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## Vertical Plume Velocity Assessment

# Lafayette Backup Generating Facility 

Santa Clara, California<br>Submitted to<br>California Energy Commission<br>Submitted by<br>

Prepared by
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## Introduction

This report presents the evaluation of the Lafayette Backup Generating Facility (LBGF) source generated plumes from the 46 Cummins diesel engines and 88 rooftop chillers on the effects on airport/aircraft operations. The Normal Y. Mineta San Jose International Airport is located approximately 0.38 miles east southeast of the LBGF. This report is based upon an analysis prepared by Atmospheric Dynamics, Inc. in accordance with the California Energy Commission (CEC) application requirements for a Small Power Plant Exemption (SPPE) pursuant to the power plant siting regulations. This analysis is but one part of a larger analysis, which seeks an SPPE Decision from the CEC.

Based on the stack parameter data, an analysis of the potential plume characteristics from the routine operation the diesel engines and rooftop chillers on vertical winds was prepared and compared to the California Energy Commission (CEC) significance criteria of 5.3 meters per second $(\mathrm{m} / \mathrm{s})$ for the average vertical plume velocities as described below.

Atmospheric Dynamics, Inc. (ADI) prepared a screening level plume vertical velocity assessment which are based on the calm wind Spillane methodology outlined in the "Aviation Safety and Buoyant Plumes" paper (Peter Best, et. al., presented at the Clean Air Conference, Newcastle, New South Wales, Australia, 2003). This methodology is also recognized as a screening tool for aviation safety set out by the Australian Civil Aviation Safety Authority (CASA) and presented in "AC 139-5(1) Plume Rise Assessments (CASA, 2012)".

The aim of this screening assessment is to conservatively determine the potential for turbulence generated by the diesel engines and rooftop chillers waste heat exhaust plumes. Part 139.370 of the Australian Civil Aviation Safety Regulations $(1998,2004)$ provides that CASA may determine that plume velocities in excess of $4.3 \mathrm{~m} / \mathrm{s}$ is or will be a potential hazard to aircraft operations. The Manual of Aviation Meteorology (Australian Bureau of Meteorology 2003) defines severe turbulence as a vertical wind gust velocity in excess of $10.6 \mathrm{~m} / \mathrm{s}$. The assumed critical vertical velocity used as a CEC significance threshold is 5.3 meters per second* $(\mathrm{m} / \mathrm{s})$ but it should be noted that the basis of the original CASA derived threshold of $4.3 \mathrm{~m} / \mathrm{s}$ has been lost in antiquity and that CASA no longer relies on the 1998 and 2004 regulations that established this critical threshold other than to note that a more rigorous analysis, which includes site specific meteorology, should be used if the $4.3 \mathrm{~m} / \mathrm{s}$ and $10.6 \mathrm{~m} / \mathrm{s}$ screening thresholds are exceeded. The screening method uses absolute worst-case assumptions of calm winds and neutral atmospheric conditions for the entire vertical extent of the plume to determine these worst-case impacts. It should be noted that these results are extremely conservative in that these worst-case conditions typically only occur during a few hours each year.

The Spillane methodology is generally applied to a limited number of plume source geometry's (turbines, power plant boilers, etc.) with the stacks arranged linearly (in a single straight-line) and separated by distances that typically exceed the individual stack diameters. For the diesel engines, this assumption was maintained. Only one engine stack was modeled consistent with the normal operational testing schedule of the emergency generator engines. For the chiller assessment, a conservative assumption was made in order to use the Spillane methodology on an atypical chiller plume configuration, which is made up of 88 chillers arranged on a twodimensional surface. Here, the methodology, as described below, assumed that all sixteen chiller cells for each chiller were merged into a single stack with an effective diameter based on the combined area of all sixteen chiller cells. In other words, a single stack was assumed to initially
describe the release parameters of the combined chiller cells in each of the 88 individual chillers. The effective plume diameter is appropriate for each individual chiller based on the close proximity and arrangement of the sixteen chiller cells.

## Screening Methodology and Vertical Plume Velocity Calculations

The Spillane methodology is based on worst-case calm wind neutral stability conditions to assess the average plume vertical velocity as a function of height. The methodology is based on wellverified laboratory and theoretical treatments of the rise and spread of a buoyant jet, both into a still ambient environment and into a light crosswind. This treatment covers in detail the initial dynamics of the plume as it exits the stack and the entrainment of ambient air into the plume as it rises directly above the stack. In addition to providing clarifications and algebraic solutions to the Spillane methodology, the 2003 Peter Best paper provides additional methodologies that also consider the enhancement of vertical velocities that may occur if the plumes from multiple identical stacks merge and form a higher buoyancy combined plume (referred to here as the enhanced Spillane methodology).

