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Annual Compliance Report

**City of Anaheim
Canyon Power Plant**

Anaheim, California

**SCAQMD
Facility ID: 153992**

**CEC Permit Number:
800-2010-001-CMF**

**Docket Number:
07-AFC-9C**

2019

Period Range

January 1, 2019 through December 31, 2019

Review and Certification

I have reviewed both technically and editorially all details, calculations, results conclusions and other appropriate written material contained herein and hereby certify that to the best of my knowledge the material presented is true, accurate and complete.

I certify that the information contained in this report is true, accurate, and complete.

Ronald Hoffard

Name


Signature

Generation Plant Manager

Title

1/30/2020

Date

Canyon Power Plant
Annual Compliance Report
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Acronyms and Abbreviations

BHP	Break horse power
Btu	British thermal unit
BACT	Best available control technology
CARB	California Air Resources Board
CFR	Code of Federal Regulations
CO	Carbon Monoxide
CO ₂	Carbon Dioxide
COA	City of Anaheim
CFR	Code of Federal Regulations
CPP	Canyon Power Plant
CT	Combustion turbine
DAHS	Data acquisition and handling
TDS	Total dissolved solids
DPF	Diesel particulate filter
EPA	Environmental Protection Agency
F.	Fahrenheit
ICE	Internal combustion engine
lbs/hr	pounds per hour
lb/lb-mol	pound per pound mol
MW	mega watts
MMBtu	million British thermal units
mmcf	million cubic feet
NH ₃	ammonia
NO	Nitrogen Oxide
NO _x	Oxides of Nitrogen
NO ₂	Nitrogen Dioxide
O ₂	Oxygen
ppm	parts per million
ppmc	parts per million corrected to 15% O ₂
RATA	relative accuracy test audit
ROG	Reactive Organic Compounds
RTU	remote terminal unit
scf	standard cubic feet (standard temperature = 68 degrees F)
SCR	selective catalytic reactor
SCAQMD	South Coast Air Quality Management District
unit	The term unit refers to the boiler/steam turbine
VOC	Volatile Organic Compounds

1.0 Facility Description:

The City of Anaheim's (COA) Canyon Power Plant (CPP) facility is located at 3071 Miraloma Avenue in Anaheim California.

The facility consists of four natural gas fired General Electric, Model LM6000PC Sprint, simple cycle combustion turbine with water injection. The gas turbine was designed with a maximum heat input of 479 MMBtu per hour with a 46 degree Fahrenheit (F.) inlet air temperature. The units are equipped with an inlet air chiller designed to maintain the gas turbine inlet temperature at 46 degrees F. at full load.

Each unit is capable of generating 50.95 megawatts.

Carbon Monoxide (CO) emission from the gas turbine are controlled by utilizing a CO oxidation catalyst located between the gas turbine and the selective catalytic reactor (SCR). The CO oxidation catalyst controls the unit's CO and volatile organic compounds (VOC) emissions. The catalyst is guaranteed to reduce the unit's CO emission rate to a maximum of 4 ppm corrected to 15% O₂ (ppmc) and the VOC to 2 ppmc, both emission rates are based on a one (1) hour averages, dry basis at 15% O₂. The CO catalyst system was designed and supplied by Englehard/BASF.

The NO_x emissions from the gas turbine are controlled by the utilizing two (2) independent systems or techniques in series. The first system utilized on this unit is the water injection system.

Water is injected into the combustor suppressing the flame temperature and reducing the 1-hour average NO_x concentration to approximately 25 ppmc at 15% oxygen prior to entry into the SCR.

The second NO_x control system utilized by the unit is the NH₃/SCR system. After passing through the CO catalyst, the exhaust gases pass through an ammonia injection grid on its way to the SCR. The ammonia (NH₃) used at this facility is in the form a 19% by weight solution of ammonium hydroxide.

The SCR catalyst utilized by the unit for NO_x control was provided by Cormetech. The reaction between the NH₃ and the SCR catalyst reduces the existing NO_x to elemental nitrogen and water, resulting in NO_x concentrations in the exhaust gas at no greater than 2.5 ppmv at 15% O₂ on a 1-hour average. The ammonia slip must be maintained below 5 ppm at 15% O₂. Each SCR is vented through a dedicated stack, which is 11.8 ft diameter and 86 ft high.

The facility is also equipped with an 1141 BHP diesel emergency internal combustion engine (ICE) (black start engine) will be used to start up the plant in the event of a loss of grid power.

The ICE, is a Caterpillar, Model C-27, rated at 1141 BHP and fired on ultra low sulfur diesel fuel. The ICE, will serve to provide power to the plant during blackout conditions. The engine is certified by the SCAQMD as an EPA Tier 2 engine on 12/31/2010. The engine is required to be permitted, rather than registered, because CPP is a RECLAIM/Title V facility.

The black start engine will be used only in emergency situations where grid power from the COA's 69 kV system is unavailable to start the CTs. The black start engine will provide power to the turbine starter motors and various other necessary pieces of support equipment to get one of the gas turbines started. Once one of the turbines has been started and providing power to the

grid, the black start engine will be shut down.

The SCAQMD's rules limit operation of an emergency ICE to 50 hours per year.

The black start engine incorporates a diesel particulate filter (DPF), which is required by LAER. The Caterpillar DPF is designed to control the particulate emissions from diesel engines. The DPF consists of 2 filters, each 15-inches diameter by 15-inches long. The DPF system has been verified by CARB under Executive Order DE-14-006-01 to reduce emissions of diesel particulate matter consistent with a Level 3 device (greater than or equal to 85 percent reduction), when used with ultra low sulfur diesel with 15 ppm or lower sulfur content. As the DPF is CARB verified, a source test is not required. With the DPF, the particulate matter emissions from the engine is reduced from 0.15 g/bhp-hr to 0.0225 g/bhp-hr.

The DPF consists of a catalyzed cordierite ceramic honeycomb with hundreds of parallel channels, is designed to reduce emissions of particulate, carbon monoxide and hydrocarbons. The catalyst on the ceramic walls oxidizes carbon monoxide into carbon dioxide, and hydrocarbons into water and carbon dioxide. The arrangement of the channels is such that the exhaust gases carrying the carbon particles are forced through the fine pores of the walls, which filter out the particles. As the carbon particles are collected on the ceramic walls, the backpressure on the engine will increase. When the temperature of the exhaust is equal to or greater than 300 °C (572 °F) for at least 30% of the duty cycle, the catalyst interacts with the collected particulates to burn the particulates into carbon dioxide and water vapor, which will pass through the DPF.

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 1
COMPLIANCE MATRIX

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 2
FACILITY OPERATIONAL STATUS REPORT

Overall Project Status

Canyon Power Plant construction was completed in August 2011. Units 3 and 4 were ready for commercial operation on July 27, 2011. Units 1 and 2 were ready for commercial operation on September 15, 2011. All four gas turbines completed commissioning and were in commercial operation for the entire compliance year 2018.

No changes to the operational status of the facility implemented or planned in 2019 year.

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 3
CEC APPROVED POST CERTIFICATION CHANGES

**No California Energy Commission (CEC) approved post certification changes
and no Title V revisions to report for CY 2019**

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 4
MISSED SUBMITTAL DEADLINES

Canyon Power Plant submitted all required compliance reports on the due dates and no missed submittal deadlines for CY 2019

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 5
PERMIT FILINGS AND PERMITS ISSUED
DURING THE PERIOD

Canyon Power Plant had no permit filings and no permits issued for CY 2019

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 6
PROJECTED COMPLIANCE TESTING
FOR THE NEXT YEAR

Projected Environmental Compliance Testing schedule in CY 2020:

Compliance Test	Frequency	Scheduled Quarter
NH3 Slip Test	Annual	3Q; 4Q
RATA Test	Annual or Semi-Annual	3Q; 4Q
Cooling Tower TDS/PM10	Quarterly	All four Quarters
Cooling Tower Legionella	Quarterly	All four Quarters
Fuel H2S Test	Monthly	January through December
Fuel Flow Accuracy	Annual	2Q
SCR Differential Pressure	Annual	2Q
SCR Inlet Temperature	Annual	2Q
NH3 Flow Meter Calibration	Annual	2Q
Linearity/CGA Test	Quarterly	All four Quarters
Particulate Matter Source Test	Tri-ennual	3Q; 4Q

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 7
ADDITIONS TO ON-SITE COMPLIANCE FILE

GENERAL PLANT

Cooling Tower Legionella test report
Cooling Tower PM10 test reports
Monthly Waste Water reports
Monthly Potable water use reports
Monthly Reclaim water use reports
Monthly natural gas burn records
Monthly natural H₂S gas test reports
Refrigerant monitor calibration report
RECLAIM RTC holdings records

CEC

Quarterly reports
Quarterly 1304 Report
Annual report
Potable water use records

CAISO

Certificate of Compliance

CARB

Greenhouse gas records
Annual refrigerant report
Annual SF6 use report

DIESEL ENGINE

Maintenance Reports
Fuel purchase records
Engine run-time records
HiBack calibration report
Engine tune up report

EIA

Annual/Monthly EIA 923 report
Annual EIA 860 report

EPA

Part 98 Greenhouse Gas reports
Certificate of Representation forms

RECLAIM

Daily submittals
Monthly submittals
Quarterly submittals
SCAQMD QCER Forms
SCAQMD 500-N Forms

SCAQMD 500-SAM Forms
SCAQMD 500-ACC Form
SCAQMD APEP Form
SCAQMD AER Report
SCAQMD Rule 218 Semi-annual reports

SCAQMD

NOV & NTCs issued by the SCAQMD
SCAQMD responses to 500-N forms

UNIT 1:**EPA**

Quarterly Acid Rain report
Quarterly Acid Rain report & feedback report
Annual Form 500-ACC

Calibration Records

Fuel flow meter calibration report
Water flow meter calibration report
NH₃ flow meter calibration report
SCR DP transducer calibration report
SCR inlet temperature transducer Cal report
SCR outlet temperature transducer Cal report

Calibration gas logs

Linearity test reports
Part 75 RATA test reports
RECLAIM RATA test reports
Rule 218 (CO) RATA test reports
NH₃ slip test reports

Tri-ennial compliance testing:
VOC emissions;
PM10 emissions; and
ROG emissions

UNIT 2:

EPA

Quarterly Acid Rain report
Quarterly Acid Rain report & feedback report
Annual Form 500-ACC

Calibration Records

Fuel flow meter calibration report
Water flow meter calibration report
NH3 flow meter calibration report
SCR DP transducer calibration report
SCR inlet temperature transducer Cal report
SCR outlet temperature transducer Cal report

Calibration gas logs
Linearity test reports
Part 75 RATA test reports
RECLAIM RATA test reports
Rule 218 (CO) RATA test reports
NH3 slip test reports

Tri-annual compliance testing:
VOC emissions;
PM10 emissions; and
ROG emissions

UNIT 3:

EPA

Quarterly Acid Rain report
Quarterly Acid Rain report & feedback report
Annual Form 500-ACC

Calibration Records

Fuel flow meter calibration report
Water flow meter calibration report
NH3 flow meter calibration report
SCR DP transducer calibration report
SCR inlet temperature transducer Cal report
SCR outlet temperature transducer Cal report

Calibration gas logs
Linearity test reports
Part 75 RATA test reports
RECLAIM RATA test reports

Rule 218 (CO) RATA test reports
NH3 slip test reports

Tri-annual compliance testing:
VOC emissions;
PM10 emissions; and
ROG emissions

UNIT 4:

EPA

Quarterly Acid Rain report
Quarterly Acid Rain report & feedback report
Annual Form 500-ACC

Calibration Records

Fuel flow meter calibration report
Water flow meter calibration report
NH3 flow meter calibration report
SCR DP transducer calibration report
SCR inlet temperature transducer Cal report
SCR outlet temperature transducer Cal report

Calibration gases logs
Linearity test reports
Part 75 RATA test reports
RECLAIM RATA test reports
Rule 218 (CO) RATA test reports
NH3 slip test reports

Tri-annual compliance testing:
VOC emissions;
PM10 emissions; and
ROG emissions

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 8
UN-PLANNED FACILITY CLOSURE PLAN REVIEW

An “Un-Planned Facility Closure Plan” was drafted and submitted to the California Energy Commission (CEC) in the First Quarter of 2014. At this time, no revisions or changes are required.

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 9

Notice of Violation and Notice to Comply
Issued in CY 2019

**Notices of Violation
Issued by the SCAQMD in the CY 2019**

NONE

**Notices to Comply
Issued by the SCAQMD in the CY 2019**

NONE

SCAQMD FORM 500-N
Title V – Deviations, Emergencies & Breakdowns
Submitted by Canyon Power Plant



South Coast Air Quality Management District

Form 500-N**Title V - Deviations, Emergencies & Breakdowns**

*This written report is in addition to requirements to verbally report certain types of incidents. Verbal reports may be made by calling AQMD at 1-800-288-7664 (1-800-CUT-SMOG) or AQMD enforcement personnel.

South Coast
AQMD

Mail To:

SCAQMD

P.O. Box 4941

Diamond Bar, CA 91765-0941

Tel: (909) 396-3385

www.aqmd.gov

Section I - Operator Information

1. Facility Name (Business Name of Operator That Appears On Permit): <u>Canyon Power Plant Unit #2 (D7)</u>		2. Valid AQMD Facility ID (Available On Permit Or Invoice Issued By AQMD): <u>153992</u>	
3. Address: (where incident occurred) <u>3071 E. Miraloma Avenue</u> <u>Anaheim</u> City		Street Address <u>CA</u> State <u>92805</u> Zip	
4. Mailing Address: (if different from Item 3) _____ City		Street Address _____ State _____ Zip	
5. Provide the name, title, and phone number of the person to contact for further information: <u>RonaldHoffard</u> Name <u>Generation Plant Manager</u> Title <u>(714) 765-4536</u> Phone #			

Section II - Reporting of Breakdowns, Deviations, and Emergencies

Type of Incident	Verbal Report Due*	Written Report Due
a. <input type="checkbox"/> Emergency under Rule 3002(g)	Within 1 hour of discovery	Within 2 working days from when the emission limit was exceeded.
b. <input type="checkbox"/> Breakdown under: <input type="checkbox"/> Rule 430 (Non-RECLAIM) <input type="checkbox"/> Rule 2004 (RECLAIM) <input type="checkbox"/> Rule 218 (Non-RECLAIM) [See Rule 218(f)(3)]	For Rules 430 & 2004 - Within 1 hour of discovery. For Rule 218 - Within 24 hours or next business day for failure/shutdown exceeding 24 hours	For Rules 430 & 2004 - Within 7 calendar days after breakdown is corrected, but no later than 30 days from start of the breakdown, unless a written extension is granted. For Rule 218 - With required semi-annual reports.
c. <input type="checkbox"/> Deviation with excess emissions [See Title V Permit, Section K, Condition No. 22B]	Within 72 hours of discovery of the deviation or shorter reporting period if required by an applicable State or Federal Regulation.	Within 14 days of discovery of the deviation.
d. <input checked="" type="checkbox"/> Other Deviation [See Title V Permit, Section K, Condition Nos. 22D & 23]	None	With required semi-annual monitoring reports.

2. The incident was first discovered by: Greg Strong on 02/20/2019 11:06 ☒ AM ☐ PM
Name Date Time

3. The incident was first reported by: Operator # 7 on 02/20/2019 11:34 ☒ AM ☐ PM
Name of AQMD Staff Person Date Time

a. ☒ Via Phone
b. ☐ In Person

Notification Number (Required): 549239 **REVISED**

4. When did the incident actually occur? 02/20/2019 10:52 ☒ AM ☐ PM
Date Time



AQMD USE ONLY	Received By:		Assigned By:		Inspector:	
	Date/Time Received:		Date/Time Assigned:		Date/Time Received Assignment:	
	Date Delivered To Team:		Date Reviewed Inspector Report:		Date Inspected Facility:	
	Team:	Sector:	Breakdown/Deviation Notification No.		Date Completed Report:	
	Recommended Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____
	Final Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____

5. Has the incident stopped? a. ☒ Yes, on: 02/20/2019 11:00 ☒ AM ☐ PM b. ☐ No
Date Time
6. What was the total duration of the incident? 0 08
Days Hours
7. For equipment with an operating cycle, as defined in Rule 430 (b)(3)(A), when was the end of the operating cycle during which the incident occurred? _____
Date Time ☐ AM ☒ PM
8. Describe the incident and identify each piece of equipment (by permit, application, or device number) affected. Attach photos (when available) of the affected equipment and attach additional pages as necessary.
During Unit #2 linearity testing the Nox spiked up due to the test gas not purging from the system.
9. The incident may have resulted in a:
a. ☒ Violation of Permit Condition(s): A99.1 NOx ppm > 2.5
b. ☐ Violation of AQMD Rule(s): _____
10. What was the probable cause of the incident? Attach additional pages as necessary.
SEE ATTACHMENT SUMMARY
11. Did the incident result in excess emissions? ☐ No ☒ Yes (Complete the following and attach calculations.)
☐ VOC _____ lbs ☒ NOx 9.300 ppm ☐ SOx _____ lbs ☐ H2S _____ lbs
☐ CO _____ lbs ☐ PM _____ lbs ☐ Other: _____ lbs pollutant
12. For RECLAIM facilities Subject to Rule 2004 (i)(3) ONLY: If excess emissions of NOx and/or SOx were reported in Item 11, do you want these emissions to be counted when determining compliance with your annual allocations?
a. ☐ Yes, for: ☐ NOx ☐ SOx b. ☐ No, for: ☐ NOx ☐ SOx
If box 12(b) above is checked, include all information specified in Rule 2004(i)(3)(B) and (C), as applicable.
13. Describe the steps taken to correct the problem (i.e., steps taken to mitigate excess emissions, equipment repairs, etc.) and the preventative measures employed to avoid future incidents. Include photos of the failed equipment if available and attach additional pages as necessary.
SEE ATTACHMENT SUMMARY
14. Was the facility operating properly prior to the incident?
a. ☒ Yes b. ☐ No, because: _____
15. Did the incident result from operator error, neglect or improper operation or maintenance procedures?
a. ☐ Yes b. ☒ No, because: _____
16. Has the facility returned to compliance?
a. ☐ No, because: _____
b. ☒ Yes (Attach evidence such as emissions calculations, contemporaneous operating logs or other credible evidence.)

Section III - Certification Statement

I certify under penalty of law that based on information and belief formed after reasonable inquiry, the statements and information in this document and in all attachments and other materials are true, accurate, and complete.

For Title V Facilities ONLY: ☒ I also certify under penalty of law that I am the responsible official for this facility as defined in AQMD Regulation XXX.

1. Signature of Responsible Official: 	2. Title of Responsible Official: GENERATION PLANT MANAGER
3. Print Name: RONALD HOFFARD	4. Date: <u>4/23/19</u> <u>02/26/2019</u> 
5. Phone #: (714) 765-4536	6. Fax #:
7. Address of Responsible Official: 3071 E. MIRALOMA AVENUE ANAHEIM CA 92805 Street # City State Zip	

AQMD 500N - Breakdown Date: 02/20/2019
Identify issue: Specialty Linearity Gas Regulator
Canyon Power Plant: Unit 2/ID# 153992
Notification: 549239

Question 8 - Describe the incident and identify each piece of equipment:

Unit 2 startup initiated at 0650 hours with a passing on-line Calibration performed at 0751 hours. Linearity/CGA testing began at 0816 hours, which required three different gas levels (low, mid, and high) to be introduced using calibration standard gases. The first gas, NOx low/CO low was introduced three times followed by O2/CO high linearity gas that resulted in a successful testing. The first of three samples of NOx high linearity gas was introduced at 1036 hours and at 1049 hours staff noticed inconsistent data. As the first NOx high sample gas completed purging, NOx spiked and caused a NOx ppm exceedance.

Question 10 – What was the probable cause of the incident?

The gas regulator on the NOx high gas cylinder failed to complete purging and caused the NOx ppm exceedance.

Question 13 – Describe the steps taken to correct the problem:

Unit 2 placed in maintenance to check and verify the CEMS analyzers and no issues found. Second, the NOx high cylinder gas regulator was tested and it was determined that the regulator did not function correctly. The gas regulator on the NOx high cylinder bottle was replaced with a new gas regulator and tested. A NOx high gas sample was introduced at 1409 hours and the NOx high gas test was successful.

Question 16 – Facility returned to compliance?

Unit 2 came returned to compliance at 1100 hours on 2/20/2019.

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
6:30	20.92 P	0.47 P	0.6 P	0.04 P	0.31 P	-0.02 P	0.3 P	0 P
6:31	20.93 P	0.46 P	0.59 P	0.04 P	0.36 P	-0.02 P	0.3 P	0 P
6:32	20.92 P	0.46 P	0.57 P	0.04 P	0.26 P	-0.02 P	0.3 P	0 P
6:33	20.92 P	0.47 P	0.59 P	0.04 P	0.31 P	-0.02 P	0.3 P	0 P
6:34	20.93 P	0.5 P	0.62 P	0.04 P	0.32 P	-0.02 P	0.3 P	0 P
6:35	20.93 P	0.49 P	0.61 P	0.03 P	0.31 P	-0.02 P	0.3 P	0 P
6:36	20.93 P	0.47 P	0.61 P	0.03 P	0.32 P	-0.02 P	0.3 P	0 P
6:37	20.92 P	0.44 P	0.6 P	0.04 P	0.35 P	-0.02 P	0.3 P	0 P
6:38	20.93 P	0.41 P	0.52 P	0.03 P	0.25 P	-0.02 P	0.3 P	0 P
6:39	20.93 P	0.42 P	0.59 P	0.03 P	0.32 P	-0.02 P	0.3 P	0 P
6:40	20.93 P	0.47 P	0.6 P	0.03 P	0.36 P	-0.02 P	0.3 P	0 P
6:41	20.93 P	0.48 P	0.59 P	0.03 P	0.34 P	-0.02 P	0.3 P	0 P
6:42	20.93 P	0.45 P	0.58 P	0.03 P	0.34 P	-0.02 P	0.3 P	0 P
6:43	20.93 P	0.46 P	0.6 P	0.03 P	0.31 P	-0.02 P	0.3 P	0 P
6:44	20.92 P	0.44 P	0.61 P	0.03 P	0.36 P	-0.02 P	0.3 P	0 P
6:45	20.92 P	0.43 P	0.56 P	0.03 P	0.3 P	-0.01 P	0.3 P	0 P
6:46	20.93 P	0.41 P	0.58 P	0.03 P	0.27 P	-0.01 P	0.3 P	0 P
6:47	20.93 P	0.41 P	0.53 P	0.03 P	0.32 P	-0.02 P	0.2 P	0 P
6:48	20.95 P	0.37 P	0.51 P	0.03 P	0.33 P	-0.02 P	0.3 P	0 P
6:49	20.59 P	0.31 P	21.54 P	0.03 P	0.3 P	-0.02 P	16.7 P	0 P
Startup 1	19.07	10.29 I	182	0.14	0.38	-0.02	84.4	0.45
2	18.66	7.54	34.79	4.95	5.34	0.2	93.8	14.12
3	18.52	5.2	5.15	10.29	14.76	3.53	114.3	36.59
4	17.92	4.2	4.18	10.29	16.69	12.59	176.2	33.04
5	17.01	3.74	3.78	10.29	14.31	22.64	247.4	21.7
6	16.28	3.16	3.25	8.72	8.36	32.31	316.8	10.92
7	15.72	2.76	2.85	7.94	7.65	42.83	400.8	9.04
8	15.01	2.82	2.89	9.9	11.54	49.8	459.4	11.68
9	14.84	3.16	3.26	10.29	20.18	49.72	460.7	19.62
10	14.83	3.52	3.58	10.29	23.86	49.81	460.1	23.19
11	14.82	3.72	3.77	10.29	21.23	49.52	459.6	20.6
12	14.81	3.81	3.87	5.62	6.49	49.93	459.9	6.29
13	14.81	3.97	3.98	1.73	1.87	49.48	459.5	1.68
14	14.82	4.14	4.16	1.4	1.53	49.68	459.2	1.36
15	14.82	4.25	4.22	1.32	1.49	49.75	458.4	1.28
16	14.83	4	4	1.22	1.37	49.57	457.3	1.19

Time	2_O2 %	2_COLOW		2_COHIGH		2_NOXLOW		2_NOXHGH		2_LOAD		2_GasFlow		2_NOX_CORR	
		ppm	ppm	ppm	ppm	ppm	ppm	ppm	ppm	MW	kw	kscfh	ppm	ppm	ppm
17	7:06	14.84	3.32	3.39	1.22	1.4	49.87	456.9	1.19						
18	7:07	14.85	2.58	2.64	1.35	1.52	49.59	456.6	1.32						
19	7:08	14.84	2.12	2.21	1.57	1.72	49.75	457	1.53						
20	7:09	14.84	2.05	2.16	1.76	1.83	49.76	456.2	1.71						
21	7:10	14.84	2.03	2.12	1.85	1.93	49.76	456.9	1.8						
22	7:11	14.84	2	2.11	1.95	2.02	49.62	456.7	1.9						
23	7:12	14.85	1.98	2.06	1.99	2.1	49.63	456.5	1.94						
24	7:13	14.85	1.95	2	2.02	2.13	49.81	456.6	1.97						
25	7:14	14.85	1.95	2.04	2.03	2.1	49.79	456.3	1.98						
26	7:15	14.84	1.99	2.1	1.99	2.08	49.57	456.4	1.94						
27	7:16	14.85	1.98	2.07	1.95	2.05	49.77	455.7	1.9						
28	7:17	14.85	1.99	2.08	1.91	2.05	49.71	456.4	1.86						
29	7:18	14.85	1.98	2.03	1.9	2.01	49.8	456.4	1.85						
30	7:19	14.85	1.95	2.01	1.9	2.02	49.59	456.3	1.85						
31	7:20	14.84	1.96	2.03	1.89	1.91	50.06	456.7	1.84						
32	7:21	14.84	2.14	2.2	1.89	1.95	49.83	456.4	1.84						
33	7:22	14.85	2.41	2.51	1.68	1.78	49.75	456.7	1.64						
34	7:23	14.84	2.54	2.62	1.49	1.58	49.73	455.9	1.45						
35	7:24	14.84	2.5	2.59	1.45	1.6	49.87	455.6	1.41						
End	7:25	14.85	2.44	2.51	1.45	1.62	49.69	455.1	1.42						
	7:26	14.84	2.43	2.45	1.48	1.61	49.74	455.2	1.44						
	7:27	14.84	2.4	2.52	1.5	1.66	49.69	455.4	1.46						
	7:28	14.84	2.42	2.5	1.52	1.66	49.84	456	1.48						
	7:29	14.85	2.45	2.5	1.55	1.63	50.01	456.1	1.51						
	7:30	14.84	2.51	2.58	1.55	1.73	49.7	457	1.51						
	7:31	14.84	2.5	2.62	1.57	1.66	49.49	456.5	1.53						
	7:32	14.84	2.5	2.6	1.59	1.62	49.79	456.8	1.55						
	7:33	14.85	2.5	2.61	1.62	1.78	49.69	457	1.58						
	7:34	14.85	2.53	2.61	1.64	1.74	49.74	456.3	1.6						
	7:35	14.84	2.54	2.63	1.65	1.72	49.63	457	1.61						
	7:36	14.84	2.56	2.62	1.67	1.79	49.41	456.6	1.63						
	7:37	14.83	2.53	2.61	1.68	1.76	49.69	456.8	1.63						
	7:38	14.83	2.48	2.6	1.7	1.79	49.64	456.9	1.65						
	7:39	14.84	2.48	2.58	1.71	1.81	49.83	457	1.66						
	7:40	14.83	2.5	2.59	1.73	1.85	49.74	457.3	1.68						
	7:41	14.83	2.51	2.62	1.74	1.81	49.82	456.9	1.69						
	7:42	14.82	2.49	2.62	1.77	1.87	49.58	457.4	1.72						

