

DOCKETED

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Document Title:	Jeffrey Reed, PhD Comments Presentation - Renewable Hydrogen Roadmap Progress Report to Stakeholders
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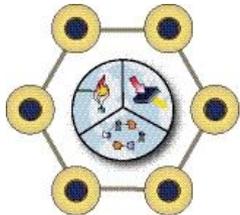
Comment Received From: Jeffrey Reed, PhD
Submitted On: 11/15/2018
Docket Number: 17-HYD-01

Presentation - Renewable Hydrogen Roadmap Progress Report to Stakeholders

Additional submitted attachment is included below.



Renewable Hydrogen Roadmap Progress Report to Stakeholders



**ADVANCED POWER
& ENERGY PROGRAM**

UNIVERSITY of CALIFORNIA • IRVINE

November 13, 2018

Renewable Hydrogen Production Technology Assessment

I. Goals and Approach

II. Technologies covered

- a. Electrochemical
- b. Thermochemical
- c. Anaerobic Digestion with Reformation

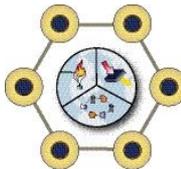
III. Technology Cost Assessment and Forecasting Approach

IV. Cost and Performance Assessment and Forecasting Results

V. Approach to Modeling Costs for Transportation through Dispensing

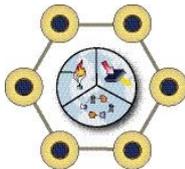
VI. Status of Other Roadmap Tasks

VII. Questions and Comments

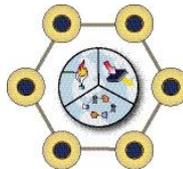
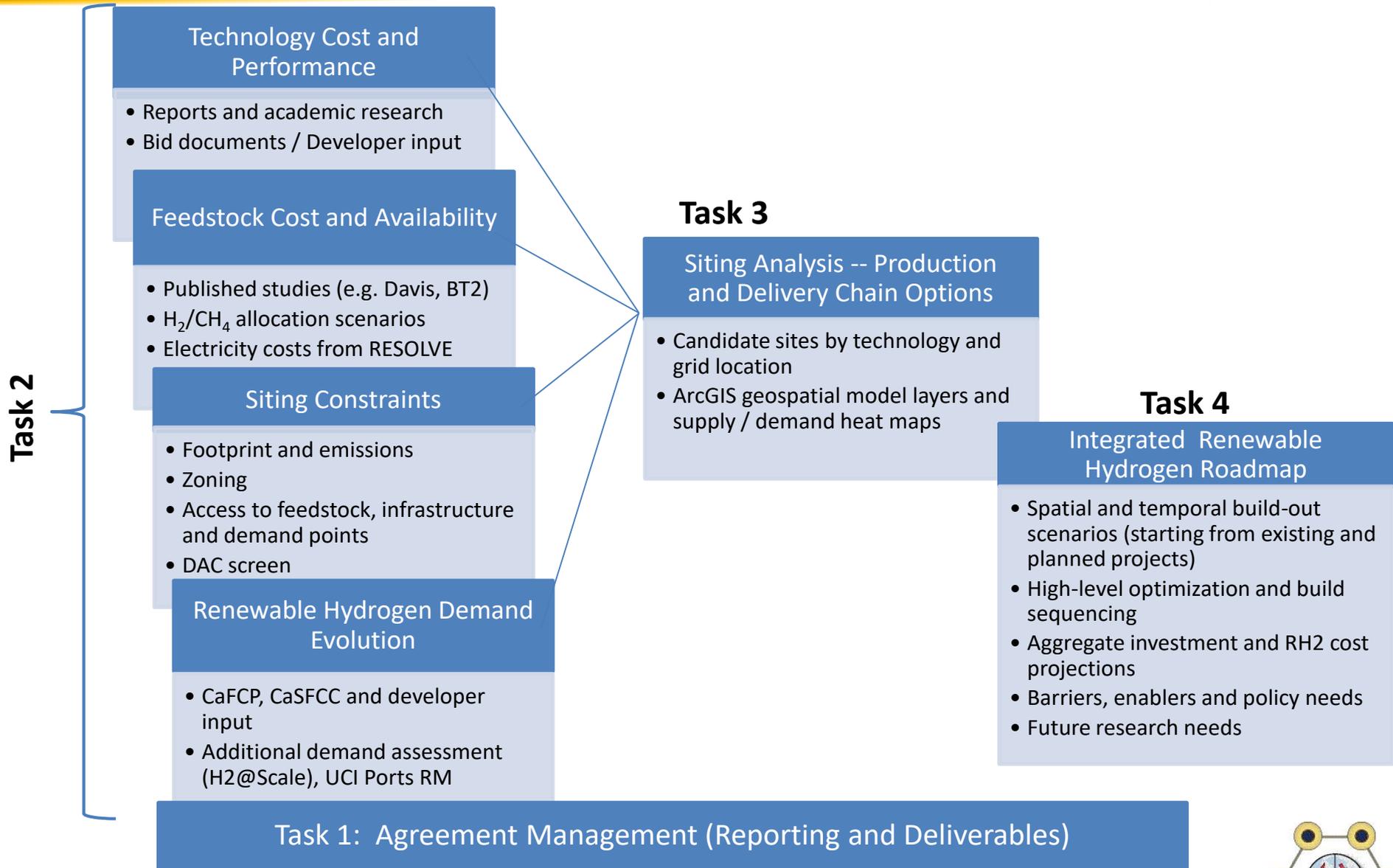


Renewable Hydrogen Roadmap Project Goals

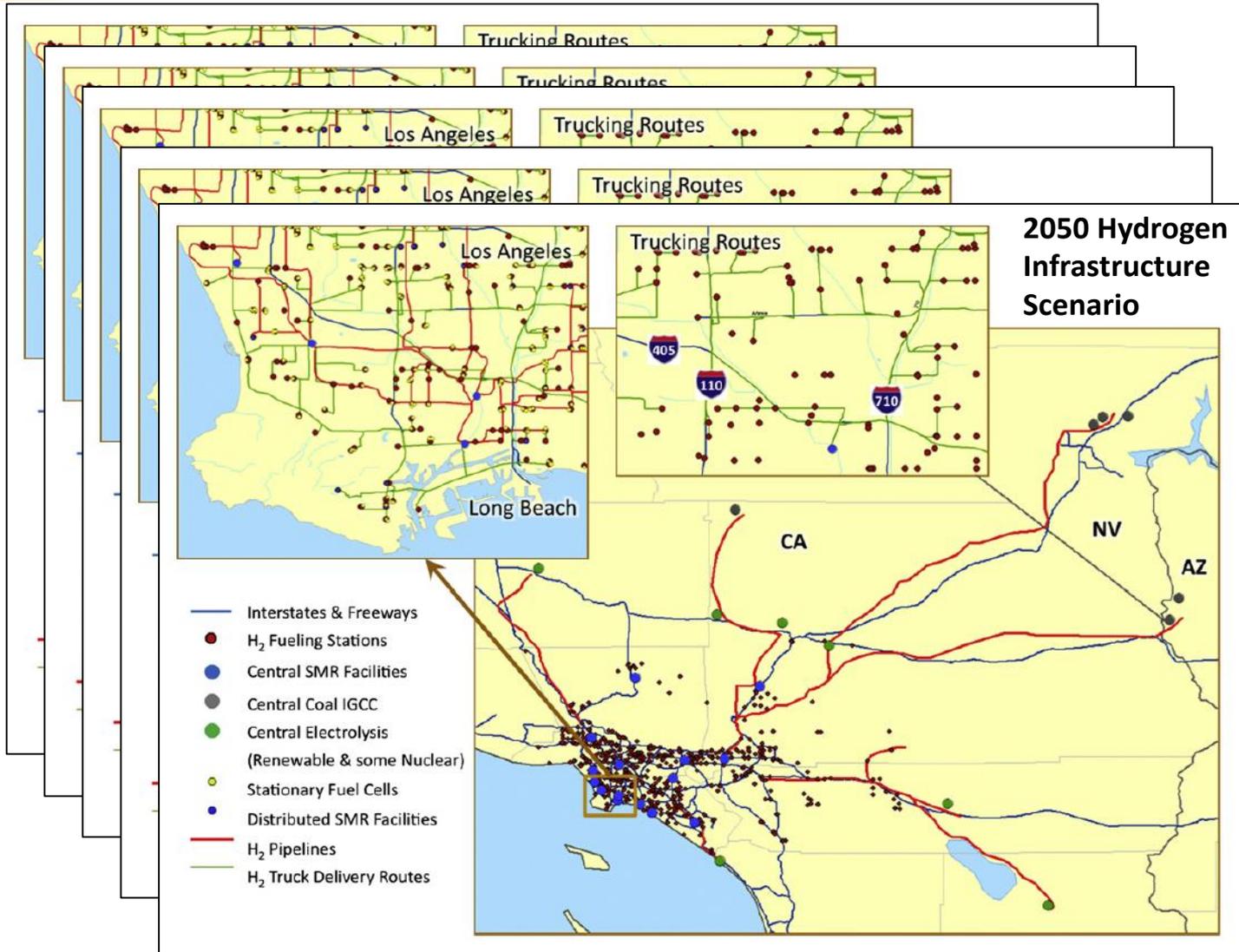
- To provide specific guidance on actions needed to ensure success over the next 5 years in establishing the foundation projects for renewable hydrogen (RH2) production to serve the growing Fuel Cell Electric Vehicle (FCEV) market
- Maximize insights and lessons learned from first-generation RH2 projects
- Project cost evolution, aggregate investment and funding support needed to reach self-sustainability based on pump price and credit value scenarios
- Provide a high-level (“20,000 foot”) roadmap through 2050 as a foundation for further refinement
- Maximize value and leverage of prior and ongoing work including the DOE H2@Scale initiative
- Engage industry stakeholders to validate conclusions and findings
- 1 year effort to conclude in June / July 2019



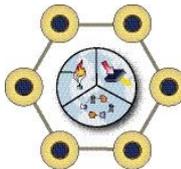
General Flow of Work Packages



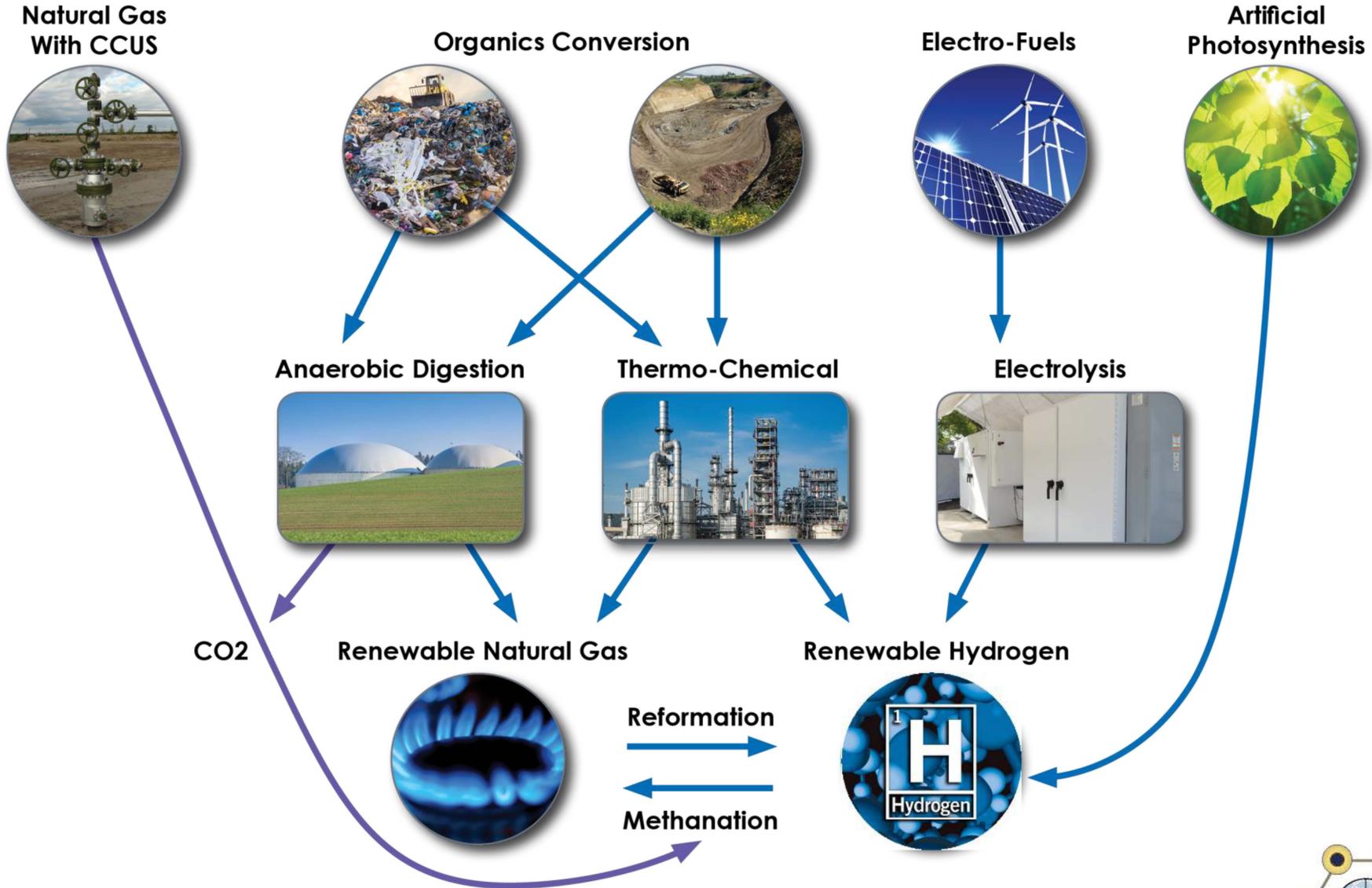
Time-Phased Renewable Hydrogen Deployment



Source: Projecting full build-out environmental impacts and roll-out strategies associated with viable hydrogen fueling infrastructure strategies. Stephens-Romero S.; Brown, T.; Carreras-Sospedra, M.; Kang, J.; Brouwer J.; Dabdub, D.; Recker, w.; Samuelsen, G. S.; Int'l Journal of Hydrogen Energy, 2011



