

APPENDIX TRANS DR-64

Thermal Plume Analysis

Plume Vertical Velocity Assessment

Walsh Backup Generating Facility

Santa Clara, California

Submitted to
California Energy Commission

Submitted by
651 Walsh Partners, LLC

Prepared by
Atmospheric Dynamics, Inc.



ATMOSPHERIC DYNAMICS, INC
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Introduction

651 Walsh Partners, LLC (WP LLC) is proposing to develop the Walsh Backup Generating Facility (WBGF). The backup generating facility will utilize 32 three-megawatt (MW) diesel fired generators along with 54 rooftop air cooled chillers. The proposed WBGF site encompasses 7.87-acres and is located at 651 Walsh Avenue in Santa Clara, California. The property is zoned Heavy Industrial. The site is currently developed with a one-story 171,259-square foot warehouse complex and associated paved parking and loading areas. The Norman Y. Mineta San José International Airport is located approximately 0.3 miles east of the site.

Based on the stack parameter data, an analysis of the potential plume characteristics from the routine operation the diesel engines and rooftop chillers on vertical winds was prepared and compared to the California Energy Commission (CEC) significance criteria of 5.3 meters per second (m/s) for the average vertical plume velocities as described below.

Atmospheric Dynamics, Inc. (ADI) prepared a screening level plume vertical velocity assessment which are based on the calm wind Spillane methodology outlined in the “*Aviation Safety and Buoyant Plumes*” paper (Peter Best, et. al., presented at the Clean Air Conference, Newcastle, New South Wales, Australia, 2003). This methodology is also recognized as a screening tool for aviation safety set out by the Australian Civil Aviation Safety Authority (CASA) and presented in “*AC 139-5(1) Plume Rise Assessments (CASA, 2012)*”.

The aim of this screening assessment is to conservatively determine the potential for turbulence generated by the diesel engines and rooftop chillers waste heat exhaust plumes. Part 139.370 of the Australian Civil Aviation Safety Regulations (1998, 2004) provides that CASA may determine that plume velocities in excess of 4.3 m/s is or will be a potential hazard to aircraft operations. The *Manual of Aviation Meteorology* (Australian Bureau of Meteorology 2003) defines severe turbulence as a vertical wind gust velocity in excess of 10.6 m/s. The assumed critical vertical velocity used as a CEC significance threshold is 5.3 meters per second* (m/s) but it should be noted that the basis of the original CASA derived threshold of 4.3 m/s has been lost in antiquity and that CASA no longer relies on the 1998 and 2004 regulations that established this critical threshold other than to note that a more rigorous analysis, which includes site specific meteorology, should be used if the 4.3 m/s and 10.6 m/s screening thresholds are exceeded. The screening method uses absolute worst-case assumptions of calm winds and neutral atmospheric conditions for the entire vertical extent of the plume to determine these worst-case impacts. It should be noted that these results are extremely conservative in that these worst-case conditions typically only occur during a few hours each year.

The Spillane methodology is generally applied to a limited number of plume source geometry’s (turbines, power plant boilers, etc.) with the stacks arranged linearly (in a single straight-line) and separated by distances that typically exceed the individual stack diameters. For the diesel engines, this assumption was maintained. Only one engine stack was modeled consistent with the normal operational testing schedule of the emergency generator engines. For the chiller assessment, a conservative assumption was made in order to use the Spillane methodology on an atypical chiller plume configuration, which is made up of 54 chillers arranged on a two-dimensional surface. Here, the methodology, as described below, assumed that all sixteen chiller cells for each chiller were merged into a single stack with an effective diameter based on the combined area of all sixteen chiller cells. In other words, a single stack was assumed to initially describe the release parameters of the combined chiller cells in each of the 54 individual chillers.

*For the Puente Power Project (Docket#15-AFC-01, TN#213674, 9/15/2016), “CEC staff ... concluded that an average velocity of 5.3 m/s is the appropriate velocity ... [for a plume velocity threshold].” The CEC staff “Plume Background Threshold” attached to the docketed document concludes with “...[CEC] staff will use 10.6 m/s peak vertical plume velocity as the new threshold. The altitude at which a plume would have a peak vertical velocity of 10.6 m/s would be the same altitude at which a plume would have an average vertical velocity of half that, 5.3 m/s.”



The effective plume diameter is appropriate for each individual chiller based on the close proximity and arrangement of the sixteen chiller cells.

Screening Methodology and Vertical Plume Velocity Calculations

The Spillane methodology is based on worst-case calm wind neutral stability conditions to assess the average plume vertical velocity as a function of height. The methodology is based on well-verified laboratory and theoretical treatments of the rise and spread of a buoyant jet, both into a still ambient environment and into a light crosswind. This treatment covers in detail the initial dynamics of the plume as it exits the stack and the entrainment of ambient air into the plume as it rises directly above the stack. In addition to providing clarifications and algebraic solutions to the Spillane methodology, the 2003 Peter Best paper provides additional methodologies that also consider the enhancement of vertical velocities that may occur if the plumes from multiple identical stacks merge and form a higher buoyancy combined plume (referred to here as the enhanced Spillane methodology).

The vertical plume assessment will involve several stages of development. For individual plumes, the stages are:

- (a) In the first stage very close to the stack exit, the high plume momentum will result in a short section in which the conditions at the center of the plume are relatively unaffected by ambient and plume buoyancy conditions. This jet phase extends from the stack exit to approximately a distance of 6.25 D above the stack (where D is the stack diameter) in calm conditions. At the end of this stage, the plume-averaged vertical velocity has decreased to half of the stack exit velocity, with a corresponding increase, or doubling, in effective plume diameter.
- (b) In the second stage, the plume responds to differences between ambient and plume buoyancy conditions, with much cooler and less turbulent ambient air being entrained into the plume from the outside regions of the plume towards the plume centerline. The momentum and buoyancy of the plume significantly influences plume rise and subsequently the dilution of the stack exhaust to decrease plume vertical velocities. This dilution is very sensitive to ambient wind speed, so the calm wind conditions considered here are extremely conservative.
- (c) In the third stage of plume development, plume rise is due entirely to the buoyancy of the plume and continues from some distance until there is an equalization of turbulence conditions within and outside the plume. This final rise is often only achieved at considerable heights/distances from the stack where the effective average vertical velocity is then close to zero. Since there is very little turbulence and near-zero vertical velocities, this stage of plume development is usually not considered for this type of analysis.

In the second stage of development, the analytical solution of the governing equations under these conditions is given by:

$$a = 0.16(z - z_v)$$
$$V = \{(Va)o^3 + 0.12Fo [(z - z_v)^2 - (6.25D - z_v)^2]\}^{1/3} / a$$



Where the subscript 'o' refers to values of the parameters at the stack outlet and the variables are:

- a plume radius (m)
- V average vertical velocity (m/s)
- z height above stack top (m)
- z_v virtual source height (m)
- D stack diameter (m)
- F_o buoyancy flux evaluated at the stack outlet (m^4s^{-3})

These are the two primary equations governing the growth of a single plume in the second stage of development under neutral calm wind conditions. Additional equations governing the first stage of single plume development as well as the interaction of multiple plumes in the second stage of development are discussed in detail in the Best paper.

For multiple stacks in the enhanced Spillane methodology, the equations governing the second stage are calculated from the point when the plumes begin to merge until they are fully merged. The plume merging begins at the height where the plume diameters equal the stack separations and the plumes are fully merged at the height where the plume diameters are equal to $2d(N-1)/2$ for three or more stacks or $2d$ for two stacks. At the fully merged height, the merged plume diameter and velocity is enhanced by the fourth root of the number of stacks. Above the fully merged plume height, the enhanced plume diameter and plume velocities follow the regular equations given for the second stage. Below the fully merged plume height for the merging phase, plume velocities are linearly interpolated by height from the single plume velocity at the height where the plumes begin to merge to the enhanced plume velocity at the fully merged plume height.