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
7:43	14.83	2.5	2.61	1.8	1.91	49.9	457.1	1.75
7:44	14.83	2.5	2.62	1.81	1.95	49.74	457.2	1.76
7:45	14.82	2.49	2.62	1.83	1.89	49.62	457.9	1.78
7:46	14.82	2.5	2.62	1.84	1.95	49.42	457.3	1.79
7:47	14.82	2.47	2.57	1.85	2.01	49.71	457.6	1.8
7:48	14.82	2.44	2.52	1.86	1.95	49.45	457.3	1.8
7:49	14.81	2.46	2.53	1.86	2.01	49.79	457.4	1.8
7:50	14.82	2.49	2.62	1.86	1.93	49.79	457.4	1.8
7:51	17.13 C	3.45 C	3.48 C	1.88 C	1.93 C	49.73	457.6	0 C
7:52	22.42 C	10.29 Cl	130.6 C	1.77 C	1.91 C	49.76	458.2	0 C
7:53	22.43 C	10.29 Cl	180.35 C	0.4 C	0.59 C	49.82	458.4	0 C
7:54	22.43 C	10.29 Cl	181.03 C	0.05 C	0.33 C	50.08	458.5	0 C
7:55	22.43 C	10.29 Cl	180.86 C	0.03 C	0.29 C	49.64	458.9	0 C
7:56	22.43 CZ	10.29 Cl	180.85 CZ	0.03 CZ	0.29 CZ	49.56	458.7	0 CZ
7:57	0 C	10.21 Cl	17.75 C	3.34 C	3.31 C	49.73	458.3	0 C
7:58	-0.02 C	9.16 C	8.97 C	8.7 C	8.27 C	49.75	458.9	0 C
7:59	-0.02 C	9.2 CZ	9 C	8.9 CS	8.49 C	49.53	458.7	0 CS
8:00	-0.02 C	9.2 CZ	3.28 C	8.9 CS	20.81 C	49.55	458.2	0 CS
8:01	-0.02 C	0.01 C	0.09 C	10.29 C	126.4 C	49.85	458.6	0 C
8:02	-0.02 C	-0.07 C	0 C	10.29 C	180.67 C	49.89	458.6	0 C
8:03	-0.02 CS	-0.05 CS	0.03 CS	10.29 C	181.52 CS	49.63	457.9	0 CS
8:04	14.76 C	0.61 C	0.73 C	10.29 C	149.35 C	49.8	458.5	0 C
8:05	14.78 C	1.52 C	1.66 C	8.19 C	17.56 C	49.78	457.1	0 C
8:06	14.78 C	2.33 C	2.37 C	4 C	3.97 C	49.92	458	0 C
8:07	14.77 C	2.5 C	2.62 C	2.9 C	2.95 C	49.96	458.3	0 C
8:08	14.77 C	2.53 C	2.61 C	2.76 C	2.8 C	49.54	458.5	0 C
8:09	14.77 C	2.55 C	2.62 C	2.69 C	2.68 C	49.73	457.7	0 C
8:10	14.78	2.53	2.61	2.44	2.52	49.93	458.2	2.35
8:11	14.78	2.49	2.57	2.35	2.44	49.69	458.1	2.27
8:12	14.77	2.48	2.61	2.29	2.29	49.58	458.7	2.2
8:13	14.78	2.47	2.55	2.19	2.29	49.86	458.2	2.11
8:14	14.78	2.51	2.6	2.09	2.23	49.78	458.3	2.01
8:15	14.77	2.54	2.62	2.02	2.08	49.77	458.7	1.94
8:16	8.39 C	2.65 C	2.7 C	1.96 C	2.02 C	49.75	457.9	0 C
8:17	0 C	3.19 C	3.25 C	3.92 C	3.82 C	49.77	457.9	0 C
8:18	-0.02 C	3.23 C	3.3 C	4.09 C	3.99 C	49.91	457.8	0 C
8:19	-0.02 C	2.87 C	2.92 C	2.51 C	2.51 C	49.8	457.6	0 C

On-line Cal

End

Lin/CGA

NOx/CO Low

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHIGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
8:20	-0.02 C	2.42 C	2.51 C	2.49 C	2.57 C	49.66	458.3	0 C
8:21	-0.01 C	2.42 CZ	2.58 C	2.49 CZ	2.55 C	49.7	458	0 CZ
8:22	-0.03 C	3.26 C	3.33 C	3.63 C	3.6 C	49.96	458.1	0 C
8:23	-0.03 C	4.5 C	4.5 C	5.57 C	5.43 C	49.69	458	0 C
8:24	-0.02 C	5.47 C	5.47 C	5.6 C	5.41 C	49.52	458	0 C
8:25	-0.02 C	5.59 C	5.57 C	5.61 C	5.49 C	49.86	458.5	0 C
8:26	-0.03 C	5.59 C	5.89 C	5.61 C	5.42 C	49.71	458.1	0 C
8:27	-0.03 C	7.14 C	7.04 C	8.66 C	8.28 C	49.93	458.1	0 C
8:28	-0.03 C	8.4 C	8.23 C	9.23 C	8.8 C	49.7	458.3	0 C
8:29	-0.03 C	9 C	8.81 C	9.23 C	8.87 C	49.73	458.7	0 C
8:30	6.01 C	9.02 CS	8.82 C	9.24 CS	8.82 C	49.81	458.5	0 CS
8:31	14.74 C	3.06 C	3.11 C	8.57 C	8.14 C	49.72	458.2	0 C
8:32	14.75 C	2.48 C	2.56 C	2.44 C	2.45 C	49.75	458.6	0 C
8:33	14.75 C	2.47 C	2.56 C	2.05 C	2.31 C	49.76	458.2	0 C
8:34	14.75	2.43	2.48	1.94	1.99	49.73	458	1.85
8:35	14.74	2.37	2.4	1.89	1.99	49.83	457.8	1.81
8:36	14.75	2.35	2.4	1.87	1.89	49.68	458	1.79
8:37	14.75	2.35	2.39	1.87	1.94	49.88	457.8	1.78
8:38	4.68 C	2.32 C	2.38 C	1.86 C	1.98 C	49.76	458.1	0 C
8:39	-0.01 C	2.37 C	2.43 C	2.36 C	2.44 C	50.13	458.1	0 C
8:40	-0.02 C	2.44 C	2.55 C	2.43 C	2.49 C	49.68	457.5	0 C
8:41	-0.02 C	2.44 C	2.51 C	2.4 C	2.44 C	49.69	457.4	0 C
8:42	-0.03 C	2.4 CZ	2.47 C	2.39 CZ	2.43 C	49.73	457.8	0 CZ
8:43	-0.03 C	2.4 CZ	2.75 C	2.39 CZ	2.53 C	49.91	458.2	0 CZ
8:44	-0.03 C	3.7 C	3.73 C	4.38 C	4.3 C	49.75	457.9	0 C
8:45	-0.03 C	4.94 C	4.92 C	5.6 C	5.45 C	49.52	458	0 C
8:46	-0.03 C	5.54 C	5.49 C	5.62 C	5.45 C	49.32	457.2	0 C
8:47	-0.03 C	5.57 C	5.57 C	5.61 C	5.47 C	49.92	456.7	0 C
8:48	-0.04 C	6.44 C	6.32 C	6.44 C	6.23 C	49.6	455.6	0 C
8:49	-0.04 C	7.7 C	7.57 C	9.12 C	8.75 C	49.83	456	0 C
8:50	-0.04 C	8.77 C	8.58 C	9.2 C	8.8 C	49.62	455.4	0 C
8:51	-0.04 C	8.98 CS	8.83 C	9.22 CS	8.84 C	49.51	456	0 CS
8:52	12.61 C	8.98 CS	6.15 C	9.22 CS	8.83 C	49.55	456	0 CS
8:53	14.71 C	2.21 C	2.3 C	5.45 C	5.28 C	50.07	457.4	0 C
8:54	14.73 C	2.04 C	2.12 C	2.34 C	2.4 C	49.76	456.7	0 C
8:55	14.72	2.03	2.12	2.2	2.26	49.55	456.9	2.1
8:56	14.72	2.04	2.1	2.13	2.2	49.64	457.8	2.03

End

Lin/CGA
NOx/COL

End

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHIGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
8:57	14.72	2.05	2.11	2.07	2.23	49.64	457.8	1.98
8:58	14.72	2.04	2.11	2.04	2.12	49.94	457.8	1.95
8:59	14.7	2.02	2.1	2.01	2.04	49.8	457.7	1.91
9:00	14.71	2.03	2.09	1.98	2.07	49.7	458.1	1.89
9:01	9.96 C	2.04 C	2.12 C	1.95 C	2.04 C	49.52	454.9	0 C
9:02	0 C	2.13 C	2.22 C	1.97 C	2.04 C	49.57	455.9	0 C
9:03	-0.02 C	2.32 C	2.39 C	2.17 C	2.18 C	49.6	455.9	0 C
9:04	-0.02 C	2.48 C	2.58 C	2.36 C	2.4 C	49.6	455.9	0 C
9:05	-0.03 C	2.52 C	2.62 C	2.39 C	2.41 C	50	456.8	0 C
9:06	-0.03 C	2.5 CZ	2.65 C	2.39 CZ	2.45 C	49.82	456.2	0 CZ
9:07	-0.03 C	3.29 C	3.33 C	3.89 C	3.85 C	49.51	456.4	0 C
9:08	-0.03 C	4.47 C	4.46 C	5.5 C	5.35 C	49.64	456.6	0 C
9:09	-0.03 C	5.4 C	5.4 C	5.58 C	5.41 C	49.73	457.1	0 C
9:10	-0.03 C	5.51 C	5.44 C	5.58 C	5.44 C	49.42	458.1	0 C
9:11	-0.03 C	5.51 C	5.89 C	5.58 C	5.67 C	49.8	458.4	0 C
9:12	-0.04 C	7.26 C	7.14 C	8.66 C	8.35 C	49.72	457.9	0 C
9:13	-0.03 C	8.55 C	8.38 C	9.22 C	8.77 C	49.99	458.2	0 C
9:14	-0.04 C	8.99 CS	8.87 C	9.24 CS	8.81 C	49.77	458.2	0 CS
9:15	9.25 C	8.99 CS	7.39 C	9.24 CS	8.86 C	49.7	458.1	0 CS
9:16	14.67 C	2.13 C	2.25 C	6.97 C	6.74 C	49.68	458	0 C
9:17	14.67 C	1.74 C	1.86 C	2.67 C	2.71 C	49.92	457.6	0 C
9:18	14.68	1.66	1.8	2.54	2.54	49.7	457.3	2.41
9:19	14.68	1.65	1.74	2.53	2.59	49.74	457.2	2.4
9:20	14.7	1.68	1.81	2.49	2.55	49.45	456.8	2.37
9:21	11.31 C	3.12 C	2.93 C	2.38 C	2.41 C	49.66	457.3	0 C
9:22	6.24 C	10.29 Cl	38.76 C	2.18 C	2.29 C	49.64	456.8	0 C
9:23	6.24 C	10.29 Cl	50.32 C	0.34 C	0.56 C	49.82	456.7	0 C
9:24	6.23 C	10.29 Cl	49.83 C	0.07 C	0.31 C	49.48	456.7	0 C
9:25	6.23 CZ	10.29 Cl	49.91 CZ	0.06 C	0.28 C	49.52	456.7	0 CZ
9:26	13.73 C	10.29 Cl	109.48 C	0.05 C	0.32 C	49.77	456.4	0 C
9:27	13.74 C	10.29 Cl	111.04 C	0.04 C	0.37 C	49.73	456.7	0 C
9:28	13.73 C	10.29 Cl	111.32 C	0.04 C	0.35 C	49.83	456.5	0 C
9:29	13.73 C	10.29 Cl	111.32 C	0.03 C	0.32 C	49.75	456.8	0 C
9:30	22.4 C	10.29 Cl	181.76 C	0.03 C	0.33 C	49.66	456.2	0 C
9:31	22.4 CS	10.29 Cl	181.99 CS	0.03 C	0.27 C	49.54	456	0 CS
9:32	22.4 CS	10.29 Cl	181.99 CS	0.02 C	0.32 C	49.9	457.3	0 CS
9:33	14.72 C	6.28 Cl	8.93 C	1.02 C	1.19 C	49.63	456.7	0 C

Time	2_O2	2_COLOW	2_COHIGH	2_NOXLOW	2_NOXHIGH	2_LOAD	2_GasFlow	2_NOX_CORR
	%	ppm	ppm	ppm	ppm	MW	kscfh	ppm
End	9:34	14.71 C	1.77 C	1.9 C	2.09 C	49.48	457.4	0 C
	9:35	14.7	1.81	1.92	2.25	49.7	457.6	2.14
	9:36	14.69	1.81	1.93	2.15	49.89	457.5	2.04
Lin/CGA	9:37	14.7	1.79	1.91	2.14	49.76	457.7	2.04
COH/O2	9:38	13.16 C	2.84 C	2.93 C	2.05 C	49.85	457.4	0 C
	9:39	6.26 C	10.29 Cl	36.74 C	2.02 C	49.51	457.4	0 C
	9:40	6.23 C	10.29 Cl	50.31 C	0.43 C	49.62	457.8	0 C
	9:41	6.23 C	10.29 Cl	50.93 C	0.04 C	49.94	457.1	0 C
	9:42	6.23 CZ	10.29 Cl	50.87 CZ	0.03 C	49.85	457.9	0 CZ
	9:43	13.72 C	10.29 Cl	102.16 C	0.02 C	49.46	457.1	0 C
	9:44	13.73 C	10.29 Cl	111.2 C	0.01 C	49.92	456.9	0 C
	9:45	13.73 C	10.29 Cl	111.15 C	0.01 C	49.75	457.3	0 C
	9:46	13.73 C	10.29 Cl	111.15 C	0.01 C	49.87	457.1	0 C
	9:47	22.39 C	10.29 Cl	179.9 C	0.01 C	49.65	456.8	0 C
	9:48	22.4 C	10.29 Cl	180.12 C	0.01 C	49.9	457.3	0 C
	9:49	22.39 CS	10.29 Cl	180.45 CS	0.01 C	49.88	457	0 CS
	9:50	14.7 C	9.48 Cl	41.59 C	0.36 C	49.97	456.3	0 C
	9:51	14.69 C	2.42 C	2.48 C	1.64 C	49.82	456.9	0 C
End	9:52	14.7 C	2.04 C	2.15 C	2.13 C	49.76	456.6	0 C
	9:53	14.69	1.88	1.99	2.02	49.68	456.8	1.92
	9:54	14.69	1.77	1.92	2.03	49.72	456.7	1.93
	9:55	14.68	1.69	1.79	2.07	49.65	457.2	1.96
	9:56	14.68	1.69	1.78	2.07	49.59	457.9	1.96
Lin/CGA	9:57	14.68	1.76	1.91	2.07	49.69	457.9	1.96
COH/O2	9:58	14.67 C	1.75 C	1.87 C	2.03 C	49.72	457.3	0 C
	9:59	8.36 C	7.97 Cl	23.34 C	2.01 C	49.88	457.7	0 C
	10:00	6.24 C	10.29 Cl	50.07 C	1.05 C	49.62	457.1	0 C
10:01	6.24 C	10.29 Cl	50.62 C	0.04 C	0.25 C	49.72	458.2	0 C
10:02	6.23 CZ	10.29 Cl	50.48 CZ	0.03 C	0.23 C	49.76	457.4	0 CZ
10:03	6.23 CZ	10.29 Cl	50.48 CZ	0.02 C	0.21 C	49.91	458.1	0 CZ
10:04	13.73 C	10.29 Cl	112.35 C	0.01 C	0.2 C	49.79	457.3	0 C
10:05	13.73 C	10.29 Cl	112.53 C	0.01 C	0.25 C	49.62	457.9	0 C
10:06	13.73 C	10.29 Cl	112.53 C	0 C	0.24 C	49.86	457.9	0 C
10:07	22.39 C	10.29 Cl	179.9 C	0 C	0.27 C	49.83	458.2	0 C
10:08	22.38 C	10.29 Cl	180.58 C	0.01 C	0.23 C	49.67	457.7	0 C
10:09	22.37 CS	10.29 Cl	180.88 CS	0.01 C	0.24 C	49.82	458.3	0 CS
10:10	22.37 CS	9.87 Cl	180.88 CS	0.13 C	0.36 C	49.73	458.3	0 CS

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHIGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
End	10:11	14.67 C	2.77 C	2.86 C	1.44 C	1.53 C	49.86	457.6
	10:12	14.68 C	1.79 C	1.88 C	1.9 C	2.03 C	50.03	457.3
	10:13	14.68	1.73	1.89	2.05	2.12	49.75	457.4
	10:14	14.67	1.73	1.88	2.04	2.03	49.67	458.1
	10:15	14.67	1.75	1.91	2.05	2.19	49.67	457.7
Lin/CGA	10:16	14.65 C	1.75 C	1.87 C	2 C	2.06 C	49.84	457.3
NOxH	10:17	0.11 C	4.95 C	4.91 C	1.99 C	2.09 C	49.75	457.5
	10:18	-0.02 C	0.13 C	0.24 C	10.29 C	31.48 C	49.56	457.6
	10:19	-0.02 C	-0.02 C	0.06 C	10.29 C	50.03 C	50.22	457.1
	10:20	5.3 C	0.01 C	0.08 C	10.29 C	50.43 CZ	50.11	457.2
	10:21	14.64 C	0.51 C	0.61 C	10.29 C	45.59 C	49.98	457.1
	10:22	14.66 C	1.26 C	1.37 C	7.22 C	11.47 C	49.92	456.8
	10:23	14.5 C	1.81 C	1.91 C	2.79 C	2.82 C	49.77	457.7
	10:24	0.06 C	1.79 C	1.88 C	5.14 C	2.82 C	49.61	456.8
	10:25	-0.02 C	1.25 C	1.38 C	10.29 C	119.97 C	49.7	458
	10:26	-0.02 C	0.51 C	0.63 C	10.29 C	180.91 C	49.61	457.9
	10:27	4.88 C	0.02 C	0.14 C	10.29 C	181.87 CS	49.81	457.4
	10:28	14.47 C	0.33 C	0.45 C	10.29 C	164.62 C	49.96	457.7
	10:29	14.48 C	0.99 C	1.12 C	9.26 C	39.08 C	49.83	456.7
	10:30	14.5 C	1.65 C	1.76 C	6.29 C	6.1 C	49.83	457.4
	10:31	14.51 C	2.07 C	2.15 C	5.24 C	5.11 C	49.53	457.2
	10:32	14.52 C	2.26 C	2.34 C	4.91 C	4.68 C	49.7	458.2
	10:33	14.67	2.14	2.23	4.26	4.18	49.55	458.4
End	10:34	14.67	1.94	2.01	2.56	2.53	49.9	458
	10:35	14.66	1.86	1.97	2.39	2.39	49.57	457.4
Lin/CGA	10:36	8.86 C	1.67 C	1.77 C	2.28 C	2.41 C	49.72	458.3
NOx H	10:37	0 C	1.59 C	1.7 C	6.27 C	7.25 C	49.64	458.1
	10:38	-0.02 C	1 C	1.11 C	10.29 C	47.57 C	49.67	457.1
	10:39	-0.02 C	0.31 C	0.43 C	10.29 C	51.61 C	49.81	456.9
	10:40	-0.02 C	-0.01 C	0.06 C	10.29 C	51.59 CZ	49.81	457.5
	10:41	-0.02 C	0 C	0.09 C	10.29 C	84.41 C	49.55	457.3
	10:42	-0.02 C	0.01 C	0.15 C	10.29 C	110.07 C	49.8	457.3
	10:43	-0.02 C	0.02 C	0.13 C	10.29 C	111.02 C	49.95	457.3
	10:44	-0.02 C	0.01 C	0.14 C	10.29 C	111.02 C	49.86	457.7
	10:45	-0.03 C	0 C	0.14 C	10.29 C	118.93 C	49.68	456.9
	10:46	-0.03 C	0.01 C	0.15 C	10.29 C	123.58 C	49.73	457.6

Time	2_O2 %	2_COLOW ppm	2_COHIGH ppm	2_NOXLOW ppm	2_NOXHGH ppm	2_LOAD MW	2_GasFlow kscfh	2_NOX_CORR ppm
Regulator issue								
10:47	-0.03 C	0.01 C	0.13 C	10.29 C	123.77 CS	49.67	457.7	0 CS
10:48	-0.03 C	0 C	0.13 C	10.29 C	119.32 C	49.81	457.8	0 C
10:49	-0.02 C	-0.01 C	0.07 C	10.29 C	112.87 C	49.74	457.5	0 C
10:50	-0.03 C	-0.02 C	0.06 C	10.29 C	112.82 C	49.77	457.9	0 C
10:51	-0.03 C	-0.03 C	0.07 C	10.29 C	112.78 C	49.68	457.3	0 C
10:52	7.9	0.05	0.13	10.29	112.8	49.6	457.3	51.19
10:53	14.58	0.76	0.91	10.29	82.68	49.99	458.5	77.19
10:54	14.59	1.77	1.86	5.88	6.87	49.76	459.7	6.54
10:55	14.59	2.52	2.58	3.61	3.62	49.65	460.2	3.38
10:56	14.6	2.43	2.5	3.31	3.26	49.97	458.5	3.1
10:57	14.58	2.39	2.44	3.16	3.13	49.97	459	2.95
10:58	14.6	2.45	2.54	3.14	3.17	49.91	458.7	2.94
10:59	14.57	2.47	2.54	3.08	3.06	49.84	459.8	2.87

11.8 ppm Exceedance
2.5 ppm Limit
9.3 ppm Over limit

SCAQMD Reclaim Audit Report(Ver:2.2)

Customer Name:	CITY OF ANAHEIM	Report Start	2/20/2019 0:00
Unit ID	D7	Report End	2/20/2019 23:59
Category	CANYON POWER PLANT	Date Generated	2/21/2019 07:14
NOx Avail	445.4		
Flow Avail	452.6		
Total NOx Mass	58.57		

Date/Time	NOx Valid Quadrants	NOx Calibration/ Maintenance	Average of Valid bias adjusted NOx ppm quadrants	Stack Flow Valid Quadrants	Stack Flow Calibration/ Maintenance	Valid bias adjusted stack flow	Average of Valid NOx lb/hr quadrants	Missing data Procedure	Daily Total
2/20/2019 0:00	4	0	0	4	0	0	0		
2/20/2019 1:00	4	0	0	4	0	0	0		
2/20/2019 2:00	4	1	0	4	1	0	0		
2/20/2019 3:00	4	1	0	4	1	0	0		
2/20/2019 4:00	4	0	0	4	0	0	0		
2/20/2019 5:00	4	0	0	4	0	0	0		
2/20/2019 6:00	4	0	2.45	4	0	0	0		
2/20/2019 7:00	4	1	2.13	4	1	3260	3.81		
2/20/2019 8:00	4	1	2.07	4	1	14402	3.66		
2/20/2019 9:00	4	1	2.18	4	1	14240	3.52		
2/20/2019 10:00	4	1	3.74	4	1	14080	3.67		
2/20/2019 11:00	2	1	3.74	2	1	13598	13.02		
2/20/2019 12:00	2	1	3.74	2	1	13917	5.89	1N LBS/HR	8.63 ppm = 13.02 lbs
2/20/2019 13:00	4	1	1.91	4	1	13917	5.89	1N LBS/HR	2.5ppm = x
2/20/2019 14:00	4	1	2.2	4	1	13996	3.2		x= (13.02*2.5)/8.63 = 3.80 lbs
2/20/2019 15:00	4	1	1.73	4	1	13993	3.68		
2/20/2019 16:00	4	0	1.02	4	1	13813	2.87		
2/20/2019 17:00	4	0	1.35	4	0	10060	1.22		
2/20/2019 18:00	4	0	1.36	4	0	10072	1.62		
2/20/2019 19:00	4	0	1.35	4	0	10031	1.62		
2/20/2019 20:00	4	0	1.35	4	0	10002	1.61		
2/20/2019 21:00	4	0	1.38	4	0	9972	1.61		
2/20/2019 22:00	4	0	0.13	4	0	9819	1.61		
2/20/2019 23:00	4	0	0	4	0	1162	0.07		
						0	0		58.57

8.63 ppm = 13.02 lbs
 2.5ppm = x
 x= (13.02*2.5)/8.63 = 3.80 lbs
 13.02-3.77 = 9.25 lbs excess emissions

CERTIFICATE OF ANALYSIS

Grade of Product: EPA Protocol

Part Number:	E02NI99E15A0093	Reference Number:	48-401148253-1
Cylinder Number:	CC147621	Cylinder Volume:	144.3 CF
Laboratory:	124 - Los Angeles (SAP) - CA	Cylinder Pressure:	2015 PSIG
PGVP Number:	B32018	Valve Outlet:	660
Gas Code:	NO,NOX,BALN	Certification Date:	Mar 21, 2018

Expiration Date: Mar 21, 2026

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig, i.e. 0.7 megapascals.

ANALYTICAL RESULTS					
Component	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates
NOX	110.0 PPM	110.2 PPM	G1	+/- 0.9% NIST Traceable	03/14/2018, 03/21/2018
NITRIC OXIDE	110.0 PPM	110.0 PPM	G1	+/- 1.0% NIST Traceable	03/14/2018, 03/21/2018
NITROGEN	Balance				

CALIBRATION STANDARDS					
Type	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date
NTRM	13010425	KAL004033	97.6 PPM NITRIC OXIDE/NITROGEN	+/- 0.8%	May 09, 2019
PRM	12367	APEX1099237	9.82 PPM NITROGEN DIOXIDE/AIR	+/- 2.0%	Jun 02, 2017
GMIS	0224201602	CC500997	5.100 PPM NITROGEN DIOXIDE/NITROGEN	+/- 2.0%	Feb 24, 2019

The SRM, PRM or RGM noted above is only in reference to the GMIS used in the assay and not part of the analysis.

ANALYTICAL EQUIPMENT		
Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration
Nicolet 6700 AHR0801551 NO	FTIR	Mar 01, 2018
Nicolet 6700 AHR0801551 NO2	FTIR	Mar 16, 2018

Triad Data Available Upon Request

In service: 2/20/19 SMD



Approved for Release



South Coast Air Quality Management District

Form 500-N**Title V - Deviations, Emergencies & Breakdowns**

*This written report is in addition to requirements to verbally report certain types of incidents. Verbal reports may be made by calling AQMD at 1-800-288-7664 (1-800-CUT-SMOG) or AQMD enforcement personnel.

South Coast
AQMD

Mail To:

SCAQMD

P.O. Box 4941

Diamond Bar, CA 91765-0941

Tel: (909) 396-3385

www.aqmd.gov

Section I - Operator Information

1. Facility Name (Business Name of Operator That Appears On Permit): <u>CANYON POWER PLANT Unit 2 (D7)</u>		2. Valid AQMD Facility ID (Available On Permit Or Invoice Issued By AQMD): <u>153992</u>	
3. Address: (where incident occurred) <u>3071 E. Miraloma Avenue</u> <u>Anaheim</u> City		Street Address <u>CA</u> State <u>92806</u> Zip	
4. Mailing Address: (if different from Item 3) City		Street Address State Zip	
5. Provide the name, title, and phone number of the person to contact for further information: <u>Ronald Hoffard</u> Name <u>Generation Plant Manager</u> Title <u>(714) 765-4536</u> Phone #			

Section II - Reporting of Breakdowns, Deviations, and Emergencies

1. This written notification is to report a(n):			
Type of Incident	Verbal Report Due*	Written Report Due	
a. <input type="checkbox"/> Emergency under Rule 3002(g)	Within 1 hour of discovery	Within 2 working days from when the emission limit was exceeded.	
b. <input checked="" type="checkbox"/> Breakdown under: <input type="checkbox"/> Rule 430 (Non-RECLAIM) <input checked="" type="checkbox"/> Rule 2004 (RECLAIM) <input type="checkbox"/> Rule 218 (Non-RECLAIM) [See Rule 218(f)(3)]	For Rules 430 & 2004 - Within 1 hour of discovery. For Rule 218 - Within 24 hours or next business day for failure/shutdown exceeding 24 hours	For Rules 430 & 2004 - Within 7 calendar days after breakdown is corrected, but no later than 30 days from start of the breakdown, unless a written extension is granted. For Rule 218 - With required semi-annual reports.	
c. <input type="checkbox"/> Deviation with excess emissions [See Title V Permit, Section K, Condition No. 22B]	Within 72 hours of discovery of the deviation or shorter reporting period if required by an applicable State or Federal Regulation.	Within 14 days of discovery of the deviation.	
d. <input type="checkbox"/> Other Deviation [See Title V Permit, Section K, Condition Nos. 22D & 23]	None	With required semi-annual monitoring reports.	
2. The incident was first discovered by: <u>GREG STRONG</u> on <u>04/08/2019</u> <u>09:00</u> <input checked="" type="radio"/> AM <input type="radio"/> PM Name Date Time			
3. The incident was first reported by: <u>OPERATOR #5</u> on <u>04/08/2019</u> <u>09:17</u> <input checked="" type="radio"/> AM <input type="radio"/> PM Name of AQMD Staff Person Date Time			
a. <input checked="" type="radio"/> Via Phone			
b. <input type="radio"/> In Person			
Notification Number (Required): <u>556458</u>			
4. When did the incident actually occur? <u>04/07/2019</u> <u>06:15</u> <input type="radio"/> AM <input checked="" type="radio"/> PM Date Time			


AQMD USE ONLY	Received By:		Assigned By:		Inspector:	
	Date/Time Received:		Date/Time Assigned:		Date/Time Received Assignment:	
	Date Delivered To Team:		Date Reviewed Inspector Report:		Date Inspected Facility:	
	Team:	Sector:	Breakdown/Deviation Notification No.		Date Completed Report:	
	Recommended Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____
	Final Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____

5. Has the incident stopped? a. ☒ Yes, on: 04/07/2019 08:05 ☐ AM ☒ PM b. ☐ No
Date Time
6. What was the total duration of the incident? 1.03
Days Hours
7. For equipment with an operating cycle, as defined in Rule 430 (b)(3)(A), when was the end of the operating cycle during which the incident occurred? _____
Date Time ☐ AM ☒ PM
8. Describe the incident and identify each piece of equipment (by permit, application, or device number) affected. Attach photos (when available) of the affected equipment and attach additional pages as necessary.
See attachment #1
9. The incident may have resulted in a:
a. ☒ Violation of Permit Condition(s): D12.1
b. ☐ Violation of AQMD Rule(s): _____
10. What was the probable cause of the incident? Attach additional pages as necessary.
See attachment #1
11. Did the incident result in excess emissions? ☒ No ☐ Yes (Complete the following and attach calculations.)
☐ VOC _____ lbs ☐ NOx _____ lbs ☐ SOx _____ lbs ☐ H2S _____ lbs
☐ CO _____ lbs ☐ PM _____ lbs ☐ Other: _____ lbs _____ pollutant
12. For RECLAIM facilities Subject to Rule 2004 (i)(3) ONLY: If excess emissions of NOx and/or SOx were reported in Item 11, do you want these emissions to be counted when determining compliance with your annual allocations?
a. ☒ Yes, for: ☐ NOx ☐ SOx b. ☐ No, for: ☐ NOx ☐ SOx
If box 12(b) above is checked, include all information specified in Rule 2004(i)(3)(B) and (C), as applicable.
13. Describe the steps taken to correct the problem (i.e., steps taken to mitigate excess emissions, equipment repairs, etc.) and the preventative measures employed to avoid future incidents. Include photos of the failed equipment if available and attach additional pages as necessary.
See attachment #1
14. Was the facility operating properly prior to the incident?
a. ☒ Yes b. ☐ No, because: _____
15. Did the incident result from operator error, neglect or improper operation or maintenance procedures?
a. ☐ Yes b. ☒ No, because: _____
16. Has the facility returned to compliance?
a. ☐ No, because: _____
b. ☒ Yes (Attach evidence such as emissions calculations, contemporaneous operating logs or other credible evidence.)