Renewable and Zero-Carbon Gas Pathways

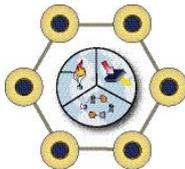


Interim Results



Stakeholder Engagement

- **Roughly 30 stakeholder interviews planned**
- **20 interviews completed spanning the supply chain:**
 - **Technology Vendors**
 - **RH2 Project Developers**
 - **Industrial Gas Companies**
 - **Hydrogen Station Developers**
 - **Consulting Engineers**
 - **Utilities**
- **Additional interviews to be conducted through end of December**



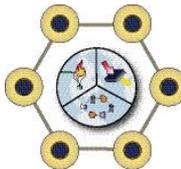
Interview Topics and Preliminary Themes

Topic Area	Themes
Market Evolution	<ul style="list-style-type: none"> • Market has “launched” but needs to scale • Most parties rely on CaFCP forecasts (upper scenario of 1M FCEV by 2030) but recognize the potential importance of applications beyond light duty vehicles particularly MD/HD
Ability to Meet Long-term Goal of \$4/kg dispensed	<ul style="list-style-type: none"> • \$2/kg uncompressed at the plant gate is challenging but possible with scale and R&D • Building scale (project and sector) is the key to cost reduction • All-in cost of \$4/kg very challenging but cost-per-mile parity (\$6 - \$8/kg dispensed) is within range by 2025 to 2030 (net of LCFS value) and around \$10/kg in the next project generation
Best Pathways in the “End Game”	<ul style="list-style-type: none"> • Diversity of views but most see a mix of technologies with both central and localized deployment • Strong trend toward LH2 supply chain
Barriers / Issues	<ul style="list-style-type: none"> • Uncertainty in LCFS credit values and in the pace of growth in demand for renewable hydrogen • Lack of reliability of supply could stall market acceleration • Need for sustained government support across budget cycles • Lack of access to low-cost renewable electricity as feedstock • Limited supply of biomethane for SMR pathways • Permitting challenges (depending on technology and location)

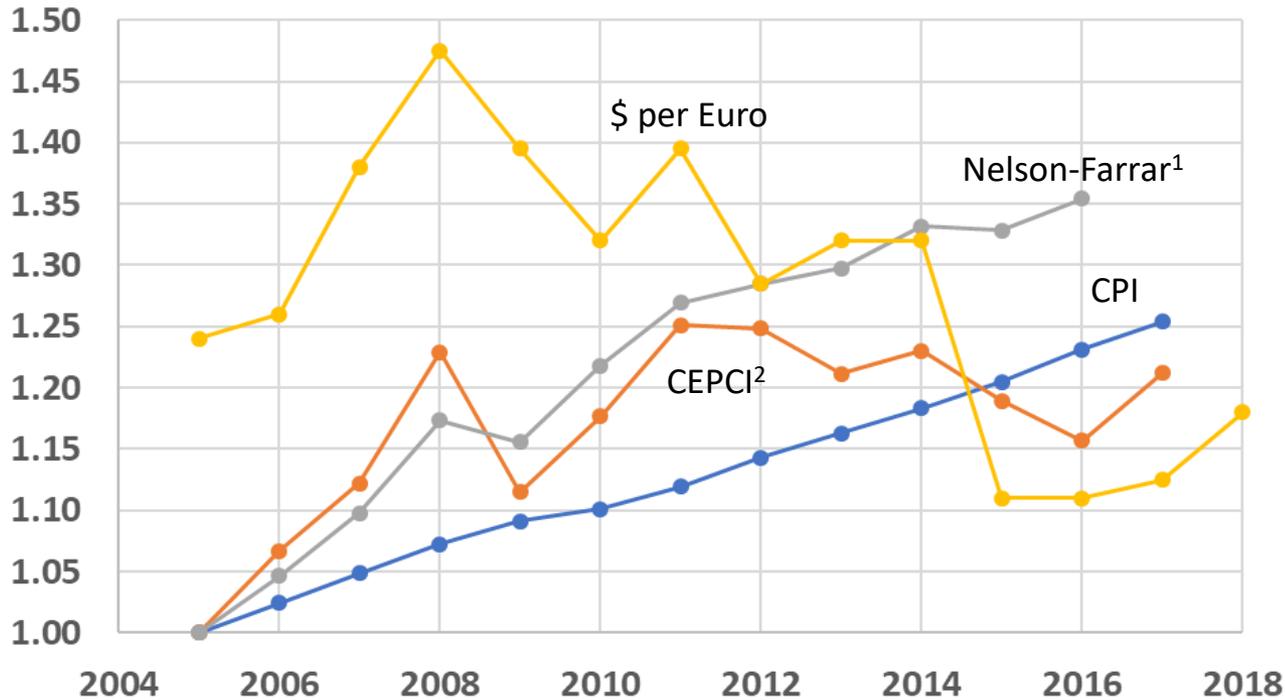


Profiling Current Cost and Performance

- **Current cost and performance (conversion efficiency) were assessed using a variety of sources**
 - **Published academic papers**
 - **Agency reports and tools (such as National Energy Research Center (NREL) reports and Hydrogen Analysis Tool (H2A) case studies**
 - **Publicly available data from CEC solicitations**
 - **Stakeholder interviews**
- **There is significant variation on reported costs due to a variety of factors including:**
 - **Differences in the equipment sets used and included in the reported costs**
 - **Varying methods used to estimate project costs (prior actual costs, bottom-up estimate using bids or costing references, combination)**
 - **Inclusion or exclusion of indirect costs (engineering, permitting, site prep) (order of 20% of total cost)**
 - **Inclusion or exclusion of “Nth Plant” adjustment (order of 25% factor)**
 - **Uncertainty in cost indexation (choice of cost indices used to normalize cost estimates made at different times)**
 - **Uncertainty in scale factors used to normalize costs of plants of differing size**
- **Non-cost parameters show less variation in reported and forecast values**



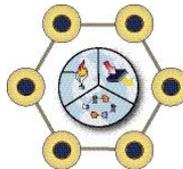
Normalization Indices



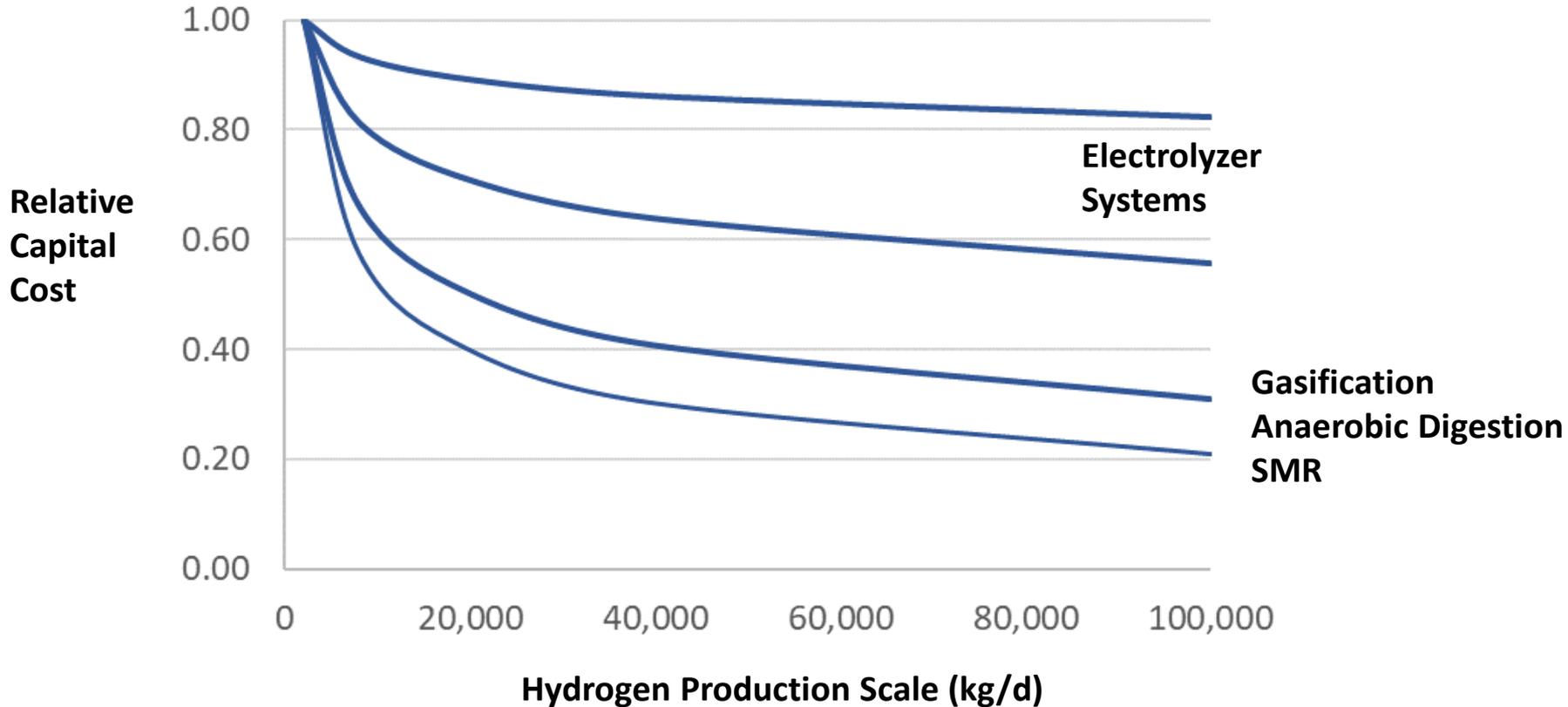
- Adjusting cost estimates with different time stamps and currencies requires currency conversion and escalation
- These conversions can introduce additional uncertainty at times when the indices are changing rapidly but applying these adjustments generally reduces the spread in the data

1 Refinery cost escalation index

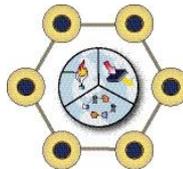
2 Chemical Engineering Plant Cost Index



Scale Dependence of Unit Cost

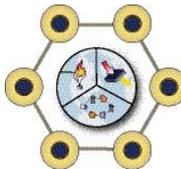


- **Electrolyzers show modest scale sensitivity while anaerobic digestion systems and gasifiers are highly scale sensitive and require scale of greater than 20,000 kg/day of hydrogen production capacity to reach minimum efficient scale**

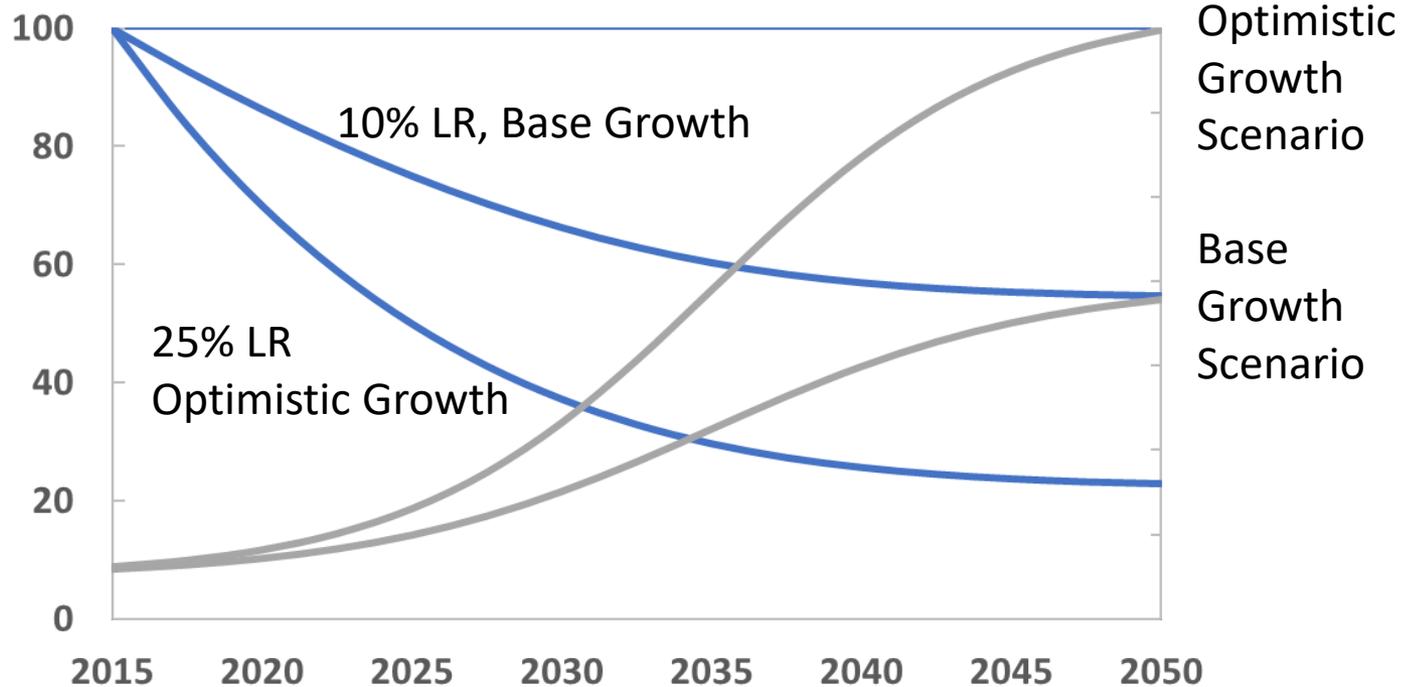


Technology Forecasting Methodology

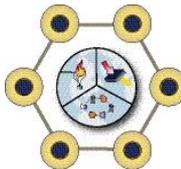
- **Technology forecasting methods**
 - Expert elicitation (researchers, equipment vendors)
 - Progress or learning rate analysis / trend analysis
 - Bottom-up analyzes based on design, bill-of-materials and production scale
 - Analogy or proxy analysis
- **Literature and reports of all three types were used for this study**
- **Dollars normalized to \$2018 using Consumer Price Index and/or Chemical Engineering Plant Cost Index (CEPCI)**