The vertical plume assessment will involve several stages of development. For individual plumes, the stages are:
(a) In the first stage very close to the stack exit, the high plume momentum will result in a short section in which the conditions at the center of the plume are relatively unaffected by ambient and plume buoyancy conditions. This jet phase extends from the stack exit to approximately a distance of 6.25 D above the stack (where D is the stack diameter) in calm conditions. At the end of this stage, the plume-averaged vertical velocity has decreased to half of the stack exit velocity, with a corresponding increase, or doubling, in effective plume diameter.
(b) In the second stage, the plume responds to differences between ambient and plume buoyancy conditions, with much cooler and less turbulent ambient air being entrained into the plume from the outside regions of the plume towards the plume centerline. The momentum and buoyancy of the plume significantly influences plume rise and subsequently the dilution of the stack exhaust to decrease plume vertical velocities. This dilution is very sensitive to ambient wind speed, so the calm wind conditions considered here are extremely conservative.
(c) In the third stage of plume development, plume rise is due entirely to the buoyancy of the plume and continues from some distance until there is an equalization of turbulence conditions within and outside the plume. This final rise is often only achieved at considerable heights/distances from the stack where the effective average vertical velocity is then close to zero. Since there is very little turbulence and near-zero vertical velocities, this stage of plume development is usually not considered for this type of analysis.

In the second stage of development, the analytical solution of the governing equations under these conditions is given by:

$$
\begin{aligned}
& a=0.16\left(z-z_{v}\right) \\
& V=\left\{(V a) o^{3}+0.12 F o\left[(z-z v)^{2}-(6.25 D-z v)^{2}\right]\right\}^{1 / 3} / a
\end{aligned}
$$

Where the subscript 'o' refers to values of the parameters at the stack outlet and the variables are:

| $a$ | plume radius $(\mathrm{m})$ |
| :--- | :--- |
| $V$ | average vertical velocity $(\mathrm{m} / \mathrm{s})$ |
| $z$ | height above stack top $(\mathrm{m})$ |
| $z_{v}$ | virtual source height $(\mathrm{m})$ |
| $D$ | stack diameter $(\mathrm{m})$ |
| $F_{o}$ | buoyancy flux evaluated at the stack outlet $\left(\mathrm{m}^{4} \mathrm{~s}^{-3}\right)$ |

These are the two primary equations governing the growth of a single plume in the second stage of development under neutral calm wind conditions. Additional equations governing the first stage of single plume development as well as the interaction of multiple plumes in the second stage of development are discussed in detail in the Best paper.

For multiple stacks in the enhanced Spillane methodology, the equations governing the second stage are calculated from the point when the plumes begin to merge until they are fully merged. The plume merging begins at the height where the plume diameters equal the stack separations and the plumes are fully merged at the height where the plume diameters are equal to $2 \mathrm{~d}(\mathrm{~N}-1) / 2$ for three or more stacks or 2 d for two stacks. At the fully merged height, the merged plume diameter and velocity is enhanced by the fourth root of the number of stacks. Above the fully merged plume height, the enhanced plume diameter and plume velocities follow the regular equations given for the second stage. Below the fully merged plume height for the merging phase, plume velocities are linearly interpolated by height from the single plume velocity at the height where the plumes begin to merge to the enhanced plume velocity at the fully merged plume height.

## Vertical Plume Velocity Calculations for the Diesel Engines

The LBGF is comprised of 44 individual large and one (1) small diesel emergency generator stacks. The small diesel emergency generator was not assessed as it would have smaller plume vertical velocities. Generator stack parameter data (plume exit velocity, plume exit temperature and stack exit diameter) were provided by Cummins. Only one (1) engine will be tested during any one hour. While the engines will be tested at minimum loads, the 100 percent load case was utilized for the worst-case plume analysis. For the engine analysis, two ambient conditions were considered: $41.0^{\circ} \mathrm{F}$, the minimum monthly mean of daily minimum temperatures, and $84.3^{\circ} \mathrm{F}$, the maximum monthly mean of daily maximum temperatures for the San Jose Airport ("Climatology of the United States No. 81 - Monthly Station Normals of Temperature, Precipitation, and Heating and Cooling Degree Days 1971-2000 - California", February 2002, and "Climatology of the United States No 20 - Monthly Station Climate Summaries, 1971-2000 - California", February 2004). These data is summarized in Table 1.

| Table 1 <br> Cummins Diesel Stack Characteristics for Vertical Plume Velocity Analysis |  |  |
| :---: | :---: | :---: |
|  | Case \# 1 | 2 |
| Ambient Temperature ( $\left.{ }^{\circ} \mathrm{F}\right)^{*}$ | 41.0 | 41.0 |
| Stack Diameter (m) | 0.7112 | 0.7112 |
| Exhaust Velocity (m/s)* | 31.20 | 31.20 |
| Exhaust Temperature (K)* | 912.0 | 912.0 |
| Stack Release Height (m) | 22.86 | 22.86 |
| Stack Buoyancy Flux ( $\mathrm{m}^{4} / \mathrm{s}^{3}$ ) | 24.58 | 23.35 |
| *Stack data provided by Cummins at 100\% load |  |  |

Screening level vertical plume velocity assessments were made for two ambient temperatures with calm winds and neutral atmospheric conditions for the cases presented in Table 1 which are based on 100 percent load. The results based on the two ambient conditions are presented in Table 2 and the output from the calculation spreadsheet provided in Attachment A.