Section III - Certification Statement

I certify under penalty of law that based on information and belief formed after reasonable inquiry, the statements and information in this document and in all attachments and other materials are true, accurate, and complete.

For Title V Facilities ONLY: ☒ I also certify under penalty of law that that I am the responsible official for this facility as defined in AQMD Regulation XXX.

1. Signature of Responsible Official: 	2. Title of Responsible Official: INTEGRATED RESOURCES MANAGER
3. Print Name: RONALD HOFFARD	4. Date: 04/12/2019
5. Phone #: (714) 765-4536	6. Fax #:
7. Address of Responsible Official: 3071 E. MIRALOMA AVENUE Anaheim CA 92806	
Street #	City State Zip

AQMD 500N Episode Date: 04/07/2019

Identify Issue: CEMS fuel flow failed to register

Canyon Power Plant: Unit 2/ID# 153992

Notification: 556458

Question 8 - Describe the incident and identify each piece of equipment:

Unit 2 dispatched at 1815 hours on April 7, 2019. During the start-up period, Unit 2 experienced an ammonia flow control valve failure to open. The Operator Technician placed the ammonia controls in manual operation and continued operation with emissions in compliance and no further incidents. During troubleshooting for ammonia valve failure to automatically open, it was discovered that there had been a loss of fuel meter data transmission to the Unit 2 control computer. Fuel flow data is the permissive that causes automatic opening of the ammonia flow control valve. The fuel flow meter is a device listed in the SCAQMD Permit to Operate, which was subsequently reported to SCAQMD as a breakdown.

Question 10 – What was the probable cause of the incident?

Staff identified a broken wire inside the fuel meter signal-converter, which prevented transmission of fuel flow data to Unit 2 controls and the CEMS (see pic #2).

Question 13 – Describe the steps taken to correct the problem:

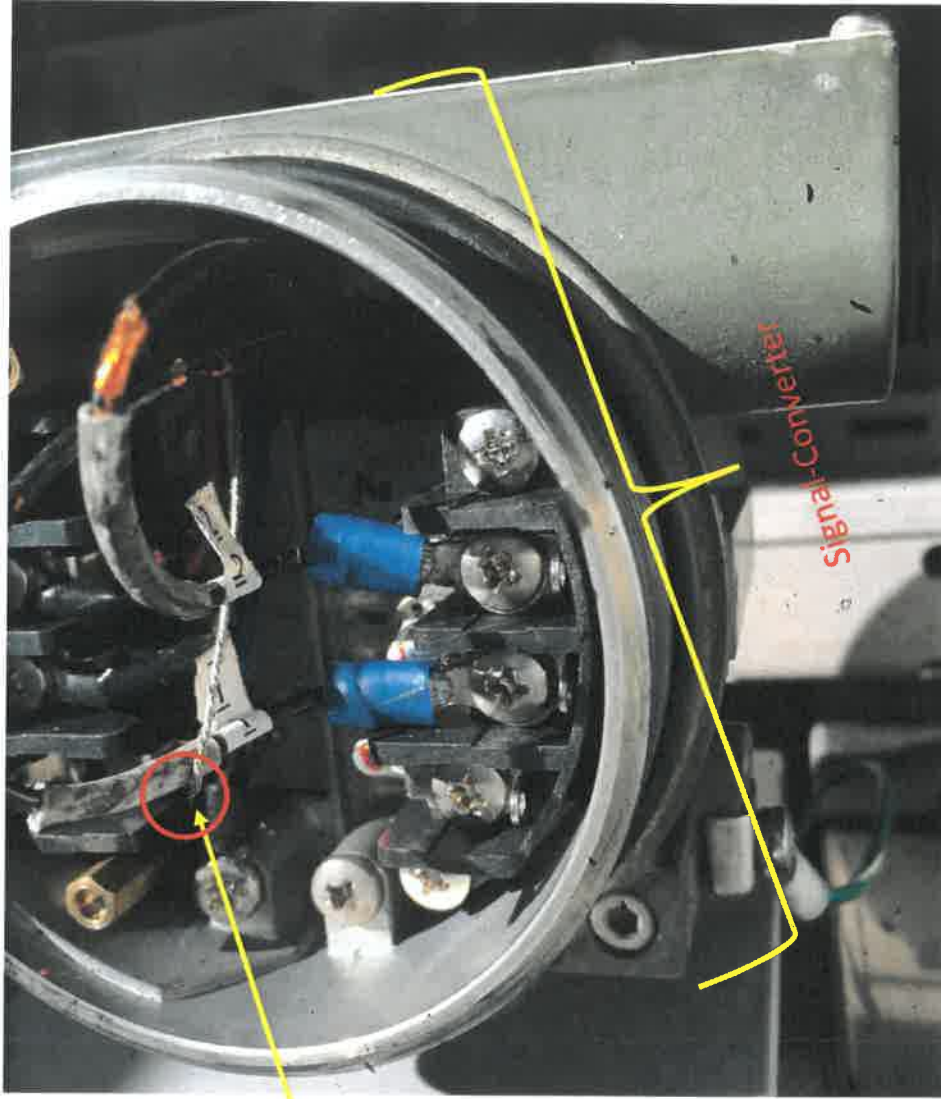
The broken wire and connection in fuel flow transmitter (FT-6246) Signal-Converter was repaired and the unit fuel flow transmitter was successfully tested on April 8, 2019.

Question 16 – Facility returned to compliance?

Unit 2 was shutdown on April 7, 2019 at 2005 hours. The troubleshooting and repairs to Unit 2 occurred on April 8, 2019 and the unit successfully tested at 1035 hours. The test results showed the CEMS registering the correct fuel flow.

Canyon Power Plant
ID#153992
4/7/19

Shielding wire
broken





South Coast Air Quality Management District

Form 500-N**Title V - Deviations, Emergencies & Breakdowns**

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Mail To:
SCAQMD
P.O. Box 4941
Diamond Bar, CA 91765-0941

Tel: (909) 396-3385
www.aqmd.gov

Section I - Operator Information

1. Facility Name (Business Name of Operator That Appears On Permit):

CANYON POWER PLANT

2. Valid AQMD Facility ID (Available On Permit Or Invoice Issued By AQMD):

153992

3. Address:

3071 E. Miraloma Avenue

(where incident occurred)

Street Address

Anaheim

City

CA

State

92806

Zip

4. Mailing Address:

(if different from Item 3)

Street Address

City

State

Zip

5. Provide the name, title, and phone number of the person to contact for further information:

Ronald Hoffard

Name

Generation Plant Manager

Title

(714) 765-4536

Phone #

Section II - Reporting of Breakdowns, Deviations, and Emergencies

1. This written notification is to report a(n):

Type of Incident

Verbal Report Due*

Written Report Due

a. ☐ Emergency under Rule 3002(g)

Within 1 hour of discovery

Within 2 working days from when the emission limit was exceeded.

b. ☐ Breakdown under:☐ Rule 430 (Non-RECLAIM)

For Rules 430 & 2004 - Within 1 hour of discovery.

For Rules 430 & 2004 - Within 7 calendar days after breakdown is corrected, but no later than 30 days from start of the breakdown, unless a written extension is granted.

☐ Rule 2004 (RECLAIM)

For Rule 218 - Within 24 hours or next business day for failure/shutdown exceeding 24 hours

For Rule 218 - With required semi-annual reports.

☐ Rule 218 (Non-RECLAIM)

[See Rule 218(f)(3)]

c. ☐ Deviation with excess emissions

[See Title V Permit, Section K, Condition No. 22B]

Within 72 hours of discovery of the deviation or shorter reporting period if required by an applicable State or Federal Regulation.

Within 14 days of discovery of the deviation.

d. ☒ Other Deviation

[See Title V Permit, Section K, Condition Nos. 22D & 23]

None

With required semi-annual monitoring reports.

2. The incident was first discovered by: **Greg Strong**

Name

on

09/07/2019

Date

06:25

Time

☐ AM☒ PM3. The incident was first reported by: **Voicemail left at 1800-CUT-SMOG**

Name of AQMD Staff Person

on

09/07/2019

Date

06:52

Time

☐ AM☒ PMa. ☒ Via Phoneb. ☐ In PersonNotification Number (Required): **578653**4. When did the incident actually occur? **09/07/2019**

Date

06:25

Time

☐ AM☒ PM


AQMD USE ONLY	Received By:		Assigned By:		Inspector:	
	Date/Time Received:		Date/Time Assigned:		Date/Time Received Assignment:	
	Date Delivered To Team:		Date Reviewed Inspector Report:		Date Inspected Facility:	
	Team:	Sector:	Breakdown/Deviation Notification No.		Date Completed Report:	
	Recommended Action:		Cancel Notification	Grant Relief	Issue NOV No.	Other:
	Final Action:		Cancel Notification	Grant Relief	Issue NOV No.	Other:

5. Has the incident stopped? a. ☒ Yes, on: 09/07/2019 06:25 ☐ AM ☒ PM b. ☐ No
Date Time
6. What was the total duration of the incident? _____
Days Hours
7. For equipment with an operating cycle, as defined in Rule 430 (b)(3)(A), when was the end of the operating cycle during which the incident occurred? _____
Date Time ☐ AM ☒ PM
8. Describe the incident and identify each piece of equipment (by permit, application, or device number) affected. Attach photos (when available) of the affected equipment and attach additional pages as necessary.
SEE SUMMARY ATTACHED
9. The incident may have resulted in a:
a. ☐ Violation of Permit Condition(s): _____
b. ☒ Violation of AQMD Rule(s): Rule 2012(c)(3)(C)
10. What was the probable cause of the incident? Attach additional pages as necessary.
SEE SUMMARY ATTACHED
11. Did the incident result in excess emissions? ☒ No ☐ Yes (Complete the following and attach calculations.)
☐ VOC _____ lbs ☐ NOx _____ lbs ☐ SOx _____ lbs ☐ H2S _____ lbs
☐ CO _____ lbs ☐ PM _____ lbs ☐ Other: _____ lbs pollutant
12. For RECLAIM facilities Subject to Rule 2004 (i)(3) ONLY: If excess emissions of NOx and/or SOx were reported in Item 11, do you want these emissions to be counted when determining compliance with your annual allocations?
a. ☒ Yes, for: ☐ NOx ☐ SOx b. ☐ No, for: ☐ NOx ☐ SOx
If box 12(b) above is checked, include all information specified in Rule 2004(i)(3)(B) and (C), as applicable.
13. Describe the steps taken to correct the problem (i.e., steps taken to mitigate excess emissions, equipment repairs, etc.) and the preventative measures employed to avoid future incidents. Include photos of the failed equipment if available and attach additional pages as necessary.
SEE SUMMARY ATTACHED
14. Was the facility operating properly prior to the incident?
a. ☒ Yes b. ☐ No, because: _____
15. Did the incident result from operator error, neglect or improper operation or maintenance procedures?
a. ☐ Yes b. ☒ No, because: proper back-up continuously
16. Has the facility returned to compliance?
a. ☐ No, because: _____
b. ☒ Yes (Attach evidence such as emissions calculations, contemporaneous operating logs or other credible evidence.)

Section III - Certification Statement

I certify under penalty of law that based on information and belief formed after reasonable inquiry, the statements and information in this document and in all attachments and other materials are true, accurate, and complete.

For Title V Facilities ONLY: ☒ I also certify under penalty of law that that I am the responsible official for this facility as defined in AQMD Regulation XXX.

1. Signature of Responsible Official: 	2. Title of Responsible Official: GENERATION PLANT MANAGER
3. Print Name: RONALD HOFFARD	4. Date: 9/18/19
5. Phone #: (714) 765-4536	6. Fax #:
7. Address of Responsible Official: 3071 E. MIRALOMA AVE ANAHEIM CA 92806	
Street #	City State Zip

SCAQMD Form 500-N Deviation Date: 09/07/2019

Identify issue: DAHS Computer server failed

Canyon Power Plant: Unit 1-4/ID# 153992

Notification: 578653

Question 8 - Describe the incident and identify each piece of equipment:

On September 7, 2019 Greg Strong, Canyon Technician, was called to operate Canyon's turbine at approximately 1400 hrs. An on-line passing Calibration was performed at approximately 1500 hrs for all four units. At 1825 hrs, Greg heard beeping sounds coming from the DAHS computer followed by a computer lock up and terminal failure. The technician attempted to reboot the DAHS computer to no avail. The four units were immediately shut down and placed in forced outage for the duration of the DAHS loss.

All analyzers in the CEMS shack that monitor each of the turbines were in working condition and were not affected by the DAHS computer crashing.

On Monday, September 9, 2019, the DAHS software vendor CEMTEK KVB-Enertec was contacted to assist with repairing or replacing Canyon's DAHS computer. A new computer arrived on Tuesday, September 10, 2019, however, the old computer was unable to operate and the vendor could not access the data to reconfigure the new computer. In-house testing was performed but the old computer was not able to reboot. The old computer was delivered to an outside company for recovery of the data from the drives.

Question 10 – What was the probable cause of the incident?

The probable cause was due to a cache controller RAID malfunction.

Question 13 – Describe the steps taken to correct the problem:

The software vendor KVB-Enertec was contacted to assist with the repairing or replacing of the DAHS computer. A new computer was received on Tuesday, September 10, 2019 and installed. The old computer was delivered to a facility to recover data from internal drives since the computer was not operable with the RAID 5 cache malfunction. The new computer was successfully reconfigured with the recovered data.

Question 16 – Facility retuned to compliance.

The DAHS computer returned to compliance on Friday, September 13, 2019 at 1130 hrs. All daily RTUs were submitted to SCAQMD. The four units operated on September 14, 2019 without issue.



South Coast Air Quality Management District

Form 500-N**Title V - Deviations, Emergencies & Breakdowns**

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Mail To:
SCAQMD
P.O. Box 4941
Diamond Bar, CA 91765-0941
Tel: (909) 396-3385
www.aqmd.gov

Section I - Operator Information

1. Facility Name (Business Name of Operator That Appears On Permit): CANYON POWER PLANT Unit 4 (D19)		2. Valid AQMD Facility ID (Available On Permit Or Invoice Issued By AQMD): 153992	
3. Address: (where incident occurred) 3071 E. Miraloma Avenue Anaheim City		Street Address CA State 92806 Zip	
4. Mailing Address: (if different from Item 3) City		Street Address State Zip	
5. Provide the name, title, and phone number of the person to contact for further information: Ronald Hoffard Name Generation Plant Manager Title (714) 765-4536 Phone #			

Section II - Reporting of Breakdowns, Deviations, and Emergencies

Type of Incident	Verbal Report Due*	Written Report Due
a. <input type="checkbox"/> Emergency under Rule 3002(g)	Within 1 hour of discovery	Within 2 working days from when the emission limit was exceeded.
b. <input checked="" type="checkbox"/> Breakdown under: <input type="checkbox"/> Rule 430 (Non-RECLAIM) <input checked="" type="checkbox"/> Rule 2004 (RECLAIM) <input type="checkbox"/> Rule 218 (Non-RECLAIM) [See Rule 218(f)(3)]	For Rules 430 & 2004 - Within 1 hour of discovery. For Rule 218 - Within 24 hours or next business day for failure/shutdown exceeding 24 hours	For Rules 430 & 2004 - Within 7 calendar days after breakdown is corrected, but no later than 30 days from start of the breakdown, unless a written extension is granted. For Rule 218 - With required semi-annual reports.
c. <input type="checkbox"/> Deviation with excess emissions [See Title V Permit, Section K, Condition No. 22B]	Within 72 hours of discovery of the deviation or shorter reporting period if required by an applicable State or Federal Regulation.	Within 14 days of discovery of the deviation.
d. <input type="checkbox"/> Other Deviation [See Title V Permit, Section K, Condition Nos. 22D & 23]	None	With required semi-annual monitoring reports.

2. The incident was first discovered by: **Jeffrey Hacker** on **10/16/2019** **04:55** ☐ AM ☒ PM
Name Date Time

3. The incident was first reported by: **Voicemail left at 1800-CUT-SMOG (Op#8)** on **10/16/2019** **05:19** ☐ AM ☒ PM
Name of AQMD Staff Person Date Time

a. ☒ Via Phone
b. ☐ In Person

Notification Number (Required): **583951**

4. When did the incident actually occur? **10/16/2019** **04:55** ☐ AM ☒ PM
Date Time

AQMD USE ONLY	Received By:		Assigned By:		Inspector:	
	Date/Time Received:		Date/Time Assigned:		Date/Time Received Assignment:	
	Date Delivered To Team:		Date Reviewed Inspector Report:		Date Inspected Facility:	
	Team:	Sector:	Breakdown/Deviation Notification No.		Date Completed Report:	
	Recommended Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____
	Final Action:		Cancel Notification	Grant Relief	Issue NOV No. _____	Other: _____

5. Has the incident stopped?	a. <input checked="" type="radio"/> Yes, on: <u>10/16/2019</u> Date	Time <u>05:00</u> <input type="radio"/> AM <input checked="" type="radio"/> PM	b. <input type="radio"/> No
6. What was the total duration of the incident?	Days _____	Hours <u>06</u> Hours MIN	
7. For equipment with an operating cycle, as defined in Rule 430 (b)(3)(A), when was the end of the operating cycle during which the incident occurred?	Date _____	Time _____	<input type="radio"/> AM <input type="radio"/> PM
8. Describe the incident and identify each piece of equipment (by permit, application, or device number) affected. Attach photos (when available) of the affected equipment and attach additional pages as necessary. See attached summary			
9. The incident may have resulted in a:			
a. <input checked="" type="checkbox"/> Violation of Permit Condition(s):	<u>A99.1 NOx ppm > 2.5</u>		
b. <input type="checkbox"/> Violation of AQMD Rule(s):	_____		
10. What was the probable cause of the incident? Attach additional pages as necessary. See attached summary			
11. Did the incident result in excess emissions? <input type="radio"/> No <input checked="" type="radio"/> Yes (Complete the following and attach calculations.)			
<input type="checkbox"/> VOC _____ lbs	<input checked="" type="checkbox"/> NOx <u>1.170</u> lbs	<input type="checkbox"/> SOx _____ lbs	<input type="checkbox"/> H2S _____ lbs
<input type="checkbox"/> CO _____ lbs	<input type="checkbox"/> PM _____ lbs	<input type="checkbox"/> Other: _____ lbs	_____ pollutant
12. For RECLAIM facilities Subject to Rule 2004 (i)(3) ONLY: If excess emissions of NOx and/or SOx were reported in Item 11, do you want these emissions to be counted when determining compliance with your annual allocations?			
a. <input checked="" type="radio"/> Yes, for: <input type="checkbox"/> NOx <input type="checkbox"/> SOx		b. <input type="radio"/> No, for: <input type="checkbox"/> NOx <input type="checkbox"/> SOx	
If box 12(b) above is checked, include all information specified in Rule 2004(i)(3)(B) and (C), as applicable.			
13. Describe the steps taken to correct the problem (i.e., steps taken to mitigate excess emissions, equipment repairs, etc.) and the preventative measures employed to avoid future incidents. Include photos of the failed equipment if available and attach additional pages as necessary. See attached summary			
14. Was the facility operating properly prior to the incident?			
a. <input checked="" type="radio"/> Yes		b. <input type="radio"/> No, because: _____	
15. Did the incident result from operator error, neglect or improper operation or maintenance procedures?			
a. <input type="radio"/> Yes		b. <input checked="" type="radio"/> No, because: <u>Quarterly maintenance is performed to stack sample cooler</u>	
16. Has the facility returned to compliance?			
a. <input type="radio"/> No, because: _____		b. <input checked="" type="radio"/> Yes (Attach evidence such as emissions calculations, contemporaneous operating logs or other credible evidence.)	
Section III - Certification Statement			
I certify under penalty of law that based on information and belief formed after reasonable inquiry, the statements and information in this document and in all attachments and other materials are true, accurate, and complete.			
For Title V Facilities ONLY: <input checked="" type="checkbox"/> I also certify under penalty of law that I am the responsible official for this facility as defined in AQMD Regulation XXX.			
1. Signature of Responsible Official: 		2. Title of Responsible Official: <u>GENERATION PLANT MANAGER</u>	
3. Print Name: <u>RONALD HOFFARD</u>		4. Date: <u>10/21/19</u>	
5. Phone #: <u>(714) 765-4536</u>		6. Fax #: _____	
7. Address of Responsible Official:			
<u>3071 E. Miraloma Ave.</u>		<u>Anaheim</u>	<u>CA</u> <u>92806</u>
Street #	City	State	Zip

AQMD 500N Episode Date: 10/16/19

Identify issue: Unit 4 Stack NOx Sample Cooler tubing disconnected

Canyon Power Plant: Unit 1/ID# 153992

Notification: 583951

Question 8 - Describe the incident and identify each piece of equipment:

Unit 4 initiated operation on 10/16/19 at 1053 am (DAHS time) to conduct RATA source testing. Unit 4 operated within the required NOx, CO and ROG permit limits until minute 1654 when the NOx ppm spiked from 2.17ppm to 20.31 in two seconds. The operators received a Unit 4 stack sample flow alarm at 1657 and proceeded to Unit 4 CEMS shack to verify the issue. The operator found that one of four sample cooler impingers had disconnected from the sample cooler. The tubing was immediately connected to the impinger and the unit returned to compliance by minute 1700 with a NOx ppm of 2.53ppm. Unit 4 continued in compliance until the unit was shut-down at 2103 hours (see attached minute data).

Question 10 – What was the probable cause of the incident?

An analyzer sample cooler tube attached to the impinger became disconnected.

Question 13 – Describe the steps taken to correct the problem:

New tubing connectors and impingers were installed, in addition, a backing plate will be installed to secure and prevent tubing from disconnecting.

Question 16 – Facility returned to compliance?

Unit 4 returned to compliance on 10/16/19 at 1700 hours.