Vertical Plume Velocity Calculations for the Diesel Engines

The WBGF is comprised of 32 individual large diesel emergency generator stacks, arranged as 16 double stacked units. The 33rd diesel emergency generator is smaller than the other 32 emergency generators, which would have lesser plume vertical velocities, and therefore was not considered further. Generator stack parameter data (plume exit velocity, plume exit temperature and stack exit diameter) were provided by Cummins. Only one (1) engine will be tested during any one hour. While the engines will be tested at minimum loads, the 100 percent load case was utilized for the worst-case plume analysis. For the engine analysis, two ambient conditions were considered: 41.0°F, the minimum monthly mean of daily minimum temperatures, and 84.3°F, the maximum monthly mean of daily maximum temperatures for the San Jose Airport (*"Climatology of the United States No. 81 – Monthly Station Normals of Temperature, Precipitation, and Heating and Cooling Degree Days 1971-2000 – California"*, February 2002, and *"Climatology of the United States No 20 – Monthly Station Climate Summaries, 1971-2000 – California"*, February 2004). These data is summarized in Table 1.

Table 1 Cummins Stack Characteristics for Vertical Plume Velocity Analysis		
Case #	1	2
Ambient Temperature (°F)*	41.0	84.3
Stack Diameter (m)	0.5588	0.5588
Exhaust Velocity (m/s)*	44.96	44.96
Exhaust Temperature (K)*	716.48	716.48



Stack Release Height (m)	16.03	16.03
Stack Buoyancy Flux (m ⁴ /s ³)	21.06	19.91

*Stack data provided by Cummins at 100% load

Screening level vertical plume velocity assessments were made for two ambient temperatures with calm winds and neutral atmospheric conditions for the cases presented in Table 1 which are based on 100 percent load. The results based on the two ambient conditions are presented in Table 2 and the output from the calculation spreadsheet provided in Attachment A.

The initial jet phase extends to a height of about 64 feet above grade level (ft-agl) for both cases. After the jet phase, plume temperature buoyancy characteristics modeled in the Spillane methodology cause a uniform decrease in plume-averaged vertical velocities, with the critical plume-averaged vertical velocity of 5.3 m/s occurring at about 92 ft-agl for Case 1 and about 93 ft-agl for Case 2. Again, the plume-averaged vertical velocities are shown in the spreadsheets provided in Attachment A.

Case #	1	2
Ambient Temperature (°F)	41.0	84.3
Single Plume Results:		
Plume-Averaged Vertical Velocity at 940 feet-agl (m/s)	1.32	1.30
Height of 5.3 m/s Plume-Averaged Vertical Velocity (feet-agl)	92.2	92.9

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the diesel engine always remain in the light turbulence category and below the significance level of 5.3 m/s at all heights above about 100 ft-agl. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.

Vertical Plume Velocity Calculations for the Rooftop Chillers

The 54 rooftop chillers are each comprised of 16 individual cells, with a cell fan diameter of 36.6 inches. Thus, the 54 chillers are generally arranged six along the longer building length (averaging 49 feet between adjacent chillers) by nine along the shorter building width (averaging 27 feet between adjacent chillers). Chiller stack parameter data (exit velocity and temperature) were provided by the applicant. An effective stack diameter for all sixteen cells was utilized for each chiller. The chillers will utilize variable speed fans and the number of fans that are operational are dependent upon ambient temperature and plant load. However, to be conservative, all



chillers/cells were assumed to be operating at full load. These data is summarized in Table 3 for the same ambient temperatures used for the engine analysis.

Table 3 Chiller Stack Characteristics for Vertical Plume Velocity Analysis		
Case #	1	2
Ambient Temperature (°F)*	41.0	84.3
Effective Stack Diameter (m)**	3.7186	3.7186
Exhaust Velocity (m/s)*	9.82	9.82
Exhaust Temperature (K)*	289.26	313.32
Stack Release Height (m)	30.30	30.30
Stack Buoyancy Flux (m⁴/s³)	12.79	11.81
*Chiller stack data provided by the applicant		
** Calculated value based on the cell diameter of 36.6 inches multiplied by the square of the number of operating cells, or $D_{\text{eff}} = 36.6 \cdot \sqrt{16}$		

The Spillane methodology was originally developed to treat multiple individual stacks that are arranged along a linear x or y direction, but not both directions at once, with stack separations much greater than the stack diameters, typical of boilers/turbines at large power plants. As noted above, the 54 chillers are generally arranged in a 6 x 9 pattern. Therefore, the enhanced Spillane methodology was based on calculating the total merging height for the largest linear direction of chiller placements (which is six chillers spaced 49 feet apart along the longer length of the building). All 54 chillers were considered in the calculation of vertical velocity plume enhancement (both at and above the totally merged height, and for the interpolation down to the plume touching height. Again, the effective single stack diameter of each chiller was based on the combined 16 cells.

Screening level vertical plume velocity assessments were made for the same ambient temperatures with calm winds and neutral atmospheric conditions as was done for the emergency generator engines. The results are presented in Table 4 and the output from the calculation spreadsheets are provided in Attachment A.

The initial jet phase extends to a height of about 176 ft-agl for both cases. The critical plume-averaged vertical velocity of 5.3 m/s occurs in the jet phase at about 170 ft-agl for both cases. The plumes touch (begin to merge) at about 254 ft-agl and are fully merged at about 867 ft-agl for both cases. Under the enhanced Spillane methodology, the merged plume-averaged vertical velocities never approach 5.3 m/s (either above the totally merged height or when interpolated down to the touching height).

Table 4 Chiller Vertical Plume Velocity Analysis Results for Reference Height		
Case #	1	2
Ambient Temperature (°F)	41.0	84.3
Single Plume Results:		
Height of 5.3 m/s Plume-Averaged Vertical Velocity (Within the Jet Phase, feet-agl)	175.7	175.7
Merged Plume Results:		
Plume-Averaged Vertical Velocity at 940 feet-agl (m/s)	3.20	3.16

From these results and for each ambient condition, the vertical plume velocities are less than the threshold value of 5.3 m/s for all heights above about 175 ft-agl and above for the chillers. The heights at which plume-averaged vertical velocities exceed 5.3 m/s only occur during the jet phase



for both cases. These cases also represent worst-case conditions of calm winds at all levels of a neutral atmosphere.

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the chillers always remain in the light turbulence category and below the significance level of 5.3 m/s at all heights above about 175 ft-agl. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.



Attachment A
Spillane Method Plume Velocity Calculations



SINGLE Plume Average Vertical Velocities for Single Walsh Large Emer.Gen Engine, 100% Load, and Maximum Stack Height - Winter Min*

"Aviation Safety and Buoyant Plumes," Peter Best, et. al.