The initial jet phase extends to a height of about 90 feet above grade level (ft-agl) for both cases. After the jet phase, plume temperature buoyancy characteristics modeled in the Spillane methodology cause a uniform decrease in plume-averaged vertical velocities, with the critical plume-averaged vertical velocity of $5.3 \mathrm{~m} / \mathrm{s}$ occurring at about 113 ft -agl for both cases

| Table 2 <br> Diesel Engine Vertical Plume Velocity Analysis Results for Reference Height |  |  |
| :---: | :---: | :---: |
| Case \# | 1 | 2 |
| Ambient Temperature ( ${ }^{\circ} \mathrm{F}$ ) | 41.0 | 84.3 |
| Single Plume Results: |  |  |
| Plume-Averaged Vertical Velocity at 200 feet-agl (m/s) | 2.77 | 2.73 |
| Height of $5.3 \mathrm{~m} / \mathrm{s}$ Plume-Averaged Vertical Velocity (feet-agl) | 112.8 | 112.9 |

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the diesel engine always remain in the light turbulence category and below the significance level of $5.3 \mathrm{~m} / \mathrm{s}$ at all heights above about $113 \mathrm{ft}-\mathrm{agl}$. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities, so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.


## Vertical Plume Velocity Calculations for the Rooftop Chillers

The 88 rooftop chillers are each comprised of 20 individual cells, with a cell fan diameter of 34 inches. The 88 chillers are generally arranged 24 along the longer building length (averaging 15 feet between adjacent chillers) by three along the shorter building width (averaging 15 feet between adjacent chillers). It should be noted that the chillers are arranged differently on the two-story part of the data center ( $8 \times 2$ ). Based on the groupings of chillers, the single and merged
plumes were based on the 24 ( $3 x 8$ ) chiller arrangement my merging plumes along the length (3 merged stacks) and width ( 8 merged stacks). Chiller stack parameter data (exit velocity and temperature) were provided by the applicant. An effective stack diameter for all 20 cells was utilized for each chiller. The chillers will utilize variable speed fans and the number of fans that are operational are dependent upon ambient temperature and plant load. However, to be conservative, all chillers/cells were assumed to be operating at full load. These data are summarized in Table 3 for the same ambient temperatures used for the engine analysis.

| Table 3 <br> Chiller Stack Characteristics for Vertical Plume Velocity Analysis |  |  |
| :---: | :---: | :---: |
| Case \# | 1 | 2 |
| Ambient Temperature ( $\left.{ }^{\circ} \mathrm{F}\right)^{*}$ | 41.0 | 84.3 |
| Effective Stack Diameter (m)** | 3.86 | 3.86 |
| Exhaust Velocity (m/s)* | 8.06 | 8.06 |
| Exhaust Temperature (K)* | 289.26 | 313.32 |
| Stack Release Height (m) | 23.81 | 23.81 |
| Stack Buoyancy Flux ( $\mathrm{m}^{4} / \mathrm{s}^{3}$ ) | 11.33 | 10.45 |
| *Chiller stack data provided by the applicant <br> ** Calculated value based on the cell diameter of 34 inches multiplied <br> or $D_{\text {eff }}=34 " \sqrt{20}$ | quare of the | perating |

The Spillane methodology was originally developed to treat multiple individual stacks that are arranged along a linear $x$ or $y$ direction, but not both directions at once, with stack separations much greater than the stack diameters, typical of boilers/turbines at large power plants. As noted above, the 88 chillers are generally arranged in a $3 \times 8$ pattern. Therefore, the enhanced Spillane methodology was based on calculating the total merging height for the largest linear direction of chiller placements (which is eight chillers spaced 24.6 feet apart along the longer length of the building). The largest grouping of $48(3 \times 16)$ chillers were considered in the calculation of vertical velocity plume enhancement (both at and above the totally merged height, and for the interpolation down to the plume touching height. Again, the effective single stack diameter of each chiller was based on the combined 20 cells.