Market Growth and Learning Rate

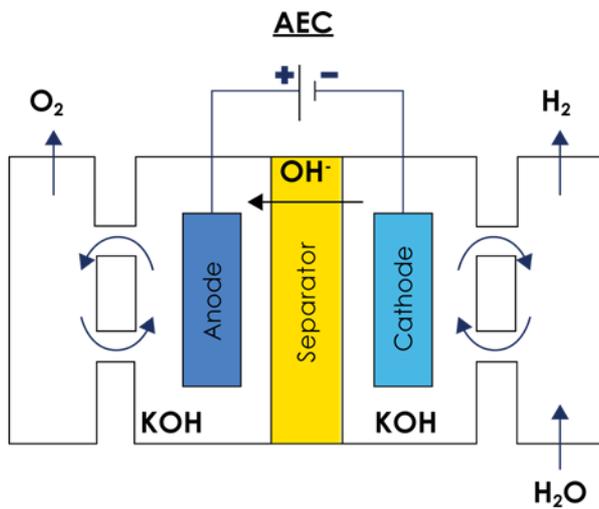


- Progress or learning rate has proven to be an accurate predictor of cost reduction for many technologies
- This group of methods forecasts a percent reduction in cost over time or as a function of cumulative production of a technology with cumulative production showing the better correlation (“Wright's Law”)
- Learning rates (cost reduction per doubling of cumulative production) of 5% to 20% are typical with higher rates more common for digital and electrochemical technologies

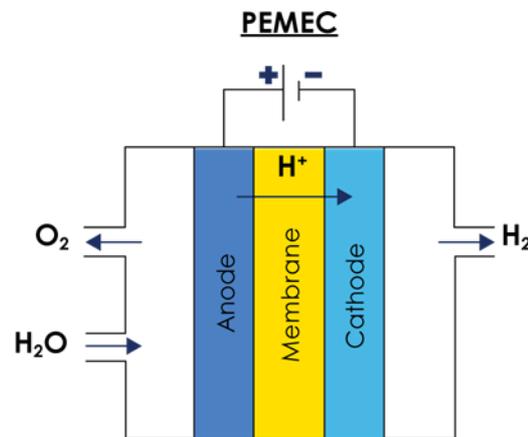


Water Electrolysis

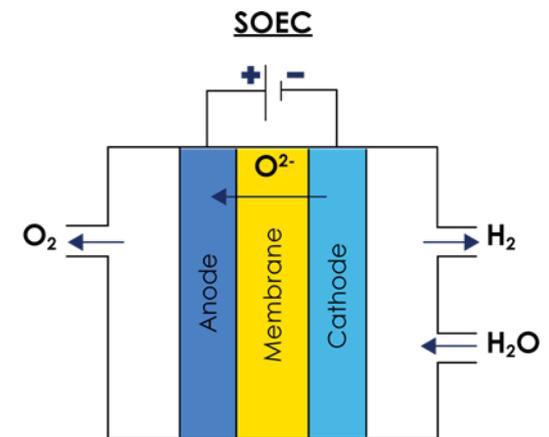
- Water electrolysis creates hydrogen by splitting water into hydrogen and oxygen by applying voltage across an electrolyte
- There are several electrolysis technologies under development featuring different electrolytes and operating temperatures



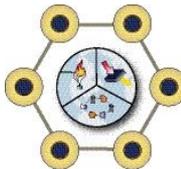
Operating Temperature 60 – 80C



50 – 80C

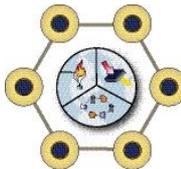


650 – 1000C

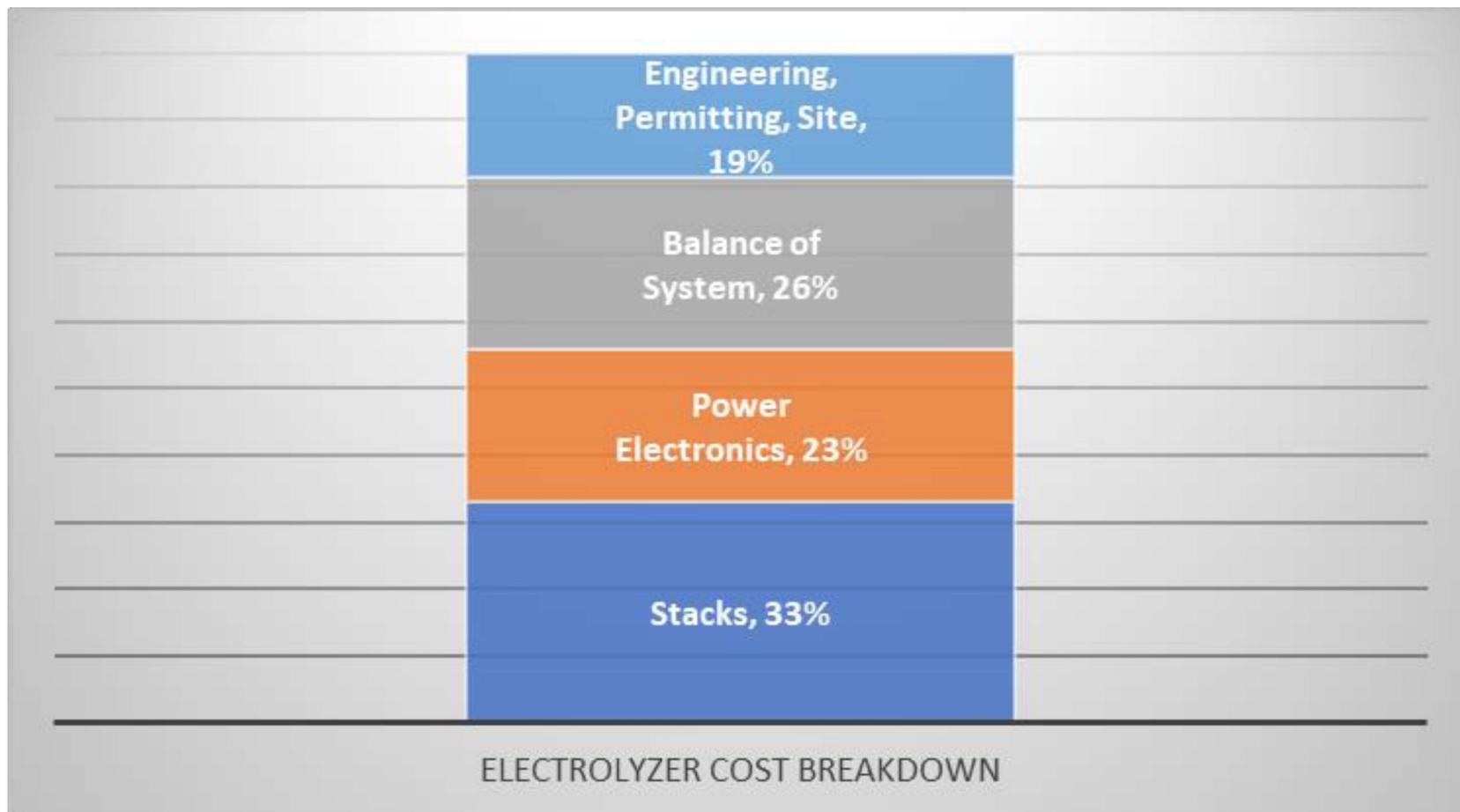


Electrolyzer Technical Maturity and Deployment Status

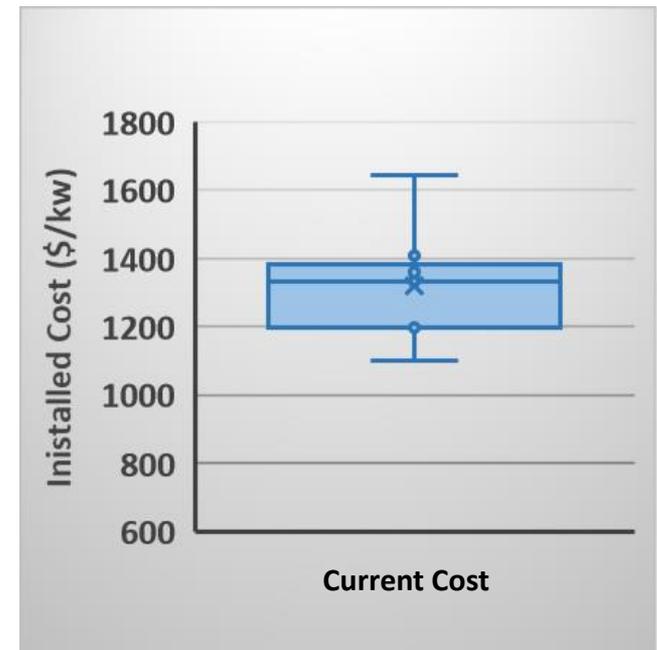
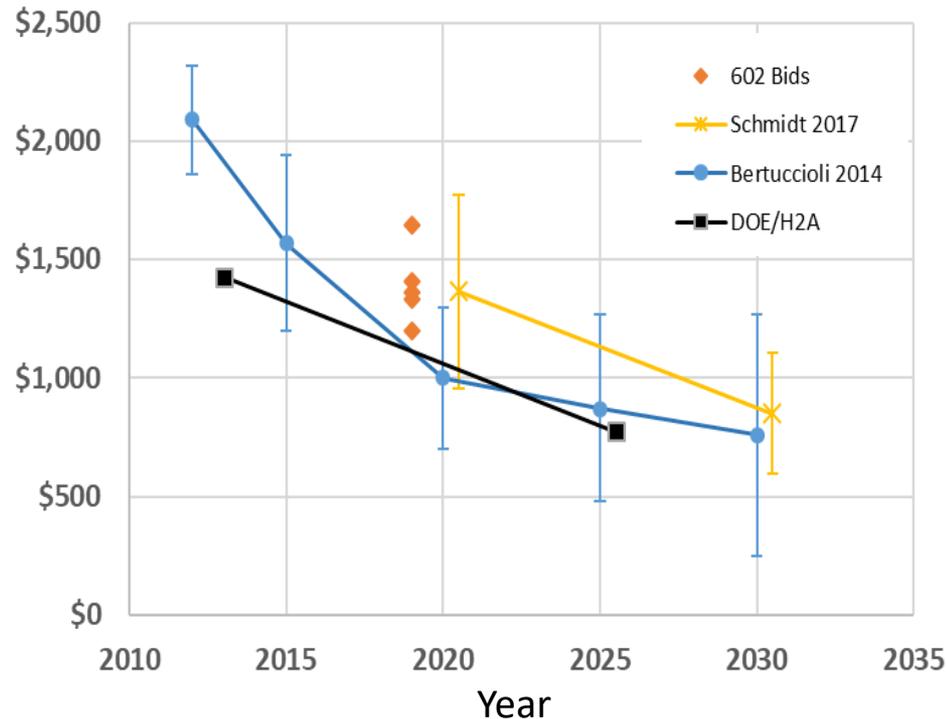
- **Alkaline electrolyzers have been in commercial deployment since the 1960's and are commercially mature and have a global cumulative capacity base of 25 GWe**
- **PEM electrolyzers have been in commercial deployment for roughly 10 years and have a global cumulative capacity base of around 1 GWe**
- **Solid oxide electrolyzers are in pre-commercial development and expected to reach commercial readiness in the early 2020's**



Typical Electrolyzer Total Project Cost Breakdown

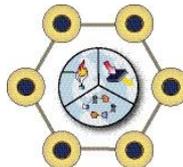


PEM Electrolyzer Cost

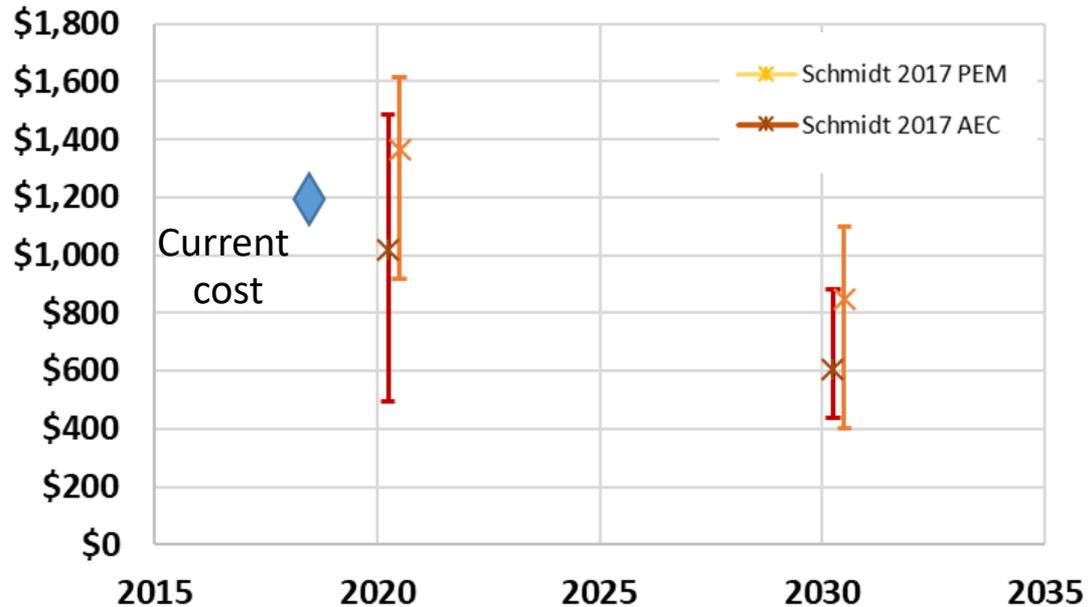


- The data from the GFO-17-602 bids are slightly higher than the other data sources but within range of the published data – the source could be price versus cost, early market added costs or inclusion of some indirect costs
- For purposes of this study, the average of the reported costs is used as the current cost basis (\$1335/kW_e installed)

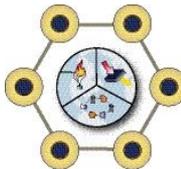
Scope: All-in installed cost excluding land, contingency and construction financing