"The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a	278.15 Kelvins	41.0 °F	0.3048 meters/foot	Constants: Assume neutral conditions ($d\theta/dz=0$ or $\theta_p=\theta_a$)
Plume Exit Conditions:		Maximum Stack Height h_s	16.03 meters	52 7/12 feet-inches	Gravity g	9.81 m/s ²
		Stack Diameter D	0.5588 meters	22 inches	λ	1.11
		Stack Velocity V_{exit}	44.96 m/s	147.52 ft/sec	λ_0	-1.0
		Volumetric Flow	11.03 cu.m/sec	23.365 ACFM	$\pi V_{exit} D^2/4$	Sect.2/Eq.1
		Stack Potential Temp θ_s	716.48 Kelvins	830 °F		
		Initial Stack Buoyancy Flux F_0	21.0642 m ³ /s ²		$g V_{exit} D^2 (1-\theta_p/\theta_s)/4 = Vol.Flow(g/\rho)(1-\theta_p/\theta_s)$	Sect.2/Eq.1
		Plume Buoyancy Flux F	N/A m ³ /s ²		$\lambda^2 g V_0^2 (1-\theta_p/\theta_s)$ for a.V. θ_p at plume height (see below)	
		No.of Stacks N	1		1.000 Multiple Stack Multiplication Factor ($N^{0.25}$)	
Conditions at End (Top) of Jet Phase:						
		Height above Stack z_{jet}	3.493 meters*	11.5 feet*	$z_{jet} = 8.25D$, meters*=meters above stack top	Sect.3/Eq.1
		Height above Ground $z_{jet}+h_s$	19.523 meters	64.1 feet		"
		Vertical Velocity V_{jet}	22.480 m/s	73.75 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	"
		Plume Top-Hat Diameter $2a_{jet}$	1.118 meters	3.7 feet	$2a_{jet} = 2D$ Conservation of momentum	"

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase

Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:

Plume Top-Hat Radius a	Solutions in Table Below		$0.16(z-z_c)$, or linear increase with height	Sect.2/Eq.6
Virtual Source Height z_c	1.316 meters*	4.3 feet*	$8.25D[1-(\theta_p/\theta_s)^{1/2}]$, meters* meters above stack top	Sect.2/Eq.6
Height above Ground z_c+h_s	17.346 meters	56.9 feet	where $(\theta_p/\theta_s)^{1/2} = (\theta_p/\theta_s)^{1/2} = 0.6231$	
Vertical Velocity V	Solutions in Table Below		$\{(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (8.25D-z_c)^2]\}^{1/3} / a$	Sect.2.1(6)
Product $(Va)_0$	7.627 m ² /s		$V_{exit} D/2(\theta_p/\theta_s)^{1/2}$	

Solve for plume-averaged vertical velocity at height 940.0 feet		286.512 meters above ground ($z'+h_s$)
Gives the following Height above Stack z'	270.482 meters*	887.4 feet*
Plume Top-Hat Diameter $2a'$	86.133 meters	282.6 feet
Vertical Velocity V	1.320 m/s	4.33 ft/sec
		$V = \{(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (8.25D-z_c)^2]\}^{1/3} / (2a'/2)$

Solve for Height of CASC critical vertical velocity V_{crit} 5.30 m/s plume-averaged vertical velocity		Critical $VV >$ Top of Jet (Spillane)
Find Height above Stack z_{crit}	12.080 meters	39.6 feet
Height above Ground $z_{crit}+h_s$	28.110 meters	92.2 feet
		Solve for $x=(z-z_c)$ simultaneously in both eqs. (i.e., Va and a)
		for $V=4.3$ m/s using the cubic equation $ax^3+bx^2+cx+d=0$, where
		$a=1$, $c=0$, and $b=-0.12F_0/(4.3^3 \cdot 0.16^3) = -4.1451$
		and $d=(0.12F_0(6.25D-z_c)^2 - (Va)_0^3)/(4.3^3 \cdot 0.16^3) = -766.69$

Interpolated Height of critical vertical velocity in Jet Phase:		#N/A feet	http://www.1728.org/cubic.htm
Find Height above Stack z_{crit}	#N/A meters	#N/A feet	gives the real solution $x = z-z_c =$
Height above Ground $z_{crit}+h_s$	#N/A meters	#N/A feet	or z (m/above stack) = 12.080
			z (ft/above ground) = 92.2

Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:

Height (feet)	(meters)	Plume Radius(m)	SingleStk VertVel(m/s)	Plume Temp(K)
Stack Rel.Ht = 52.6				
	0.00	0.279	44.96	
55.0	0.73	0.338	40.24	
60.0	2.26	0.459	30.48	
Top of jet = 64.1				
	3.51	0.559	22.48	
70.0	5.31	0.638	12.50	373.34
80.0	8.35	1.126	7.48	329.40
90.0	11.40	1.614	5.57	311.59
Spillane 5.3 m/s Height = 92.2				
	12.08	1.722	5.30	308.99
100.0	14.45	2.101	4.60	302.01
110.0	17.50	2.589	4.02	296.13
120.0	20.55	3.077	3.64	292.23
130.0	23.59	3.564	3.38	289.50
140.0	26.64	4.052	3.15	287.51
150.0	29.69	4.540	2.99	286.01
200.0	44.93	6.978	2.49	282.14
250.0	60.17	9.417	2.23	280.80
300.0	75.41	11.855	2.05	279.83
350.0	90.65	14.293	1.92	279.39
400.0	105.89	16.732	1.82	279.10
450.0	121.13	19.170	1.73	278.91
500.0	136.37	21.609	1.68	278.77
600.0	166.85	26.485	1.55	278.59
700.0	197.33	31.362	1.47	278.49
800.0	227.81	36.239	1.40	278.41
900.0	258.29	41.116	1.34	278.36
1000.0	288.77	45.993	1.29	278.33
1100.0	319.25	50.869	1.25	278.30
1200.0	349.73	55.746	1.21	278.28
1300.0	380.21	60.623	1.18	278.26
1400.0	410.69	65.500	1.15	278.25
1500.0	441.17	70.377	1.12	278.24
1600.0	471.65	75.253	1.10	278.23
1700.0	502.13	80.130	1.07	278.22
1800.0	532.61	85.007	1.05	278.21
1900.0	563.09	89.884	1.03	278.21
2000.0	593.57	94.761	1.01	278.20

Jet Phase Eqs: 5 foot intervals

Linearly interpolated from Stack Rel.Ht to Top of Jet

Spillane Equations:

$$V_{plume} = \{(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (8.25D-z_c)^2]\}^{1/3} / a$$

$$a = 0.16(z-z_c)$$

$$\theta_p = \theta_s [1 + (1-\theta_p/\theta_s) (\pi V_{plume} D^2 / (4V_{exit} D^2))^{0.25}]^{-2}$$

Max<5.30 m/s

50 foot intervals

100 foot intervals

*Winter Min = Monthly Mean of Minimum Daily Temperatures for 1971-2000 (Lowest in December)
 NOAA Sources: Climatology of the United States No.81 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



SINGLE Plume Average Vertical Velocities for Single Walsh Large Emer.Gen Engine, 100% Load, and Maximum Stack Height - Summer Max*
 "Aviation Safety and Buoyant Plumes," Peter Beat, et. al.

"The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oaky, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a	302.21 Kelvins	84.3 °F	0.3048 meters/foot
Plume Exit Conditions:		Maximum Stack Height h_s	16.03 meters	52 7/12 feet-inches	Gravity g 9.81 m/s ²
		Stack Diameter D	0.5588 meters	22 inches	λ 1.11
		Stack Velocity V_{exit}	44.96 m/s	147.52 ft/sec	λ_0 -1.0
		Volumetric Flow	11.03 cu.m/sec	23,365 ACFM	$\pi V_{exit} D^2 / 4$
		Stack Potential Temp θ_s	716.46 Kelvins	830 °F	Sect.2/Eq.1
		Initial Stack Buoyancy Flux F_0	19.9080 m ⁴ /s ³		$g V_{exit} D^2 (1-\theta_p/\theta_s) / 4 = Vol.Flow(g/h)(1-\theta_p/\theta_s)$
		Plume Buoyancy Flux F	N/A m ⁴ /s ³		$\lambda^2 g V a^2 (1-\theta_p/\theta_s)$ for a, V, θ_p at plume height (see below)
		No. of Stacks N	1		1.000 Multiple Stack Multiplication Factor ($N^{0.25}$)
Conditions at End (Top) of Jet Phase:					
		Height above Stack z_{jet}	3.493 meters*	11.5 feet*	$z_{jet} = 6.25D$, meters*=meters above stack top
		Height above Ground $z_{jet}+h_s$	19.523 meters	64.1 feet	
		Vertical Velocity V_{jet}	22.480 m/s	73.75 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$
		Plume Top-Hat Diameter $2a_{jet}$	1.118 meters	3.7 feet	$2a_{jet} = 2D$ Conservation of momentum