Screening level vertical plume velocity assessments were made for the same ambient temperatures with calm winds and neutral atmospheric conditions as was done for the emergency generator engines. The results are presented in Table 4 and the output from the calculation spreadsheets are provided in Attachment A.

The initial jet phase extends to a height of about 157.3 ft -agl for both cases. The critical plumeaveraged vertical velocity of $5.3 \mathrm{~m} / \mathrm{s}$ occurs in the jet phase at about 132.4 ft -agl for both cases. The plumes touch (begin to merge) at about 246 ft -agl and are fully merged at about 1,233 ft-agl for both cases. Under the enhanced Spillane methodology, the merged plume-averaged vertical velocities never approach $5.3 \mathrm{~m} / \mathrm{s}$ (either above the totally merged height or when interpolated down to the touching height).

| Table 4Chiller Vertical Plume Velocity Analysis Results for Reference Height |  |  |
| :---: | :---: | :---: |
| Case \# | 1 | 2 |
| Ambient Temperature ( ${ }^{\circ} \mathrm{F}$ ) | 41.0 | 84.3 |
| Single Plume Results: |  |  |
| Height of $5.3 \mathrm{~m} / \mathrm{s}$ Plume-Averaged Vertical Velocity (Within the Jet Phase, feet-agl) | 132.4 | 132.4 |
| Merged Plume Results: |  |  |
| Plume-Averaged Vertical Velocity at 1,000 feet-agl (m/s) | 3.50 | 3.42 |

From these results and for each ambient condition, the vertical plume velocities are less than the threshold value of $5.3 \mathrm{~m} / \mathrm{s}$ for all heights above about $132 \mathrm{ft}-\mathrm{agl}$ and above for the chillers. The heights at which plume-averaged vertical velocities exceed $5.3 \mathrm{~m} / \mathrm{s}$ only occur during the jet phase for both cases. These cases also represent worst-case conditions of calm winds at all levels of a neutral atmosphere.

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the chillers always remain in the light turbulence category and below the significance level of $5.3 \mathrm{~m} / \mathrm{s}$ at all heights above about $132 \mathrm{ft}-\mathrm{agl}$. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.


## Attachment A Spillane Method Plume Velocity Calculations






SINGLE/Approximated Plume Average Vertical Velocities for LBGF Chillers using CEC Staff Methodology - Winter Min*
Based on 48 chillers w/ 20 cells/chiller. Calc' "Aviation Safety and Buoyant Plumes," Peter Best, et. al
eff.diam for each chiller with each cell at 34"ID "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume
( 220,110 ACFM total for each chiller). from a Gas-Turbine Power Station at Oakey, Queensland, Australia " Dr. K. T. Spillane

Ambient Conditions: ions:
Plume Exit Conditions:

| Plume Exit Conditions: |
| ---: | ---: |
| Individual Chiller Stack Diameter $\mathrm{D}_{\mathrm{s}}$ |
| Stack Velocity $\mathrm{V}_{\text {exit }}$ |

from a Gas-Turbine Power Station
Constants: Assume neutral conditions ( $\mathrm{d} \theta / \mathrm{dz}=0$ or $\theta_{\mathrm{a}}=\theta_{\mathrm{e}}$ )
278.15 Kelvins

|  | $41.0^{\circ} \mathrm{F}$ |
| :---: | :---: |
|  |  |
|  |  |



Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase

| Plume Top-Hat Radius a | Solutions in Table Below |  | $0.16\left(z-z_{v}\right)$, or linear increase with height |  | Sect.2/Eq. 6 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Virtual Source Height $z_{v}$ | 0.468 meters* | 1.5 feet* | $6.25 \mathrm{D}\left[1-\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}\right.$, | ers*=meters above stack top | Sect.2/Eq. 6 |
| Height above Ground $\mathrm{z}_{\mathrm{v}}+\mathrm{h}_{\mathrm{s}}$ | 24.282 meters | 79.7 feet |  | where $\left(\theta_{\mathrm{a}} / \theta_{\mathrm{s}}\right)^{1 / 2}=\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}=$ | 0.9806 |
| Vertical Velocity V | Solutions | low | $\left\{(\mathrm{Va})_{0}{ }^{3}+0.12 \mathrm{~F}_{0}[\right.$ | , $\left.\left.)^{2}-\left(6.25 D-z_{v}\right)^{2}\right]\right\}^{(1 / 3)} / \mathrm{a}$ | Sect.2.1(6) |
| Product (Va)。 | $15.265 \mathrm{~m}^{2} / \mathrm{s}$ |  | $\mathrm{V}_{\text {exit }} \mathrm{D} / 2\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}$ |  |  |

Single Chiller Results:
Single Chiller Results:
Solve for plume-averaged vertical velocity at
Gives the following Height above Stack $z^{\prime}$

| at height | 940.0 | feet | 28 |
| :---: | :---: | :---: | :---: |
| 262.698 | meters* | 861.9 | feet* |
| 83.914 | meters | 275.3 | feet |