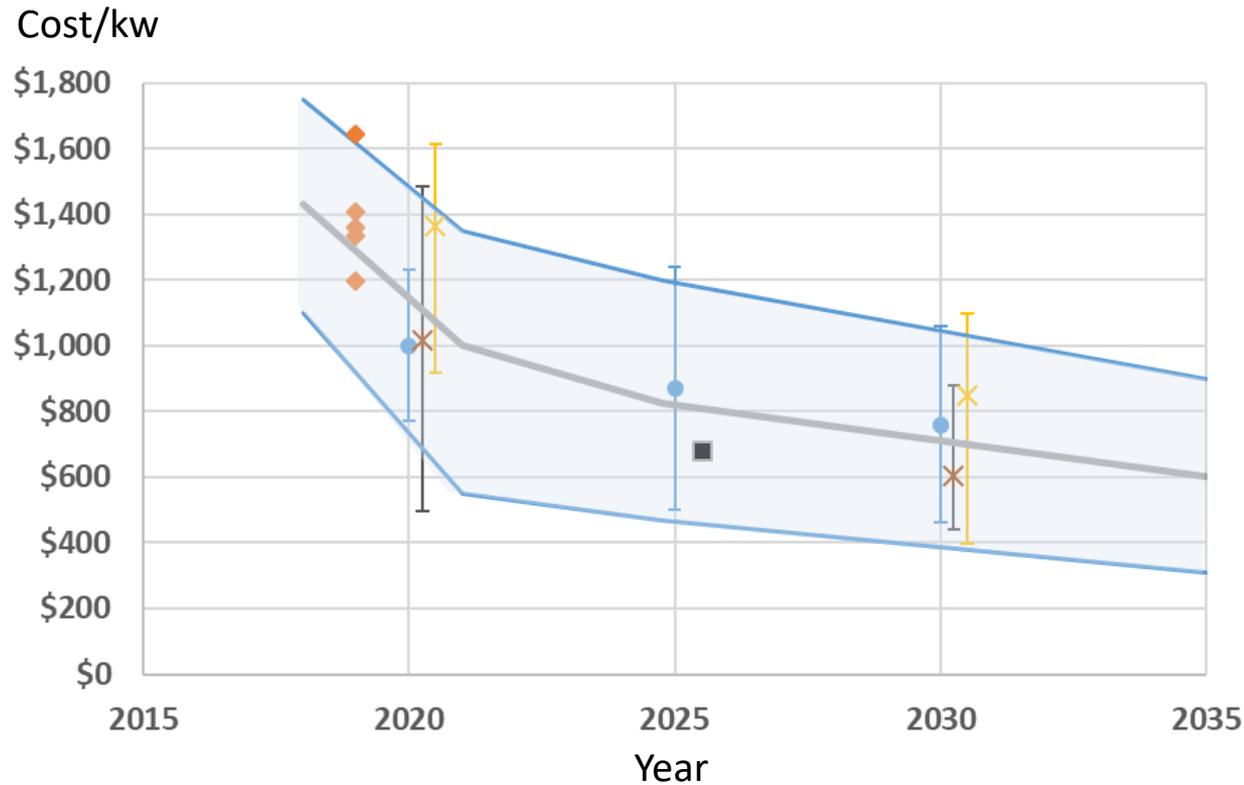
Alkaline Electrolyzer Costs



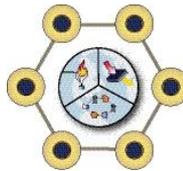
- Alkaline electrolyzer costs are estimated to be 20% to 40% below PEM costs but PEM costs are declining more rapidly to costs are expected to converge over time



Electrolyzer Cost Forecast



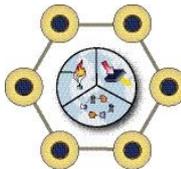
- The various data sources are relatively consistent in their assessment of the rate of cost reduction although there is spread in the forecast costs at each time point
- High, Base and Low cost ranges have been established to capture the range of the forecast data
- Solid oxide electrolyzers are expected to enter the mix in the early 2020's – costs are expected to be within the forecast envelop



Current and 2030 Forecast Electrolyzer Performance Data

Parameter	2018 Value	2030 Value
Stack Electricity Use	49.2	46.7
Total System Electricity Use	54.6	50.2
Stack Life	60,000 hours	85,000 hours
Fixed Maintenance O&M	3 – 3.2% of Capex	Pro-rate with Capex

- **The above values are taken from the DOE current and future H2A Case studies for PEM electrolysis**
- **Values are consistent with the forecasts in Schmidt and Bertuccioli**



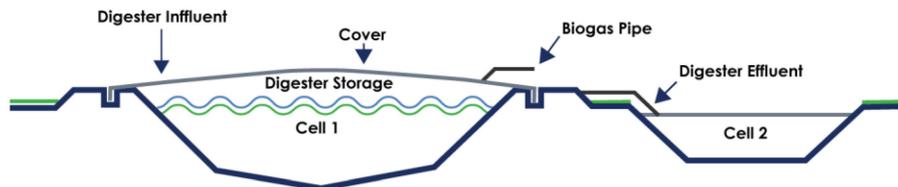
Anaerobic Digestion

- **Anaerobic digestion is the decomposition of organic matter in an oxygen-free environment**
 - **The primary products are methane and CO₂**
 - **Feedstocks include animal waste, food waste, sewage, green waste and other materials**
 - **Anaerobic digestion is suitable for biogenic feedstock with relatively high moisture content**
- **Product gas requires CO₂ separation and other conditioning steps if it is to be pipeline injected or used as vehicle fuel**
- **Renewable hydrogen pathways require reformation of the product methane into hydrogen**

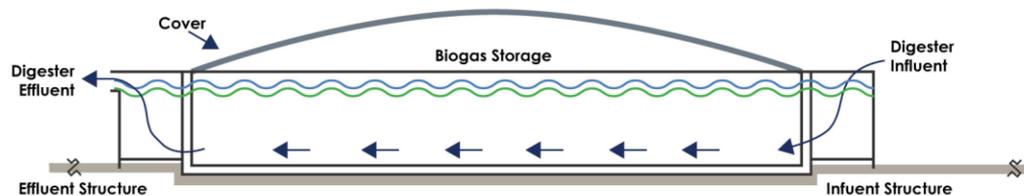


There are a variety of AD technologies

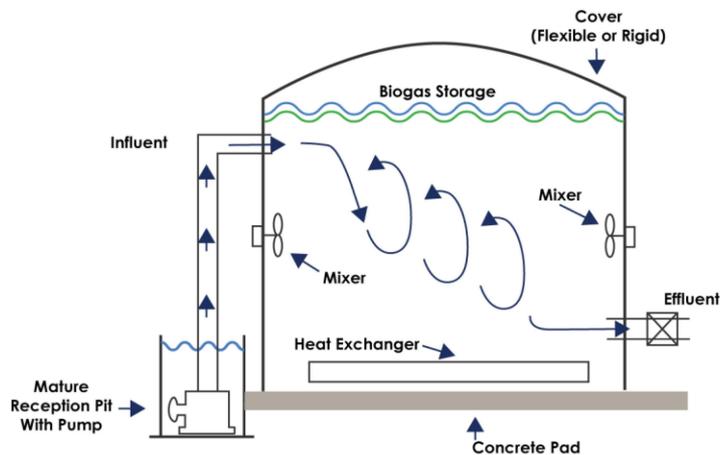
Covered Lagoon



Plug Flow

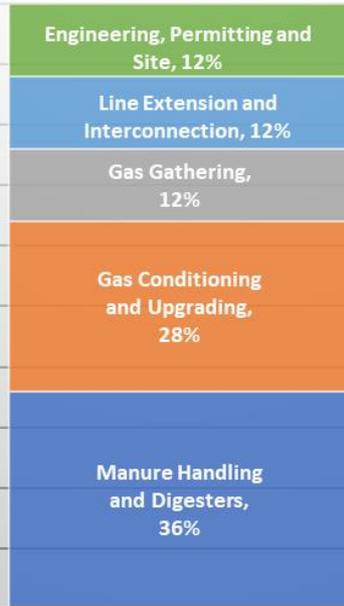


Complete Mix



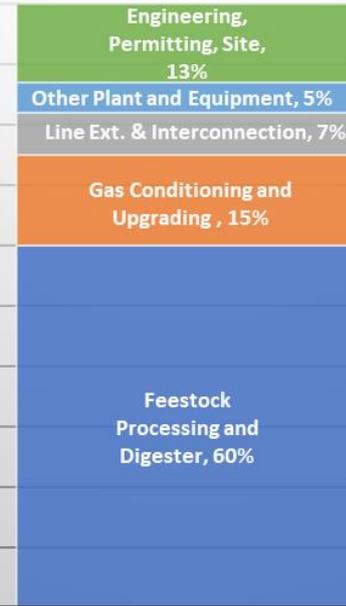
Representative Cost Breakdowns

\$100 - \$200/(MMBTU/yr)



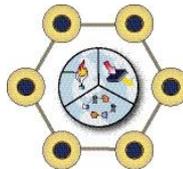
DAIRY CLUSTER COST BREAKDOWN

\$200 - \$300/(MMBTU/yr)

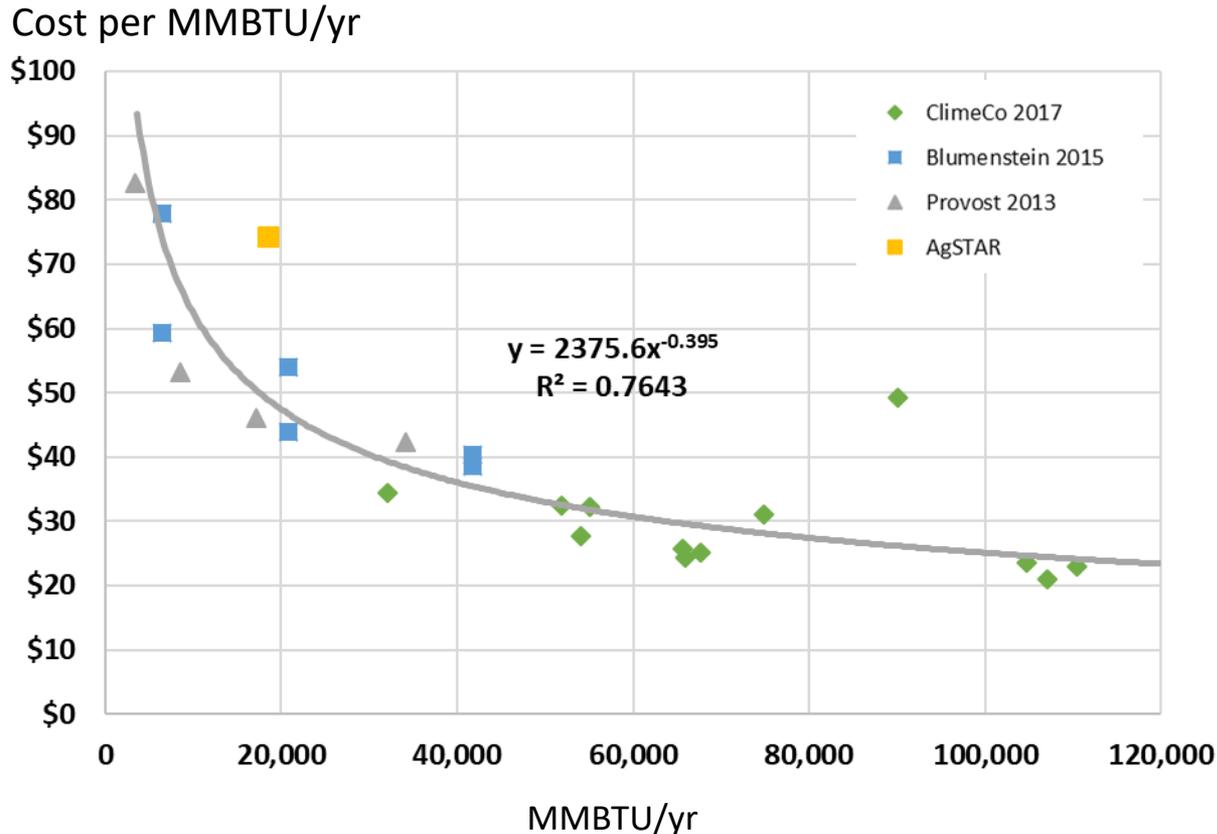


FOODWASTE DIGESTER COST BREAKDOWN

Scope: Total project cost excluding contingency, land purchase and construction financing



Double Lined Covered Lagoon Dairy Digester Costs

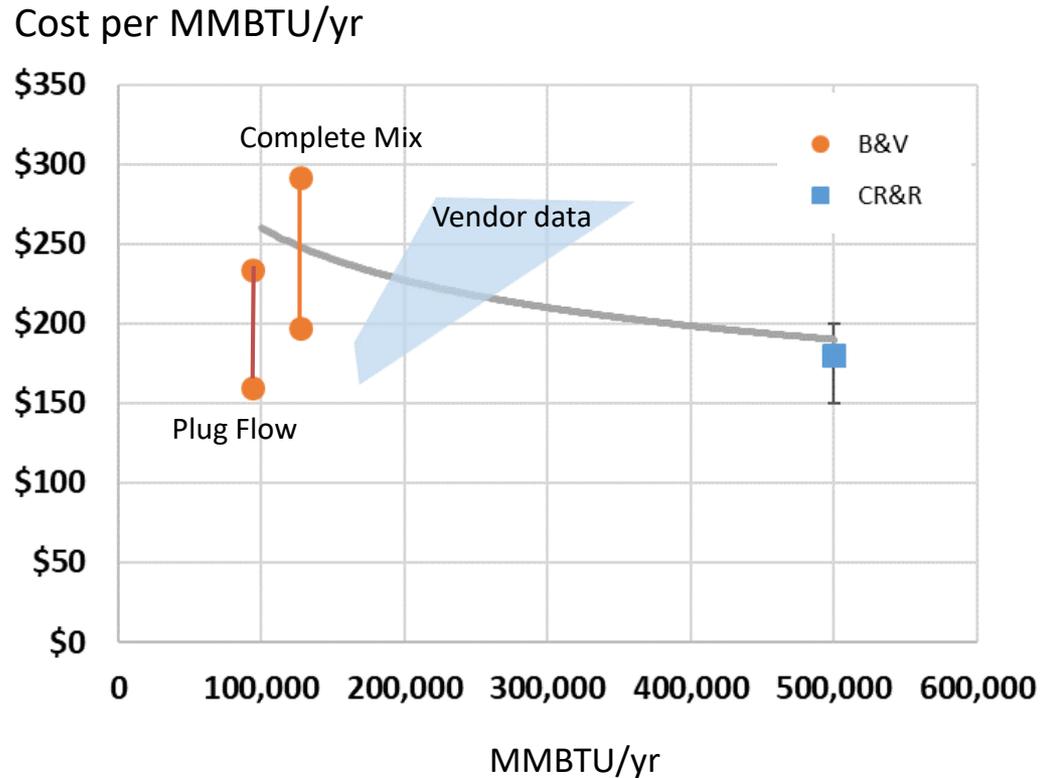


- **Scope: Double-lined covered lagoon and manure handling**
- **Data correlation is very good with the exception of two outliers**
- **Uncertainty band of +/- 20% captures nearly all the data**