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase

Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:

Plume Top-Hat Radius a	Solutions in Table Below	$0.16(z-z_c)$, or linear increase with height	Sect.2/Eq.6
Virtual Source Height z_c	1.224 meters*	$6.25D[1-(\theta_p/\theta_s)^{1/2}]$, meters*=meters above stack top	Sect.2/Eq.6
Height above Ground z_c+h_s	17.254 meters	56.5 feet	where $(\theta_p/\theta_s)^{1/2} = (\theta_p/\theta_s)^{1/2} = 0.6495$
Vertical Velocity V	Solutions in Table Below	$\{[(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (6.25D-z_c)^2]]^{1/3}\} / a$	Sect.2.1(B)
Product $(Va)_0$	8.158 m ² /s	$V_{exit} D / 2 (\theta_p/\theta_s)^{1/2}$	

Solve for plume-averaged vertical velocity at height 940.0 feet	286.512 meters above ground ($z+h_s$)
Gives the following Height above Stack z'	270.482 meters*
Plume Top-Hat Diameter $2a'$	86.162 meters
Vertical Velocity V	1.285 m/s
	887.4 feet*
	282.7 feet
	4.25 ft/sec
	$2a' = 2 * 0.16(z' - z_c)$
	$V = [(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (6.25D-z_c)^2]]^{1/3} / (2a'/2)$

Solve for Height of CASC critical vertical velocity V_{crit} 5.30 m/s plume-averaged vertical velocity

Find Height above Stack z_{crit}	12.272 meters	40.3 feet	Solve for $x=(z-z_c)$ simultaneously in both eqs. (i.e., Va and a)
Height above Ground $z_{crit}+h_s$	28.302 meters	92.9 feet	for $V=4.3$ m/s using the cubic equation $ax^3+bx^2+cx+d=0$, where
			$a=1, c=0$, and $b=-0.12F_0/(4.3^3 * 0.16^3) = -3.9178$
			and $d=[0.12F_0(6.25D-z_c)^2 - (Va)_0^3]/(4.3^3 * 0.16^3) = -870.20$

Interpolated Height of critical vertical velocity in Jet Phase:

Find Height above Stack z_{crit}	#N/A meters	#N/A feet	http://www.1728.org/cubic.htm
Height above Ground $z_{crit}+h_s$	#N/A meters	#N/A feet	gives the real solution $x = z - z_c =$
			or z (m/above stack) =
			z (ft/above ground) =

Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:

Height (feet)	(meters)	Plume SingleStk	Plume Temp(K)
above ground	above stack	Radius(m)	VertVal(m/s)
Stack Ref.Ht = 52.6	0.00	0.279	44.96
55.0	0.73	0.338	40.24
60.0	2.26	0.459	30.46
Top of jet = 64.1	3.51	0.559	22.48
70.0	5.31	0.653	12.70
80.0	8.35	1.141	7.80
90.0	11.40	1.628	5.65
Spillane 5.3 m/s Height = 92.9	12.27	1.768	5.30
100.0	14.45	2.116	4.64
110.0	17.50	2.604	4.04
120.0	20.55	3.091	3.64
130.0	23.59	3.579	3.35
140.0	26.64	4.067	3.14
150.0	29.69	4.555	2.97
200.0	44.93	6.993	2.46
250.0	60.17	9.431	2.19
300.0	75.41	11.870	2.01
350.0	90.65	14.308	1.89
400.0	105.89	16.747	1.76
450.0	121.13	19.185	1.70
500.0	136.37	21.623	1.63
600.0	166.85	26.500	1.53
700.0	197.33	31.377	1.44
800.0	227.81	36.254	1.37
900.0	258.29	41.131	1.32
1000.0	288.77	46.007	1.27
1100.0	319.25	50.884	1.22
1200.0	349.73	55.761	1.19
1300.0	380.21	60.638	1.16
1400.0	410.69	65.515	1.13
1500.0	441.17	70.391	1.10
1600.0	471.65	75.268	1.07
1700.0	502.13	80.145	1.05
1800.0	532.61	85.022	1.03
1900.0	563.09	89.899	1.01
2000.0	593.57	94.775	1.00

Jet Phase Eqs: 5 foot Intervals

Linearly Interpolated from Stack Ref.Ht to Top of Jet

Spillane Equations:

$V_{plume} = \{[(Va)_0^3 + 0.12F_0 [(z-z_c)^2 - (6.25D-z_c)^2]]^{1/3}\} / a$

$a = 0.16(z-z_c)$

$\theta_p = \theta_s (1 + (1 - \theta_p/\theta_s) (V_{plume} D / (4V_{plume} a^2))^{0.25})^2$

10 foot Intervals

Max < 5.30 m/s

50 foot Intervals

100 foot Intervals

*Summer Max = Monthly Mean of Maximum Daily Temperatures for 1971-2000 (Highest in July)
 NOAA Sources: Climatology of the United States No.81 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



SINGLE/Approximated Plume Average Vertical Velocities for Walsh Chillers using CEC Staff Methodology - Winter Min*

Based on 54 chillers w/ 16 cells/chiller. Calc' "Aviation Safety and Buoyant Plumes," Peter Best, et al.
 eff.diam for each chiller with each cell at 38.6" ID "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume
 (226,000 ACFM total for each chiller) from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a		Constants: Assume neutral conditions (dB/dz=0 or $\theta_a=\theta_b$)	
		278.15 Kelvins	41.0 °F	0.3048 meters/feet	
Plume Exit Conditions:				Gravity g	9.81 m/s ²
	Stack Height h_s	30.30 meters	99 5/12 feet-inches	λ	1.11
<i>Individual Chiller</i>	Stack Diameter D	3.7186 meters	146.4 inches	λ_0	-1.0
	Stack Velocity V_{exit}	9.82 m/s	32.22 ft/sec	$4Vol/(80\pi D^2)$	
<i>Individual Chiller</i>	Volumetric Flow	108.86 cu.m/sec	226,000 ACFM	$\pi V_{exit} D^2/4$	Sec.2.7f1
	Stack Potential Temp θ_s	289.28 Kelvins	61.0 °F		
	Initial Stack Buoyancy Flux F_0	12.7935 m ³ /s ³	20.0 ΔT(°F)	$g V_{exit} D^2 (1-\theta_b/\theta_s)/4 = Vol.Flow(g/m^3)(1-\theta_b/\theta_s)$	Sec.2.7f1
	Plume Buoyancy Flux F	N/A m ³ /s ³		$\lambda^2 g V_a^2 (1-\theta_b/\theta_s)$ for a.V. θ_b at plume height (see below)	
	Number of Chillers n	54		2.711 Multiple Stack Multiplication Factor ($n^{0.25}$)	

Conditions at End (Top) of Jet Phase:					
	Height above Stack z_{jet}	23.241 meters*	76.3 feet*	$z_{jet} = 6.25D$, meters*=meters above stack top	Sec.3.7f1
	Height above Ground $z_{jet}+h_s$	53.543 meters	175.7 feet		
	Vertical Velocity V_{jet}	4.911 m/s	16.11 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	
	Plume Top-Hat Diameter $2a_{jet}$	7.437 meters	24.4 feet	$2a_{jet} = 2D$ Conservation of momentum	

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase

Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:

Solutions in Table Below					
Plume Top-Hat Radius a	0.451 meters*	1.5 feet*	$0.18(z-z_{jet})$, or linear increase with height		Sec.2/Eq.6
Virtual Source Height z_v	30.753 meters	100.9 feet	$6.25D[1-(\theta_b/\theta_s)]^{1/2}$, meters*=meters above stack top		Sec.2/Eq.6
Height above Ground z_v+h_s			where $(\theta_b/\theta_s)^{1/2} = (\theta_b/\theta_s)^{1/2} = 0.9806$		
Vertical Velocity V	Solutions in Table Below		$[(Va)_0^2 + 0.12F_0 [(z-z_{jet})^2 - (6.25D-z_{jet})^2]^{1/2}] / a$		Sec.2.1(6)
Product (Va) ₀	17.908 m ³ /s		$V_{exit} D/2(\theta_b/\theta_s)^{1/2}$		