286.512 meters above ground $\left(z^{\prime}+h_{s}\right)$

| Plume Top-Hat Diameter 2a' | 83.914 meters | 275.3 feet |
| ---: | :---: | :---: | :---: |
| Vertical Velocity V | $\mathbf{1 . 0 9 2} \mathbf{~ m} / \mathbf{s}$ | $3.58 \mathrm{ft} / \mathrm{sec}$ |


| $2 a^{\prime}=2^{*} 0.16\left(z^{\prime}-z_{v}\right)$ | Sect.2/Eq.6 |
| :--- | :--- |
| $V=\left\{(V a)_{o}{ }^{3}+0.12 F_{0}\left[\left(z-z_{v}\right)^{2}-\left(6.25 D-z_{v}\right)^{2}\right]\right\}^{(1 / 3)} /\left(2 a^{\prime} / 2\right)$ | Sect.2/Eq.6 |

Solve for Height of CASC critical vertical velocity $\mathrm{V}_{\text {crit }} \quad 5.30 \mathrm{~m} / \mathrm{s}$ plume-averaged vertical velocity $\quad$ Critical VV < Top of Jet Find Height above Stack $z_{\text {crit }} \quad$ \#N/A meters $\quad \mathrm{N} / \mathrm{A}$ feet Solve for $\mathrm{x}=\left(\mathrm{z}-\mathrm{z}_{\mathrm{v}}\right)$ simultaneously in both eqs. (i.e., Va and a) Height above Ground $z_{\text {crit }}+h_{s}$ \#N/A meters \#N/A feet for $V=V_{\text {crit }}$ using the cubic equation $a x^{3}+b x^{2}+c x+d=0$, where | $\mathrm{a}=1, \mathrm{c}=0$, and $\mathrm{b}=-\left(0.12 \mathrm{~F}_{\mathrm{o}}\right) /\left(\mathrm{V}_{\text {crit }^{3}} 0.16^{3}\right)=$ | -2.22917 |
| :--- | :--- |
| $\left[0.12 \mathrm{~F}_{0}\left(6.25 \mathrm{D}-\mathrm{z}_{\mathrm{v}}\right)^{2}-(\mathrm{Va})_{0}{ }^{3}\right] /\left(\mathrm{V}_{\text {crit }}{ }^{3} 0.16^{3}\right)=$ | -4584.19 |

Interpolated Height of critical vertical velocity in Jet Phase: Find Height above Stack $z_{\text {crit }} \quad 16.537$ meters Height above Ground $z_{\text {crit }}+h_{s} \quad 40.352$ meters http://www.1728.org/cubic.htm | or $z(\mathrm{~m} /$ above stack $)=$ | 17.857 |
| ---: | ---: |
| $z(\mathrm{ft} /$ above ground $)=$ | 136.7 |

Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:



|  | "Aviation Safety and Buoyant Plumes," Peter Best, et. al. |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Merged |  |  |  |  |  |  |  |
| Ambient Conditions: |  | Plume from Two Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane |  |  |  |  |  |  |
|  |  |  |  |  | Constants: | sume ne | utral conditions ( $\mathrm{d} \theta / \mathrm{dz}=0$ or | $\theta_{\mathrm{a}}=\theta_{\mathrm{e}}$ ) |
| Ambient Potential Temp $\theta_{\mathrm{a}}$ | 278.15 | Kelvins | 41.0 | ${ }^{\circ} \mathrm{F}$ |  | 0.3048 | meters/feet |  |
| Plume Exit Conditions: |  |  |  |  | Gravity g | 9.81 | $\mathrm{m} / \mathrm{s}^{2}$ |  |
| Stack Height $\mathrm{h}_{\text {s }}$ | 23.81 | meters | 78 2/12 | feet-inches | $\lambda$ | 1.11 |  |  |
| Individual Stack Diameter D | 3.86213661 | meters | 152.1 | inches | $\lambda_{0}$ | $\sim 1.0$ |  |  |
| Stack Velocity $\mathrm{V}_{\text {exit }}$ | 8.06 | $\mathrm{m} / \mathrm{s}$ | 26.45 | $\mathrm{ft} / \mathrm{sec}$ | $4 \mathrm{Vol} /\left(60 \pi \mathrm{D}^{2}\right)$ |  |  |  |
| Individual Volumetric Flow | 94.44 | cu.m/sec | 200,110 | ACFM | $\pi V_{\text {exit }} \mathrm{D}^{2} / 4$ |  |  | Sect.2/41 |
| Stack Potential Temp $\theta_{\text {s }}$ | 289.26 | Kelvins | 61.0 | ${ }^{\circ} \mathrm{F}$ |  |  |  |  |
| Initial Stack Buoyancy Flux $\mathrm{F}_{\text {o }}$ | 11.33 | $\mathrm{m}^{4} / \mathrm{s}^{3}$ | 20.0 | $\Delta T\left({ }^{\circ} \mathrm{F}\right)$ | $g V_{\text {exit }} D^{2}\left(1-\theta_{2}\right.$ | /4 $=\mathrm{V}$ | ol.Flow(g/r)(1-9/ $/ \theta_{\mathrm{s}}$ ) | Sect.2/41 |
| Plume Buoyancy Flux F | N/A | $\mathrm{m}^{4} / \mathrm{s}^{3}$ |  |  | $\lambda^{2} \mathrm{gVa}{ }^{2}\left(1-\theta_{\mathrm{a}} /\right.$ | ) for $\mathrm{a}, \mathrm{V}$, | $\theta_{\mathrm{p}}$ at plume height (see belo |  |
| Total Number of Stacks n | 48 |  |  |  |  |  |  |  |
| Average Adjacent Stack Separation d | 7.50 | meters | 24.6 | feet | Calcs based | multiple | plume treatment in Peter Be | st Paper: |
| Number of Stacks along Orientation N | 16 |  |  |  | plume veloci | s increa | sed by $\mathrm{N}^{0.25}$ at the height wher | e plumes |
|  |  |  |  |  | fully merged | terp. bel | low ht, single merged stack a | bove ht ) |
| Conditions at End (Top) of Jet Phase: |  |  |  |  |  |  |  |  |
| Height above Stack $\mathrm{z}_{\text {jet }}$ | 24.138 | meters* | 79.2 | feet* | $z_{\text {jet }}=6.25 \mathrm{D}$, | meters*= | meters above stack top | Sect.3/41 |
| Height above Ground $\mathrm{z}_{\text {jet }}+\mathrm{h}_{\text {s }}$ | 47.952 | meters | 157.3 | feet |  |  |  | " |
| Vertical Velocity $\mathrm{V}_{\text {jet }}$ | 4.031 | $\mathrm{m} / \mathrm{s}$ | 13.22 | $\mathrm{ft} / \mathrm{sec}$ | $\mathrm{V}_{\text {jet }}=0.5 \mathrm{~V}_{\text {ex }}$ | $=\mathrm{V}_{\text {exit }} / 2$ |  | " |
| Plume Top-Hat Diameter $2 \mathrm{a}_{\mathrm{jet}}$ | 7.724 | meters | 25.3 | feet | $2 \mathrm{a}_{\text {jet }}=2 \mathrm{D}$ |  | Conservation of momentum |  |



Plume Merging - Based on Single Plume Calculations where:

| Begin Merging Plume Top-Hat Diameter 2a $\mathrm{t}_{\text {touch }}$ | 7.500 | meters | 24.6 | feet |
| :---: | :---: | :---: | :---: | :---: |
| Height above Stack $z_{\text {touch }}$ | 23.906 | meters* | 78.4 | feet* |
| Height above Ground $z_{\text {touch }}+h_{s}$ | 47.720 | meters | 156.6 | feet |
| Vertical Velocity $\mathrm{V}_{\text {touch }}$ | 4.065 | $\mathrm{m} / \mathrm{s}$ | 13.3 | $\mathrm{ft} / \mathrm{sec}$ |
| Total Merging Plume Top-Hat Diameter $2 \mathrm{a}_{\text {full }}$ | 112.500 | meters | 369.1 | feet |
| Height above Stack $\mathrm{z}_{\text {full }}$ | 352.031 | meters* | 1155.0 | feet* |
| Height above Ground $\mathrm{z}_{\text {full }}+\mathrm{h}_{\text {s }}$ | 375.845 | meters | 1233.1 | feet |
| Vertical Velocity $\mathrm{V}_{\text {full }}$ | 0.986 | $\mathrm{m} / \mathrm{s}$ | 3.2 | $\mathrm{ft} / \mathrm{sec}$ |
| Product ( $\left.\mathrm{V}^{3} \mathrm{a}\right)_{\text {tull }}$ | 54 | $\mathrm{m}^{4} / \mathrm{s}^{3}$ |  |  |