CANYON POWER PLANT
ID # 153992

U4

DAHS MINUTE DATA

Time	4_NOXPPM ppm	4_NOX_CORR ppm	status	4_LOAD MW	4_GasFlow kscfh	status	4_NH3_Flow #/hr	status	4_H2O_FLOW k#/hr	status	4_NOxC_1H ppm/hr
15:44	2.69	2.45		50.19	461.4		79.26		24.6		2.29
15:45	2.79	2.54		50.19	461.1		81.39		24.6		2.29
15:46	2.8	2.55		50.17	461.8		82.57		24.8		2.29
15:47	2.68	2.44		50.26	461.5		82.42		24.8		2.29
15:48	2.43	2.21		50.09	462.1		81.55		24.9		2.29
15:49	2.29	2.09		50.28	461.8		80.92		24.7		2.29
15:50	2.33	2.12		50.35	461.3		80.91		24.6		2.29
15:51	2.51	2.29		50.22	461.5		80.86		24.7		2.29
15:52	2.62	2.39		50.09	461.3		81.35		24.7		2.29
15:53	2.61	2.38		50.33	461.4		81.42		24.6		2.29
15:54	2.54	2.32		50.06	460.9		81.21		24.6		2.29
15:55	2.5	2.28		50.11	460.6		80.9		24.6		2.29
15:56	2.51	2.29		50.08	460.9		80.88		24.6		2.29
15:57	2.55	2.33		50.06	460.8		80.89		24.6		2.29
15:58	2.56	2.34		50.16	460.9		80.97		24.6		2.29
15:59	2.55	2.33		50.1	460.9		80.98		24.6		2.29
16:00	2.55	2.33		50.24	460		80.99		24.6		2.78
16:01	2.56	2.33		50.08	460.9		81.03		24.6		2.78
16:02	2.57	2.35		50.04	460.5		80.98		24.6		2.78
16:03	2.58	2.35		50.31	461.4		81.05		24.7		2.78
16:04	2.59	2.36		50.21	461.5		81.03		24.7		2.78
16:05	2.6	2.37		50.23	460.6		81.15		24.6		2.78
16:06	2.62	2.39		49.96	461.6		81.14		24.7		2.78
16:07	2.61	2.38		50.04	460.8		81.38		24.6		2.78
16:08	2.58	2.35		50.13	461.2		81.47		24.6		2.78
16:09	2.57	2.34		50.01	461.5		81.46		24.6		2.78
16:10	2.55	2.33		50.1	461.3		81.42		24.6		2.78
16:11	2.53	2.31		50.21	461		81.41		24.6		2.78
16:12	2.53	2.31		50.27	461.1		81.35		24.6		2.78
16:13	2.53	2.31		50.19	461.1		81.4		24.6		2.78
16:14	2.5	2.28		50.23	460.9		81.45		24.6		2.78
16:15	2.5	2.28		50.17	460.7		81.39		24.6		2.78
16:16	2.49	2.27		50.21	461.1		81.44		24.6		2.78
16:17	2.5	2.28		50.2	460.8		81.38		24.6		2.78
16:18	2.51	2.29		50.17	461.3		81.42		24.6		2.78
16:19	2.51	2.29		50.24	461.1		81.33		24.6		2.78
16:20	2.51	2.29		50.09	461.3		81.45		24.6		2.78
16:21	2.5	2.28		50.24	461.8		81.38		24.7		2.78
16:22	2.51	2.29		50.23	461.7		81.38		24.7		2.78
16:23	2.52	2.29		50.08	462.1		81.42		24.7		2.78
16:24	2.54	2.31		50.09	461.7		81.28		24.7		2.78
16:25	2.58	2.33		50.03	462.4		81.67		24.7		2.78
16:26	2.63	2.37		50.17	462.4		81.58		25		2.78
16:27	2.65	2.39		50.18	462.8		81.98		24.6		2.78
16:28	2.57	2.33		50.05	462.1		81.91		24.6		2.78

CANYON POWER PLANT
ID # 153992
U4

Time	4_NOXPPM ppm	4_NOX_CORR ppm	status	4_LOAD MW	status	4_GasFlow kscfh	status	4_NH3_Flow #/hr	status	4_H2O_FLOW k#/hr	status	4_NOxC_1H ppm/hr
16:29	2.6	2.35		50.14		463		82.04		24.7		2.78
16:30	2.71	2.45		50.2		462.2		82.2		24.6		2.78
16:31	2.69	2.43		50.19		462.9		82.51		24.6		2.78
16:32	2.7	2.44		50.27		462.3		82.63		24.6		2.78
16:33	2.7	2.45		50.23		461.7		83.3		24.6		2.78
16:34	2.65	2.4		50.32		462.1		84.1		24.6		2.78
16:35	2.53	2.3		50.2		462.1		83.99		24.7		2.78
16:36	2.39	2.17		50.13		462.4		84.05		24.7		2.78
16:37	2.29	2.09		50.2		462.1		81.13		24.7		2.78
16:38	2.3	2.09		50.27		462.1		81.1		24.6		2.78
16:39	2.42	2.2		50.27		462.2		81.12		24.7		2.78
16:40	2.54	2.31		50.19		462		81.04		24.8		2.78
16:41	2.53	2.3		50.24		461.9		81.07		24.8		2.78
16:42	2.49	2.26		50.08		462.9		81.02		24.9		2.78
16:43	2.46	2.24		50.04		462.2		81.07		24.7		2.78
16:44	2.44	2.22		50.17		461.9		81.08		24.8		2.78
16:45	2.47	2.25		50.23		461.9		81.1		24.7		2.78
16:46	2.48	2.26		50.19		462.4		80.98		24.7		2.78
16:47	2.45	2.23		50.34		462.3		81.08		24.8		2.78
16:48	2.44	2.22		50.19		462.3		81.02		24.8		2.78
16:49	2.44	2.23		50.26		462		81.02		24.7		2.78
16:50	2.43	2.22		50.16		462		80.99		24.8		2.78
16:51	2.41	2.19		50.32		462.5		80.96		24.8		2.78
16:52	2.4	2.19		50.07		462.7		81.07		24.8		2.78
16:53	2.41	2.19		50.22		462.6		80.96		24.8		2.78
16:54	2.45	2.17		50.2		463		80.81		24.8		2.78
16:55	11.32	9.65		50.25		462.4		80.68		24.8		2.78
16:56	22.75	20.31		50.06		462.9		80.5		24.9		2.78
16:57	5.96	5.38		50.22		462.9		80.37		24.7		2.78
16:58	2.82	2.55		50.2		463		80.49		24.7		2.78
16:59	2.85	2.58	2.78	50.17		462		81.09		25		2.78
17:00	2.8	2.53		50.1		464.6		84.2		25.3		2.15
17:01	1.98	1.79		50.15		462.2		84.32		24.6		2.15
17:02	2.4	2.17		50.05		462.8		84.38		24.6		2.15
17:03	2.44	2.21		50.23		462.2		84.61		24.7		2.15
17:04	2.41	2.18		50.25		463.2		84.79		24.7		2.15
17:05	2.37	2.15		50.03		462.8		84.79		24.8		2.15
17:06	2.3	2.09		50.05		462.7		84.79		24.8		2.15
17:07	2.24	2.03		50.26		462.8		84.28		24.8		2.15
17:08	2.21	2.01		50.21		462.7		84.17		24.7		2.15
17:09	2.23	2.03		50.26		462.5		84.12		24.8		2.15
17:10	2.25	2.05		50.08		462.2		84.18		24.6		2.15
17:11	2.25	2.05		50.13		462.6		84.24		24.7		2.15
17:12	2.25	2.05		50.32		462.5		84.17		24.8		2.15
17:13	2.23	2.03		50.13		462.2		84.26		24.8		2.15

The stack sample cooler one of the
tubes to the impinger disconnected

The tubing connected to impinger NOx
ppm returned to compliance

15-MIN DATA

Time	Days	Temp.	Humidity
1	1	25	60
2	2	26	62
3	3	27	65
4	4	28	68
5	5	29	70
6	6	30	72
7	7	31	75
8	8	32	78
9	9	33	80
10	10	34	82
11	11	35	85
12	12	36	88
13	13	37	90
14	14	38	92
15	15	39	95
16	16	40	98
17	17	41	100
18	18	42	100
19	19	43	100
20	20	44	100
21	21	45	100
22	22	46	100
23	23	47	100
24	24	48	100
25	25	49	100
26	26	50	100
27	27	51	100
28	28	52	100
29	29	53	100
30	30	54	100
31	31	55	100
32	32	56	100
33	33	57	100
34	34	58	100
35	35	59	100
36	36	60	100
37	37	61	100
38	38	62	100
39	39	63	100
40	40	64	100
41	41	65	100
42	42	66	100
43	43	67	100
44	44	68	100
45	45	69	100
46	46	70	100
47	47	71	100
48	48	72	100
49	49	73	100
50	50	74	100
51	51	75	100
52	52	76	100
53	53	77	100
54	54	78	100
55	55	79	100
56	56	80	100
57	57	81	100
58	58	82	100
59	59	83	100
60	60	84	100
61	61	85	100
62	62	86	100
63	63	87	100
64	64	88	100
65	65	89	100
66	66	90	100
67	67	91	100
68	68	92	100
69	69	93	100
70	70	94	100
71	71	95	100
72	72	96	100
73	73	97	100
74	74	98	100
75	75	99	100
76	76	100	100
77	77	100	100
78	78	100	100
79	79	100	100
80	80	100	100
81	81	100	100
82	82	100	100
83	83	100	100
84	84	100	100
85	85	100	100
86	86	100	100
87	87	100	100
88	88	100	100
89	89	100	100
90	90	100	100
91	91	100	100
92	92	100	100
93	93	100	100
94	94	100	100
95	95	100	100
96	96	100	100
97	97	100	100
98	98	100	100
99	99	100	100
100	100	100	100

CANYON POWER PLANT
ID# 153992
U4

HOURLY DATA

SCAQMD Reclaim Audit Report (Ver:2.2)										
Customer Name:		CITY OF ANAHEIM		Report Start		10/16/2019 0:00				
Unit ID		D19		Report End		10/16/2019 23:59				
Category		CANYON POWER PLANT		Date Generated		10/17/2019 11:31				
NOx Avail		437.8								
Flow Avail		438.9								
Total NOx Mass		43.72								
Date/Time	NOx Valid Quadrants	NOx Calibration/ Maintenance	Average of Valid bias adjusted ppm quadrants	Stack Flow Valid Quadrants	Stack Flow Calibration/ Maintenance	Average of Valid bias adjusted stack flow	Average of Valid NOx lb/hr quadrants	Missing data Procedure	Daily Total	
10/16/2019 0:00	4	0	0	4	0	0	0			
10/16/2019 1:00	4	0	0	4	0	0	0			
10/16/2019 2:00	4	1	0	4	1	0	0			
10/16/2019 3:00	4	0	0	4	0	0	0			
10/16/2019 4:00	4	0	0	4	0	0	0			
10/16/2019 5:00	4	0	0	4	0	0	0			
10/16/2019 6:00	3	1	0	3	1	0	0			
10/16/2019 7:00	4	0	0	4	0	0	0			
10/16/2019 8:00	4	0	0	4	0	0	0			
10/16/2019 9:00	4	0	0	4	0	0	0			
10/16/2019 10:00	4	0	1.65	4	0	2890	2.28			
10/16/2019 11:00	4	1	3.16	4	1	13826	5.23			
10/16/2019 12:00	4	0	2.45	4	0	13661	4			
10/16/2019 13:00	4	0	2.52	4	0	13646	4.11			
10/16/2019 14:00	4	0	2.48	4	0	13637	4.05			
10/16/2019 15:00	4	0	2.51	4	0	13635	4.09			
10/16/2019 16:00	4	0	3.22	4	0	13582	5.22			
10/16/2019 17:00	4	0	2.37	4	0	13619	3.85			
10/16/2019 18:00	4	0	2.47	4	0	13640	4.02			
10/16/2019 19:00	4	1	2.51	4	1	13582	4.07			
10/16/2019 20:00	4	0	1.73	4	0	13299	2.75			
10/16/2019 21:00	4	0	0.07	4	0	1389	0.05			
10/16/2019 22:00	4	0	0	4	0	0	0			
10/16/2019 23:00	4	0	0	4	0	0	0		43.72	

3.22 ppm = 5.22 lbs
2.5 ppm = x
x = (5.22*2.5)/3.22 = 4.05 lbs
5.22-4.05 = 1.17 lbs excess emissions

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 10
CONDITION HAZ-1

List of Hazardous Materials contained at the facility:

- **Aqua Ammonia 19%**
- **Batteries**
- **Bromine**
- **Calibration gases for the CEMS**
- **CO₂**
- **Diesel Fuel**
- **Fire suppression chemicals**
- **Florescent light bulbs**
- **Freon for the chiller systems R-123**
- **Gas Turbine oil**
- **Gas compressor oil**
- **Reagents for the water treatment system**
- **SF₆ in switch gear**
- **Anti-scalent RL 9007**
- **Sodium Hydroxide**
- **ChemTreat BL124**
- **Microbiocide ChemTreat CL2156**
- **Closed System Buffer Formula 6150**
- **ChemTreat CL6855**
- **12.5% Sodium Hypochlorite Solution**
- **RL 1125**
- **Simple Green**
- **ChemTreat CL41**
- **ChemTreat CL6855**
- **Formula 2530LT**
- **Conntect 5000**
- **Powerback Concentrate with Anti-Foam Agent**

Location Information					Chemical Identification					Fire Code Hazard Class Information		
1a*	201	202	203	204	205	206	207*	208	209	210a	210b	215
CERSID	ChemicalLocation	CLConfidential	MapNumber	GridNumber	ChemicalName	TradeSecret	CommonName	EHS	CASNumber	PFCodeHazardClass	SFCodeHazardClass	LargestContainer
10445230	RO WATER TREATMENT	N	1	E-1, F-1		N	ANTISCALENT RL 9007	N				350
10445230	AMMONIA STORAGE TANK		1	D-3		N	AQUA AMMONIA (19%)	N		5	31	10000
10445230	BENEATH BACK-UP GENERATOR	N	1	D-4		N	DIESEL FUEL	N		2		500
10445230	IN TURBINE ENGINES and DRUM STORAGE AREA	N	1	B5, F3-6		N	MOBIL JET OIL II	N		3		150
10445230	ELECTRIC GENERATORS AND DRUM STORAGE AREA	N	1	B5, F3-6		N	MOBIL DTE LIGHT OIL	N		4		500
10445230	HYDRAULIC STARTERS AND DRUM STORAGE AREA	N	1	B5, F3-6			MOBIL DTE 25 OIL	N		4		55
10445230	NATURAL GAS COMPRESSORS AND DRUM STORAGE AREA	N	1	B5, F1-G1		N	MOBIL PEGASUS 805 OIL	N		4		55
10445230	IN TRANSFORMERS	N	1	G 3-6,			MINERAL OIL	N		4		5680
10445230	RO WATER TREATMENT	Y	1	D2	SODIUM HYDROXIDE		CAUSTIC SODA 50%	N		5		330
10445230	NEAR COOLING TOWER AND IN DRUM STORAGE AREA	N	1	D-2		N	BIOCIDE (CHEMTREAT CL41)	N				330
10445230	NEAR COOLING TOWER AND IN DRUM STORAGE AREA		1	B5, E2		N	SODIUM HYPOCHLORITE SOLUTION	N		5		330
10445230	WAREHOUSE AND NEAR EXHAUST TOWERS	N				N	CALIBRATION GAS	N				150
10445230	DRUM STORAGE AREA		1	B5	PROPANE		PROPANE	N	74-98-6	8		290
10445230	SUBSTATION BUILDING	N	1	D7, E7	SULFUR HEXAFLUORIDE	N	SF6	N	2551-62-4			2400
10445230	IN FIRE FIGHTING EQUIPMENT - VARIOUS AREAS	N	1	C5, D4, F1, G1	CARBON DIOXIDE	N	CO2	N	124-38-9			437
10445230	Chiller Enclosure		1	E-2	Freon R-123	N	Freon	N	306-83-2			920
10445230	WATER TREATMENT	N	1	E-1		N	MICROBIOCIDIC CL206 CHEMTREAT	N				120
10445230	WATER TREATMENT	N				N	ChemTreat BL 124	N		5		320
10445230	WATER TREATMENT	N				N	ChemTreat CL 2156	N		5		320
10445230	WATER TREATMENT	N				N	ChemTreat CL6855	N		5		320
10445230	DRUM STORAGE AREA					N	Simple Green	N				55



California Environmental Protection Agency
Air Resources Board
 Phone: 1 (916) 324-2517
 Email: reftrackinfo@arb.ca.gov



File Report for "Canyon Power Plant"

Year of Filing: 2018

Submitted Date: 02/21/2019

Company Profile

Company Name : City of Anaheim Federal tax ID : *****970

Contact Person Details

Person Name : Mr. Ronald Hoffard (Generation Manager)

Phone : Contact: 7147654536

Email : rhoffard@anaheim.net

Mailing Address Information

3071 East Miraloma Ave.
 Anaheim, 92806
 CA

Billing Address Information

3071 East Miraloma Ave.
 Anaheim, 92806
 Anaheim

Facility Profile

Facility Name : Canyon Power Plant Federal tax ID : *****970

Contact Person Details

Person Name : Mr. Ronald Hoffard (Generation Manager)

Phone : Contact: 7147654536

Email : rhoffard@anaheim.net

Mailing Address Information

3071 East Miraloma Ave.
 Anaheim, 92806
 CA

Billing Address Information

3071 East Miraloma Ave.
 Anaheim, 92806
 Anaheim

Refrigeration System Listing

Number	System ID	Full Charge (lbs)	Refrigerant Type	Installation Date	Temperature Class	Equipment Type	Manufacturer	Operational Status	Model	Model Year	Serial Number	Location	Floor Plan (Y/N)
1	CH-100	5200.00	R-123	05/12/2011	Medium	Chiller	Trane	Normal Operation	CDHF3000	2011	L10A00350	North side of facility, in dedicated chiller enclosure.	Y
2	CH-200	5200.00	R-123	05/12/2011	Medium	Chiller	Trane	Normal Operation	CDHF3000	2011	L10B00882	North side of facility, in dedicated chiller enclosure.	Y

Leak detection System

Number	ALD ID	Refrigeration System ID	Installation Date	ALD Type	Detection Limit	Alarm Set Point	Concentration Monitor Type	Manufacturer	Number of Sensors	Sensor Type	Sensor Manufacturer	Location of Sensors/Inlets
1	301-IRF A	CH-100CH-200	05/12/2011	Concentration Monitor (Direct System)	10.00	100	0	Honeywell	2	Infra red	Vulcain/honeywell	1 foot above floor

Refrigeration System Inspection and Servicing

Number	Service Date	System ID	Leaks Detected?	Date Leak Detected	Date Leak Repaired	Number of Days	Refrigerant Added (lbs)	Cause of Leak	Service Provided	Date of Initial VT	Date of Follow-up VT	Purpose of Added Refrigerant	Technician Name	Certificate #	Certificate Type
1	01/22/2018	CH-200	No			0	0.00								
2	01/24/2018	CH-200	No			0	0.00								
3	01/26/2018	CH-200	No			0	0.00								
4	01/29/2018	CH-200	No			0	0.00								
5	01/29/2018	CH-200	No			0	0.00								
6	01/29/2018	CH-100	No			0	0.00								
7	01/30/2018	CH-200	No			0	0.00								
8	01/31/2018	CH-200	No			0	0.00								
9	07/18/2018	CH-100	No			0	0.00								
10	07/31/2018	CH-200	No			0	0.00								
11	08/02/2018	CH-200	No			0	0.00								
12	11/27/2018	CH-200	No			0	0.00								

Leak Detection System Inspection and Servicing

Number	Service Date	ALD ID	Service Type	Description of Service
1	09/10/2018	301-IRF A	Calibration	Performed calibration test on Ref. monitor and calibrated both sensors

Refrigerant Purchase Information

Type	Total Purchased (lbs.)	Total Charged (lbs.)	Total Recovered (lbs.)	Total Stored (lbs.)	Total Shipped (lbs.)
R-123	0.00	0.00	0.00	0.00	0.00

Comment

Submitted By: Ronald Hoffard



California Environmental Protection Agency
Air Resources Board
Phone: (916) 324-2517
Email: reftrackinfo@arb.ca.gov



Online Payment Receipt

Invoice No: 115527

Dated: 2019-02-21

Invoice For Year: 2018

Payment Amount: \$370.00

ARB Reference Code: RMP

Transaction Time: 02/21/2019 03:12:43 PM

Payment Transaction Id: 210219E3C-BED05555-8EF4-4E53-A66C-40E7876DA65F

Payment Result: APPROVAL

Payment Approval Code: 021645



California Environmental Protection Agency
Air Resources Board
Phone: (916) 324-2517
Email: rmp@arb.ca.gov
URL: www.arb.ca.gov/rmp/rmp.htm

Invoice Detail

Invoice No: 115527

Invoice For Year: 2018

ARB REFERENCE CODE: RMP

Dated: 02/21/2019

City of Anaheim				
#	Facility Name	Amount Due(\$)	Exemption	Total (\$)
1	Canyon Power Plant (CIT003-001)	370.00	0	370.00
TOTAL CHARGES				370.00

Please return a copy on the invoice with your payment to the address below.

"Checks should be made payable to the California Air Resources Board.

If required for your company records, the CARB Federal Tax ID is 68-0288069. A \$10 service fee may apply for returned checks."

Air Resources Board

Attn: Accounting

P.O. Box 1436

1001 I St., Floor 20

Sacramento, CA 95812-1436

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 11
CONDITION HAZ-8

In the annual compliance report, the project owner shall include the following statements:

“All current project employee and appropriate contractor background investigations have been performed and that updated certification statements have been appended to the operations security plan”.

All current project employee and appropriate contractor background investigations have been performed and that updated certification statements have been appended to the operations security plan.

“The operations security plan includes all current hazardous materials transport vendor certifications for security plans and employee background investigations”.

The operations security plan includes all current hazardous materials transport vendor certifications for security plans and employee background investigations.

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 12
SOIL & WATER USE REPORT-7

Monthly Water Reading Reports

Company: City of Anaheim/Canyon Power Plant
 Plant Location: 3071 E. Miraloma Ave.
 City/State/Zip: Anaheim, CA 92806

Period Start: 1/1/2019
 Period End: 12/31/2019

Recycle Water Usage

Annual Total Gallons	Annual Total Acre Feet	Monthly Average Gallons	Monthly Average Acre Feet	Monthly Minimum Gallons	Monthly Minimum Acre Feet	Monthly Maximum Gallons	Monthly Maximum Acre Feet	Average Gallons Per Day
19,563,004	60.04	1,630,250	5.00	1,003,135	3.08	2,457,344	7.54	53,895

Company: City of Anaheim/Canyon Power Plant
 Plant Location: 3071 E. Miraloma Ave.
 City/State/Zip: Anaheim, CA 92806

Period Start: 1/1/2018
 Period End: 12/31/2018

Potable Water Usage

Annual Total Gallons	Annual Total Acre Feet	Monthly Average Gallons	Monthly Average Acre Feet	Monthly Minimum Gallons	Monthly Minimum Acre Feet	Monthly Maximum Gallons	Monthly Maximum Acre Feet	Average Gallons Per Day
106,201	0.33	4,425	0.01	0.00	0.00	13,600	0.04	146

Annual Data

	Recycle Water		Portable Water	
	Annual Total Acre Feet	Annual Total Gallons	Annual Total Acre Feet	Annual Total Gallons
2017	73.21	23,854,364	0.41	134,469
2018	73.09	23,817,912	6.99	2,277,132
2019	60.04	19,563,004	0.33	106,201
Average	68.78	22,411,760	2.58	839,267
Min	60.04	19,563,004	0.33	106,201
Max	73.21	23,854,364	6.99	2,277,132

Company: City of Anaheim
Plant Location: 3071 E. Miraloma Ave.
City/State/Zip: Anaheim, CA 92806

Period Start: 1/1/2019
Period End: 12/31/2019

Recycled Water Usage

Date	Start Cubic-ft	End Cubic-ft	Total Cubic-ft	Month gal	Daily gal	Month Acre-ft
1/1/2019	17,633,900.00	17,768,000	134,100.00	1,003,135.05	32,359.20	3.08
2/1/2019	17,768,000.00	18,096,500	328,500.00	2,457,344.25	87,762.29	7.54
3/1/2019	18,096,500.00	18,256,800	160,300.00	1,199,124.15	38,681.42	3.68
4/1/2019	18,256,800.00	18,496,700	239,900.00	1,794,571.95	59,819.07	5.51
5/1/2019	18,496,700.00	18,631,100	134,400.00	1,005,379.20	32,431.59	3.09
6/1/2019	18,631,100.00	18,851,600	220,500.00	1,649,450.25	54,981.68	5.06
7/1/2019	18,851,600.00	19,127,500	275,900.00	2,063,869.95	66,576.45	6.33
8/1/2019	19,127,500.00	19,422,000	294,500.00	2,203,007.25	71,064.75	6.76
9/1/2019	19,422,000.00	19,697,900	275,900.00	2,063,869.95	68,795.67	6.33
10/1/2019	19,697,900.00	19,887,600	189,700.00	1,419,050.85	45,775.83	4.35
11/1/2019	19,887,600.00	20,044,500	156,900.00	1,173,690.45	39,123.02	3.60
12/1/2019	20,044,500.00	20,249,100	204,600.00	1,530,510.30	49,371.30	4.70
Annual Total:			2,615,200.00	19,563,003.60		60.04
Average:			217,933.33	1,630,250.30	53,895.19	5.00
Monthly Minimum:			134,100.00	1,003,135.05		3.08
Monthly Maximum:			328,500.00	2,457,344.25		7.54

Company: City of Anaheim
Plant Location: 3071 E. Miraloma Ave.
City/State/Zip: Anaheim, CA 92806

Period Start: 1/1/2019
Period End: 12/31/2019

Potable Water Usage

HCF-1

Date	Start Cubic-ft	End Cubic-ft	Total Cubic-ft	Month gal	Daily gal	Month Acre-ft
1/1/2019	828,400.00	828,500	100.00	748.05	24.13	0.00
2/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
3/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
4/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
5/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
6/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
7/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
8/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
9/1/2019	828,500.00	828,500	0.00	0.00	0.00	0.00
10/1/2019	828,500.00	828,600	100.00	748.05	24.13	0.00
11/1/2019	828,600.00	828,600	0.00	0.00	0.00	0.00
12/1/2019	828,600.00	828,600	0.00	0.00	0.00	0.00
Annual Total:			200.00	1,496.10		0.00
Average:			16.67	124.68	4.02	0.00
Monthly Minimum:			0.00	0.00		0.00
Monthly Maximum:			100.00	748.05		0.00

HCF-2

Date	Start Cubic-ft	End Cubic-ft	Total Cubic-ft	Month gal	Daily gal	Month Acre-ft
1/1/2019	211,862.00	211,865.00	3.00	22.44	0.72	0.00
2/1/2019	211,865.00	213,250.00	1,385.00	10,360.49	370.02	0.03
3/1/2019	213,250.00	214,093.00	843.00	6,306.06	203.42	0.02
4/1/2019	214,093.00	215,436.00	1,343.00	10,046.31	334.88	0.03
5/1/2019	215,436.00	217,045.00	1,609.00	12,036.12	388.26	0.04
6/1/2019	217,045.00	218,312.00	1,267.00	9,477.79	315.93	0.03
7/1/2019	218,312.00	219,116.00	804.00	6,014.32	194.01	0.02
8/1/2019	219,116.00	220,349.00	1,233.00	9,223.46	297.53	0.03
9/1/2019	220,349.00	221,967.00	1,618.00	12,103.45	403.45	0.04
10/1/2019	221,967.00	223,785.00	1,818.00	13,599.55	438.70	0.04
11/1/2019	223,785.00	225,321.00	1,536.00	11,490.05	383.00	0.04
12/1/2019	225,321.00	225,859.00	538.00	4,024.51	129.82	0.01
Annual Total:			13,997.00	104,704.56		0.32
Average:			1,166.42	8,725.38	288.31	0.03
Monthly Minimum:			3.00	22.44		0.00
Monthly Maximum:			1,818.00	13,599.55		0.04

Summary for both meters

Annual Total:	14,197.00	106,200.66	0.33
Average:	591.54	4425.03	146.17
Monthly Minimum:	0.00	0.00	0.00
Monthly Maximum:	1,818.00	13,599.55	0.04

OCWD/Anaheim Distribution & Sale of GWRS Water Supplied

TO Anaheim Public Utilities Dept.
Attn: Al Shaikh
201 S. Anaheim Blvd. Suite #601
Anaheim, CA 92805

CUSTOMER ID: **20250**
RATE: **\$552 / AF**
ACCOUNT: **1001.41500**
AGMT NO: **6075**

METER ID: **21024735**
UNIT: **GALLONS**
MULTIPLIER: **X1000**
FISCAL YEAR: **2018-2019**
READ DATE: **2/28/2019**

LOCATION:	CANYON POWER PLANT (CPP)					
MONTH:	JULY 2018	AUGUST 2018	SEPT 2018	OCT 2018	NOV 2018	DEC 2018
(1) Beginning Read	136,971	141,149	145,803	145,803	147,896	150,051
(2) Ending Read	141,149	145,803	145,803	147,896	150,051	151,312
Total Units (Gallons x1000)	4,178,000	4,654,000	0	2,093,000	2,155,000	1,261,000
Total Acre Feet	12.82	14.29	0.00	6.42	6.63	3.90
AMOUNT DUE:	\$7,076.64	\$7,888.08	\$0.00	\$3,543.84	\$3,659.76	\$2,152.80

LOCATION:	CANYON POWER PLANT (CPP)					
MONTH:	JAN 2019	FEB 2019	MAR 2019	APR 2019	MAY 2019	JUNE 2019
(1) Beginning Read	151,312	152,312	154,774	156,113	157,901	159,043
(2) Ending Read	152,312	154,774	156,113	157,901	159,043	160,867
Total Units (Gallons x1000)	1,000,000	2,462,000	1,339,000	1,788,000	1,142,000	1,824,000
Total Acre Feet	3.07	7.56	4.11	5.49	3.51	5.60
AMOUNT DUE:	\$1,694.64	\$4,173.12	\$2,268.72	\$3,030.48	\$1,937.52	\$3,091.20

OCWD/Anaheim Distribution & Sale of GWRS Water Supplied

TO Anaheim Public Utilities Dept.
Attn: Al Shaikh
201 S. Anaheim Blvd. Suite #601
Anaheim, CA 92805

CUSTOMER ID: **20250**
RATE: **\$602 / AF**
ACCOUNT: **1001.41500**
AGMT NO: **6075**

METER ID: **21024735**
UNIT: **GALLONS**
MULTIPLIER: **X1000**
FISCAL YEAR: **2019-2020**
READ DATE: **12/31/2019**

LOCATION:	CANYON POWER PLANT (CPP)					
MONTH:	JULY 2019	AUGUST 2019	SEPT 2019	OCT 2019	NOV 2019	DEC 2019
(1) Beginning Read	160,867	162,779	164,926	166,194	168,196	169,901
(2) Ending Read	162,779	164,926	166,194	168,196	169,901	172,311
Total Units (Gallons x1000)	1,912,000	2,147,000	1,268,000	2,002,000	1,705,000	2,410,000
Total Acre Feet	5.87	6.59	3.89	6.15	5.23	7.40
AMOUNT DUE:	\$3,533.74	\$3,967.18	\$2,341.78	\$3,702.30	\$3,148.46	\$4,448.78

LOCATION:	CANYON POWER PLANT (CPP)					
MONTH:	JAN 2020	FEB 2020	MAR 2020	APR 2020	MAY 2020	JUNE 2020
(1) Beginning Read						
(2) Ending Read						
Total Units (Gallons x1000)						
Total Acre Feet						
AMOUNT DUE:						

Wastewater Flow Meter Calibration Report

January 14, 2019

Ms. Mila Kleinbergs
Source Control Program
Orange County Sanitation Districts
10844 Ellis Avenue
Fountain Valley, CA 92708

Subject: Effluent Flow Meter Hydraulic Calibration Report

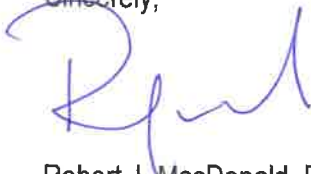
Facility: City of Anaheim
Canyon Power Plant
3071 E. Miraloma Ave.
Anaheim, CA 92806
I.W. Permit No. 1-600296

Dear Ms. Kleinbergs,

Enclosed is our report on the effluent flow meter hydraulic calibration completed at the subject facility on January 10, 2019. The calibration was conducted in accordance with requirements of the Orange County Sanitation District, and the meter was determined to be operating within $\pm 5\%$ accuracy limits for the entire range tested.