Single Chiller Results:

Solve for plume-averaged vertical velocity at height		940.0 feet	286.512 meters above ground (z'+h _s)		
Give the following Height above Stack z'	258.210 meters*	840.8 feet*			
Plume Top-Hat Diameter 2a'	81.843 meters	268.5 feet	$2a' = 2*0.16(z'-z_{jet})$		Sec.2/Eq.6
Vertical Velocity V	1.154 m/s	3.79 ft/sec	$V = [(Va)_0^2 + 0.12F_0 [(z'-z_{jet})^2 - (6.25D-z_{jet})^2]^{1/2}] / (2a'/2)$		Sec.2/Eq.6

Solve for Height of CASC critical vertical velocity V_{crit} 5.30 m/s plume-averaged vertical velocity Critical VV < Top of Jet

Find Height above Stack z_{crit}		#N/A meters	#N/A feet	Solve for x=(z-z _{jet}) simultaneously in both eqs. (i.e., Va and a)	
Height above Ground $z_{crit}+h_s$	#N/A meters	#N/A feet		for $V=V_{crit}$ using the cubic equation $ax^3+bx^2+cx+d=0$, where	
			$a=1, c=0$, and $b=[-0.12F_0/(V_{crit}^2*0.16)]= -2.51757$		
			and $d=[0.12F_0(6.25D-z_{jet})^2 - (Va)_0^2]/(V_{crit}^2*0.16) = -8107.12$		

Interpolated Height of critical vertical velocity in Jet Phase:

Find Height above Stack z_{crit}	21.398 meters	70.2 feet	http://www.1728.org/cubic.htm		
Height above Ground $z_{crit}+h_s$	51.700 meters	169.6 feet	gives the real solution $x = z-z_v = 20.9641$		
			or z'(m/above stack) = 21.415		
			z'(ft/above ground) = 169.7		

Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:

Height (feet) above ground	Height (meters) above stack	Plume Radius(m)	Plume SingleStk VertVel(m/s)	Plume Temp(K)
Stack Rel.Ht = 99.4	0.00	1.859	9.82	
100.0	0.18	1.874	9.78	
120.0	6.27	2.361	8.50	
140.0	12.37	2.849	7.21	
160.0	18.47	3.337	5.92	
Single Jet 5.3 m/s Height = 169.8	21.40	3.571	5.30	
Top of Single jet = 175.7	23.24	3.719	4.91	
180.0	24.58	3.858	4.67	282.39
200.0	30.66	4.833	3.83	281.44
220.0	36.75	5.808	3.29	280.80
240.0	42.85	6.784	2.91	280.35
260.0	48.95	7.759	2.64	280.01
280.0	55.04	8.735	2.43	279.74
300.0	61.14	9.710	2.26	279.53
350.0	76.38	12.148	1.87	279.18
400.0	91.62	14.587	1.79	278.92
450.0	106.86	17.025	1.65	278.76
500.0	122.10	19.464	1.55	278.65
550.0	137.34	21.902	1.47	278.57
600.0	152.58	24.340	1.41	278.50
650.0	167.82	26.779	1.36	278.45
700.0	183.06	29.217	1.31	278.41
800.0	213.54	34.094	1.24	278.36
900.0	244.02	38.971	1.18	278.31
1000.0	274.50	43.848	1.13	278.29
1100.0	304.98	48.724	1.08	278.26
1200.0	335.46	53.601	1.05	278.25
1300.0	365.94	58.478	1.02	278.23
1400.0	396.42	63.355	0.99	278.22
1500.0	426.90	68.232	0.96	278.22
2000.0	579.30	92.616	0.87	278.19
2500.0	731.70	117.000	0.80	278.18
3000.0	884.10	141.384	0.75	278.17
3500.0	1036.50	165.768	0.71	278.17
4000.0	1188.90	190.152	0.68	278.16
4500.0	1341.30	214.536	0.65	278.16
5000.0	1493.70	238.920	0.63	278.16

Jet Phase Eqs: 20 ft Intervals
 Linearly Interpolated from Stack Rel.Ht to Top of Jet

Spillane Equations:
 $V_{plume} = [(Va)_0^2 + 0.12F_0 [(z-z_{jet})^2 - (6.25D-z_{jet})^2]^{1/2}] / a$
 $a = 0.18(z-z_{jet})$
 $\theta_p = \theta_s [1 + (1 - \theta_b/\theta_s) (V_{plume} D^2 / (4 V_{plume}^2 a^2))]^{1/2}$

CEC Staff Equation:
 $V_{avg} = n^{0.25} V_{exit}$

Brigg's Equation:
 $V_{avg} = (2/3) \times 1.8^{0.25} \times F_{avg}^{0.143} \times U^{0.125} \times z^{0.143}$
 where $F_{avg} = n F_0$

50 ft Intervals
 Max < 5.3 m/s

100 ft Intervals

500 ft Intervals

*Winter Min = Monthly Mean of Minimum Daily Temperatures for 1971-2000 (Lowest in December)
 NOAA Sources: Climatology of the United States No.61 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



MERGED (along length) Plume Average Vertical Velocities for Walsh Chillers using CEC Staff Methodology - Winter Min*
 *Aviation Safety and Buoyant Plumes," Peter Best, et al.
 "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Merged
 Plume from Two Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a	278.15 Kelvins	41.0 °F	0.3043 meters/feet
Plume Exit Conditions:		Stack Height h_s	30.30 meters	99.5/12 feet/inches	Gravity g 9.81 m/s ²
		Stack Diameter D	3.71856 meters	146.4 inches	λ 1.11
		Stack Velocity V_{exit}	9.82 m/s	32.22 ft/sec	λ_c ~1.0
		Individual Volumetric Flow	106.66 cu.m/sec	226,000 ACFM	$4Vol/(60\pi D^2)$
		Stack Potential Temp θ_s	289.26 Kelvins	61.0 °F	$\pi V_{exit} D^2/4$
		Initial Stack Buoyancy Flux F_b	12.79 m ⁴ /s ³	20.0 ΔT(°F)	Sect.2¶1
		Plume Buoyancy Flux F_p	N/A m ⁴ /s ³		$gV_{exit} D^2(1-\theta_p/\theta_s)/4 = Vol.Flow(g/m^3)(1-\theta_p/\theta_s)$
		Total Number of Stacks n	54		$\lambda^2 g V a^2 (1-\theta_p/\theta_s)$ for a $V_p \theta_p$ at plume height (see below)
		Average Adjacent Stack Separation d	14.94 meters	49.0 feet	
		Number of Stacks along Orientation N	6		

Constants: Assume neutral conditions ($\delta \rho/\rho = 0$ or $\theta_p = \theta_s$)
 Calcs based on multiple plume treatment in Peter Best Paper:
 plume velocities increased by $N^{2/3}$ at the height where plumes
 fully merged (interp. below ht, single merged stack above ht)

Conditions at End (Top) of Jet Phase:

Height above Stack z_{jet}	23.241 meters*	76.3 feet*	$z_{jet} = 6.25D$, meters*=meters above stack top	Sect.3¶1
Height above Ground $z_{jet}+h_s$	53.543 meters	175.7 feet		
Vertical Velocity V_{jet}	4.911 m/s	16.11 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	*
Plume Top-Hat Diameter $2a_{jet}$	7.437 meters	24.4 feet	$2a_{jet} = 2D$	Conservation of momentum *

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet and Merging Phases
 Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:

Single Plume Values: Plume Top-Hat Radius a	Used in Plume Merging Only	$a = 0.16(z-z_s)$, or linear increase with height	Sect.2/Eq.6
Virtual Source Height z_s	0.451 meters*	1.5 feet*	$z_s = 6.25D[1-(\theta_p/\theta_s)^{1/2}]$, meters*=meters above stack top
Height above Ground z_s+h_s	30.753 meters	100.9 feet	where $(\theta_p/\theta_s)^{1/2} = (\theta_p/\theta_s)^{1/2} = 0.9906$
Single Plume Values: Vertical Velocity V	Used in Plume Merging Only	$\{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]^{1/2}\} / a$	Sect.2.1(6)
Product $(Va)_s$	17.906 m ⁴ /s		$V_{exit}(D/2)(\theta_p/\theta_s)^{1/2}$

Plume Merging - Based on Single Plume Calculations where:

Begin Merging Plume Top-Hat Diameter $2a_{touch}$	14.940 meters	49.0 feet	$2a_{touch} = d$, (or $a_{touch} = d/2$)	Sect.3¶3
Height above Stack z_{touch}	47.138 meters*	154.7 feet*	$z_{touch} = z_s + d/(2*0.16)$, meters*=meters above stack top	
Height above Ground $z_{touch}+h_s$	77.440 meters	254.1 feet		
Vertical Velocity V_{touch}	2.709 m/s	8.9 ft/sec	$V_{touch} = \{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]^{1/2}\} / a$	
Total Merging Plume Top-Hat Diameter $2a_{full}$	74.700 meters	245.1 feet	$2a_{full} = 2d(N-1)/2$, (or $a_{full} = d(N-1)/2$) FOR 2 STACKS, $2a_{full} = 2d$	
Height above Stack z_{full}	233.888 meters*	767.3 feet*	$z_{full} = z_s + 2d/(2*0.16)$, meters*=meters above stack top	
Height above Ground $z_{full}+h_s$	264.190 meters	866.8 feet		
Vertical Velocity V_{full}	1.194 m/s	3.9 ft/sec	$V_{full} = \{(Va)_s^3 + 0.12F_b [(z_{full}-z_s)^2 - (6.25D-z_s)^2]^{1/2}\} / a_{full}$	
Product $(V^3a)_{full}$	64 m ⁴ /s ³			

Conditions at End (Top) of Merging Phase - Define new values for V_{full} and a_{full} in Merged Plume calculations (based on TOTAL number of stacks):

Merged Plume Values: Plume Diameter $2a$	Solutions in Table Below		$2a = 2 \times (a_{full} + 0.16(z-z_{full}))$, or linear increase with height
Revised Merged Plume Radius a_m	101.249 meters	332.2 feet	where $a_m = n^{0.25} a_{full}$ where Total Merging Occurs
Revised Merged Plume Velocity V_m	3.236 m/s	10.62 ft/sec	and $V_m = n^{0.25} V_{full}$ where Total Merging Occurs
Revised Virtual Source Height z_{full}	233.888 meters*	767.3 feet*	Height above stack where Total Merging Occurs (shown above)
Revised Vertical Velocity V	Solutions in Tables Below		$V = \{(n^{0.25} V_{full} a_{full})^{1/3}\}^{1/3}$ for heights above total merging elevation $V = V_{touch} + (V_m - V_{touch}) * (z - z_{touch}) / (z_{full} - z_{touch})$ for heights below total merging elevation

Multiple Plume Calculations

Solve for plume-averaged vertical velocity at height	940.0 feet	286.512 meters above ground ($z+h_s$)	
Give the following Height above Stack z	256.210 meters*	840.6 feet*	REGULAR EQNS
Plume Top-Hat Radius a	104.820 meters	343.9 feet	$a = a_m + 0.16(z-z_{full})$ if $z > z_{full}$
Vertical Velocity V	3.188 m/s	10.49 ft/sec	$V = \{(n^{0.25} V_{full} a_{full})^{1/3}\}^{1/3}$ if $z > z_{full}$ $V = V_{touch} + (V_m - V_{touch}) * (z - z_{touch}) / (z_{full} - z_{touch})$ if $z < z_{full}$
Solve for Height of CASC critical vertical velocity V_{crit}	5.30 m/s		BEFORE TOUCHING Critical $VV < Top$ of Jet
Find Height above Stack z_{crit}	JET meters	JET feet	$z_{crit} = z_{full} + \{(n^{0.25} V_{full} a_{full})^{1/3} - a_m\} / 0.16$ if $V_{crit} < V_m$
Height above Ground $z_{crit}+h_s$	JET meters	JET feet	$z_{crit} = z_{touch} + (z_{full} - z_{touch}) * (V_{crit} - V_{touch}) / (V_m - V_{touch})$ if $V_{crit} > V_m$

Table of MERGED Plume-Averaged Vertical Velocities starting at Touching Height:

Height (feet)	(meters)	Plume Radius(m)	Plume Vel(m/s)	Vert.
Begin Merging (touch) = 254.1	47.15	7.470	2.71	
260.0	48.95	#N/A	2.71	
280.0	55.04	#N/A	2.73	
300.0	61.14	#N/A	2.75	
350.0	76.36	#N/A	2.79	
400.0	91.62	#N/A	2.83	
450.0	106.86	#N/A	2.88	
500.0	122.10	#N/A	2.92	
550.0	137.34	#N/A	2.96	
600.0	152.58	#N/A	3.01	
650.0	167.82	#N/A	3.05	
700.0	183.06	#N/A	3.09	
800.0	213.54	#N/A	3.18	
End Merging (full/mp) = 866.8	233.90	101.249	3.24	
900.0	244.02	102.889	3.22	
1000.0	274.50	107.746	3.17	
1100.0	304.98	112.623	3.12	
1200.0	335.46	117.500	3.08	
1300.0	365.94	122.377	3.04	
1400.0	396.42	127.253	3.00	
1500.0	426.90	132.130	2.96	
2000.0	579.30	158.514	2.80	
2500.0	731.70	180.898	2.67	
3000.0	884.10	205.282	2.56	
3500.0	1036.50	229.666	2.46	
4000.0	1188.90	254.050	2.38	
4500.0	1341.30	278.434	2.31	
5000.0	1493.70	302.818	2.25	

Single Plume Eqns (see Single Plume spreadsheet)
 $V_{full} = \{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]^{1/2}\} / a$
 $a = 0.16(z-z_s)$
 $\theta_p = \theta_s [1 + (1 - \theta_p/\theta_s) * (V_{full} D^2 / (4V_{plume} * a^2 * h^2))]$
 Interpolated Layer Eqns
 $V = V_{touch} + (V_m - V_{touch}) * (z - z_{touch}) / (z_{full} - z_{touch})$

Merged Plume Eqns
 $V = \{(n^{0.25} V_{full} a_{full})^{1/3}\}^{1/3}$
 $a = a_m + 0.16(z-z_{full})$



SINGLE/Approximated Plume Average Vertical Velocities for Walsh Chillers using CEC Staff Methodology - Summer Max*

Based on 54 chillers w/ 16 cells/chiller. Calc' "Aviation Safety and Buoyant Plumes," Peter Best, et al.
 eff.diam for each chiller with each cell at 38.6" ID "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume
 (226,000 ACFM total for each chiller) from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a	302.21 Kelvins	84.3 °F	0.3048 meters/feet
Plume Exit Conditions:		Stack Height h_s	30.30 meters	99 5/12 feet-inches	Gravity g 9.81 m/s ²
Individual Chiller		Stack Diameter D	3.7186 meters	146.4 inches	λ 1.11
		Stack Velocity V_{exit}	9.82 m/s	32.22 ft/sec	λ_0 -1.0
Individual Chiller		Volumetric Flow	108.86 cu.m/sec	226,000 ACFM	$4Vol/(80\pi D^2)$
		Stack Potential Temp θ_s	313.32 Kelvins	104.3 °F	$\pi V_{exit} D^2/4$ Sect.2.71
		Initial Stack Buoyancy Flux F_0	11.8065 m ³ /s ³	20.0 ΔT(°F)	$gV_{exit} D^2(1-\theta_s/\theta_a)/4 = Vol.Flow(g/m^3)(1-\theta_s/\theta_a)$ Sect.2.71
		Plume Buoyancy Flux F	N/A	m ³ /s ³	$\lambda^2 g Va^2(1-\theta_s/\theta_a)$ for a.V. θ_s at plume height (see below)
		Number of Chillers n	54		2.711 Multiple Stack Multiplication Factor ($n^{0.25}$)