Scope: digester system, manure handling, peripherals



Complete Mix Digester Costs



- **Less data available on complete mix systems but, for the scope considered, costs are in the range of \$225 +/- 25% over the size range considered**
- **Additional data gathering is on progress**

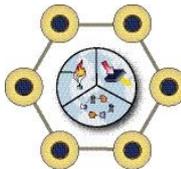
Scope: All-in installed cost excluding construction financing



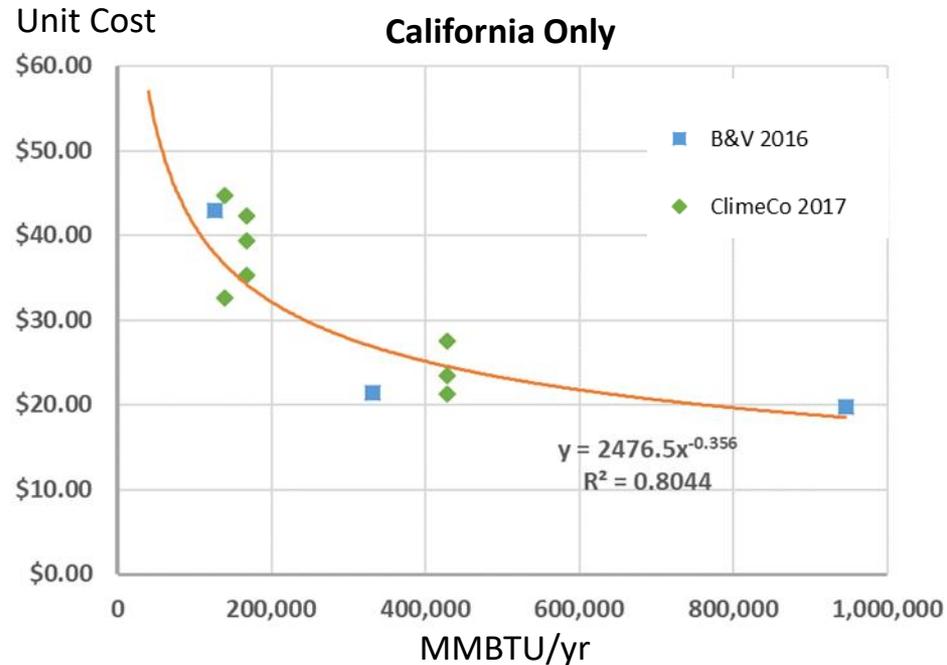
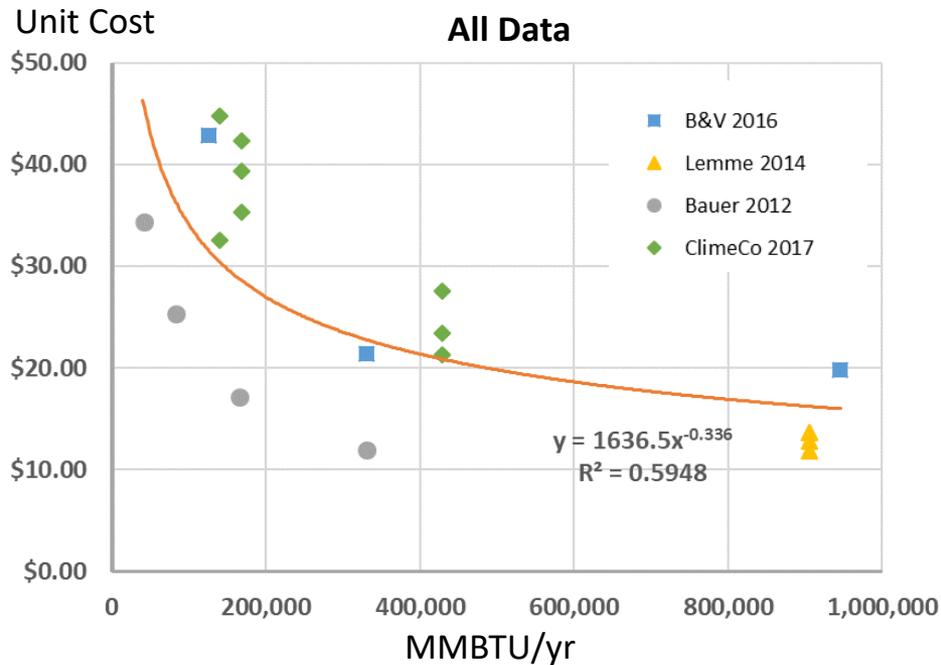
Biogas Conditioning and Upgrading

- **Biomethane projects have employed a variety of gas upgrading technologies**
 - Pressure Swing Adsorption
 - Membranes
 - Amine Scrubbers
 - Water Scrubbers
 - Cryo separation (not fully commercial)

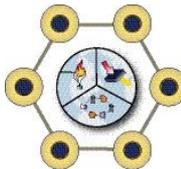
- **There is project-to-project variation in cost based on raw biogas composition**
 - Methane fraction
 - Presence of sulfur, nitrogen, siloxanes and other constituents



Conditioning and Upgrading Costs



- Data consistency is relatively good with the various technologies grouping within +/- 10%
- Scale factor approximately 0.65
- California-only data shows a high degree of consistency (correlation)

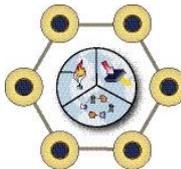


Methane Reformation

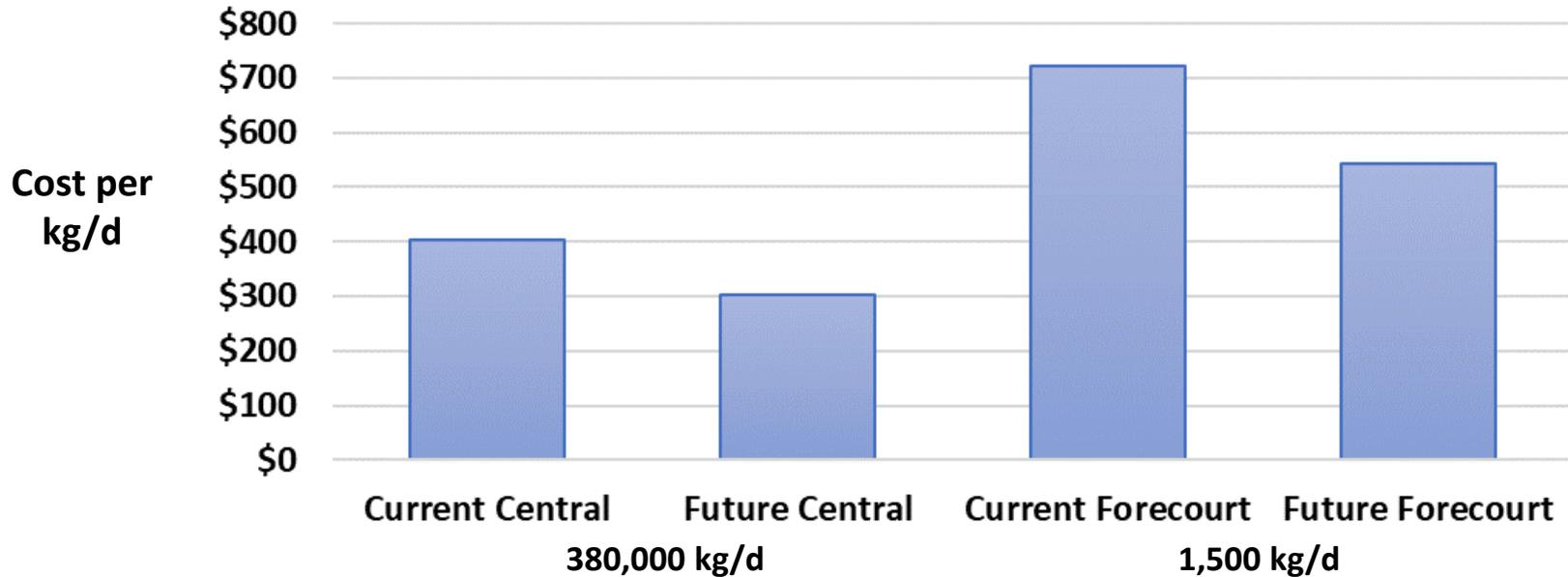
- The pathways that yield methane or a high methane fraction require reformation
- Steam Methane Reformation is the most widely used process



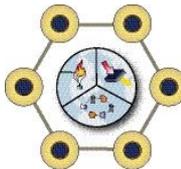
- Other concepts are being pursued
 - Dry reforming
 - Partial oxidation / chemical looping
 - Autothermal
 - Catalyst, plasma-stimulated and other concepts
- Reducing cost at small production scale (2,000 kg/d) is an important research focus



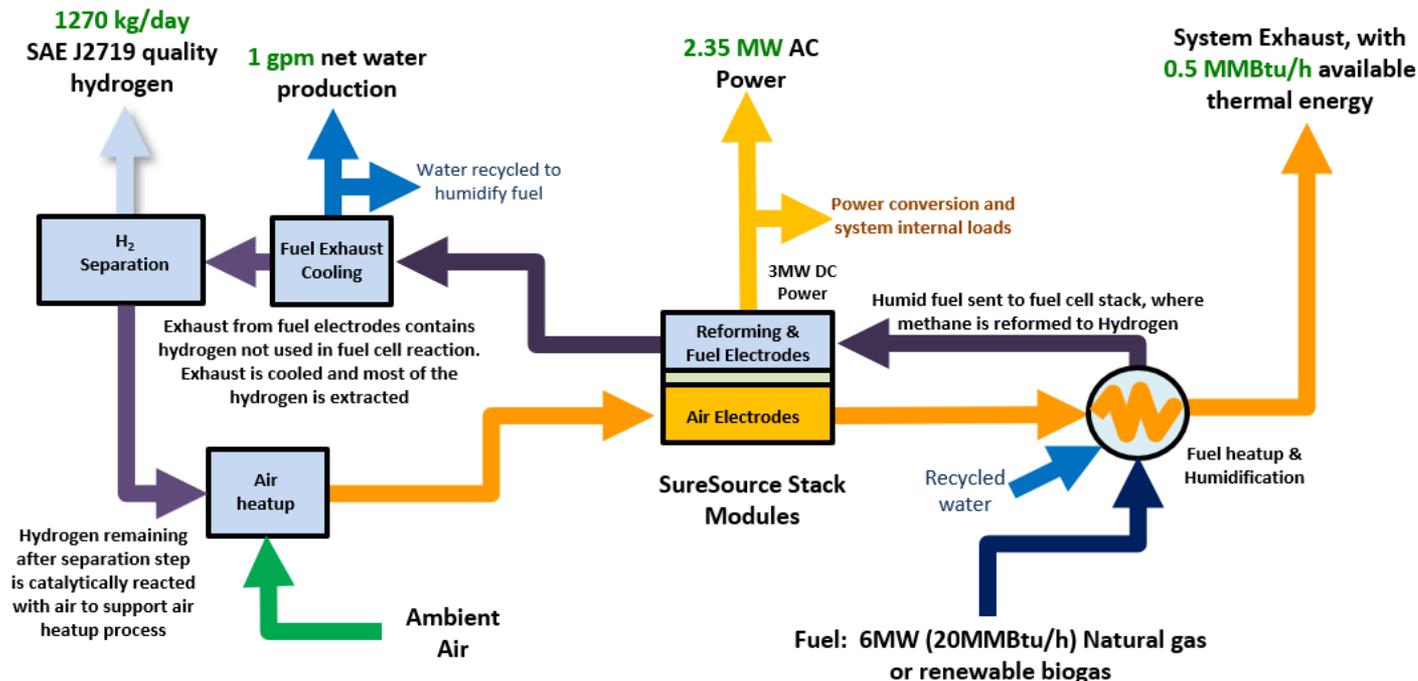
Reformer Cost forecast



- DOE H2A model predicts 25% capital cost reduction over a 10-year horizon
- Further literature review planned



Tri-generation

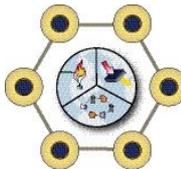


- Tri-generation is a concept in which fuel cell systems using RNG as the primary fuel produce electricity, hydrogen and heat
- Project at POLB employing this concept under development
- Techno-economic assessment in progress
- Electricity revenue is key to net hydrogen production cost



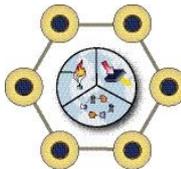
Reformed Biomethane Cost Reduction Potential

- **Additional assessment needed (e.g. time series data on cost digester costs in Europe)**
- **Like other RH2 technologies, scaling the supply chain will contribute to lower costs**
- **Soft costs and contingencies will benefit from repeat effect**
- **Expect a 5% to 10% learning rate by analogy with other technologies**

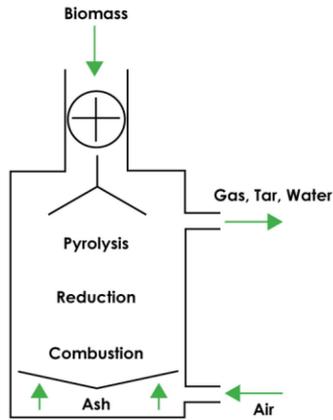


Thermochemical Conversion

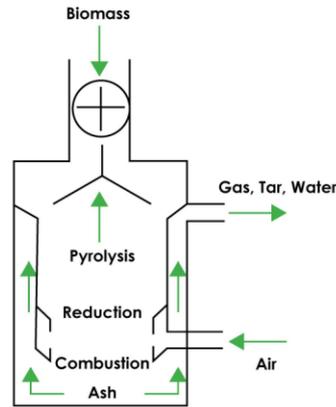
- **There are several types of processes for creating hydrogen from organic feedstock including**
 - **Gasification**
 - **Pyrolysis**
 - **Hydrothermal processing**
- **All of these processes use heat to evolve the volatile hydrocarbons from biomass to create syngas which is further to create hydrogen, methane or liquids**
- **The cost and performance assessment focuses on gasification as a proxy for this group**