If you have any questions regarding this calibration report, please contact me directly, or Bertha A. Hernandez, Environmental Services Specialist.

Sincerely,



Robert J. MacDonald, P.E., CPP
President & Principal Engineer

enclosures

cc: Bertha A Hernandez, Environmental Services Specialist

**WASTEWATER FLOW METER
HYDRAULIC CALIBRATION**

PREPARED BY



FOR

**City of Anaheim
Canyon Power Plant
3071 E. Miraloma Ave.
Anaheim, CA 92806**

I.W. Permit No. 1-600296

January 10, 2019



EFFLUENT FLOW METER CALIBRATION REPORT

Company Name: City of Anaheim Permit No.: 1-600296

Discharge Address: 3071 E. Miraloma Ave. Anaheim, CA 92806

Mailing Address: 201 S. Anaheim Blvd. Suite 1101 Anaheim, CA 92805

Meter Location *[Use Meter Location Form (page 3) to identify location]*

☐ a ☐ b ☐ c ☐ d ☒ Other: (Attach sketch)

Effluent Meter Description

Open Channel

A. Flume:

☐ Parshall Flume

☐ Palmer-Bowlus Flume

☐ Trapezoidal

☐ Other, Specify: _____

B. Weir.

☐ V-notch

☐ Rectangular

☐ Trapezoidal

☐ Other, Specify: _____

C. Other

Description: _____

In-line

☒ Magnetic

☐ Propeller

☐ Ultrasonic

☐ Other, Specify: _____

Effluent Meter Description

Primary Element

Size: 4"

Manufacturer: Badger

Meter Series 2000

Secondary Element

Manufacturer: N/A

Recorder's 100% span = N/A GPM

Totalizer Units: = 1 Gallons per Count

Sampling Signal Contact Closure Frequency: 1 closure per N/A gallons discharged.

Current Facility Wastewater Discharge Rate to Sewer Determined by Calibration Engineer

Average 200 GPM

Peak 300 GPM



EFFLUENT FLOW METER CALIBRATION REPORT

5. Calibration Results

Type of Calibration: ☒ Hydraulic ☐ Instrument

Calibration System		Existing Meter				Error (%)	
Flow Rate GPM	Total Discharge Gallons	Primary Element's Head	Flow Rate, GPM		Total Discharge Gallons	Recorder	Totalizer
			Indicator	Recorder			
287.8	970	--	289.76	--	978	--	0.8%
250.3	813	--	251.11	--	816	--	0.4%
203.4	732	--	206.07	--	741	--	1.2%
153.3	501	--	152.73	--	499	--	-0.4%
110.8	388	--	109.82	--	393	--	1.3%

A copy of all data collected and of any calculations performed must be attached to this form.

6. Method of Calibration Results *(attach additional sheets if necessary)*

Hydraulic: (For in line flow meters describe calibration/simulator system)

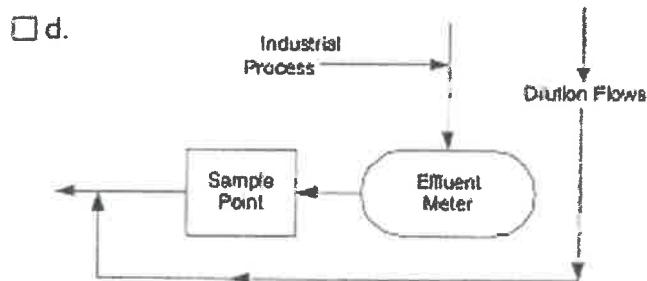
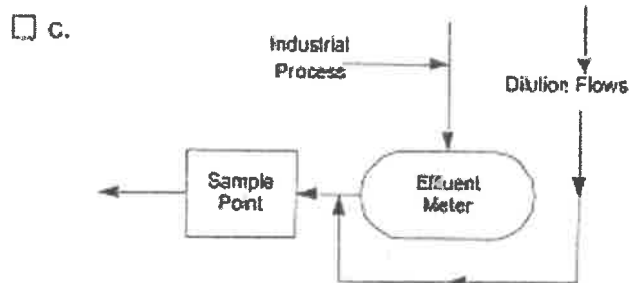
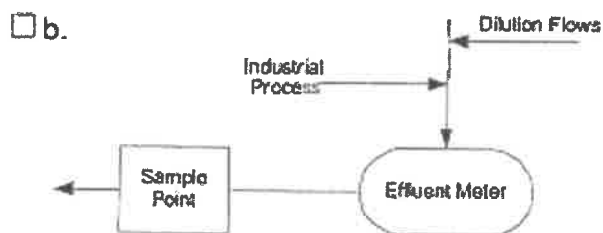
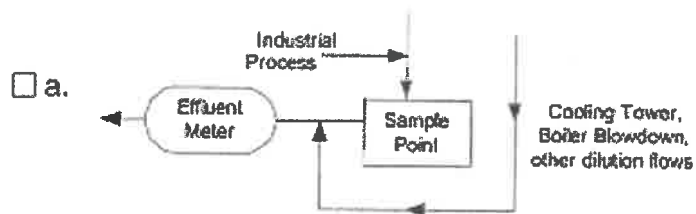
Various flow rates were achieved using 150' of 2.5" fire hose from a local hydrant to the test meter. A 2" Halliburton turbine was used to measure the water flow. At each rate tested, the meter totalizer was timed using an electronic stopwatch for a number of counts. The accumulated volume was then compared to the actual volume to determine the totalizer accuracy.

Instrument:

7. Corrective Measures *(describe condition of flow meter prior to calibration and state if any adjustments were made):*

No corrective measures were required.

EFFLUENT FLOW METER LOCATION FORM

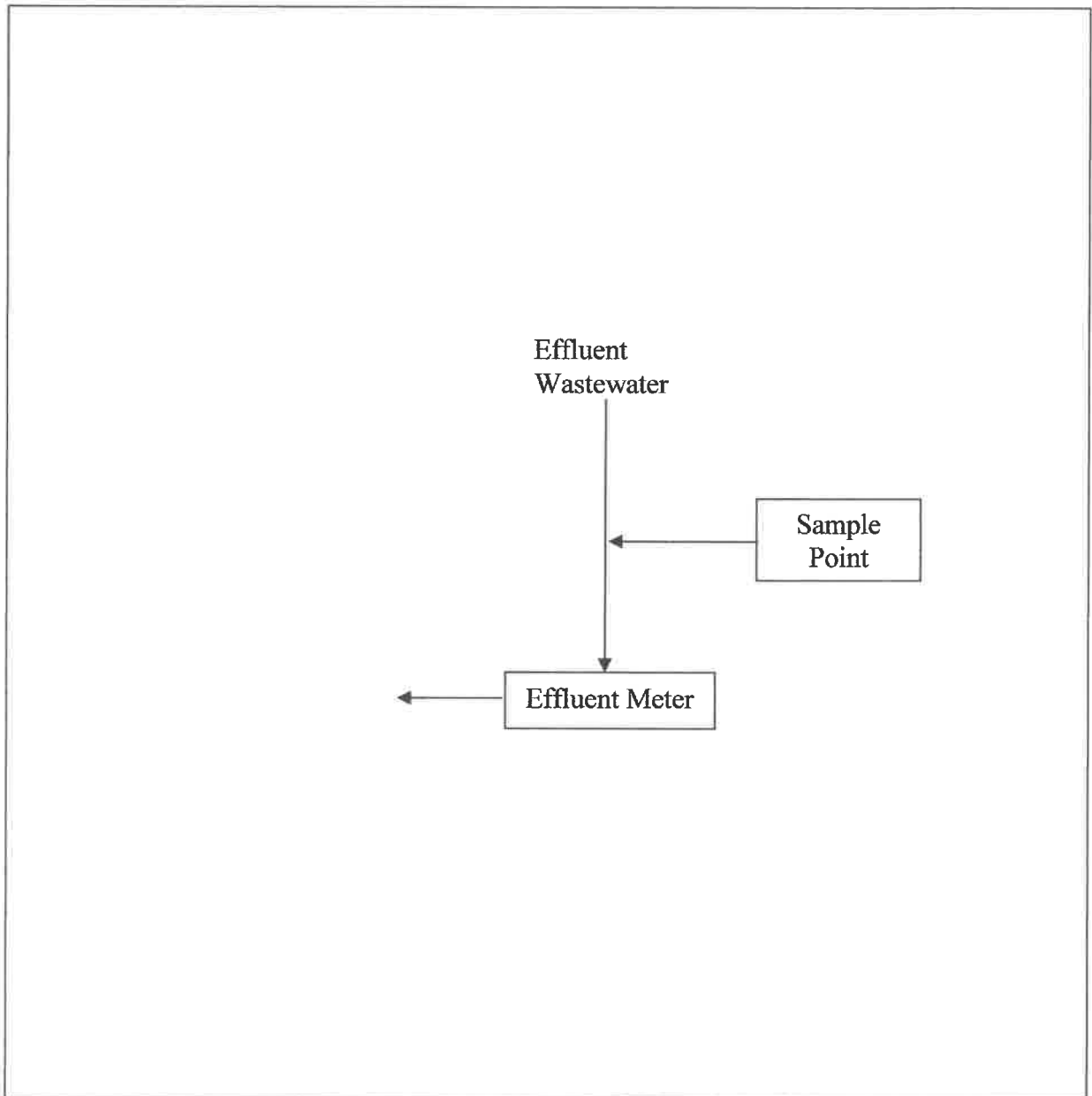


☒ Other

Please provide a schematic of the location of the effluent flow meter

Attachment:

Effluent Flow Meter Location





CERTIFICATION OF CALIBRATION CHECK

(Certification of Test Results by a California Registered Professional Engineer)

I hereby certify that I am knowledgeable in the field of wastewater flow measurement and that I have supervised the calibration of the flow monitoring system as described on the previous page, and also have reviewed and approved all details of the method of calibration. I consider the calibration method and procedures used to be technically sound, and assume professional responsibility for the validity and accuracy of the results reported.

(Signature)

Robert J. MacDonald, P.E.

(Full Name – Please Print or Type)



M29874 Expires 6/30/20

(California Professional
Engineering Certification No.)

Mechanical

(Engineering Discipline)

1/14/19

(Date)

CERTIFICATION OF TEST RESULTS BY AN ADMINISTRATIVE OFFICIAL OF THE COMPANY

City of Anaheim

(Company Name)

1-600296

(Permit No.)

I hereby certify that the flow monitoring system certified as properly calibrated above is so arranged and operated, so as to accurately measure and record the industrial wastewater flow to the sewer system.

(Signature)

RONALD HOFFARD

(Full Name – Please Print or Type)

GENERATION PLANT MANAGER

(Administrative Position in Company)

1/25/19

(Date)

Appendix:

Calculations Sheet
Field Calibration Data
Calibration Certificate

Wastewater Flowmeter Calibration

COMPANY: City of Anaheim - Canyon Power Plant DISCHARGE ADDRESS: 3071 E. Miraloma Ave. Anaheim, CA 92806 MAILING ADDRESS: 201 S. Anaheim Blvd. Ste 601, Anaheim, CA 92805 CONTACT: Bertha A Hernandez TELEPHONE: 714-765-7481 I.W.: 1-600296 Client-Job #: F14M828										DATE: 01/10/19 INSTRUMENTATION HYDRAULIC X CALIBRATION ENGINEER(S): PAZ / GOMEZ TEST EQUIPMENT: 2" Turbine Meter										ELEMENT: 4" Pipe INSTRUMENT: 4" Badger Meter M2000 EQUATION: n/a K FACTOR: n/a RANGE (dist.): FT RANGE (GPM): GPM TOTALIZER (start): 72712915 TOTALIZER (end): 72719388 REC. (100%) GPM: -- AVE. RATE: 200 PK Q: 300 SAMPLER: n/a TOTALIZER (X): 1									
COLUMN ID	A	B	C	D	E	F	G	H	I	(F - C) / C	(H - A) / A	(I - A) / A																	
CALCULATION																													
TEST SYSTEM																													
HEAD (ft.)	Q (gpm)	x	Time	=	V (gal)	TOTALIZER (x1000)			CHART		INDICATOR																		
						end	-	start	=	V (gal)	%	Q (gpm)	HEAD (ft.)	Q (gpm)	Totalizer	Chart	Indicator												
--	287.8	x	3.37	=	970	15150	-	14172	=	978	--	--	289.76			0.8%	--	0.7%											
--	250.3	x	3.25	=	813	16402	-	15586	=	816	--	--	251.11			0.4%	--	0.3%											
--	203.4	x	3.60	=	732	17591	-	16850	=	741	--	--	206.07			1.2%	--	1.3%											
--	153.3	x	3.27	=	501	18499	-	18000	=	499	--	--	152.73			-0.4%	--	-0.4%											
--	110.8		3.50	=	388	19321	-	18928	=	393	--	--	109.82			1.3%	--	-0.9%											

Recorder: MAX = <u> </u> GPM AVG = <u>200</u> PK = <u>300</u> Sampler: Contact Closure = <u>N/A</u> gallons/pulse		Totalizer: Finish: <u>12719388</u> Start: <u>72712915</u> Diff: <u>6473</u> MULT: <u>1</u> Total: <u>6473</u> gallons		Client: <u>City of Anaheim - Canyon Power Plant</u> Date: <u>1/10/19</u> IWH#: <u>1-600296</u> Element: <u>4" Pipe</u> Instrument: <u>4" Badger Meter M2000</u> Recorder: <u>--</u>	
---	--	---	--	---	--

Calibrated Flows and Data												
Turbine		Manometer - inches			Duration	Total	Meter		Recorder		Totalizer	
		cycles	gpm	+			-	Δ	w.c.	gpm	%	Reading
	287.8				3.37	970						978 0.8
	250.3				3.25	813						816 0.4
	203.4				3.60	732						741 1.2
	153.3				3.27	501						499 -0.4
	110.8				3.50	388						393 1.3

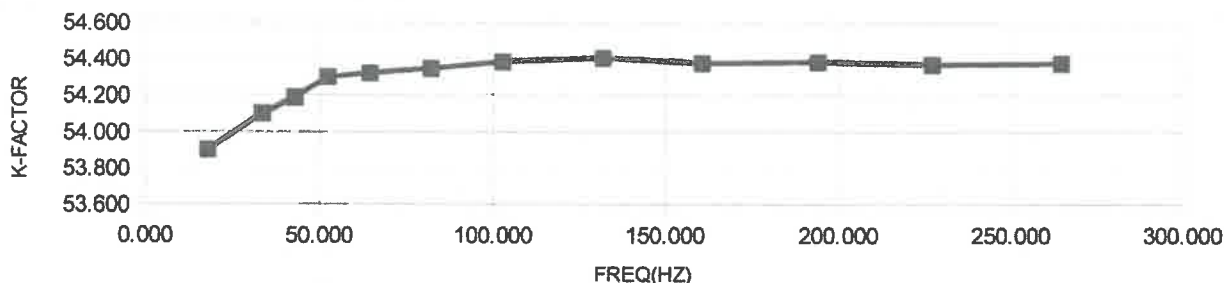
Calibration Type Instrumentation <input checked="" type="checkbox"/> Hydraulic	Notes: <div style="margin-bottom: 20px;"> $\begin{array}{r} ① \quad 15150 \\ - 14172 \\ \hline 978 \end{array}$ </div> <div style="margin-bottom: 20px;"> $\begin{array}{r} ② \quad 17591 \\ - 16850 \\ \hline 741 \end{array}$ </div> <div> $\begin{array}{r} ③ \quad 19321 \\ - 18928 \\ \hline 393 \end{array}$ </div>
---	--

Hydraulic Meter Used: <input type="checkbox"/> Turbine Meter, 1", Haliburton, Threaded <input type="checkbox"/> Turbine Meter, 1.5", XO Technologies, 150# Flange <input checked="" type="checkbox"/> Turbine Meter, 2", Haliburton, flanged <input type="checkbox"/> Turbine Meter, 4", XO Technologies, 150# Flange <input type="checkbox"/> Turbine Meter, 4", Haliburton, flanged Other: _____	K: <u>4.86</u>
---	----------------

CERTIFICATE OF CALIBRATION

CUSTOMER:	CONSERVTECH, COMMERCE, CA	CALIBRATION DATE:	07/20/17
VSR NUMBER:	9075	CALIBRATION DUE:	07/20/18
INST. MANUFACTURER:	HALLIBURTON	PROCEDURE:	NAVAIR17-20MG-01
INST. DESCRIPTION:	TURBINE METER	CALIBRATION FLUID:	H2O @ 70F
MODEL NUMBER:	458.99101 (2")	ARRIVAL CONDITIONS:	WITHIN MFG. SPEC.
SERIAL NUMBER:	2BF3677	RETURNED CONDITIONS:	WITHIN MFG. SPEC.
RATED UNCERTAINTY:	+/- .5% R.D.	AMBIENT CONDITIONS:	763mmHGA 48%RH 68°F
UNCERTAINTY GIVEN:	TOTAL measurement uncertainty +/- 151% RD K=2 CERTIFICATE FILE #: 420148.2017		
NOTES:	** CALIBRATED WITH DMC. SENSOR COIL **		

TEST POINT NUMBER	INDICATED UUT FREQ(HZ)	DM.STD. ACTUAL GPM	ACTUAL K-FACTOR PUL/GAL.
1	18.006	20.044	53.898
2	33.579	37.241	54.099
3	42.935	47.541	54.187
4	52.375	57.875	54.299
5	64.475	71.215	54.321
6	82.011	90.545	54.345
7	102.912	113.545	54.382
8	131.972	145.552	54.402
9	160.632	177.252	54.374
10	194.098	214.152	54.382
11	227.135	250.662	54.369
12	264.758	292.152	54.374



STANDARDS USED:

A710 (SERAFIN VOLUME PROVER 0-100GPM) +/- .022% BY VOLUME CMC +/- 2% RD FLOW TRACE# 1446135470,1453296155	DUE	01/16/18
A350 (PLATFORM SCALE & TANK: 10,000LBS/ 50-2800GPM) +/- .07LBS +/- BY MASS TRACE# 1446135470,1453296155	DUE	12/09/17
A14 (VOLUME PROVER 5-50GPM)+/- .02% BY VOLUME CMC +/- .151% RD FLOW TRACE# 1446135470,1453296155	DUE	12/07/17

All instruments used in the performance of the shown calibration have traceability to the National Institute of Standards and Technology (NIST). The uncertainty ratio between the calibration standards (DM.STD.) used and the unit under test (UUT) is a minimum of 4:1, unless otherwise noted. Calibration has been performed per the shown procedure number, in accordance with ISO 10012:2003, ISO 17025:2005, ANSI/NCSL-Z-540.3, and/or MIL-STD-45662A. Test methods: API2530-92 & ASME MFC-3M-1989.

Dick Munns Company • 11133 Winners Circle • Los Alamitos, CA 90720
Phone (714) 827-1215 • Fax (714) 827-0823

This Calibration Certificate shall not be reproduced except, in full, without approval by DICK MUNN COMPANY. The data shown applies only to the instrument being calibrated and under the stated conditions of calibration.

Date:

Approved By:

Calibration Technician:

7/20/17

[Signature]

[Signature]

Page 1 of 1

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 13
SOIL & WATER REPORTS-8

**OCSD Wastewater Quality Semi-Annual
Monitoring Reports**

TX Result Report

P 1

04/18/2019 16:15

Serial No. A7PY011022705

TC: 27558

Addressee	Start Time	Time	Prints	Result	Note
OCSD	04-18 16:08	00:06:47	008/008	OK	

Note

TMR:Timer TX, POL:Polling, ORG:Original Size Setting, FME:Frame Erase TX,
 DP6:Page Separation TX, MIX:Mixed Original TX, CALL:Manual TX, CSAC:CSAC,
 FWD:Forward, PC:PC-FAX, BND:Double-Sided Binding Direction, Sp:Special Original,
 FCODE:F-Code, RTX:Re-TX, RLV:Relay, MBX:Confidential, BUL:Bulletin, SIP:SIP Fax,
 IPADR:IP Address Fax, I-FAX:Internet Fax

Result

OK: Communication OK, S-OK: Stop Communication, PW-OFF: Power Switch OFF,
 TEL: RX from TEL, NG: Other Error, Cont: Continue, No Ans: No Answer,
 Refuse: Receipt Refused, Busy: Busy, M-Full:Memory Full, LOVR:Receiving length Over,
 POVR:Receiving page Over, FIL:File Error, DC:Decode Error, MDN:MDN Response Error,
 DSN:DSN Response Error, PRINT:Compulsory Memory Document Print,
 DEL:Compulsory Memory Document Delete, SEND:Compulsory Memory Document Send.



CITY OF ANAHEIM
PUBLIC UTILITIES DEPARTMENT
 Environmental Services
 Letter of Transmittal

To:	Ms. Mila Kleinbergs Orange County Sanitation District Resource Protection Division 10844 Ellis Avenue Fountain Valley, CA 92708-7018	Date:	04/28/2019
		Project	Canyon Power Plant 3071 E. Miraloma Ave. Anaheim, CA 92806
		Subject:	Semi-Annual Self-Monitoring

We are sending you:

Copy of Original	Description
1	Completed Semi-Annual Form OCSD Self-Monitoring Form for City of Anaheim Canyon Power Plant (Permit No. 1-600296).

These are transmitted:

<input type="checkbox"/> 1 As requested	<input type="checkbox"/> For your action	<input type="checkbox"/> For your files
<input type="checkbox"/> For approval	<input type="checkbox"/> For your review	<input type="checkbox"/> For your information

Via: ☐ US Mail ☒ FAX # 8 of pgs. ☐ Hand Delivery
 (714) 593-7799

Remarks:

Please contact me at (714) 765-7481 or bhernandez@anaheim.net if you have any questions regarding this submittal.

By: 
 Bertha A Hernandez, Environmental Services Specialist



CITY OF ANAHEIM
PUBLIC UTILITIES DEPARTMENT
Environmental Services
Letter of Transmittal

To:	Ms. Mila Kleinbergs Orange County Sanitation District Resource Protection Division 10844 Ellis Avenue Fountain Valley, CA 92708-7018	Date:	04/28/2019
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(714) 593-7799

Remarks:

Please contact me at (714) 765-7481 or bhernandez@anaheim.net if you have any questions regarding this submittal.

By: 
Bertha A Hernandez, Environmental Services Specialist



ORANGE COUNTY SANITATION DISTRICT SELF-MONITORING FORM

March 14, 2019

Ronald Hoffard, GENERATION PLANT MANAGER
City of Anaheim, Canyon Power Plant
3071 E Miraloma Ave.
Anaheim, CA 92806

Subject: **REMINDER TO CONDUCT SELF-MONITORING**
Permit No. 1-600296 (previously listed as)

Please be reminded that Self-Monitoring must be conducted between **April 01, 2019 -- April 16, 2019** in accordance with your company's permit requirements. Self-Monitoring must be conducted during a production day in accordance with the guidelines detailed in your company's permit.

It is your responsibility to comply with the requirements set forth in your company's permit. Failure to comply with all the directives, conditions, and requirements of the permit may result in enforcement action against your company.

If your company's permit shows a self-monitoring requirement for total toxic organics (TTOs) and your company has received a waiver from this self-monitoring, you are now required to submit a signed TTOs SMR form to us to comply with the TTO waiver requirements of the U.S. Environmental Protection Agency. Please indicate in the "Sample Comments" that you have received a TTOs self-monitoring waiver from us.

For permittees that have monthly as well as quarterly and/or semi-annual self-monitoring requirements, the forms may list more than the SMR constituents required for the monthly self-monitoring. We ask that you adhere to your permit's self-monitoring requirements and sample only for the constituent(s) required on a monthly basis, except when the quarterly and semi-annual self-monitoring are also required in the same month, in which case all constituents listed on the form must be analyzed for as specified in your permit.

Finally, for those who are required to submit meter readings, a list of the meter readings submitted within the last year is attached to the SMR form for your reference and comparison to current readings.

Thank you for your patience and cooperation. If you have any questions, please contact Mila Kleinbergs at 714-593-7408.

Mila Kleinbergs
Senior Engineer



**ORANGE COUNTY SANITATION DISTRICT
SELF-MONITORING FORM**

SMR No.: S-121862

SMR Type: Standard

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously)

Sampling Dates: 04/01/2019 to 04/16/2019

Submit By Date: 04/30/2019

Sample Start Date: 04/08/2019

Sample End Date: 04/09/2019

Sample Start Time: 0930 AM

Sample End Time: 1000 AM

Sampling Point Location: Sampling Structure located in the center of the site

Contact Person: RONALD HOFFARD

Contact Phone: (714) 765-4536

Contact Email: RHOFFARD@ANAHEIM.NET

☐ No Discharge

Water Meter Readings: (If this is a batch discharge, enter volume only)

Location	Meter Type	Meter ID	Stop Reading	Start Reading	Volume	Units	Digits	Int
Center of site adjacent to the final clarifier/vault	Effluent Flow Meter	EM-1-600296	<u>76362506</u>	<u>76322767</u>	<u>39739</u>	G	9	

Composite

Sample Results: (If constituent is not detected or is less than detection limit, enter as reported in the lab results.)

Constituent	Result	Units	EPA Method
BOD T	<u>ND</u>	mg/L	<u>SM 5210B</u>
TSS	<u>ND</u>	mg/L	<u>SM 2540D</u>

Sample Comments: _____

To Submit Data - Fax: (714) 593-7799 or
Mail: Orange County Sanitation District, Resource
Protection Division, 10844 Ellis Avenue, Fountain Valley,
CA, 92708-7018



Questions: Contact Melissa Soriano at 714-593-7448 PB



**ORANGE COUNTY SANITATION DISTRICT
SELF-MONITORING FORM**

SMR No.: S-121862

SMR Type: Standard

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously)

**This form must be completely filled out and Laboratory Analysis Report
and Chain of Custody must be attached.**

Please check if composite sample was obtained using an automatic sampling device: () Yes () No

In accordance with 40 CFR 403.12, the results presented herein must be verified and signed under penalty of perjury by: (i) a responsible corporate officer; (ii) general partner or proprietor; or (iii) a representative who has responsibility for the overall operation of the permitted facility, who has been authorized by the corporate officer, general partner or proprietor to sign such reports, and such authorization has been made in writing and submitted to the District.

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons who manage the system, or those persons directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations. [40 C.F.R. § 403.6(a)(2)(ii) (2005)]

R Hoffard
Signature (Ronald Hoffard)

GENERATION PLANT MANAGER

Title (GENERATION PLANT MANAGER)

4/12/19
Date

RONALD HOFFARD
Print Name

To Submit Data - Fax: (714) 593-7799 or

Mail: Orange County Sanitation District, Resource

Protection Division, 10844 Ellis Avenue, Fountain Valley,
CA, 92708-7018

Questions: Contact Melissa Soriano at 714-593-7448 PB



**ORANGE COUNTY SANITATION DISTRICT
SELF-MONITORING FORM**

SMR No.: S-121862

SMR Type: Standard

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously)

Sample Location: Compliance

<u>Meter Type</u>	<u>Equipment</u> <u>Name</u>	<u>Event ID</u>	<u>Start - End Date</u>	<u>End</u>	<u>Reading</u>	<u>Start</u>	<u>Vol</u>	
EFFLUENT	EM-1-600296	121861	10/1/2018 - 10/2/2018	68740935 Gallon	68688798 Gallon	49556	GPD	
EFFLUENT	EM-1-600296	121860	4/2/2018 - 4/3/2018	61898932 Gallon	61824052 Gallon	74880	GPD	

To Submit Data - Fax: (714) 593-7799 or

Mail: Orange County Sanitation District, Resource

Protection Division, 10844 Ellis Avenue, Fountain Valley,
CA, 92708-7018

Questions: Contact Melissa Soriano at 714-593-7448 PB



REPORT

3337 MICHELSON DRIVE, SUITE CN 750
IRVINE, CA 92612
(714) 730-6239 • FAX (714) 730-6462
www.truesdail.com

Client: City of Anaheim - Canyon Water Power Plant
3071 E Miraloma Ave
Anaheim, CA 92806

Work Order No.: 19D0146
Printed: 04/18/2019

Attention: Bertha Hernandez

Project Name: Canyon Power Plant Semi-Annually Wastewater

Project Number: Canyon Power Plant

P.O. Number: MA-106-491110 (exp 8/31/18)

CASE NARRATIVE

Date & Time Installed: 04/08/2019; 09:30 AM
Date & Time Removed: 04/09/2019; 10:00 AM

Flow Start Number: 76322767 GAL
Flow Stop Number: 76362506 GAL
Total Flow, GPD: 39739

SAMPLE RECEIPT SUMMARY

Sample ID	Laboratory ID	Matrix	Type	Date Sampled	Date Received
1-600296 Composite	19D0146-01	Wastewater	Composite	04/09/2019 10:00	04/09/2019 15:05

DEFINITIONS

Symbol	Definition
C	GGA recovery was less than the method acceptance limit.
DF	Dilution Factor
MDL	Method Detection Limit
ND	Not Detected
RL	Reporting Limit

Respectfully yours,

Shelly Brady
Customer Service Manager



TRUESDAIL LABORATORIES, INC.

Client: City of Anaheim - Canyon Water Powe

Project Name:

Canyon Power Plant Semi-Annually Wastewater

Project Number:

Canyon Power Plant

Printed: 04/18/2019

1-600296 Composite
19D0146-01 (Wastewater)

Analyte	Result	RL	Units	DF	Batch	Analyzed	Analyst	Method	Notes
---------	--------	----	-------	----	-------	----------	---------	--------	-------

ALS Truesdail

Wet Chemistry

Total Dissolved Solids	86.0	12.5	mg/L	1	1904389	04/17/2019 17:33	ADD	SM 2540 C	
Total Suspended Solids	ND	2.50	mg/L	1	1904278	04/11/2019 12:00	KKL	SM 2540 D	

General Chemistry

Biochemical Oxygen Demand	ND	2.00	mg/L	1	1904306	04/15/2019 16:45	SMC	SM 5210B - 5 Day	C
---------------------------	----	------	------	---	---------	------------------	-----	------------------	---

This report applies to the sample(s), or product(s), investigated and is not necessarily indicative of the quality or condition of apparently identical or similar products. As a mutual protection to clients, the public, and these laboratories, this report is submitted and accepted for the exclusive use of the client to whom it is addressed. This report shall not be reproduced without the written consent of Truesdail Laboratories, Inc., and must be reproduced in its entirety.



3337 Michelson Drive, Suite CN750, Irvine, CA 92612
(714) 730-6239 - FAX (714) 730-6462

TURNAROUND TIME: Normal TAT 
 DATE: 4/8 - 4/9/19 PAGE: 1 OF 1

19D0146

METHODS

[illegible]

TX Result Report

P 1

10/17/2019 15:47

Serial No. A7PY011022705

TC: 38339

Addressee	Start Time	Time	Prints	Result	Note
OCSD	10-17 15:40	00:06:48	008/008	OK	

Note TMR:Timer TX, POL:Polling, ORG:Original Size Setting, FME:Frame Erase TX, DPS:Page Separation TX, MIX:Mixed Original TX, CALL:Manual TX, CSAC:CSAC, FWD:Forward, PC:PC-FAX, BND:Double-Sided Binding Direction, Sp:Special Original, FCODE:F-code, RTX:Re-TX, RLY:Relay, MBX:Confidential, BUL:Bulletin, SIP:SIP Fax, IPADR:IP Address Fax, I-FAX:Internet Fax

Result OK: Communication OK, S-OK: Stop Communication, PW-OFF: Power Switch OFF, TEL: RX from TEL, NS: Other Error, Cont: Continue, No Ans: No Answer, Refuse: Receipt Refused, Busy: Busy, M-Full:Memory Full, LOVR:Receiving Length Over, POVR:Receiving page Over, Fil:File Error, DC:Decode Error, MDN:MDN Response Error, DSN:DSN Response Error, PRINT:Compulsory Memory Document Print, DEL:Compulsory Memory Document Delete, SEND:Compulsory Memory Document Send.



CITY OF ANAHEIM
PUBLIC UTILITIES DEPARTMENT
 Environmental Services
 Letter of Transmittal

To:	Ms. Mila Kleinbergs Orange County Sanitation District Resource Protection Division 10844 Ellis Avenue Fountain Valley, CA 92708-7018	Date:	10/17/2019
		Project	Canyon Power Plant 3071 E. Miraloma Ave. Anaheim, CA 92806
		Subject:	Semi-Annual Self-Monitoring

We are sending you:

Copy of Original	Description
1	Completed Semi-Annual Form OCSD Self-Monitoring Form for City of Anaheim Canyon Power Plant (Permit No. 1-600296).

These are transmitted:

<input checked="" type="checkbox"/> 1 As requested	<input type="checkbox"/> For your action	<input type="checkbox"/> For your files
<input type="checkbox"/> For approval	<input type="checkbox"/> For your review	<input type="checkbox"/> For your information

Via: ☐ US Mail ☒ FAX # 8 of pgs. ☐ Hand Delivery
 (714) 693-7799

Remarks:

Please contact me at (714) 765-7481 or bhernandez@anaheim.net if you have any questions regarding this submittal.

By: Bertha A Hernandez, Environmental Services Specialist



CITY OF ANAHEIM
PUBLIC UTILITIES DEPARTMENT
Environmental Services
Letter of Transmittal

To:	Ms. Mila Kleinbergs Orange County Sanitation District Resource Protection Division 10844 Ellis Avenue Fountain Valley, CA 92708-7018	Date:	10/17/2019
		Project:	Canyon Power Plant 3071 E. Miraloma Ave. Anaheim, CA 92806
		Subject:	Semi-Annual Self-Monitoring

We are sending you:

Copy of Original	Description
1	Completed Semi-Annual Form OCSD Self-Monitoring Form for City of Anaheim Canyon Power Plant (Permit No. 1-600296).

These are transmitted:

<input checked="checked" type="checkbox"/> 1	As requested	<input type="checkbox"/>	For your action	<input type="checkbox"/>	For your files
<input type="checkbox"/>	For approval	<input type="checkbox"/>	For your review	<input type="checkbox"/>	For your information

Via: ☐ US Mail ☒ FAX # 8 of pgs. ☐ Hand Delivery
(714) 593-7799

Remarks:

Please contact me at (714) 765-7481 or bhernandez@anaheim.net if you have any questions regarding this submittal. *BAD*

By: Bertha A Hernandez, Environmental Services Specialist



ORANGE COUNTY SANITATION DISTRICT SELF-MONITORING FORM

September 15, 2019

Ronald Hoffard, GENERATION PLANT MANAGER
City of Anaheim, Canyon Power Plant
3071 E Miraloma Ave.
Anaheim, CA 92806

Subject: **REMINDER TO CONDUCT SELF-MONITORING**
Permit No. 1-600296 (previously listed as 1-600296)

Please be reminded that Self-Monitoring must be conducted between **October 01, 2019 -- October 16, 2019** in accordance with your company's permit requirements. Self-Monitoring must be conducted during a production day in accordance with the guidelines detailed in your company's permit.

It is your responsibility to comply with the requirements set forth in your company's permit. Failure to comply with all the directives, conditions, and requirements of the permit may result in enforcement action against your company.

If your company's permit shows a self-monitoring requirement for total toxic organics (TTOs) and your company has received a waiver from this self-monitoring, you are now required to submit a signed TTOs SMR form to us to comply with the TTO waiver requirements of the U.S. Environmental Protection Agency. Please indicate in the "Sample Comments" that you have received a TTOs self-monitoring waiver from us.

For permittees that have monthly as well as quarterly and/or semi-annual self-monitoring requirements, the forms may list more than the SMR constituents required for the monthly self-monitoring. We ask that you adhere to your permit's self-monitoring requirements and sample only for the constituent(s) required on a monthly basis, except when the quarterly and semi-annual self-monitoring are also required in the same month, in which case all constituents listed on the form must be analyzed for as specified in your permit.

Finally, for those who are required to submit meter readings, a list of the meter readings submitted within the last year is attached to the SMR form for your reference and comparison to current readings.

Thank you for your patience and cooperation. If you have any questions, please contact Mila Kleinbergs at 714-593-7408.

Mila Kleinbergs
Senior Engineer



ORANGE COUNTY SANITATION DISTRICT SELF-MONITORING FORM

SMR No.: S-145451

SMR Type: Standard

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously 1-600296)

Sampling Dates: 10/01/2019 to 10/16/2019Submit By Date: 10/31/2019Sample Start Date: 10/07/2019Sample End Date: 10/08/2019Sample Start Time: 12:30 pmSample End Time: 12:30 pm

Sampling Point Location: Sampling Structure located in the center of the site

Contact Person: RONALD HOFFARDContact Phone: (714) 765-4536Contact Email: RHOFFARD@ANAHEIM.NET☐ No Discharge

Water Meter Readings: (If this is a batch discharge, enter volume only)

Location	Meter Type	Meter ID	Stop Reading	Start Reading	Volume	Units	Digits	Int
Center of site adjacent to the final clarifier/vault	Effluent Flow Meter	EM-1-600296	<u>82189068</u>	<u>82165784</u>	<u>23284</u>	G	9	

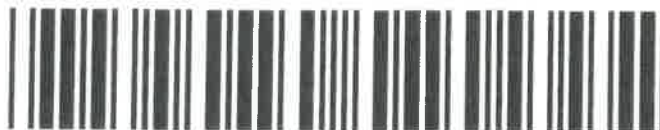
Composite

Sample Results: (If constituent is not detected or is less than detection limit, enter as reported in the lab results.)

Constituent	Result	Units	EPA Method
BOD T	<u>6.76</u>	mg/L	<u>SM-5210B</u>
TSS	<u>ND</u>	mg/L	<u>SM-2540D</u>

Sample Comments: _____

To Submit Data - Fax: (714) 593-7799 or
 Mail: Orange County Sanitation District, Resource
 Protection Division, 10844 Ellis Avenue, Fountain Valley,
 CA, 92708-7018



Questions: Contact Isabel Melendez at 714-593-7313

Ronald Hoffard, please initial each page and submit all pages

**ORANGE COUNTY SANITATION DISTRICT
SELF-MONITORING FORM****SMR No.: S-145451****SMR Type: Standard**

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously 1-600296)

**This form must be completely filled out and Laboratory Analysis Report
and Chain of Custody must be attached.**Please check if composite sample was obtained using an automatic sampling device: ☒ Yes () No

In accordance with 40 CFR 403.12, the results presented herein must be verified and signed under penalty of perjury by: (i) a responsible corporate officer; (ii) general partner or proprietor; or (iii) a representative who has responsibility for the overall operation of the permitted facility, who has been authorized by the corporate officer, general partner or proprietor to sign such reports, and such authorization has been made in writing and submitted to the District.

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons who manage the system, or those persons directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations. [40 C.F.R. § 403.6(a)(2)(ii) (2005)]

Signature (Ronald Hoffard)

Title (GENERATION PLANT MANAGER)

Date

RONALD HOFFARD

Print Name

To Submit Data - Fax: (714) 593-7799 or**Mail:** Orange County Sanitation District, Resource
Protection Division, 10844 Ellis Avenue, Fountain Valley,
CA, 92708-7018**Questions:** Contact Isabel Melendez at 714-593-7313

Ronald Hoffard, please initial each page and submit all pages



**ORANGE COUNTY SANITATION DISTRICT
SELF-MONITORING FORM**

SMR No.: S-145451

SMR Type: Standard

City of Anaheim, Canyon Power Plant

General Pretreatment Regulations For Existing And New Sources Of Pollution

Permit No. 1-600296 (previously 1-600296)

Sample Location: Compliance

<u>Meter Type</u>	<u>Equipment Name</u>	<u>Event ID</u>	<u>Start - End Date</u>	<u>End</u>	<u>Reading</u>	<u>Start</u>	<u>Vol</u>	
EFFLUENT	EM-1-600296	145450	4/8/2019 - 4/9/2019	76362506 Gallon	76322767 Gallon	38928	GPD	
EFFLUENT	EM-1-600296	121861	10/1/2018 - 10/2/2018	68740935 Gallon	68688798 Gallon	49556	GPD	

To Submit Data - Fax: (714) 593-7799 or

Mail: Orange County Sanitation District, Resource
Protection Division, 10844 Ellis Avenue, Fountain Valley,
CA, 92708-7018

Questions: Contact Isabel Melendez at 714-593-7313

Ronald Hoffard, please initial each page and submit all pages



ALS - Truesdail Laboratories
3337 Michelson Drive, Suite CN750
Irvine, CA 92612
T +1 714 730 6239

Report

Client: City of Anaheim - Canyon Water Power Plant
3071 E Miraloma Ave
Anaheim, CA 92806

Work Order No.: 19J0112

Printed: 10/17/2019

Attention: Bertha Hernandez

Project Name: Canyon Power Plant Semi-Annually Wastewater

Project Number: Canyon Power Plant

P.O. Number: MA-106-491110 (exp 8/31/18)

CASE NARRATIVE

Date & Time Installed: 10/7/19; 12:30 PM

Date & Time Removed: 10/8/19; 12:30 PM

Flow Start Number: 82165784 GAL

Flow Stop Number: 82189068 GAL

Total Flow, GPD: 23284

SAMPLE RECEIPT SUMMARY

<u>Sample ID</u>	<u>Laboratory ID</u>	<u>Matrix</u>	<u>Type</u>	<u>Date Sampled</u>	<u>Date Received</u>
1-600296 Composite	19J0112-01	Wastewater	Composite	10/08/2019 12:30	10/08/2019 15:44

DEFINITIONS

<u>Symbol</u>	<u>Definition</u>
C	Blank unseeded oxygen depletion exceeded the method acceptance limit of 0.2 mg/L.
DF	Dilution Factor
MDL	Method Detection Limit
ND	Not Detected
RL	Reporting Limit

Respectfully yours,

Joseph Bryan Harding For Shelly Brady
Customer Service Manager

This report applies to the sample(s), or product(s), investigated and is not necessarily indicative of the quality or condition of apparently identical or similar products. As a mutual protection to clients, the public, and these laboratories, this report is submitted and accepted for the exclusive use of the client to whom it is addressed. This report shall not be reproduced without the written consent of ALS-Truesdail Laboratories, Inc., and must be reproduced in its entirety



TRUESDAIL
LABORATORIES, INC.

Client: City of Anaheim - Canyon Water Power PI

Project Name: Canyon Power Plant Semi-Annually Wastewater

Project Number: Canyon Power Plant

Printed: 10/17/2019

1-600296 Composite

19J0112-01 (Wastewater)

Analyte	Result	RL	Units	DF	Batch	Analyzed	Analyst	Method	Notes
---------	--------	----	-------	----	-------	----------	---------	--------	-------

ALS Truesdail

Wet Chemistry

Total Dissolved Solids	128	25.0	mg/L	1	1910324	10/16/2019 16:13	VHD	SM 2540 C	
Total Suspended Solids	ND	2.63	mg/L	1	1910323	10/16/2019 00:00	SMC	SM 2540 D	

General Chemistry

Biochemical Oxygen Demand	6.76	2.00	mg/L	1	1910216	10/14/2019 12:45	SMC	SM 5210B - 5 Day	C
---------------------------	------	------	------	---	---------	------------------	-----	------------------	---

This report applies to the sample(s), or product(s), investigated and is not necessarily indicative of the quality or condition of apparently identical or similar products. As a mutual protection to clients, the public, and these laboratories, this report is submitted and accepted for the exclusive use of the client to whom it is addressed. This report shall not be reproduced without the written consent of ALS-Truesdail Laboratories, Inc., and must be reproduced in its entirety.



3337 Michelson Drive, Suite CN750, Irvine, CA 92612
(714) 730-6239 - FAX (714) 730-6462

X TURNAROUND TIME Normal TA: 10/7-10/8/19 PAGE: 1

X **TURNAROUND TIME** **Normal** **TA** **1** **C**

195012

METHODS

[illegible]

OC Sanitation District
No Violations or Corrective Actions
to report for CY 2019

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 14

VIS-4

VIS-4: Surface Treatment of Project Structures and Buildings

Condition of Certification VIS-4 requires a status report of the surface treatment maintenance for the structures and buildings in the Annual Compliance Report. The report shall specify the following:

1. The condition of surfaces of all structures and buildings at the end of the reporting year 2018:

- a. Butler Building (Administrative and Warehouse)
- b. Main Electrical Enclosure (MEE)
- c. Balance of Plan (BOPEE)
- d. Substation Building
- e. Chiller
- f. RO Skid (open wall with roof sheet metal covering)
 - i. The exterior building material is fabricated sheet metal. The colors and finishes do not create excessive glare and consistent with local policies and ordinances. All structure and buildings visual inspection showed no trouble items and all are in good working order.
- g. Gas Turbines (4 identical units)

2. Maintenance activities that occurred in CY 2019:

- a. May Planned Outage
 - i. Semi-annual maintenance performed
- b. December Planned Outage
 - i. Semi-annual maintenance performed

3. Schedule maintenance activities for CY 2020:

- a. May 2019 Planned Outage
 - i. Semi-annual maintenance
- b. December 2019 Planned Outage
 - i. Semi-annual maintenance

Status report regarding condition of Structures and Buildings

The photographs below shows the surface treatment of project structures and buildings. All buildings comply with condition VIS-4.



Warehouse Building (1/28/20)



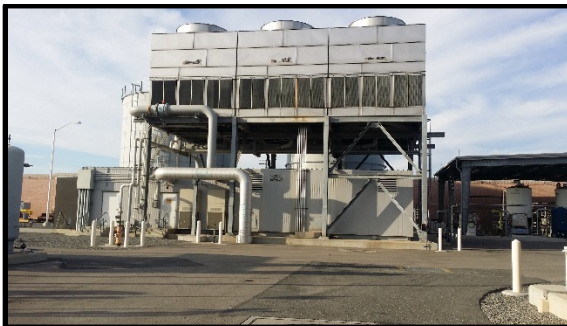
Administrative Building (1/28/20)



Main Electrical Enclosure Building (1/28/20)



Substation Building (1/28/20)



Chiller Building (1/28/20)



RO Skid Structure (1/28/20)



Balance of Plant Building (1/28/20)



LM 6000 Turbines (1/28/20)

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 15
LANDSCAPE SCREENING

VIS-5: Landscape Screening

Condition of Certification VIS-5 requires a status report in the Annual Compliance Report regarding landscape maintenance activities. At the Canyon Power Plant the landscape maintenance activities were performed according to the contract and consistent with policies and requirements of the City of Anaheim plan and zoning ordinance.

The contracted company performed the following landscape maintenance activities:

Contracted Landscape Services – Landscape West Mgmt. Service, Inc. (Period: Jan 1, through December 31, 2019)

Activity Type	Frequency
<u>Weed Control</u> Landscape areas Hardscape areas Gravel areas	2x/wk. 1x/Mo
<u>Fertilization</u> Shrubs Ground cover Trees	As needed
<u>Pest Control</u> Rodents	As needed
<u>Irrigation Maintenance</u> Inspect all Sprinklers/Systems	2x/wk.
<u>Trees</u> Canopy Trees	As needed
<u>Maintenance/Clean-Up</u> Ground Cover and Shrubs Trash & Litter at Landscape area Trash & Litter at enclosed gravel areas Monthly Inspection	2x/wk.

The photographs below taken by staff on 1/28/20 of the landscape maintenance demonstrating compliance pursuant VIS-5 condition:

Landscaping - Exterior Plants



Miraloma Avenue, south wall



Miraloma Avenue, south wall



Miraloma Avenue, south wall



East-wall ivy

Landscaping - Interior Plant



Administration Building



Administration and Warehouse Building



Warehouse Building

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 16

AQ-9
NH3 SLIP TESTING

TEST REPORT FOR AMMONIA SLIP TEST AT CANYON POWER PLANT UNIT 1 FACILITY ID: 153992, DEVICE ID: D1

Prepared For:

Canyon Power Plant
3071 E. Mira Loma Avenue
Anaheim, California 92806

For Submittal To:

South Coast Air Quality Management District
21865 Copley Drive
Diamond Bar, California 91765-4178

Prepared By:

Montrose Air Quality Services, LLC
1631 E. St. Andrew Pl.
Santa Ana, California 92705
(714) 282-8240

Sean Donovan

Test Date: **July 23, 2019**
Production Date: **August 22, 2019**
Report Number: **W002AS-543377-RT-221**



CONFIDENTIALITY STATEMENT

Except as otherwise required by law or regulation, this information contained in this communication is intended exclusively for the individual or entity to which it is addressed. This communication may contain information that is proprietary, privileged or confidential or otherwise legally exempt from disclosure. If you are not the named addressee, you are not authorized to read, print, retain, copy, or disseminate this message or any part of it.

REVIEW AND CERTIFICATION

All work, calculations, and other activities and tasks performed and presented in this document were carried out by me or under my direction and supervision. I hereby certify that, to the best of my knowledge, Montrose operated in conformance with the requirements of the Montrose Quality Management System and ASTM D7036-04 during this test project.

Signature: Sean Donovan Date: 8/21/2019
Name: Sean Donovan Title: Client Project Manager

I have reviewed, technically and editorially, details, calculations, results, conclusions, and other appropriate written materials contained herein. I hereby certify that, to the best of my knowledge, the presented material is authentic, accurate, and conforms to the requirements of the Montrose Quality Management System and ASTM D7036-04.

Signature: Mike Chowsanitphon Date: 8/21/2019
Name: Mike Chowsanitphon Title: Reporting Manager

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1.0 INTRODUCTION AND SUMMARY

Montrose Air Quality Services, LLC (MAQS), was contracted the Canyon Power Plant to perform an ammonia slip test at Unit 1 as required by the facility Permit (Facility ID 153992) Condition Number D29.2. This report documents the results of the ammonia slip tests performed on July 23, 2019. The test was performed by Sean Donovan, Henry Lee, and Robert Howard. Sean Donovan was the on-site qualified individual for MAQS. Bertha Hernandez coordinated the test for Canyon Power Plant.

The test consisted of duplicate ammonia tests performed at 50 MW. The test program followed the procedures described in the initial compliance test protocol (MAQS document R038842). The results of the test are summarized in Table 1-1. The table shows that the ammonia slip from this unit was less than the permitted limit of 5 ppm corrected to 15% O₂.

**TABLE 1-1
AMMONIA SLIP TEST RESULTS SUMMARY**

Parameter	Units	Result ⁽¹⁾	Limit
NH ₃	ppm	1.9	--
NH ₃	ppmc	1.7	5

(1) Maximum of duplicate runs, as required by SCAQMD Method 207.1

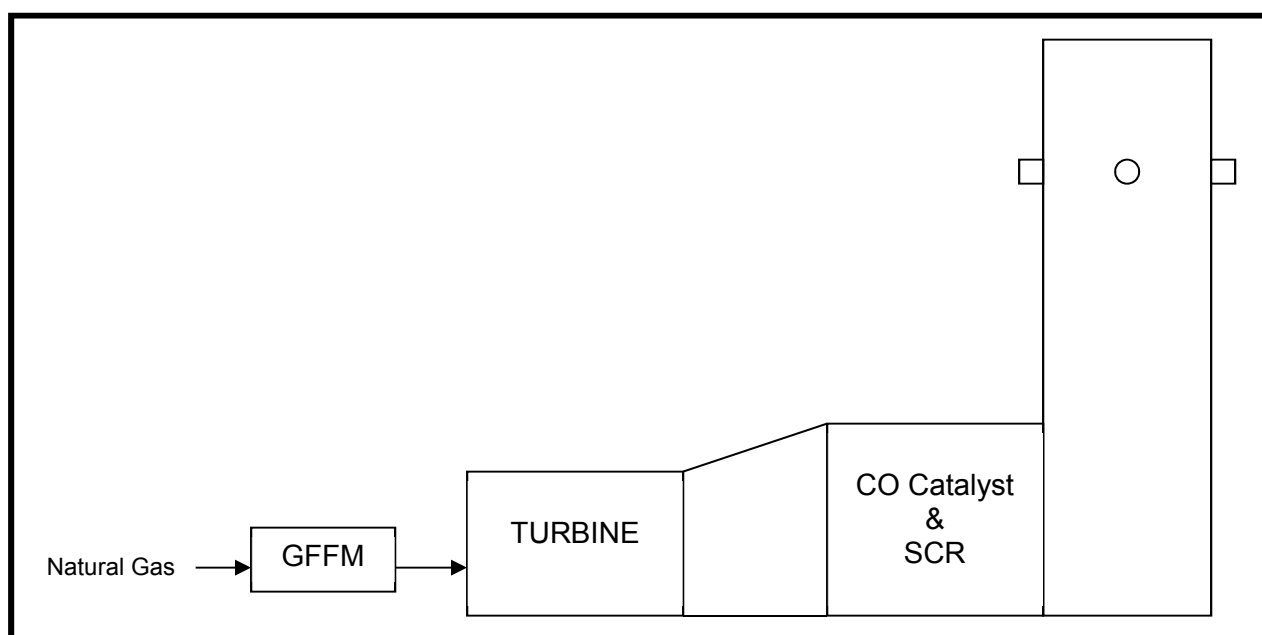
Section 2 of this document provides a brief description of the unit, test conditions, sample location, and CEMS. Details of the test procedures are provided in Section 3. Section 4 provides the results of each individual test. All raw data, calculations, quality assurance data, unit operating conditions, and CEMS data are provided in the appendices.

2.0 UNIT AND CEMS DESCRIPTION

2.1 UNIT DESCRIPTION

The City of Anaheim Canyon Power Plant is located at 3071 E. Mira Loma Avenue, Anaheim, California 92806. The facility consists of four identical generating units. Each unit consists of a natural gas fired, GE Model LM6000PC Sprint simple cycle, gas turbine. The units are natural gas fired with a rated heat input of 479 MMBtu per hour at 46 degrees Fahrenheit, with water injection. The units are equipped with a CO catalyst and Selective Catalytic Reduction (SCR) system for NO_x control. Figure 2-1 presents a block diagram of the unit.

**FIGURE 2-1
UNIT BLOCK DIAGRAM**



Stack Inside Diameter:	11 feet, 8 inches
Distance from Upstream Disturbance:	23 feet, 4 inches (2.0 Diameters)
Distance from Stack Exit:	16 feet, 6 inches (1.4 Diameters)

2.2 TEST CONDITIONS

The tests were performed with the unit operating at an average load of 50 MW. Tests were performed while the unit was firing natural gas and operating under normal conditions. Unit operation was established by the Canyon Power Plant operators.

2.3 SAMPLE LOCATION

The measurements were made from sample ports located on the exhaust stack. There are four sample ports equally spaced at this location. The stack inside diameter at the sample plane is 11 feet, 8 inches. The sample ports are located 23 feet, 4 inches (2.0 diameters) downstream of the nearest flow disturbance and 16 feet, 6 inches (1.4 diameters) from the stack exit.

3.0 TEST DESCRIPTION

Flue gas samples were collected non-isokinetically using a SCAQMD Method 207.1 sample train. The samples were collected using a 12-point traverse at the exhaust stack location. Each test was performed over a 60 minute interval. The sample gas was drawn through a glass probe, Teflon sample line, two impingers each containing 100 ml of 0.1N H₂SO₄, an empty impinger, an impinger containing silica gel, and a dry gas meter. The optional nozzle and filter were not used since the source is natural gas fired. The contents of the sample line and the first three impingers were recovered and analyzed by SCAQMD Method 207.1 for ammonia concentration by Ion Specific Electrode analysis.

Stack O₂ and NO_x concentrations and stack volumetric flow rate data were recorded from the Continuous Emission Monitoring System (CEMS) which is installed on the unit. These data were used to correct the ammonia concentration to 15% O₂.

4.0 TEST RESULTS AND OVERVIEW

4.1 TEST RESULTS

The results of the test are summarized in Table 4-1. The results show that the ammonia slip was 1.7 ppm @ 15% O₂ which is less than the permitted limit of 5 ppm @ 15% O₂.

**TABLE 4-1
AMMONIA SLIP TEST RESULTS
CANYON POWER PLANT UNIT 1
JULY 23, 2019**

Parameter	Units	Run 1	Run 2	Average	Maximum ⁽¹⁾	Limit
Test		1-NH ₃ -U1	2-NH ₃ -U1			--
Date		7/23/2019	7/23/2019			--
Time		0700/0806	0834/0940			--
O ₂ ⁽²⁾	%	14.43	14.41	14.42	--	--
Stack Flow ⁽²⁾	dscfm @ T _{ref}	227,992	227,992	227,992	--	--
NO _x ⁽²⁾	ppmc	2.4	2.3	2.3	--	2.5
NH ₃	ppm	1.9	1.8	1.9	1.9	--
NH ₃	ppmc	1.7	1.7	1.7	1.7	5
NH ₃	lb/hr	1.2	1.1	1.1	1.2	--
NH ₃	lb/MMBtu	0.002	0.002	0.002	0.002	--
NH ₃	lb/MMSCF	2.5	2.4	2.4	2.5	--

(1) Maximum of duplicate test runs, as required by SCAQMD Method 207.1

(2) From facility CEMS

APPENDIX A RAW DATA

Appendix A.1

Sample Data Sheets

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA - Canyon
 LOCATION: Unit 1
 DATE: 7/23/19
 RUN NO: 1-NH3-41
 OPERATOR: RH/RL
 METER BOX NO: 19-WCS
 METER ΔH@: 1.745
 METER Yd: 1.011
 STACK AREA, FT²: 106.90
 TRAVERSE POINTS, MIN/POINT: 5/12
 ΔH= N/A X ΔP:
 Probe Condition, pre/post test: ✓/✓
 Silica Gel Expanded, Y/N: N
 Filter Condition after Test: N/A
 Check Weight: 749.91 / 500.0

AMBIENT TEMPERATURE: ~70
 BAROMETRIC PRESSURE: 29.65
 ASSUMED MOISTURE: ~13%
 PITOT TUBE COEFF, Cp: N/A
 PROBE ID NO/MATERIAL: 9155
 PROBE LENGTH: 6
 NOZZLE ID NO/MATERIAL: N/A
 NOZZLE DIAMETER: N/A
 FILTER NO/TYPE: N/A
 PRE-TEST LEAK RATE: 60.005 CFM@ 15 in. Hg.
 POST-TEST LEAK RATE: 60.005 CFM@ 14 in. Hg.
 PITOT LEAK CHECK - PRE: ✓ POST:
 CHAIN OF CUSTODY: SAMPLE CUSTODIAN SD
 SAMPLER RL
 SAMPLE CUSTODIAN SD

Imp. # Contents Post-Test - Pre-Test = Difference
 1 H₂SO₄ 922.7 723.0
 2 H₂SO₄ 777.4 772.1
 3 MT 653.4 652.8
 4 SG 919.9 909.2
 LR 100.0
 Total:

Point	Time	Meter Volume, ft ³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
3	0700	631.700	N/A	1.5	N/A	61.4	~1.1	58	73 72	3		N/A
2	0705	635.135		1.5				56	74 72	3		
1	0710	638.575		1.5				54	75 72	3		
PL	0715	641.256										
3	0717	641.856		1.5				58	77 74	3		
2	0722	645.260		1.5				56	79 73	3		
1	0727	649.125		1.5				55	80 76	3		
PL	0732	652.031										
3	0734	652.031		1.5				57	79 76	3		
2	0739	655.495		1.5				55	80 77	3		
1	0741	658.450		1.5				56	80 77	3		
PL	0749	662.334										
3	0751	662.339		1.5				58	80 78	3		
2	0756	665.700		1.5				56	79 78	3		
1	0801	669.125		1.5				55	81 80	3		
PL	0808	672.186										
Average:												

Comments: X 0806 PH 7-23-19

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA - Canyon
 LOCATION: Unit 1
 DATE: 7/23/19
 RUN NO: 2-NH3-41
 OPERATOR: RH/HLC
 METER BOX NO: 14-WLS
 METER ΔH@: 1-745
 METER Yd: 1-011
 STACK AREA, FT²: 106.90
 TRAVERSE POINTS, MIN/POINT: 5/12
 ΔH= N/A X ΔP: ✓
 Probe Condition, pre/post test: ✓
 Silica Gel Expanded, Y/N: N/A
 Filter Condition after Test: N/A
 Check Weight: 449.5/500.0

AMBIENT TEMPERATURE: ~75°
 BAROMETRIC PRESSURE: 29.65
 ASSUMED MOISTURE: 12%
 PITOT TUBE COEFF, Cp: N/A
 PROBE ID NO/MATERIAL: glass
 PROBE LENGTH: 6'
 NOZZLE ID NO/MATERIAL: N/A
 NOZZLE DIAMETER: N/A
 FILTER NO/TYPE: N/A
 PRE-TEST LEAK RATE: 2.00 CFM@ 15 in. Hg.
 POST-TEST LEAK RATE: 1.00 CFM@ 15 in. Hg.
 PITOT LEAK CHECK - PRE: ✓ POST: ✓
 CHAIN OF CUSTODY: SAMPLE CUSTODIAN SD
SAMPLER GH
SAMPLE CUSTODIAN SD

Imp. # Contents Post-Test - Pre-Test = Difference
 1 H₂O 969.5 768.4
 2 H₂O 738.5 751.6
 3 N₂ 682.2 680.7
 4 SL 938.4 929.3
 NR H₂O 100
 Total:

Point	Time	Meter Volume, ft³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
1	0834	673.600	1.1	1.5	~14	~14	~14	58	82	3		
2	0839	676.315	1.1	1.5				56	81	3		
1	0844	680.115	1.1	1.5				53	80	3		
SL	0844	683.512										
3	0851	683.562	1.5	1.5				58	82	3		
2	0856	687.045	1.5	1.5				51	84	3		
1	0901	690.360	1.5	1.5				54	85	3		
SL	0906	693.678										
3	0908	693.678	1.5	1.5				57	86	3		
2	0913	697.095	1.5	1.5				55	85	3		
1	0918	700.450	1.5	1.5				56	90	3		
SL	0923	703.122										
3	0927	703.122	1.5	1.5				58	90	3		
2	0930	707.140	1.5	1.5				55	90	3		
1	0935	710.505	1.5	1.5				53	91	3		
END	0940	713.316										
Average:												

Comments: * 754.9 SD 7/23/19

Appendix A.2 Laboratory Data

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS

Project #: 002AS-543377 District Method: SCAQMD 207.1 Sample Date: 7/23/2019
 Client/Location: SCPPA - Canyon Power Plant Calibration Date: 7/29/2019 Analysis Date: 7/29/2019
 Sample Location: Unit 1 Calibration Curve: $y = -56.2679x + 86.8429$ Analyst's Initials: KC
 Test #'s: 1, 2 NH₃ R²: 1.0000

Sample	Electrode Potential (mV)	TV (ml)	Conc. $\mu\text{g NH}_3 - \text{N} / \text{ml}$	Cavg ($\mu\text{g NH}_3 - \text{N} / \text{ml}$)	$\mu\text{g NH}_3 / \text{sample}$	Comments/ Temp/pH
Standard Check: 28 $\mu\text{g NH}_3 / \text{ml}$	2.1	—	28.469	28.469	—	Percent Recovery: <u>T=22°C 102% recovery</u>
Repeat 28 $\mu\text{g NH}_3 / \text{ml}$	2.1	—	28.469	—	—	T=22°C
1 - NH ₃	69.7	640.2	1.969	1.969	1532.149	T=22°C pH<2
Repeat 1 - NH ₃	69.7	—	1.969	—	—	T=22°C
2 - NH ₃	75.9	755.0	1.541	1.563	1434.087	T=22°C pH<2
Repeat 2 - NH ₃	75.2	—	1.584	—	—	T=22°C
Spike 2 - NH ₃	10.1	—	20.752	20.794	—	T=22°C
Repeat Spike 2 - NH ₃	10.0	—	20.835	—	—	T=22°C
28 $\mu\text{g NH}_3 / \text{ml}$	2.4	—	28.133	28.189	—	T=22°C 101% recovery
Repeat 28 $\mu\text{g NH}_3 / \text{ml}$	2.3	—	28.245	—	—	T=22°C
0.1N H ₂ SO ₄ Reagent blank	178.0	—	0.027	0.027	—	T=22°C
Repeat 0.1N H ₂ SO ₄ Reagent blank	178.5	—	0.027	—	—	T=22°C
Field blank	171.0	—	0.036	0.036	—	T=22°C
Repeat Field blank	171.4	—	0.035	—	—	T=22°C
DI H ₂ O blank	176.3	—	0.029	0.029	—	T=22°C
Repeat DI H ₂ O blank	176.8	—	0.029	—	—	T=22°C
28 $\mu\text{g NH}_3 / \text{ml}$	2.3	—	28.245	28.245	—	T=22°C 101% recovery
Repeat 28 $\mu\text{g NH}_3 / \text{ml}$	2.3	—	28.245	—	—	T=22°C

Notes: Total volume of samples and standards used: 100 ml
 Volume of pH adjusting ISA used in ml: 2 ml
 Absorbing solution: 0.1N H₂SO₄

Calculations: Conc. ($\mu\text{g NH}_3 - \text{N} / \text{ml}$) = $10^{(P-B)/M}$
 P = electrode potential, B = y-intercept and M = slope
 Cavg = average result of duplicate analyses ($\mu\text{g NH}_3 - \text{N} / \text{ml}$) = $(C_1 + C_2) / 2$
 $\mu\text{g NH}_3 / \text{sample} = \text{Cavg} \times 17.03 / 14.01 \times \text{TV}$
 $\text{mg} / \text{sample} = \mu\text{g} / \text{sample} \div 1000$
 $\text{ppm NH}_3 = \text{mg NH}_3 / \text{sample} \times 1 / \text{Vstd} \times 1 / 454000 \times \text{SV} / 17 \times 10^6$

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS CALCULATION

Project Number: 002AS-543377
 Client/ Location: SCPPA-Canyon Power Plant
 Sample Location: Unit 1
 District Method: SCAQMD 207.1
 Sample Date: 7/23/2019
 Analysis Date: 7/29/2019
 Analyst's Initials: KC
 Calibration Curve Slope -58.2879
 Y-intercept 86.8429
 R² 1.0000
 probe 9

Sample	P mV	Conc. µg NH ₃ /ml as N	C avg as N	TV (ml)	C avg as NH ₃	µg NH ₃ / sample
28 ug NH ₃ / ml as N	2.1	28.469				
Repeat 28 ug NH ₃ /ml as N	2.1	28.469	28.469	NA	34.605	NA
1-NH ₃	69.7	1.969				
Repeat 2- NH ₃	69.7	1.969	1.969	640.2	2.393	1532.149
2-NH ₃	75.9	1.541				
Repeat 2- NH ₃	75.2	1.584	1.563	755	1.899	1434.087
spike 2-NH ₃	10.1	20.752				
Repeat 2-NH ₃ spike	10.0	20.835	20.794	NA	25.276	NA
28 NH ₃ /ml as N	2.4	28.133				
Repeat 28 ug NH ₃ /ml as N	2.3	28.245	28.189	NA	34.285	NA
Reagent Blank	178.0	0.027				
Repeat Reagent Blank	178.5	0.027	0.027	NA	0.033	NA
Field Blank	171.0	0.036				
Repeat Field Blank	171.4	0.035	0.036	NA	0.043	NA
DI H ₂ O Blank	176.3	0.029				
Repeat DI H ₂ O Blank	176.8	0.029	0.029	NA	0.035	NA
28 NH ₃ /ml as N	2.3	28.245				
Repeat 28 ug NH ₃ /ml as N	2.3	28.245	28.245	NA	34.333	NA

Notes:

Measured Concentration of Ammonia (C) in µg NH₃ / ml as N

$$C=10^{(P-B)/M}$$

P = electrode potential (mV), M=slope and B=intercept

Average Measured Ammonia Concentration (Cavg) = (C1 + C2)/2

where C1, C2 results from duplicate analyses (µg NH₃/ml as N)

Cavg (µg NH₃/ml as NH₃) = Cavg (µg NH₃/ ml as N) * 17.03/ 14.01

µg NH₃ / sample = Cavg (µg NH₃/ml as NH₃) * TV

Used 100 ml of samples and standards with 2 ml ISA and constant stirring rate.

All solutions turned blue and remained blue with ISA unless otherwise indicated.

Sample PH and Temperatures can be found on the laboratory datasheet.

Maximum samples (including blanks) between 28 ug/ml check standard is 5 samples analyzed in duplicate.

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS QUALITY CONTROL

Project Number: 002AS-543377
 Client/ Location: SCPPA-Canyon Power Plant
 Sample Location: Unit 1
 District Method: SCAQMD 207.1
 Sample Date: 7/23/2019
 Analysis Date: 7/29/2019
 Analyst's Initials: KC

Sample	% recovery	RPD %	RPA %
28 ug NH3 / ml as N			
Repeat 28 ug NH3/ml as N	NA	0.00	1.674
1-NH3			
Repeat 2- NH3	NA	0.00	NA
2-NH3			
Repeat 2- NH3	NA	-2.77	NA
spike 2-NH3			
Repeat 2-NH3 spike	100.16	-0.40	NA
28 NH3/ml as N			
Repeat 28 ug NH3/ml as N	NA	-0.40	0.674
Reagent Blank			
Repeat Reagent Blank	NA	1.98	NA
Field Blank			
Repeat Field Blank	NA	1.58	NA
DI H2O Blank			
Repeat DI H2O Blank	NA	1.98	NA
28 NH3/ml as N			
Repeat 28 ug NH3/ml as N	NA	0.00	0.873

Notes:

spike: 100 ml sample + 2 ml (1000 µg NH₃ / ml as N)

Matrix Spike Percent Recovery (%R)

%R = (C spike*0.104 - Csample*0.102)/2 *100

Cspike = average result of matrix spike (µg NH₃/ ml as N)

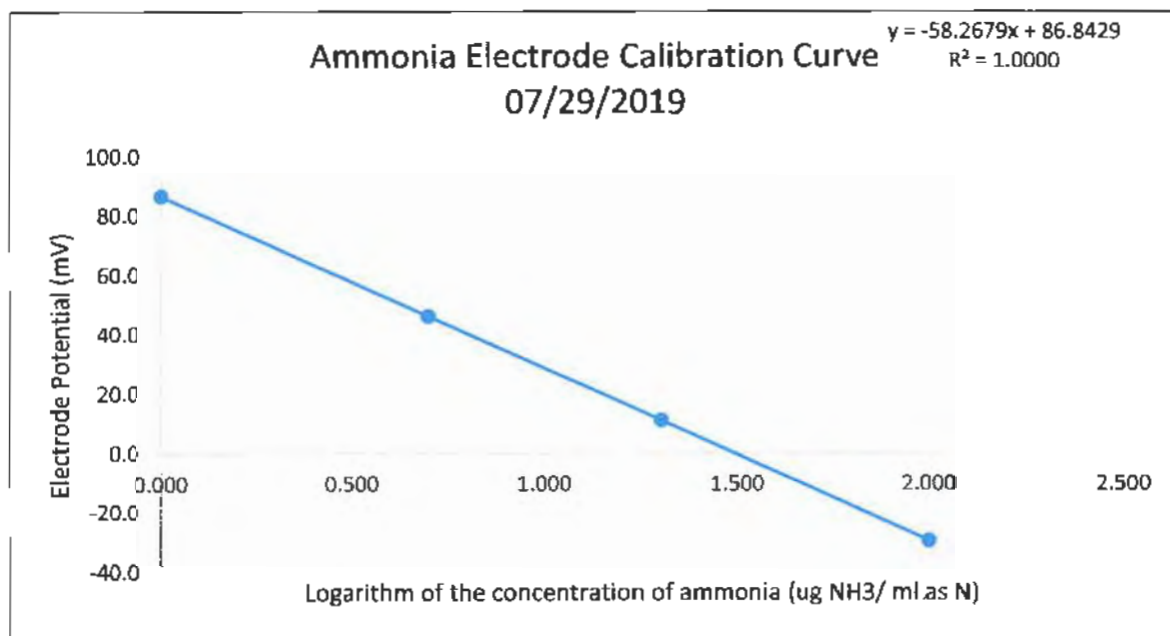
Relative Percent Difference (RPD) = (C1-C2)/ Cavg *100 (must be 5% or less)

Relative Percent Accuracy (RPA) (must be 10% or less)

RPA = (Cavg-theoretical value of standard)/ theoretical value of standard * 100

AMMONIA ELECTRODE CALIBRATION CURVE

NH ₃ concentration (µg NH ₃ / ml as N)	log NH ₃ concentration	Electrode potential (mV)	Sample Temperature (C)	Room Temperature (C)
1	0.000	86.8	22.1	22
5	0.699	46.2	22	22
20	1.301	11.0	22.7	22
100	2.000	-29.7	22.8	22



probe 9
slope -58.2679
y-intercept 86.8429

Concentration (µg NH ₃ / ml as N)	Value LR line	Difference	% Difference
1	1.0017	0.0017	0.1698
5	4.9833	-0.0167	-0.3338
20	20.0274	0.0274	0.1368
100	100.0279	0.0279	0.0279

Calculation:

Regression Line: $P = M \cdot \log(\mu\text{g of NH}_3 / \text{ml as N}) + B$

Measured Concentration of Ammonia (C) in µg / ml NH₃ as N: $C = 10^{(P-B)/M}$

where P = electrode potential, M= slope (must be -57 ± 3) and B= intercept

All standards were prepared in 0.04N H₂SO₄ and allowed to equilibrate to room temperature.

Appendix A.3

QA/QC Data

SEMI-ANNUAL DRY GAS METER/ORIFICE CALIBRATION

Office Method - Triplicate Runs/Four Calibration Points
English Meter Box Units, English K' Factor
Filename: M:\Santa Ana\Equipment\Calibrations\Dry Gas Meters\19-wcs\2019\semi annual cal 19wcs 2-1-19.xlsj\WCS
File Modified From: APEX 522 Series Meter box Calibration
Revised: 4/8/2035

ID #: C-5000
Date: 19-wcs
Bar. Pressure: 29.38 (in Hg)
Performed By: R. Howard
Meter Serial #: 2/1/2019

CRITICAL ORIFICE READINGS											
dH (in H ₂ O)	DRY GAS METER READINGS					CRITICAL ORIFICE READINGS					
	Time (min)	Volume Initial (cu ft)	Volume Final (cu ft)	Volume Total (cu ft)	Initial Temps. Inlet (deg F)	Final Temps. Inlet (deg F)	Orifice Serial# (number)	K' Orifice Coefficient (see above)	Actual Vacuum (in Hg)	Ambient Temperature Initial (deg F)	Average (deg F)
0.13	25.00	704.500	709.690	5.190	55.0	56.0	33	0.1553	15.0	56.0	56.0
0.13	25.00	709.990	714.877	5.187	55.0	58.0	33	0.1553	15.0	56.0	56.0
0.13	25.00	714.877	720.063	5.186	56.0	58.0	33	0.1553	15.0	56.0	56.0
0.61	12.00	746.000	751.275	5.275	60.0	60.0	48	0.3465	14.0	58.0	58.0
0.61	12.00	751.275	756.561	5.276	60.0	61.0	48	0.3465	14.0	58.0	58.0
0.61	12.00	756.561	761.825	5.274	61.0	61.0	48	0.3465	14.0	58.0	58.0
1.90	7.00	762.200	767.505	5.305	62.0	65.0	63	0.5888	12.0	57.0	57.0
1.90	7.00	767.505	772.827	5.322	65.0	66.0	63	0.5888	12.0	57.0	57.0
1.90	7.00	-	778.139	5.312	65.0	66.0	63	0.5898	12.0	57.0	57.0
3.50	5.00	729.500	734.596	5.196	60.0	62.0	73	0.8202	11.5	56.0	56.0
3.50	5.00	734.596	739.891	5.195	62.0	64.0	73	0.8202	11.5	56.0	56.0
3.50	5.00	739.891	745.091	5.200	64.0	65.0	73	0.8202	11.5	56.0	56.0

WET GAS METER				DRY GAS METER				ORIFICE			
VOLUME CORRECTED		VOLUME CORRECTED		VOLUME CORRECTED		VOLUME CORRECTED		CALIBRATION FACTOR		CALIBRATION FACTOR	
Vm(std) (cu ft)	Vm(std) (liters)	Vm(std) (cu ft)	Vm(std) (liters)	Vm(std) (cu ft)	Vm(std) (liters)	Vm(std) (cu ft)	Vm(std) (liters)	Y Value (number)	dH@ Value (in H ₂ O)	Individual Run	Individual Office
5.323	150.8	5.329	150.9	5.329	150.9	5.329	150.9	1.001	1.783	Pass	Ymax - Ymin < 0.010?
5.313	150.5	5.329	150.9	5.329	150.9	5.329	150.9	1.003	1.779	Pass	0.98 < Y/Yd < 1.02?
5.304	150.2	5.329	150.9	5.329	150.9	5.329	150.9	1.005	1.778	Pass	
				Average				1.003	1.780	Pass	Pass
5.381	152.4	5.477	155.1	5.477	155.1	5.477	155.1	1.018	1.681	Pass	
5.376	152.3	5.477	155.1	5.477	155.1	5.477	155.1	1.019	1.679	Pass	
5.372	152.1	5.477	155.1	5.477	155.1	5.477	155.1	1.020	1.679	Pass	
				Average				1.019	1.680	Pass	Pass
5.405	153.1	5.434	153.9	5.434	153.9	5.434	153.9	1.005	1.806	Pass	
5.412	153.3	5.434	153.9	5.434	153.9	5.434	153.9	1.004	1.804	Pass	
5.399	152.9	5.434	153.9	5.434	153.9	5.434	153.9	1.007	1.802	Pass	
				Average				1.005	1.804	Pass	Pass
5.337	151.2	5.412	153.3	5.412	153.3	5.412	153.3	1.014	1.718	Pass	
5.324	150.8	5.412	153.3	5.412	153.3	5.412	153.3	1.017	1.716	Pass	
5.321	150.7	5.412	153.3	5.412	153.3	5.412	153.3	1.017	1.716	Pass	
				Average				1.018	1.717	Pass	Pass

SIGNED: Signature on File

Date:

2/1/2019



DIGITAL TEMPERATURE READOUT CALIBRATION

Digital Temperature Readout ID: 19-WCS
 Readout Description: Control Box
 Date: 7/2/2019
 Performed By: JG/DA/RH/JS

Calibrated Thermocouple ID: TC-CAL
 T1 Reference Thermometer ID: 242196
 T2 Reference Thermometer ID: 242196
 T3 Reference Thermometer ID: 242167

T/C I.D.	Readout I.D.	T/C - Readout °F				Reference Thermometer °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
TC-CAL												
T3 (Oil)	19-WCS	350	350	350	350	358	358	358	358	8.0	1.0%	Pass
T2 (Boiling H ₂ O)	19-WCS	210	210	210	210	212	212	212	212	2.0	0.3%	Pass
T1 (Ice/Water)	19-WCS	38	36	36	36	32	32	32	32	4.0	0.8%	Pass

1) Difference % (°R) = Difference (°F) / (Average Tref + 460)

2) Pass if all Differences are less than 1.5% (°R)

Thermocouple Source Readings

Microscopic Surface Readings												
T/C Source S/N		T/C - Readout °F				T/C Source °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
T4 (~650 F)	S/N 106970	657	657	657	657	650	650	650	650	7.0	0.6%	Pass
T3 (~370 F)	S/N 106970	369	369	369	369	370	370	370	370	1.0	0.1%	Pass
T2 (~212 F)	S/N 106970	210	210	210	210	212	212	212	212	2.0	0.3%	Pass
T1 (~32 F)	S/N 106970	29	29	29	29	32	32	32	32	3.0	0.6%	Pass

1) Difference % (°R) = Difference (°F) / (Average Tref + 460)

2) Pass if all Differences are less than 1.5% (°R)

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCRIP A - Canyon
 LOCATION: Unit 1
 DATE: 7/23/19
 RUN NO: FB-NH3
 OPERATOR: RH
 METER BOX NO: 19-WCS
 METER ΔH@: 1.745
 METER Yd: 1.011
 STACK AREA, FT²: 106.90
 TRAVERSE POINTS, MIN/POINT: —
 ΔH= — X ΔP:
 Probe Condition, pre/post test: ✓/✓
 Silica Gel Expanded, Y/N: N
 Filter Condition after Test: N/A
 Check Weight: 449.9 / 500.0

AMBIENT TEMPERATURE: ~70°
 BAROMETRIC PRESSURE: 29.65
 ASSUMED MOISTURE: 12%₁₀
 PITOT TUBE COEFF, Cp: N/A
 PROBE ID NO/MATERIAL: 51635
 PROBE LENGTH: 6'
 NOZZLE ID NO/MATERIAL: N/A
 NOZZLE DIAMETER: N/A
 FILTER NO/TY: N/A
 PRE-TEST LEAK RATE: 40.005 CFM@ 12 in. Hg.
 POST-TEST LEAK RATE: 40.004 CFM@ 13 in. Hg.
 PITOT LEAK CHECK - PRE: N/A POST: N/A
 CHAIN OF CUSTODY: SAMPLE CUSTODIAN SD
SAMPLER RH
SAMPLE CUSTODIAN SD

Imp. # Contents Post-Test - Pre-Test = Difference
 1 H₂SO₄ 853.0 751.6
 2 H₂SO₄ 770.0 777.7
 3 MT 683.9 683.9
 4 SG 906.9 906.9
 CR H₂O 106
 Total: _____

Point	Time	Meter Volume, ft ³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
FLUO												
FLUO												
Average:												

Comments: _____

CLIENT:	SCPPA - Canyon Power Plant	PROJECT #:	WD02AS-543377	TEST DATE(S):	7/23/2019
LOCATION:	U1	SAMPLER(S):	RH/HL		
SAMPLE LOCATION:	Stack	PROJECT MANAGER:	SD		
TEST METHOD(S):	SCAQMD 207.1	DATE DUE:	7/30/2019		
OUTSIDE LAB REQUIRED?:	No	COMPLIANCE TEST?:	Yes		

[illegible]

RELEASED BY	DATE/TIME	RECEIVED BY	DATE/TIME
Robert Howard / Kab	7-25-19 / 1440	[Signature]	7/26/19 8:00

ANALYSIS REQUIRED:	NH ₃ by SCAQMD 207.1 (ISE)
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MONITROSE

Date of Last Revision 9/1/2017

Chain of Custody - DS834001 - Excel
Master Document Storage\Forms\Datasheets\Lab Forms

APPENDIX B FACILITY CEMS DATA

1-Nit3-01

Average Values Report
Generated: 7/23/2019 09:17Company: City Of Anaheim
Plant: 3071 Miraloma Ave.,
City/St: Anaheim, CA, 92806
Source: unit1Period Start: 7/23/2019 07:01
Period End: 7/23/2019 08:06
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