Conditions at End (Top) of Jet Phase:		Height above Stack z_{jet}	23.241 meters*	76.3 feet*	$z_{jet} = 6.25D$, meters*=meters above stack top	Sect.3.71
		Height above Ground $z_{jet}+h_s$	53.543 meters	175.7 feet		-
		Vertical Velocity V_{jet}	4.911 m/s	16.11 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	-
		Plume Top-Hat Diameter $2a_{jet}$	7.437 meters	24.4 feet	$2a_{jet} = 2D$ Conservation of momentum	-

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase

Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:		Plume Top-Hat Radius a	Solutions in Table Below	0.16(z-z _{jet}), or linear increase with height	Sect.2/Eq.6	
		Virtual Source Height z_v	0.416 meters*	1.4 feet*	6.25D[1-(θ_s/θ_a) ^{1/2}], meters*=meters above stack top	Sect.2/Eq.6
		Height above Ground z_v+h_s	30.718 meters	100.8 feet	where (θ_s/θ_a) ^{1/2} = (θ_s/θ_a) ^{1/2} = 0.9821	
		Vertical Velocity V	Solutions in Table Below	$[(Va)^2 + 0.12F_0 [(z-z_v)^2 - (6.25D-z_v)^2]^{1/2}] / a$	Sect.2.1(6)	
		Product (Va) ₀	17.934 m ² /s	$V_{exit} D/2(\theta_s/\theta_a)^{1/2}$		

Single Chiller Results:		Solve for plume-averaged vertical velocity at height	940.0 feet	286.512 meters above ground (z'+h _s)
		Plume Top-Hat Diameter $2a'$	81.854 meters	268.6 feet
		Vertical Velocity V	1.126 m/s	3.69 ft/sec

Solve for Height of CASC critical vertical velocity V_{crit}		5.30 m/s plume-averaged vertical velocity	Critical VV < Top of Jet
		Find Height above Stack z_{crit}	#N/A meters
		Height above Ground $z_{crit}+h_s$	#N/A meters

Interpolated Height of critical vertical velocity in Jet Phase:		Find Height above Stack z_{crit}	21.398 meters	70.2 feet
		Height above Ground $z_{crit}+h_s$	51.700 meters	169.6 feet

Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:

Height (feet) above ground	Height (meters) above stack	Plume Radius(m)	Plume SingleStk VertVel(m/s)	Plume Temp(K)
Stack Rel.Ht = 99.4	0.00	1.869	9.82	
100.0	0.18	1.874	9.78	
120.0	6.27	2.361	8.50	
140.0	12.37	2.849	7.21	
160.0	18.47	3.337	5.92	
Single Jet 5.3 m/s Height = 169.8	21.40	3.571	5.30	
Top of Single jet = 175.7	23.24	3.719	4.91	
180.0	24.58	3.883	4.67	306.45
200.0	30.66	4.839	3.82	305.51
220.0	36.75	5.814	3.27	304.88
240.0	42.85	6.789	2.89	304.42
260.0	48.95	7.765	2.61	304.08
280.0	55.04	8.740	2.40	303.82
300.0	61.14	9.716	2.24	303.61
350.0	76.38	12.154	1.84	303.24
400.0	91.62	14.592	1.76	303.00
450.0	106.86	17.031	1.62	302.84
500.0	122.10	19.469	1.52	302.72
550.0	137.34	21.908	1.44	302.84
600.0	152.58	24.346	1.38	302.57
650.0	167.82	26.784	1.33	302.52
700.0	183.06	29.223	1.28	302.46
800.0	213.54	34.100	1.21	302.42
900.0	244.02	38.976	1.15	302.38
1000.0	274.50	43.853	1.10	302.35
1100.0	304.98	48.730	1.06	302.33
1200.0	335.46	53.607	1.02	302.31
1300.0	365.94	58.484	0.99	302.30
1400.0	396.42	63.360	0.96	302.29
1500.0	426.90	68.237	0.94	302.28
2000.0	579.30	92.621	0.85	302.25
2500.0	731.70	117.005	0.78	302.24
3000.0	884.10	141.389	0.73	302.23
3500.0	1036.50	165.773	0.69	302.23
4000.0	1188.90	190.157	0.66	302.22
4500.0	1341.30	214.541	0.64	302.22
5000.0	1493.70	238.925	0.61	302.22

Jet Phase Eqs: 20 ft Intervals

Linearly Interpolated from Stack Rel.Ht to Top of Jet

Spillane Equations:

$$V_{plume} = [(Va)^2 + 0.12F_0 [(z-z_v)^2 - (6.25D-z_v)^2]^{1/2}] / a$$

$$a = 0.16(z-z_v)$$

$$\theta_p = \theta_a [1 + (1 - (\theta_s/\theta_a)) (V_{plume} D^2 / (4 V_{plume} a^2 \lambda^2))]^{-1}$$

CEC Staff Equation:

$$V_{plume} = n^{0.25} V_{exit}$$

Brigg's Equation:

$$V_{plume} = (2/3) \times 1.6^{0.25} \times F_{plume}^{0.167} \times n^{0.125} \times z^{-1.167}$$

where $F_{plume} = nF_0$

50 ft Intervals

Max<5.3 m/s

100 ft Intervals

500 ft Intervals

*Summer Max = Monthly Mean of Maximum Daily Temperatures for 1971-2000 (Highest in July)

NOAA Sources: Climatology of the United States No.61 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



MERGED (along length) Plume Average Vertical Velocities for Walsh Chillers using CEC Staff Methodology - Winter Min*
 *Aviation Safety and Buoyant Plumes," Peter Best, et. al.
 "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Merged
 Plume from Two Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

Ambient Conditions:		Ambient Potential Temp θ_a	302.21 Kelvins	84.3 °F	0.3048 meters/feet
Plume Exit Conditions:		Stack Height h_s	30.30 meters	99.5/12 feet/inches	Gravity g 9.81 m/s ²
		Individual Stack Diameter D	3.71856 meters	146.4 inches	λ 1.11
		Stack Velocity V_{exit}	9.82 m/s	32.22 ft/sec	λ_c ~1.0
		Individual Volumetric Flow	106.66 cu.m/sec	226,000 ACFM	$4Vol/(60\pi D^2)$
		Stack Potential Temp θ_s	313.32 Kelvins	104.3 °F	$\pi V_{exit} D^2/4$ Sect.2#1
		Initial Stack Buoyancy Flux F_b	11.81 m ⁴ /s ³	20.0 ΔT(°F)	$gV_{exit} D^2(1-\theta_p/\theta_s)/4 = Vol.Flow(g/m^3)(1-\theta_p/\theta_s)$ Sect.2#1
		Plume Buoyancy Flux F_p	N/A m ⁴ /s ³		$\lambda^2 g V a^2 (1-\theta_p/\theta_s)$ for a.V. θ_p at plume height (see below)
		Total Number of Stacks n	54		
		Average Adjacent Stack Separation d	14.94 meters	49.0 feet	
		Number of Stacks along Orientation N	6		

Constants: Assume neutral conditions ($\delta/\delta_z=0$ or $\theta_s=\theta_a$)
 Calcs based on multiple plume treatment in Peter Best Paper:
 plume velocities increased by $N^{2/3}$ at the height where plumes
 fully merged (interp. below ht, single merged stack above ht)