Product Va given by equations below:

| $\mathrm{a}=0.16\left(\mathrm{z}-\mathrm{z}_{\mathrm{v}}\right)$, or linear increase with height |
| :--- |
| $z_{\mathrm{v}}=6.25 \mathrm{D}\left[1-\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}\right]$, meters ${ }^{*}=$ meters above stack to |
| where $\left(\theta_{\mathrm{a}} / \theta_{\mathrm{s}}\right)^{1 / 2}=\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}=$ |
| Sect.2/Eq.6 |
| 0.9806 |
| $\left\{(\mathrm{Va})_{\mathrm{o}}{ }^{3}+0.12 \mathrm{~F}_{\mathrm{o}}\left[\left(\mathrm{z}-\mathrm{z}_{\mathrm{v}}\right)^{2}-\left(6.25 \mathrm{D}-\mathrm{z}_{\mathrm{v}}\right)^{2}\right]\right\}^{(1 / 3)} / \mathrm{a}$ | Sect.2.1(6)

$V_{\text {exit }}(\mathrm{D} / 2)\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)^{1 / 2}$
Conservation of momentum
Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet and Merging Phases
$2 \mathrm{a}_{\text {touch }}=\mathrm{d}$, (or $\left.\mathrm{a}_{\text {touch }}=\mathrm{d} / 2\right)$
$z_{\text {touch }}=z_{v}+d /\left(2^{*} 0.16\right)$, meters* ${ }^{*}=$ meters above stack top
$V_{\text {touch }}=\left\{(\mathrm{Va})_{0}{ }^{3}+0.12 F_{0}\left[\left(z-z_{v}\right)^{2}-\left(6.25 \mathrm{D}-z_{v}\right)^{2}\right]\right\}^{(1 / 3)} / a$ $2 \mathrm{a}_{\text {full }}=2 \mathrm{~d}(\mathrm{~N}-1) / 2$, (or $\left.\mathrm{a}_{\text {full }}=\mathrm{d}(\mathrm{N}-1) / 2\right)$ FOR 2 STACKS, $2 \mathbf{a}_{\text {full }}=2 \mathrm{~d}$ $z_{\text {full }}=\mathrm{z}_{\mathrm{v}}+2 \mathrm{~d} /\left(2^{*} 0.16\right)$, meters ${ }^{*}=$ meters above stack top
$V_{\text {full }}=\left\{(\mathrm{Va})_{\mathrm{o}}{ }^{3}+0.12 F_{0}\left[\left(z_{\text {full }}-z_{\mathrm{v}}\right)^{2}-\left(6.25 \mathrm{D}-\mathrm{z}_{\mathrm{v}}\right)^{2}\right]\right\}^{(1 / 3)} / \mathrm{a}_{\text {full }}$

| Conditions at End (Top) of Merging Phase - Define new values for $\mathrm{V}_{\text {full }}$ and $\mathrm{a}_{\text {full }}$ in Merged P |  |  |
| :---: | :---: | :---: |
| Merged Plume Values: Plume Diameter 2a | Solutions in Table Below |  |
| Revised Merged Plume Radius $\mathrm{a}_{\mathrm{m}}$ | 148.058 meters | 485.8 |
| Revised Merged Plume Velocity $\mathrm{V}_{\mathrm{m}}$ | $2.596 \mathrm{~m} / \mathrm{s}$ | 8.5 |
| Revised Virtual Source Height $\mathrm{z}_{\text {full }}$ | 352.031 meters* | 1155. |
| Revised Vertical Velocity V | Solutions in Tables Below |  |

Multiple Plume Calculations

| Solve for plume-averaged vertical veloc | t height | 940.0 | feet | 2 |
| :---: | :---: | :---: | :---: | :---: |
| Gives the following Height above Stack z | 262.698 | meters* | 861.9 | feet* |
| Plume Top-Hat Radius a | \#N/A | meters | \#N/A | feet |
| Vertical Velocity V | 2.996 | $\mathrm{m} / \mathrm{s}$ | 9.83 | $\mathrm{ft} / \mathrm{se}$ |
|  |  |  |  |  |
| Solve for Height of CASC critical vertical | ty $\mathrm{V}_{\text {crit }}$ | 5.30 | m/s |  |
| Find Height above Stack $z_{\text {crit }}$ | JET | meters | JET |  |
| Height above Ground $\mathrm{z}_{\text {crit }}+\mathrm{h}_{\text {s }}$ |  | meters | JET | feet |

Table of MERGED Plume-Averaged Vertical Velocities starting at Touching Height:

| Height (feet) | (meters) | Plume | Vert. |
| :---: | :---: | :---: | :---: |
| above ground | above stack | Radius(m) | $\mathrm{Vel}(\mathrm{m} / \mathrm{s})$ |
| Begin Merging (touch) $=156.6$ | 23.92 | 3.750 | 4.06 |
| 160.0 | 24.95 | \#N/A | 4.06 |
| 180.0 | 31.05 | \#N/A | 4.03 |
| 200.0 | 37.15 | \#N/A | 4.01 |
| 220.0 | 43.24 | \#N/A | 3.98 |
| 240.0 | 49.34 | \#N/A | 3.95 |
| 260.0 | 55.43 | \#N/A | 3.92 |
| 300.0 | 67.63 | \#N/A | 3.87 |
| 350.0 | 82.87 | \#N/A | 3.80 |
| 400.0 | 98.11 | \#N/A | 3.73 |
| 450.0 | 113.35 | \#N/A | 3.66 |
| 500.0 | 128.59 | \#N/A | 3.60 |
| 550.0 | 143.83 | \#N/A | 3.53 |
| 600.0 | 159.07 | \#N/A | 3.46 |
| 650.0 | 174.31 | \#N/A | 3.39 |
| 700.0 | 189.55 | \#N/A | 3.32 |
| 800.0 | 220.03 | \#N/A | 3.19 |
| 900.0 | 250.51 | \#N/A | 3.05 |
| 1000.0 | 280.99 | \#N/A | 2.91 |
| 1100.0 | 311.47 | \#N/A | 2.78 |
| 1200.0 | 341.95 | \#N/A | 2.64 |
| End Merging (full/mp) = 1233.1 | 352.03 | 148.058 | 2.60 |
| 1300.0 | 372.43 | 151.322 | 2.58 |
| 1400.0 | 402.91 | 156.198 | 2.55 |
| 1500.0 | 433.39 | 161.075 | 2.52 |
| 2000.0 | 585.79 | 185.459 | 2.41 |
| 2500.0 | 738.19 | 209.843 | 2.31 |
| 3000.0 | 890.59 | 234.227 | 2.23 |
| 3500.0 | 1042.99 | 258.611 | 2.16 |
| 4000.0 | 1195.39 | 282.995 | 2.09 |
| 4500.0 | 1347.79 | 307.379 | 2.04 |
| 5000.0 | 1500.19 | 331.763 | 1.98 |

Single Plume Eqns (see Single Plume spreadsheet)
$\mathrm{V}_{\text {plume }}=\left\{(\mathrm{Va})_{0}{ }^{3}+0.12 \mathrm{~F}_{\mathrm{o}}\left[\left(\mathrm{z}-\mathrm{z}_{\mathrm{v}}\right)^{2}-\left(6.25 \mathrm{D}-\mathrm{z}_{\mathrm{v}}\right)^{2}\right]\right\}^{1 / 3} / \mathrm{a}$
$a=0.16\left(z-z_{v}\right)$
$\theta_{\mathrm{p}}=\theta_{\mathrm{s}}\left(1+\left(1-\left(\theta_{\mathrm{e}} / \theta_{\mathrm{s}}\right)\right)^{*}\left(\mathrm{~V}_{\text {exit }} \mathrm{D}^{2} /\left(4 \mathrm{~V}_{\text {plume }}{ }^{*} \mathrm{a}^{2 *} \lambda^{2}\right)\right)\right)$
Interpolated Layer Eqns
20 ft Intervals
$\mathrm{V}^{\prime}=\mathrm{V}_{\text {touch }}+\left(\mathrm{V}_{\mathrm{m}}-\mathrm{V}_{\text {touch }}\right)^{*}\left(\mathrm{z}^{\prime}-\mathrm{Z}_{\text {touch }}\right) /\left(\mathrm{Z}_{\text {full }}-\mathrm{Z}_{\text {touch }}\right)$


SINGLE/Approximated Plume Average Vertical Velocities for Lafayette Chillers using CEC Staff Methodology - Summer Max* Based on 88 chillers w/ 20 cells/chiller. Calc' "Aviation Safety and Buoyant Plumes," Peter Best, et. al. eff.diam for each chiller with each cell at 34" ID "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume (220,110 ACFM total for each chiller).
from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:
Ambient Potential Temp $\theta_{a}$
Plume Exit Conditions:

| Plume Exit Conditions: |
| :---: |
| Stack Height $\mathrm{h}_{\text {s }}$ |
| Individual Chiller Stack Diameter ${ }^{\text {\% }}$ |
| Stack Velocity $\mathrm{V}_{\text {exit }}$ |
| Individual Chiller Volumetric Flow |
| Stack Potential Temp $\theta_{\text {s }}$ |
| Initial Stack Buoyancy Flux Fo |
| Plume Buoyancy Flux F |
| Number of Chillers n |
| Conditions at End (Top) of Jet Phase: |
| Height above Stack $\mathrm{z}_{\text {jet }}$ |
| Height above Ground $\mathrm{z}_{\text {jet }}+\mathrm{h}_{\text {s }}$ |
| Vertical Velocity $\mathrm{V}_{\text {jet }}$ |
| Plume Top-Hat Diameter 2ajet |

Constants: Assume neutral conditions ( $\mathrm{d} \theta / \mathrm{dz}=0$ or $\theta_{\mathrm{a}}=\theta_{e}$ )

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase