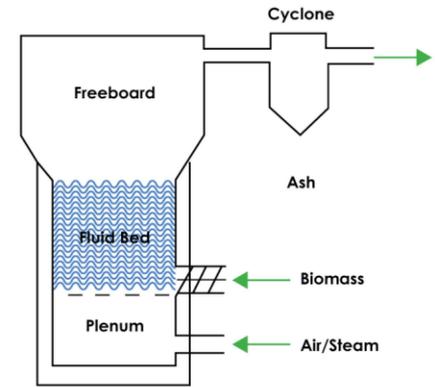
Gasifier Types



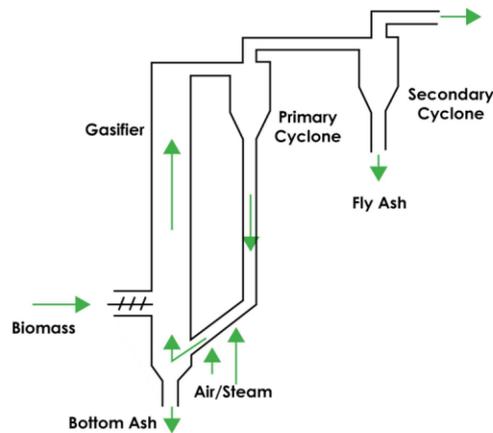
Updraft Gasifier



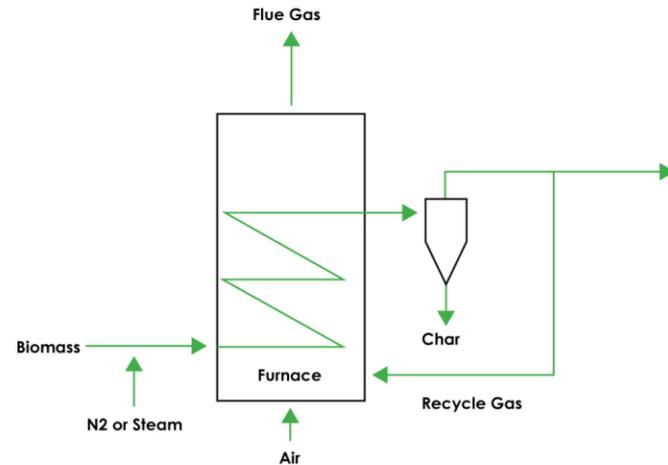
Downdraft Gasifier



Fluid-Bed Gasifier



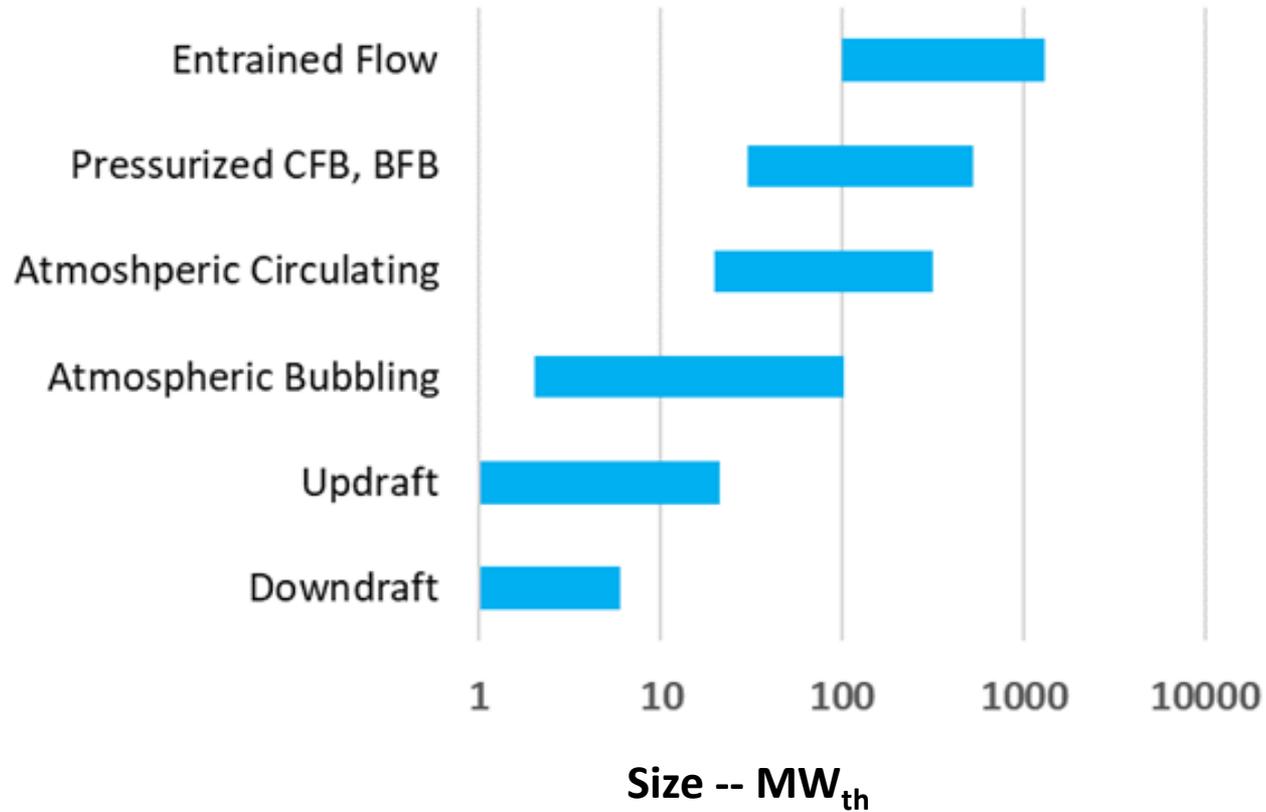
Circulating Fluid-Bed Gasifier



Entrained Flow Gasifier

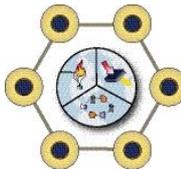


Size Range by Gasifier Type

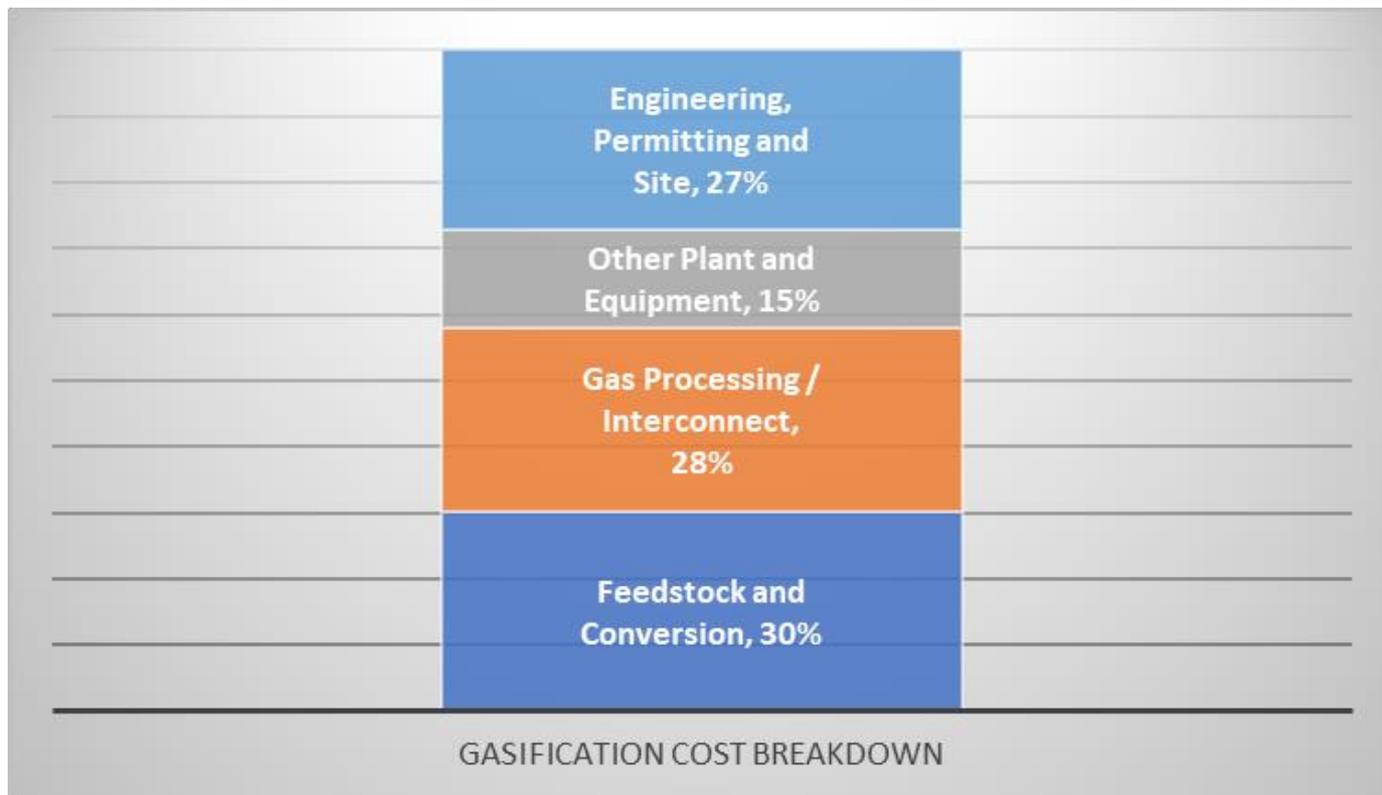


Gasifier Technical Maturity and Deployment Status

- **Gasification technology has been in development since the 1960's, primarily for coal gasification**
- **Biomass gasification has been under development since the 1980's**
 - **Most projects have used biomass as a blend-stock for coal gasifiers**
 - **Biomass-only gasification is at the pilot and early commercial stage**
- **Databases show 50 - 90 biomass gasification facilities worldwide with ~10 in California**
 - **Majority are sub megawatt and many are in CHP applications**
 - **No dominant technology**



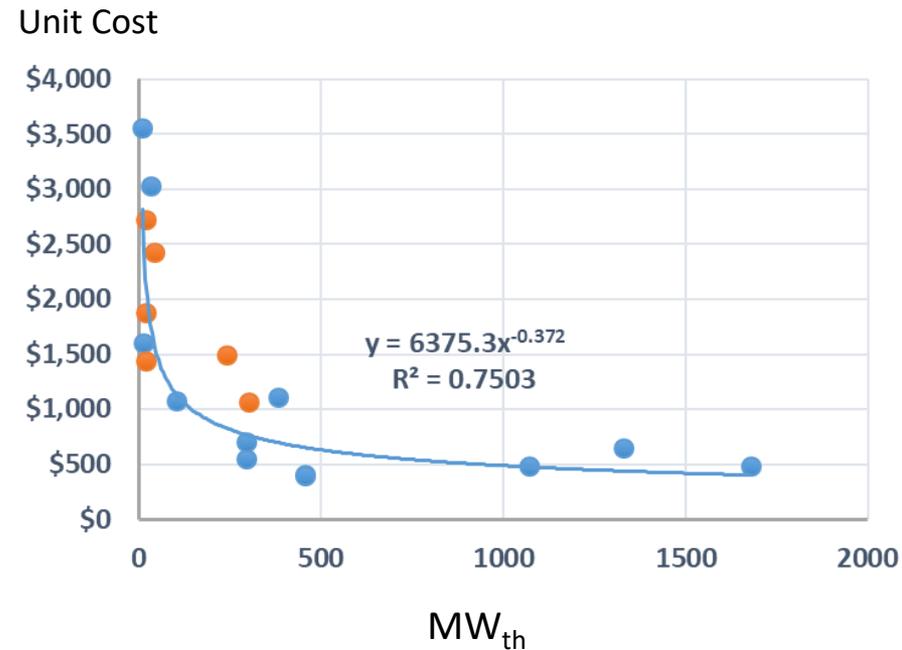
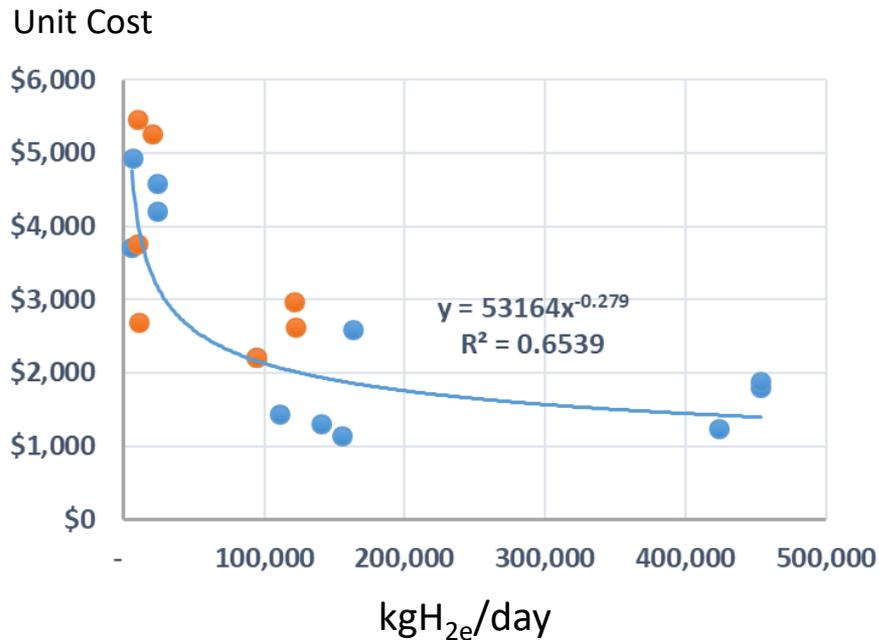
Typical Cost Breakdown for All-in Gasification Project



Costs exclude contingency, construction financing and land acquisition



Gasification System Costs – Current



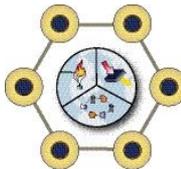
- Total system cost can be normalized based on feedstock input quantity (MW_{th}) or on product volume – the correlation is slightly better based on input
- The scale factor is between 0.63 and 0.72 based on the data used here – this is consistent with values reported in the literature and shows that plant size of around 100 MTH₂/day (~300 MW_{th}) is the minimum efficient scale

Scope: complete system exclusive of construction financing costs and contingency

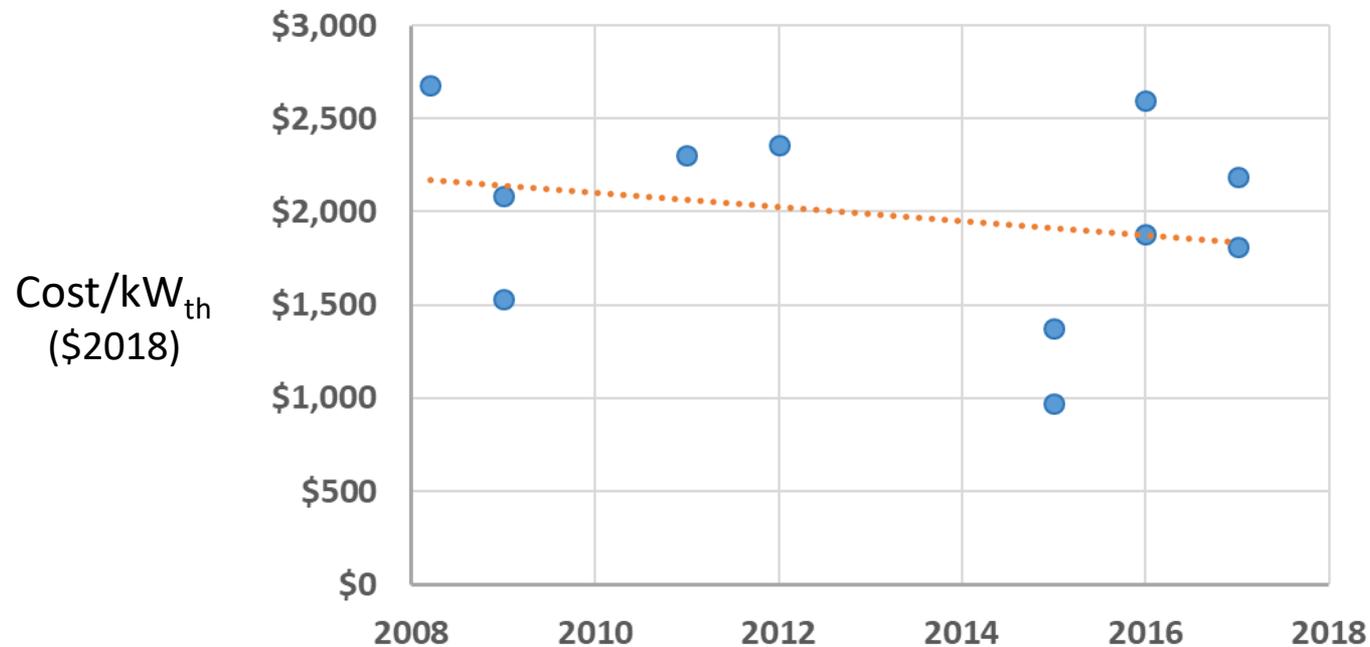


Gasification Cost Forecast

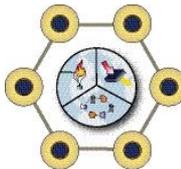
- Literature on future cost improvement potential for gasification systems is limited
- H2A “future case” shows a 7% improvement in cost based on a specific set of design improvements to the circulating bed technology (1 technology generation)
- A 2004 study by the National Academy of Science estimated a 50% capital cost reduction potential for a 24,000 kg/d facility from early unit to fully learned out
- Other studies identify potential improvements leading to a 50% cost reduction assuming that all the identified innovations and improvements are successful (not likely)
- Neither coal nor biogas gasification projects show a statistically significant learning-rate correlation to date – but, in the case of biomass, the installed base is very low so significant learning effect would not be expected
- If biomass systems were to exhibit a learning rate of 10% (using GTCC as a proxy) and 15% annual growth in installations beginning in 2020 they would achieve cost reduction of roughly 20% by 2030
- For purposes of this study, an improvement in cost of 10% to 30% with a base case of 20% will be used from current costs through 2030 following a typical progress curve shape



Biomass Gasification Cost Progression



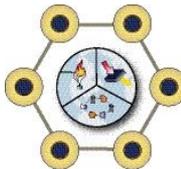
- The trendline for normalized gasification cost shows 2% year decline but the trend is not statistically significant
- Indicative of the low rate of system additions to date yielding little learning effect



Current and 2030 Forecast Gasification Performance Data

Parameter	2018 Value	2030 Value
Gasification Efficiency	65%-70%	5% relative improvement
Total System Efficiency	50%	5% relative improvement
Fixed Maintenance O&M	5% of Capex	Pro-rata with Capex

- **The above values are taken from the DOE current and future H2A Case studies for gasification**



Plant Gate to Customer

- Utilize H₂ Delivery and Scenario Analysis Model (HDSAM)
 - Resolves terminal, transport, and refueling station costs

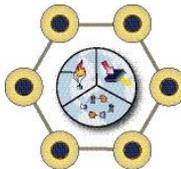
Main inputs:

- Population of area served
- Area served
- Vehicles/person
- Miles driven/vehicle/yr
- H2 market type: **urban**, rural interstate, combined
- Transport mode
- H2 vehicle market %
- HRS capacity
- Production volume estimates: low, mid, high

Estimate based on population that can be served from a given production facility

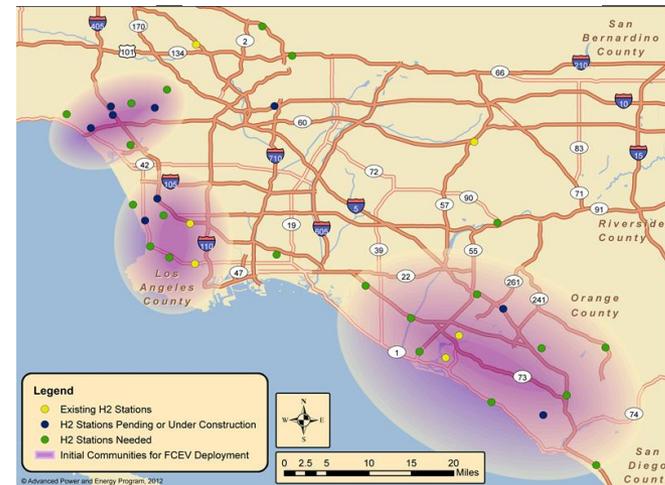
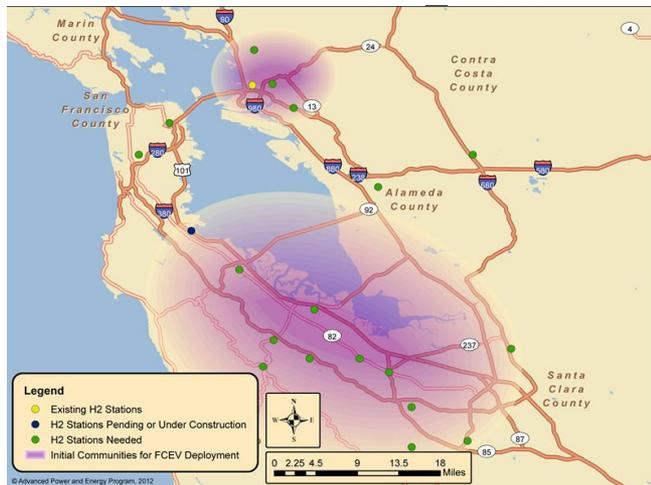
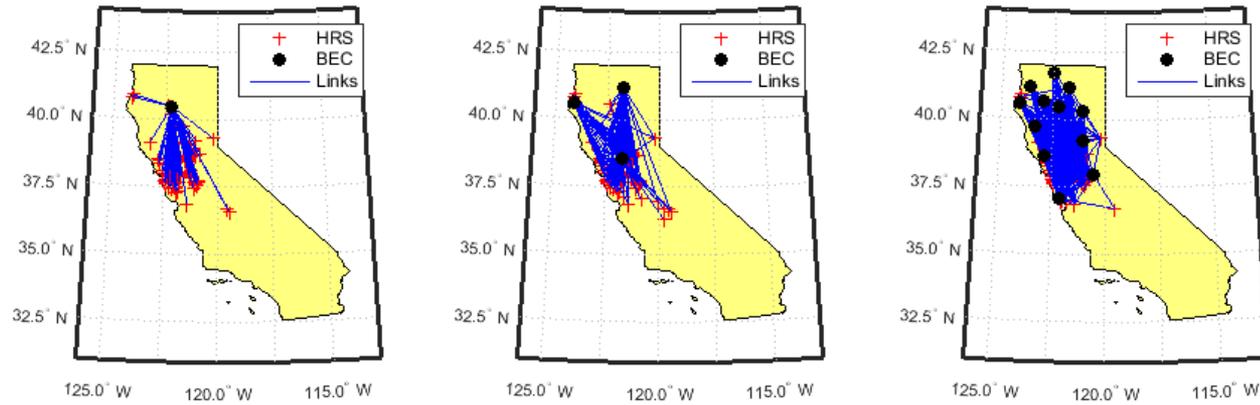
Default

Liquid Truck



Plant Gate to Customer

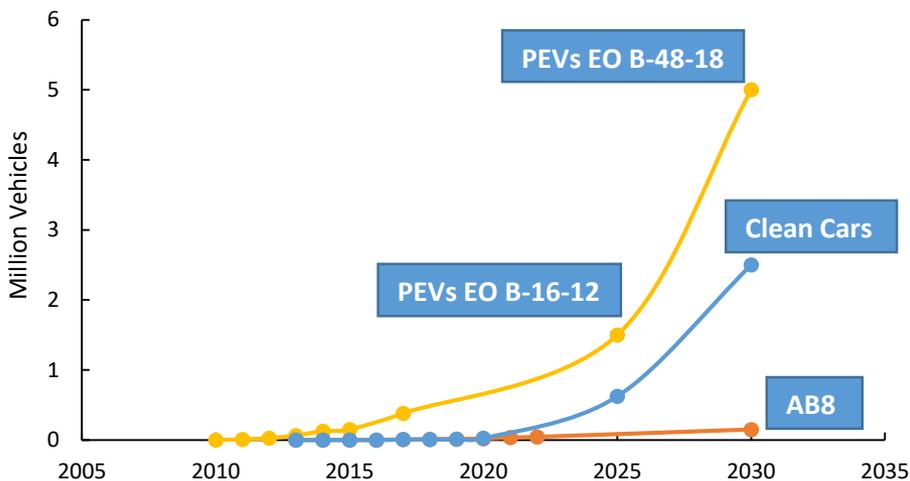
- Area served and Population
 - Calculate areas and population using GIS tools and LandScan data



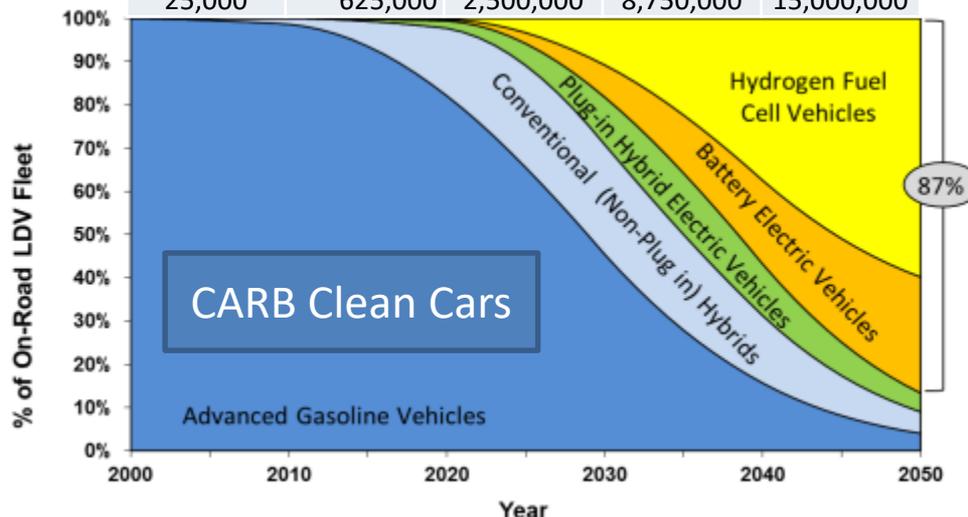
Plant Gate to Customer

- H2 vehicle market %
 - Align projection with statewide goals

● PEVs ● CARB AB8 ● CARB Clean Cars



2020	2025	2030	2040	2050
0.10%	2.50%	10%	35%	60%
25,000	625,000	2,500,000	8,750,000	15,000,000



■ Range of Mandatory Period Data ■ Range of Optional Period Data
◆ Reported Mandatory Period Estimates ◆ Reported Optional Period Estimates
▲ April Registrations ● October Registrations

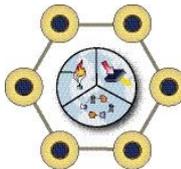
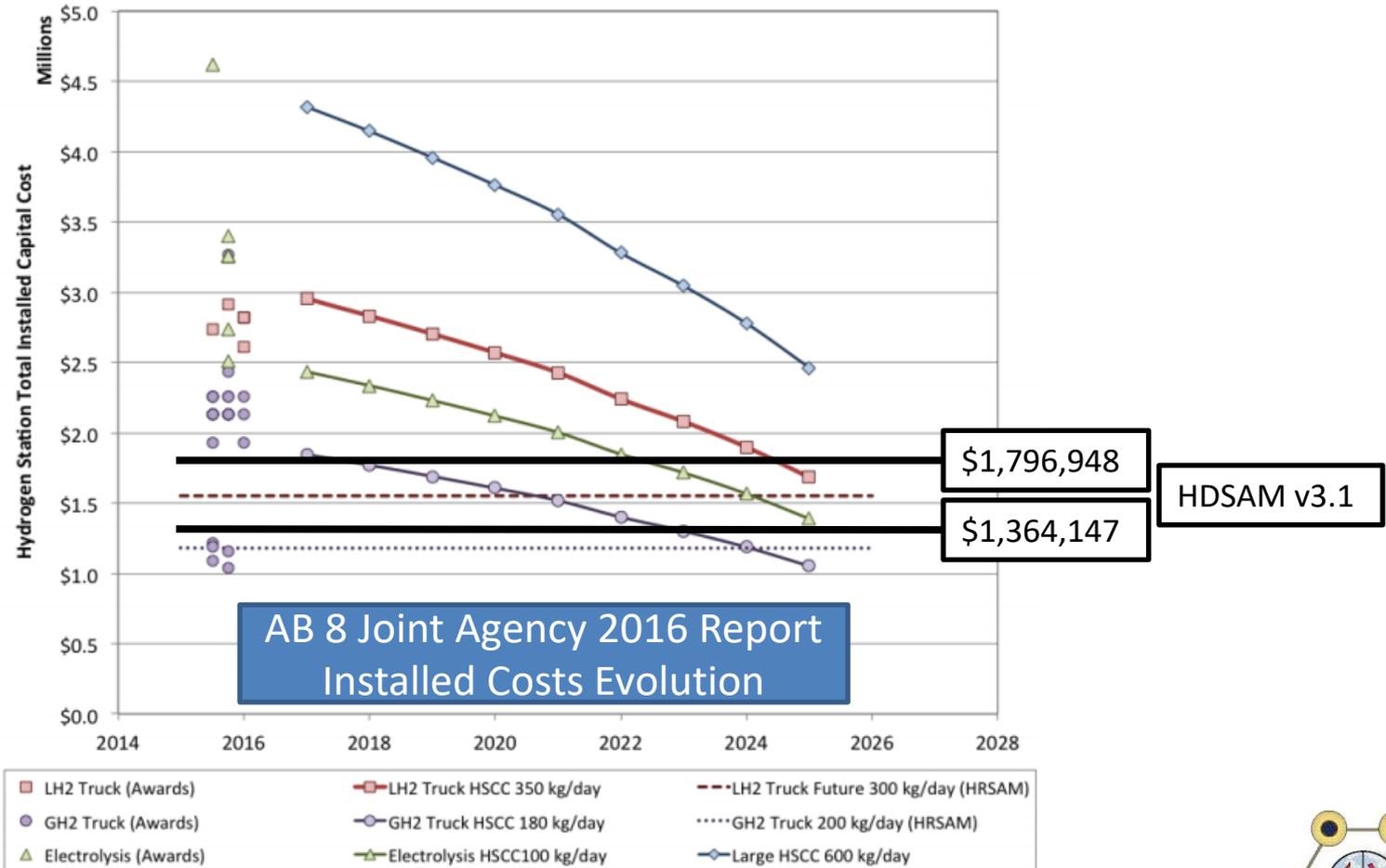
Plant Gate to Customer

