forced Outage Rate (%)	1.30%	1.30%
Typical Net Capacity Factor – Class 5 (%)	34%	22%
Typical Net Capacity Factor – Class 4 (%)	31%	22%
Typical Net Capacity Factor – Class 3 (%)	28%	22%
Annual Output Degradation (%/yr)	0.25%	1.00%

End

Thank you for your attention

QUESTIONS?