Conditions at End (Top) of Jet Phase:

Height above Stack z_{jet}	23.241 meters*	76.3 feet*	$z_{jet} = 6.25D$, meters*=meters above stack top	Sect.3#1
Height above Ground $z_{jet}+h_s$	53.543 meters	175.7 feet		
Vertical Velocity V_{jet}	4.911 m/s	16.11 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	*
Plume Top-Hat Diameter $2a_{jet}$	7.437 meters	24.4 feet	$2a_{jet} = 2D$	Conservation of momentum *

Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet and Merging Phases
 Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:

Single Plume Values: Plume Top-Hat Radius a	Used in Plume Merging Only	$a = 0.16(z-z_s)$, or linear increase with height	Sect.2/Eq.6	
Virtual Source Height z_s	0.418 meters*	1.4 feet*	$z_s = 6.25D[1-(\theta_p/\theta_s)^{1/2}]$, meters*=meters above stack top	Sect.2/Eq.6
Height above Ground z_s+h_s	30.718 meters	100.8 feet	where $(\theta_p/\theta_s)^{1/2} = (\theta_p/\theta_s)^{1/2} \approx 0.9821$	
Single Plume Values: Vertical Velocity V	Used in Plume Merging Only	$\{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]\}^{1/3} / a$	Sect.2.1(6)	
Product $(Va)_s$	17.934 m ⁴ /s		$V_{exit}(D/2)(\theta_p/\theta_s)^{1/2}$	

Plume Merging - Based on Single Plume Calculations where:

Begin Merging Plume Top-Hat Diameter $2a_{touch}$	14.940 meters	49.0 feet	$2a_{touch}=d$, (or $a_{touch}=d/2$)	Sect.3#3
Height above Stack z_{touch}	47.103 meters*	154.5 feet*	$z_{touch} = z_s + d/(2*0.16)$, meters*=meters above stack top	
Height above Ground $z_{touch}+h_s$	77.405 meters	254.0 feet		
Vertical Velocity V_{touch}	2.690 m/s	8.8 ft/sec	$V_{touch} = \{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]\}^{1/3} / a$	
Total Merging Plume Top-Hat Diameter $2a_{full}$	74.700 meters	245.1 feet	$2a_{full}=2d(N-1)/2$, (or $a_{full}=d(N-1)/2$) FOR 2 STACKS, $2a_{full}=2d$	
Height above Stack z_{full}	233.853 meters*	767.2 feet*	$z_{full} = z_s + 2d/(2*0.16)$, meters*=meters above stack top	
Height above Ground $z_{full}+h_s$	264.155 meters	866.7 feet		
Vertical Velocity V_{full}	1.164 m/s	3.8 ft/sec	$V_{full} = \{(Va)_s^3 + 0.12F_b [(z_{full}-z_s)^2 - (6.25D-z_s)^2]\}^{1/3} / a_{full}$	
Product $(V^3a)_{full}$	59 m ⁴ /s ³			

Conditions at End (Top) of Merging Phase - Define new values for V_{full} and a_{full} in Merged Plume calculations (based on TOTAL number of stacks):

Merged Plume Values: Plume Diameter $2a$	Solutions in Table Below		$2a = 2 \times (a_{full} + 0.16(z-z_{full}))$, or linear increase with height
Revised Merged Plume Radius a_m	101.249 meters	332.2 feet	where $a_m = n^{0.25} a_{full}$ where Total Merging Occurs
Revised Merged Plume Velocity V_m	3.156 m/s	10.35 ft/sec	and $V_m = n^{0.25} V_{full}$ where Total Merging Occurs
Revised Virtual Source Height z_{full}	233.853 meters*	767.2 feet*	Height above stack where Total Merging Occurs (shown above)
Revised Vertical Velocity V	Solutions in Tables Below		$V = \{(n^{0.25} V_{full})^3 + 0.12F_b [(z-z_{full})^2 - (6.25D-z_s)^2]\}^{1/3} / a$ for heights above total merging elevation

Multiple Plume Calculations

Solve for plume-averaged vertical velocity at height	940.0 feet	286.512 meters above ground ($z+h_s$)	
Plume Top-Hat Radius a	104.826 meters	343.9 feet	REGULAR EQNS
Vertical Velocity V	3.120 m/s	10.24 ft/sec	$a = a_{full} + 0.16(z-z_{full})$ if $z > z_{full}$
			$V = \{(n^{0.25} V_{full})^3 + 0.12F_b [(z-z_{full})^2 - (6.25D-z_s)^2]\}^{1/3}$ if $z > z_{full}$
			$V = V_{touch} + \{(V_m - V_{touch})^3 (z-z_{touch}) / (z_{full}-z_{touch})\}^{1/3}$ if $z_{touch} < z < z_{full}$
			$V =$ single plume values if $z < z_{touch}$
Solve for Height of CASC critical vertical velocity V_{crit}	5.30 m/s		BEFORE TOUCHING Critical $VV <$ Top of Jet
Find Height above Stack z_{crit}	JET meters	JET feet	$z_{crit} = z_{full} + \{(n^{0.25} V_{full})^3 / (V_{crit}^3) - a_m\} / 0.16$ if $V_{crit} < V_m$
Height above Ground $z_{crit}+h_s$	JET meters	JET feet	$z_{crit} = z_{touch} + \{(V_m - V_{touch})^3 (z_{crit}-z_{touch}) / (V_{crit} - V_{touch})\}^{1/3}$ if $V_{crit} > V_m$

Table of MERGED Plume-Averaged Vertical Velocities starting at Touching Height:

Height (feet)	(meters)	Plume Radius(m)	Vert. Vel(m/s)
Begin Merging (touch) = 254.0	47.12	7.470	2.69
260.0	48.95	#N/A	2.70
280.0	55.04	#N/A	2.71
300.0	61.14	#N/A	2.73
350.0	76.38	#N/A	2.76
400.0	91.62	#N/A	2.80
450.0	106.86	#N/A	2.84
500.0	122.10	#N/A	2.88
550.0	137.34	#N/A	2.92
600.0	152.58	#N/A	2.95
650.0	167.82	#N/A	2.99
700.0	183.06	#N/A	3.03
800.0	213.54	#N/A	3.11
End Merging (full/mp) = 866.7	233.87	101.249	3.16
900.0	244.02	102.875	3.14
1000.0	274.50	107.752	3.09
1100.0	304.98	112.629	3.05
1200.0	335.46	117.505	3.00
1300.0	365.94	122.382	2.96
1400.0	396.42	127.259	2.92
1500.0	426.90	132.136	2.89
2000.0	579.30	158.520	2.73
2500.0	731.70	180.904	2.60
3000.0	884.10	205.288	2.49
3500.0	1036.50	229.672	2.40
4000.0	1188.90	254.056	2.32
4500.0	1341.30	278.440	2.25
5000.0	1493.70	302.824	2.19

Single Plume Eqns (see Single Plume spreadsheet)
 $V_{full} = \{(Va)_s^3 + 0.12F_b [(z-z_s)^2 - (6.25D-z_s)^2]\}^{1/3} / a$
 $a = 0.16(z-z_s)$
 $\theta_p = \theta_s [1 + (1 - \theta_p/\theta_s) (V_{full} D^2 / (4V_{plume} a^2 h^2))]$
 Interpolated Layer Eqns
 $V = V_{touch} + \{(V_m - V_{touch})^3 (z-z_{touch}) / (z_{full}-z_{touch})\}^{1/3}$

Merged Plume Eqns
 $V = \{(n^{0.25} V_{full})^3 + 0.12F_b [(z-z_{full})^2 - (6.25D-z_s)^2]\}^{1/3} / a$
 $a = a_{full} + 0.16(z-z_{full})$