- **HRS Capacity**
 - **1000 kg/d: 2020-2025**
 - **2000 kg/d: 2025-2030**
- **Production volume estimates**
 - **Mid: 2020-2025**
 - **High: 2025-2030**



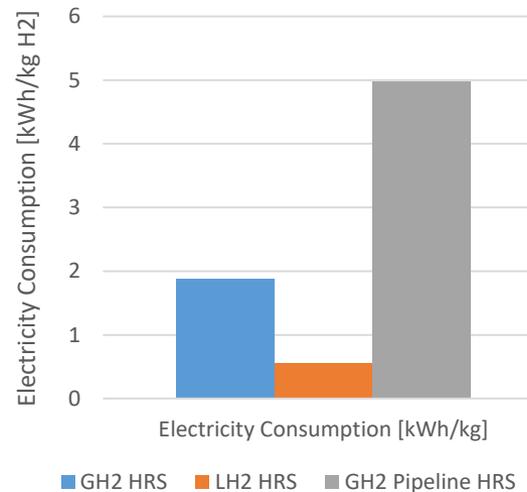
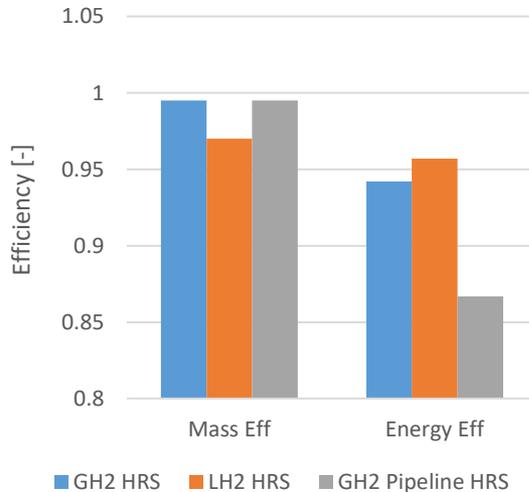
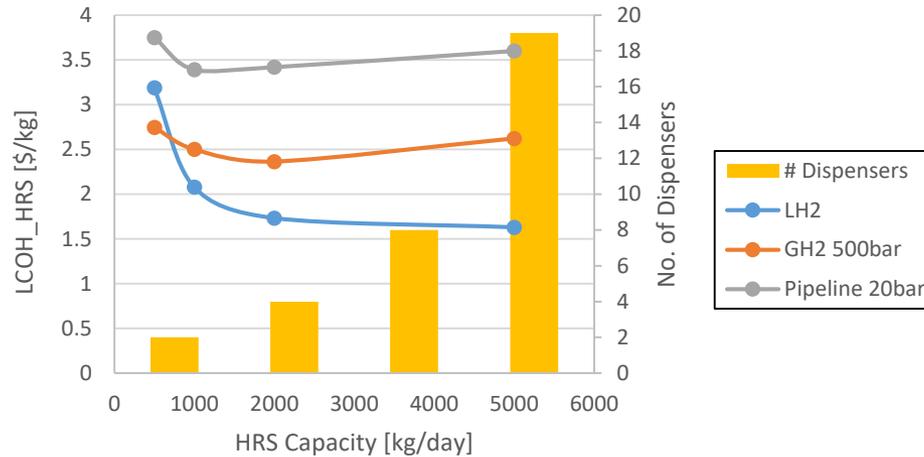
Plant Gate to Customer

- HRS Installed Cost Evolution
 - Use numbers from AB 8 Joint Agency Report 2016

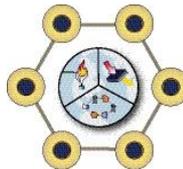
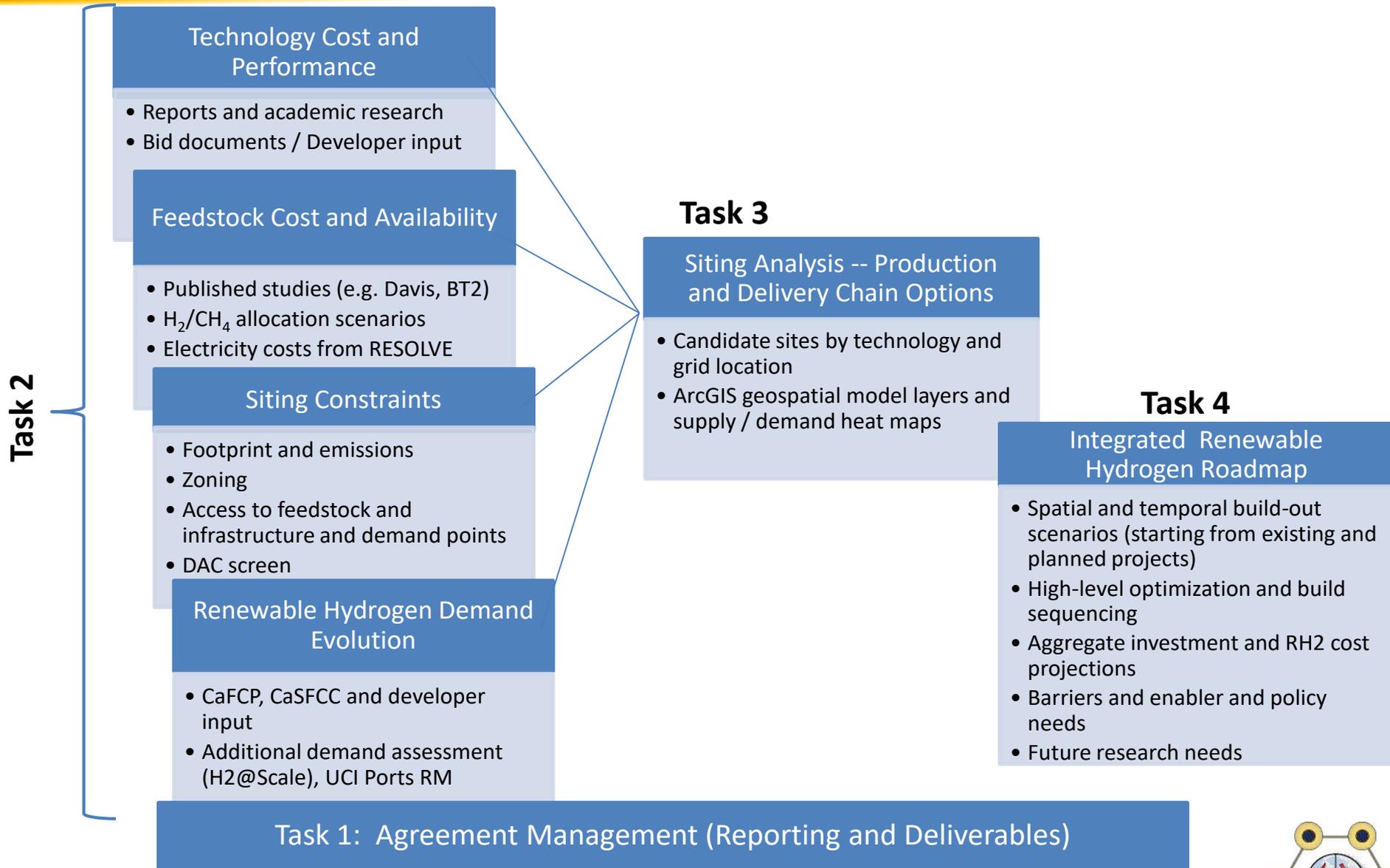


Plant Gate to Customer

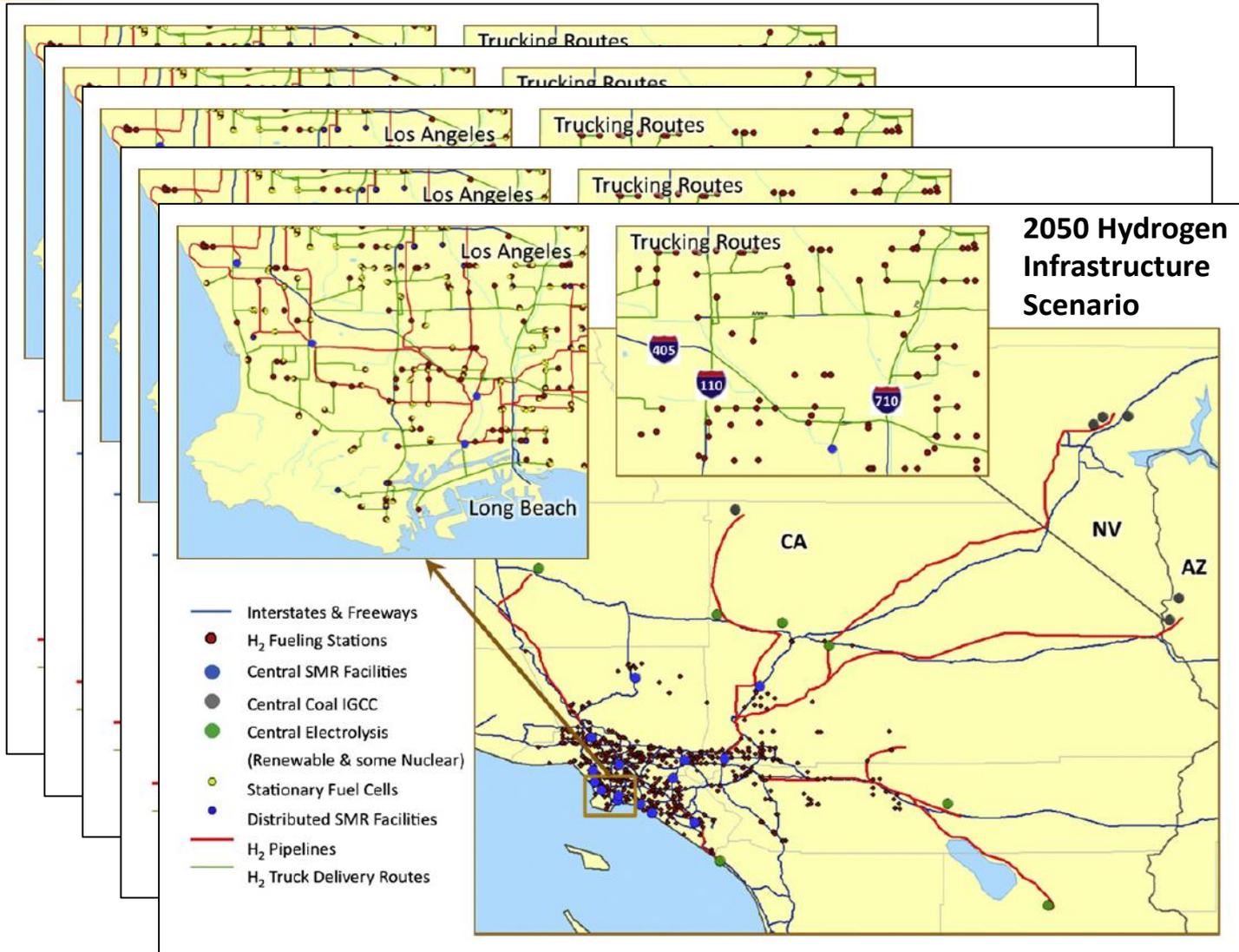
- Sample Output for HRS costs



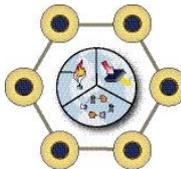
Further Steps in Roadmap Development



Time-Phased Renewable Hydrogen Deployment

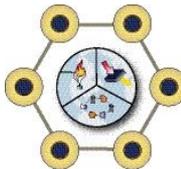


Source: Projecting full build-out environmental impacts and roll-out strategies associated with viable hydrogen fueling infrastructure strategies. Stephens-Romero S.; Brown, T.; Carreras-Sospedra, M.; Kang, J.; Brouwer J.; Dabdub, D.; Recker, w.; Samuelsen, G. S.; Int'l Journal of Hydrogen Energy, 2011



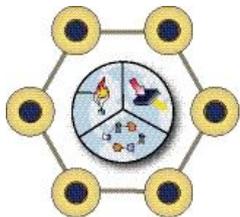
Some Key Products as the Work Proceeds

- **Complete reference specification by technology and size including plant exist conditions for plant-gate \$/kg calcs**
- **Feedstock, siting and market analysis**
- **Aggregate investment requirements over time**
- **Progression of cost of dispensed hydrogen over time**
- **Carbon credit values needed for break even over time (LCFS, RIN and other)**
- **Policy recommendations**
- **Points of highest leverage for RD&D**





Questions?



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