Period Start:	Average 1_O2 %	Average 1_NOXPPM ppm	Average 1_NOX_CORR ppm	Average 1_NOX_LBHR #/hr	Average 1_NOX_LBMM #/MMBTU	Average 1_GasFlow kscfh	Average 1_LOAD MW	Average 1_STACKFLOW kscfm	Average 1_COPPM ppm	Average 1_CO_CORR ppm	Average 1_CO_LBHR #/hr
07/23/2019 07:01	14.44	2.64	2.41	4.44	0.009	470.1	49.70	231.8	3.10	2.83	3.16
07/23/2019 07:02	14.45	2.60	2.38	4.44	0.009	470.3	49.75	232.3	3.02	2.76	3.06
07/23/2019 07:03	14.43	2.54	2.32	4.45	0.009	471.3	49.81	232.1	2.99	2.73	3.02
07/23/2019 07:04	14.43	2.55	2.33	4.46	0.009	471.4	49.80	232.1	3.00	2.74	3.02
07/23/2019 07:05	14.44	2.59	2.37	4.45	0.009	471.3	49.81	232.4	2.96	2.70	3.02
07/23/2019 07:06	14.42	2.58	2.35	4.46	0.009	472.2	49.88	232.1	2.90	2.64	2.93
07/23/2019 07:07	14.44	2.59	2.37	4.44	0.009	469.5	49.66	231.5	2.89	2.64	2.91
07/23/2019 07:08	14.44	2.59	2.37	4.45	0.009	471.0	49.78	232.3	3.07	2.80	3.12
07/23/2019 07:09	14.44	2.57	2.35	4.44	0.009	470.2	49.72	231.9	3.33	3.04	3.36
07/23/2019 07:10	14.44	2.55	2.33	4.45	0.009	470.7	49.77	232.1	3.08	3.00	3.31
07/23/2019 07:11	14.43	2.55	2.33	4.45	0.009	471.1	49.82	232.0	3.25	2.78	3.07
07/23/2019 07:12	14.44	2.59	2.37	4.45	0.009	470.5	49.82	232.0	3.02	2.76	3.06
07/23/2019 07:13	14.43	2.61	2.38	4.46	0.009	471.7	49.84	232.3	3.30	3.01	3.37
07/23/2019 07:14	14.42	2.60	2.37	4.46	0.009	471.9	49.87	232.0	3.43	3.12	3.47
07/23/2019 07:15	14.42	2.62	2.39	4.46	0.009	472.0	49.87	232.0	3.30	3.00	3.32
07/23/2019 07:16	14.42	2.64	2.40	4.46	0.009	471.8	49.87	231.9	3.18	2.90	3.22
07/23/2019 07:17	14.42	2.66	2.42	4.46	0.009	471.4	49.82	231.8	3.19	2.90	3.22
07/23/2019 07:18	14.43	2.65	2.42	4.45	0.009	470.8	49.76	231.8	3.17	2.89	3.21
07/23/2019 07:19	14.45	2.62	2.40	4.44	0.009	469.9	49.68	232.1	3.14	2.87	3.16
07/23/2019 07:20	14.44	2.57	2.35	4.44	0.009	470.3	49.73	231.9	3.06	2.79	3.11
07/23/2019 07:21	14.45	2.51	2.30	3.94	0.008	469.1	49.67	231.7	3.10	2.84	3.15
07/23/2019 07:22	14.45	2.50	2.29	3.95	0.008	470.3	49.75	232.3	3.30	3.02	3.36
07/23/2019 07:23	14.45	2.49	2.28	3.95	0.008	470.3	49.76	232.3	3.34	3.06	3.41
07/23/2019 07:24	14.44	2.50	2.28	3.94	0.008	469.0	49.70	231.3	3.16	2.89	3.20
07/23/2019 07:25	14.46	2.50	2.29	3.93	0.008	468.2	49.65	231.6	3.13	2.87	3.15
07/23/2019 07:26	14.45	2.47	2.26	3.94	0.008	468.8	49.70	231.5	3.24	2.96	3.25
07/23/2019 07:27	14.45	2.46	2.25	3.94	0.008	469.2	49.76	231.8	3.36	3.07	3.40
07/23/2019 07:28	14.43	2.47	2.25	3.95	0.008	469.8	49.81	231.3	3.31	3.02	3.35
07/23/2019 07:29	14.44	2.52	2.30	3.94	0.008	469.2	49.77	231.4	3.13	2.86	3.15
07/23/2019 07:30	14.44	2.56	2.34	4.44	0.009	470.0	49.81	231.8	3.07	2.80	3.11
07/23/2019 07:31	14.43	2.55	2.33	4.45	0.009	470.6	49.90	231.7	3.08	2.81	3.11
07/23/2019 07:32	14.42	2.58	2.35	4.45	0.009	470.8	49.87	231.4	2.94	2.68	2.97
07/23/2019 07:33	14.43	2.63	2.40	4.45	0.009	471.2	49.93	232.0	2.84	2.59	2.87
07/23/2019 07:34	14.43	2.65	2.42	4.44	0.009	469.9	49.79	231.4	2.79	2.54	2.81
07/23/2019 07:35	14.44	2.64	2.41	4.45	0.009	470.6	49.89	232.1	2.75	2.51	2.77
07/23/2019 07:36	14.42	2.64	2.40	4.45	0.009	470.4	49.89	231.2	2.75	2.50	2.77
07/23/2019 07:37	14.42	2.66	2.42	4.44	0.009	470.0	49.82	231.1	2.82	2.57	2.86
07/23/2019 07:38	14.45	2.69	2.46	4.42	0.009	468.2	49.68	231.2	2.78	2.54	2.80
07/23/2019 07:39	14.44	2.63	2.40	4.43	0.009	468.6	49.79	231.1	2.84	2.59	2.85
07/23/2019 07:40	14.45	2.60	2.38	4.42	0.009	467.8	49.67	231.1	3.25	2.97	3.29
07/23/2019 07:41	14.45	2.58	2.36	4.44	0.009	469.8	49.85	232.0	3.47	3.17	3.50
07/23/2019 07:42	14.42	2.55	2.32	4.44	0.009	470.3	49.88	231.2	3.42	3.11	3.46
07/23/2019 07:43	14.42	2.60	2.37	4.45	0.009	470.7	49.92	231.4	3.08	2.80	3.11
07/23/2019 07:44	14.42	2.66	2.42	4.45	0.009	470.9	49.90	231.5	3.00	2.73	3.02
07/23/2019 07:45	14.42	2.67	2.43	4.45	0.009	471.0	49.93	231.6	2.89	2.63	2.92
07/23/2019 07:46	14.41	2.68	2.44	4.45	0.009	470.7	49.90	231.0	2.75	2.50	2.77
07/23/2019 07:47	14.42	2.70	2.46	4.44	0.009	469.7	49.80	230.9	2.69	2.45	2.71
07/23/2019 07:48	14.44	2.69	2.46	4.43	0.009	468.5	49.72	231.0	2.70	2.47	2.71
07/23/2019 07:49	14.43	2.64	2.41	4.44	0.009	470.1	49.87	231.5	2.72	2.48	2.76

1-24-23-41

Period Start:		Average 1_O2 %	Average 1_NOXPPM ppm	Average 1_NOX_CORR ppm	Average 1_NOX_LBHR #/hr	Average 1_NOX_LBHM #/MBTU	Average 1_GasFlow kscfh	Average 1_LOAD MW	Average 1_STACKFLOW kscfh	Average 1_COPPM ppm	Average 1_CO_CORR ppm	Average 1_CO_LBHR #/hr
07/23/2019 07:50	14.42	2.63	2.39	2.45	4.45	0.009	470.4	49.87	231.2	2.76	2.51	2.77
07/23/2019 07:51	14.42	2.69	2.45	2.45	4.44	0.009	470.3	49.89	231.2	2.77	2.52	2.81
07/23/2019 07:52	14.41	2.69	2.45	2.45	4.45	0.009	470.9	49.87	231.1	2.92	2.65	2.97
07/23/2019 07:53	14.42	2.53	2.30	2.30	3.95	0.008	470.3	49.85	231.2	3.10	2.82	3.11
07/23/2019 07:54	14.42	2.45	2.23	2.23	3.95	0.008	470.1	49.78	231.1	3.16	2.88	3.21
07/23/2019 07:55	14.44	2.47	2.26	2.26	3.93	0.008	468.3	49.68	230.9	3.08	2.81	3.10
07/23/2019 07:56	14.43	2.44	2.23	2.23	3.95	0.008	470.5	49.85	231.7	3.23	2.95	3.26
07/23/2019 07:57	14.40	2.43	2.21	2.21	3.95	0.008	470.7	49.88	230.7	3.49	3.17	3.51
07/23/2019 07:58	14.42	2.49	2.27	2.27	3.95	0.008	470.1	49.84	231.1	3.68	3.35	3.70
07/23/2019 07:59	14.42	2.53	2.30	2.30	3.95	0.008	470.1	49.85	231.1	3.51	3.20	3.55
07/23/2019 08:00	14.41	2.52	2.29	2.29	3.95	0.008	470.3	49.87	230.8	3.29	2.99	3.31
07/23/2019 08:01	14.42	2.53	2.30	2.30	3.95	0.008	470.1	49.83	231.1	3.10	2.82	3.11
07/23/2019 08:02	14.42	2.53	2.30	2.30	3.94	0.008	469.1	49.78	230.6	3.09	2.81	3.10
07/23/2019 08:03	14.43	2.51	2.29	2.29	3.93	0.008	468.0	49.71	230.4	3.31	3.02	3.34
07/23/2019 08:04	14.44	2.46	2.25	2.25	3.94	0.008	468.6	49.75	231.1	3.77	3.44	3.79
07/23/2019 08:05	14.44	2.41	2.20	2.20	3.94	0.008	469.1	49.79	231.4	4.11	3.75	4.14
07/23/2019 08:06	14.42	2.41	2.19	2.19	3.96	0.008	470.9	49.91	231.5	4.07	3.71	4.10
Daily Average*	14.43	2.57	2.35	2.35	4.27	0.009	470.2	49.81	231.5	3.13	2.85	3.16
Maximum*	14.46	2.70	2.46	2.46	4.46	0.009	472.2	49.93	232.4	4.11	3.75	4.14
07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019
Minimum*	14.40	2.41	2.19	2.19	3.93	0.008	467.8	49.65	230.4	2.69	2.45	2.71
07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019
	7:57	8:06	8:06	8:03	8:03	8:06	7:40	7:25	8:03	7:47	7:47	7:48

* Does not include Invalid Averaging Periods ('N/A')

Average Values Report

Generated: 7/23/2019 10:52

Company: City Of Anaheim
Plant: 3071 Miraloma Ave.,
City/St: Anaheim, CA, 92806
Source: unit1

Period Start: 7/23/2019 08:35
Period End: 7/23/2019 09:40
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

Period Start:	Average 1_O2 %	Average 1_NOXPPM ppm	Average 1_NOX_CORR ppm	Average 1_NOX_LBHR #/hr	Average 1_NOX_LBHM #/hr	Average 1_GasFlow kscfm	Average 1_LOAD MW	Average 1_STACKFLOW kscfm	Average 1_COPPM ppm	Average 1_CO_CORR ppm	Average 1_CO_LBHR #/hr
07/23/2019 08:35	14.40	2.50	2.27	3.97	0.008	472.6	49.89	231.6	3.24	2.94	3.27
07/23/2019 08:36	14.42	2.54	2.31	4.45	0.009	471.1	49.73	231.6	3.05	2.78	3.07
07/23/2019 08:37	14.44	2.51	2.29	3.95	0.008	470.3	49.68	231.9	3.08	2.81	3.11
07/23/2019 08:38	14.43	2.45	2.23	3.95	0.008	470.2	49.70	231.5	3.26	2.97	3.31
07/23/2019 08:39	14.43	2.40	2.19	3.95	0.008	470.0	49.66	231.4	3.46	3.16	3.50
07/23/2019 08:40	14.43	2.40	2.19	3.96	0.008	471.2	49.82	232.0	3.52	3.21	3.56
07/23/2019 08:41	14.40	2.41	2.19	3.97	0.008	472.4	49.91	231.5	3.43	3.11	3.47
07/23/2019 08:42	14.40	2.46	2.23	3.96	0.008	471.9	49.83	231.3	3.31	3.00	3.32
07/23/2019 08:43	14.41	2.50	2.27	3.96	0.008	471.7	49.82	231.5	3.28	2.98	3.32
07/23/2019 08:44	14.41	2.49	2.26	3.96	0.008	471.9	49.88	231.6	3.38	3.07	3.42
07/23/2019 08:45	14.39	2.48	2.25	3.96	0.008	471.9	49.82	230.9	3.59	3.25	3.62
07/23/2019 08:46	14.42	2.50	2.28	3.96	0.008	471.2	49.73	231.7	3.57	3.25	3.61
07/23/2019 08:47	14.43	2.49	2.27	3.95	0.008	470.3	49.70	231.2	3.40	3.10	3.41
07/23/2019 08:48	14.43	2.45	2.23	3.96	0.008	471.4	49.79	232.1	3.44	3.14	3.47
07/23/2019 08:49	14.40	2.43	2.21	3.97	0.008	472.2	49.84	231.4	3.59	3.26	3.62
07/23/2019 08:50	14.43	2.45	2.23	3.95	0.008	470.0	49.66	231.4	3.58	3.26	3.60
07/23/2019 08:51	14.43	2.44	2.23	3.95	0.008	470.5	49.73	231.7	3.58	3.26	3.61
07/23/2019 08:52	14.43	2.39	2.18	3.95	0.008	470.1	49.65	231.5	3.76	3.43	3.80
07/23/2019 08:53	14.43	2.35	2.14	3.96	0.008	471.4	49.76	232.1	3.88	3.54	3.91
07/23/2019 08:54	14.43	2.35	2.14	3.95	0.008	470.1	49.68	231.5	3.68	3.36	3.70
07/23/2019 08:55	14.44	2.36	2.16	3.95	0.008	470.8	49.72	232.2	3.57	3.26	3.61
07/23/2019 08:56	14.42	2.35	2.14	3.97	0.008	472.4	49.88	232.2	3.63	3.31	3.67
07/23/2019 08:57	14.40	2.35	2.13	3.97	0.008	472.5	49.84	231.6	3.61	3.28	3.67
07/23/2019 08:58	14.42	2.48	2.26	3.96	0.008	471.1	49.78	231.6	3.41	3.10	3.46
07/23/2019 08:59	14.42	2.59	2.36	4.46	0.009	471.5	49.78	231.8	3.57	3.25	3.61
07/23/2019 09:00	14.42	2.61	2.38	4.46	0.009	471.8	49.81	231.9	3.88	3.53	3.91
07/23/2019 09:01	14.41	2.61	2.37	4.46	0.009	472.5	49.85	231.9	4.01	3.65	4.07
07/23/2019 09:02	14.41	2.64	2.40	4.46	0.009	471.9	49.80	231.6	3.94	3.58	3.96
07/23/2019 09:03	14.42	2.64	2.40	4.45	0.009	471.3	49.73	231.7	3.79	3.45	3.81
07/23/2019 09:04	14.42	2.61	2.38	4.46	0.009	471.4	49.75	231.8	3.66	3.33	3.71
07/23/2019 09:05	14.42	2.58	2.35	4.46	0.009	472.5	49.84	232.3	3.58	3.26	3.62
07/23/2019 09:06	14.39	2.59	2.35	4.47	0.009	472.7	49.89	231.3	3.55	3.22	3.57
07/23/2019 09:07	14.40	2.65	2.41	4.45	0.009	472.1	49.82	231.4	3.67	3.33	3.72
07/23/2019 09:08	14.41	2.69	2.45	4.46	0.009	471.6	49.82	231.5	3.91	3.55	3.96
07/23/2019 09:09	14.42	2.69	2.45	4.45	0.009	471.3	49.77	231.7	4.01	3.65	4.06
07/23/2019 09:10	14.42	2.68	2.44	4.46	0.009	471.7	49.77	231.9	3.90	3.55	3.96
07/23/2019 09:11	14.42	2.67	2.43	4.44	0.009	470.1	49.68	231.1	3.64	3.31	3.65
07/23/2019 09:12	14.43	2.65	2.42	4.44	0.009	469.6	49.69	231.2	3.71	3.38	3.75
07/23/2019 09:13	14.42	2.61	2.38	4.46	0.009	471.5	49.76	231.8	4.22	3.84	4.26
07/23/2019 09:14	14.42	2.58	2.35	4.45	0.009	470.5	49.68	231.3	4.44	4.04	4.50
07/23/2019 09:15	14.43	2.57	2.34	4.44	0.009	470.3	49.67	231.6	4.07	3.71	4.10
07/23/2019 09:16	14.43	2.56	2.33	4.44	0.009	470.3	49.69	231.6	3.64	3.32	3.65
07/23/2019 09:17	14.43	2.55	2.33	4.45	0.009	470.6	49.71	231.7	3.50	3.19	3.56
07/23/2019 09:18	14.42	2.55	2.32	4.46	0.009	471.7	49.83	231.9	3.40	3.10	3.42
07/23/2019 09:19	14.41	2.59	2.35	4.46	0.009	472.5	49.88	231.9	3.43	3.12	3.47
07/23/2019 09:20	14.42	2.66	2.42	4.46	0.009	471.9	49.84	232.0	3.35	3.05	3.37
07/23/2019 09:21	14.41	2.70	2.45	4.46	0.009	471.9	49.85	231.6	3.17	2.88	3.22
07/23/2019 09:22	14.41	2.70	2.45	4.46	0.009	471.9	49.84	231.6	3.11	2.83	3.12
07/23/2019 09:23	14.40	2.69	2.44	4.46	0.009	472.2	49.90	231.4	3.15	2.86	3.17

4.1
2-NH3-42

Period Start:	Average 1_O2 %	Average 1_NOXPPM PPM	Average 1_NOX_CORR PPM	Average 1_NOX_LBHR #/hr	Average 1_NOX_LBMM #/MMBTU	Average 1_GasFlow kscfh	Average 1_LOAD MW	Average 1_STACKFIM kscfm	Average 1_COPPM PPM	Average 1_CO_CORR PPM	Average 1_CO_LBHR #/hr
07/23/2019 09:24	14.40	2.70	2.45	4.46	0.009	471.9	49.85	231.3	3.22	2.92	3.27
07/23/2019 09:25	14.41	2.73	2.48	4.46	0.009	471.5	49.85	231.5	3.31	3.01	3.37
07/23/2019 09:26	14.40	2.72	2.47	4.46	0.009	472.1	49.91	231.4	3.41	3.10	3.42
07/23/2019 09:27	14.40	2.71	2.46	4.45	0.009	470.9	49.75	230.8	3.60	3.27	3.61
07/23/2019 09:28	14.42	2.71	2.47	4.45	0.009	470.8	49.76	231.4	3.67	3.34	3.71
07/23/2019 09:29	14.41	2.67	2.43	4.45	0.009	470.8	49.76	231.1	3.55	3.23	3.56
07/23/2019 09:30	14.41	2.66	2.42	4.45	0.009	470.6	49.75	231.0	3.31	3.01	3.36
07/23/2019 09:31	14.41	2.68	2.44	4.46	0.009	471.7	49.87	231.5	3.39	3.08	3.42
07/23/2019 09:32	14.39	2.69	2.44	4.46	0.009	472.5	49.90	231.2	3.46	3.14	3.47
07/23/2019 09:33	14.39	2.74	2.48	4.46	0.009	471.8	49.87	230.9	3.40	3.08	3.42
07/23/2019 09:34	14.39	2.78	2.52	4.47	0.009	472.7	49.91	231.3	3.20	2.90	3.23
07/23/2019 09:35	14.40	2.67	2.42	4.45	0.009	470.9	49.68	230.8	3.10	2.81	3.11
07/23/2019 09:36	14.42	2.47	2.25	3.95	0.008	469.8	49.65	231.0	3.17	2.89	3.21
07/23/2019 09:37	14.41	2.30	2.09	3.95	0.008	470.0	49.68	230.7	3.33	3.03	3.36
07/23/2019 09:38	14.42	2.27	2.07	3.96	0.008	471.2	49.79	231.7	3.39	3.09	3.41
07/23/2019 09:39	14.39	2.36	2.14	3.96	0.008	471.1	49.77	230.6	3.35	3.04	3.36
07/23/2019 09:40	14.41	2.47	2.25	3.95	0.008	470.6	49.76	231.0	3.29	2.99	3.31
Daily Average*	14.41	2.55	2.32	4.24	0.009	471.3	49.78	231.5	3.53	3.21	3.56
Maximum*	14.44	2.78	2.52	4.47	0.009	472.7	49.91	232.3	4.44	4.04	4.50
07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019
Minimum*	14.39	2.27	2.07	3.95	0.008	469.6	49.65	230.6	3.05	2.78	3.07
07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019	07/23/2019
9:39	9:38	9:38	9:38	9:40	9:40	9:12	9:36	9:39	8:36	8:36	8:36

* Does not include Invalid Averaging Periods ("N/A")

APPENDIX C CALCULATIONS

Appendix C.1

General Emissions Calculations

GENERAL EMISSION CALCULATIONS

I. Stack Gas Velocity

A. Stack gas molecular weight, lb/lb-mole

$$MW_{dry} = 0.44 * \%CO_2 + 0.32 * \%O_2 + 0.28 * \%N_2$$

$$MW_{wet} = MW_{dry} * (1 - B_{wo}) + 18 * B_{wo}$$

B. Absolute stack pressure, iwg

$$P_s = P_{bar} + \frac{P_{sg}}{13.6}$$

C. Stack gas velocity, ft/sec

$$V_s = 2.9 * C_p * \sqrt{\Delta P} * \sqrt{T_s} * \sqrt{\frac{29.92 * 28.95}{P_s * MW_{wet}}}$$

II. Moisture

A. Sample gas volume, dscf

$$V_{mstd} = 0.03342 * V_m * (P_{bar} + \frac{\Delta H}{13.6}) * \frac{T_{ref}}{T_m} * Y_d$$

B. Water vapor volume, scf

$$V_{wstd} = 0.0472 * V_{lc} * \frac{T_{ref}}{528 ^\circ R}$$

C. Moisture content, dimensionless

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

III. Stack gas volumetric flow rate

A. Actual stack gas volumetric flow rate, wacfm

$$Q = V_s * A_s * 60$$

B. Standard stack gas flow rate, dscfm

$$Q_{sd} = Q * (1 - B_{wo}) * \frac{T_{ref}}{T_s} * \frac{P_s}{29.92}$$

IV. Gaseous Mass Emission Rates, lb/hr

$$M = \frac{\text{ppm} * MW_i * Q_{sd} * 60}{SV * 10^6}$$

V. Emission Rates, lb/MMBtu

$$\frac{\text{lb}}{\text{MMBtu}} = \frac{\text{ppm} * MW_i * F}{SV * 10^6} * \frac{20.9}{20.9 - \%O_2}$$

VI. Percent Isokinetic

$$I = \frac{17.32 * T_s (V_{mstd})}{(1-Bwo) * 0 * V_s * P_s * Dn2} * \frac{520^{\circ}R}{T_{ref}}$$

VII. Particulate emissions

(a) Grain loading, gr/dscf
 $C = 0.01543 (M_n/V_{mstd})$

(b) Grain loading at 12% CO₂, gr/dscf
 $C_{12\% CO_2} = C (12/\% CO_2)$

(c) Mass emissions, lb/hr
 $M = C * Q_{sd} * (60 \text{ min/hr}) / (7000 \text{ gr/lb})$

(d) Particulate emission factor
 $\text{lb}/10^6 \text{ Btu} = C * \frac{1 \text{ lb}}{7000 \text{ gr}} * F * \frac{20.9}{20.9 - \% O_2}$

Nomenclature:

A_s	= stack area, ft ²
B_{wo}	= flue gas moisture content, dimensionless
$C_{12\%CO_2}$	= particulate grain loading, gr/dscf corrected to 12% CO ₂
C	= particulate grain loading, gr/dscf
C_p	= pitot calibration factor, dimensionless
D_n	= nozzle diameter, in.
F	= fuel F-Factor, dscf/MMBtu @ 0% O ₂
H	= orifice differential pressure, iwg
I	= % isokinetics
M_n	= mass of collected particulate, mg
M_i	= mass emission rate of specie i, lb/hr
MW	= molecular weight of flue gas, lb/lb-mole
M_{wi}	= molecular weight of specie i: SO ₂ : 64 NO _x : 46 CO: 28 HC: 16
t	= sample time, min.
ΔP	= average velocity head, iwg = $(\sqrt{\Delta P})^2$
P_{bar}	= barometric pressure, inches Hg
P_s	= stack absolute pressure, inches Hg
P_{sg}	= stack static pressure, iwb
Q	= wet stack flow rate at actual conditions, wacfm
Q_{sd}	= dry standard stack flow rate, dscfm
SV	= specific molar volume of an ideal gas at standard conditions, ft ³ /lb-mole
T_m	= meter temperature, °R
T_{ref}	= reference temperature, °R
T_s	= stack temperature, °R
V_s	= stack gas velocity, ft/sec
V_{lc}	= volume of liquid collected in impingers, ml
V_m	= uncorrected dry meter volume, dcf
V_{mstd}	= dry meter volume at standard conditions, dscf
V_{wstd}	= volume of water vapor at standard conditions, scf
Y_d	= meter calibration coefficient

Appendix C.2

Spreadsheet Summaries

SCAQMD 207.1 EXAMPLE CALCULATION
TEST NUMBER: 1-NH3-U1

Identifier	Description	Units	Equation	Value
A	Reference Temperature	F	--	60
B	Reference Temperature	R	$A + 460$	520
C	Meter Calibration Factor (Yd)	--	--	1.011
D	Barometric Pressure	" Hg	--	29.65
E	Meter Volume	acf	--	40.786
F	Meter Temperature	F	--	76.9
G	Meter Temperature	R	$F + 460$	536.9
H	Delta H	" H ₂ O	--	1.5
I	Meter Volume (standard)	dscf	$0.03342 * E * (D + H/13.6) * B/G * C$	39.721
J	Liquid Collected	grams	--	116.3
K	Water vapor volume	scf	$0.0472 * J * B/528$	5.406
L	Moisture Content	--	$K/(K + I)$	0.120
M	Gas Constant	ft-lbf/lb-mole-R	--	1545.33
N	Specific Molar Volume	SCF/lb-mole	$385.3 * B / 528$	379.5
O	F-Factor	dscf/MMBtu	--	8,710
P	HHV	Btu/SCF	--	1,050
Q	Mass Conversion Factor	lb/ug	--	2.2046E-09
R	O ₂ Correction Factor	--	--	15
S	Stack Flow Rate @ 68 F	dscfm	--	231,500
T	Stack Flow Rate @ Tref	dscfm	$S * B/528$	227,992
U	Mass NH ₃	ug	--	1,532
V	Mass NH ₃	lb	$U * Q$	3.38E-06
W	MW of NH ₃	lb/lb-mole	--	17.03
X	NH ₃	ppm	$(V * N * 10^9)/(I * W)$	1.9
Y	Flue Gas O ₂	%	--	14.43
Z	NH ₃	ppmc	$X * (20.9 - R)/(20.9 - Y)$	1.7
AA	NH ₃	lb/hr	$X * T * W * 60/(N * 10^6)$	1.2
AB	NH ₃	lb/MMBtu	$(X * W * O)/(385.3 * 10^6) * 20.9/(20.9 - Y)$	0.002
AC	NH ₃	lb/MMSCF	$AB * P$	2.5

Note:

(1) Some values may be slightly different from those shown on the run sheets due to round off errors. This page is intended to show the calculation methodology only.

SCAQMD METHOD 207.1 DATA WORKSHEET AND SUMMARY

Facility.....	Canyon		Parameter.....		NH₃
Unit.....	U1		Fuel.....		Natural gas
Sample Location.....	Stack		Data By.....		SD
Test Number.....	1-NH3-U1	2-NH3-U1	Average	Maximum	Limit
Reference Temperature (°F).....	60	60			
Test Date.....	7/23/2019	7/23/2019			
Test Method.....	SCAQMD 207.1	SCAQMD 207.1			
Sample Train.....	19-WCS	19-WCS			
Meter Calibration Factor.....	1.011	1.011			
Stack Area (ft ²).....	106.90	106.90			
Sample Time (Minutes).....	60	60			
Barometric Pressure ("Hg).....	29.65	29.65			
Start/Stop Time	0700/0806	0834/0940			
Meter Volume (acf).....	40.786	40.216			
Meter Temperature (°F).....	76.9	84.8			
Meter Pressure (iwg).....	1.5	1.5			
Liquid Volume (ml).....	116.3	115.5			
Stack O ₂ (%).....	14.43	14.41	14.42	(from facility CEMS)	
Unit Load (MW).....	50	50	49.8		
Standard Sample Volume (SCF).....	39.721	38.598			
Moisture Fraction.....	0.120	0.122			
Stack Flow Rate (dscfm, 68 °F).....	231,500	231,500	231,500	(from facility CEMS)	
Stack Flow Rate (@ Tref).....	227,992	227,992	227,992		
Gas Constant (ft-lbf/lb-mole-R).....	1545.33	1545.33			
Molecular Weight NH ₃ (lb/lb-mole).....	17.03	17.03			
Specific Molar Volume (ft ³ /lb-mole).....	379.5	379.5			
F-Factor (dscf/MMBtu).....	8,710	8,710			
HHV(Btu/SCF).....	1,050	1,050			
Mass Conversion (lb/ug).....	2.2046E-09	2.2046E-09			
O ₂ Correction Factor (%).....	15	15			
Mass NH ₃ (ug).....	1,532	1,434			
Mass NH ₃ (lb).....	3.38E-06	3.16E-06			
NH ₃ (ppmv, flue gas).....	1.9	1.8	1.9	1.9	
NH ₃ (ppmv @ O ₂ Correction Factor) ..	1.7	1.7	1.7	1.7	5
NH ₃ (lb/hr).....	1.2	1.1	1.1	1.2	
NH ₃ (lb/MMBtu).....	0.002	0.002	0.002	0.002	
NH ₃ (lb/MMSCF).....	2.5	2.4	2.4	2.5	

Note: SCAQMD Method 207.1 requires the higher of the duplicate runs be reported as the test result.

APPENDIX D QUALITY ASSURANCE

Appendix D.1

Quality Assurance Program Summary

QUALITY ASSURANCE PROGRAM SUMMARY

As part of Montrose Air Quality Services, LLC (MAQS) ASTM D7036-04 certification, MAQS is committed to providing emission related data which is complete, precise, accurate, representative, and comparable. MAQS quality assurance program and procedures are designed to ensure that the data meet or exceed the requirements of each test method for each of these items. The quality assurance program consists of the following items:

- Assignment of an Internal QA Officer
- Development and use of an internal QA Manual
- Personnel training
- Equipment maintenance and calibration
- Knowledge of current test methods
- Chain-of-custody
- QA reviews of test programs

Assignment of an Internal QA Officer: MAQS has assigned an internal QA Officer who is responsible for administering all aspects of the QA program.

Internal Quality Assurance Manual: MAQS has prepared a QA Manual according to the requirements of ASTM D7036-04 and guidelines issued by EPA. The manual documents and formalizes all of MAQS QA efforts. The manual is revised upon periodic review and as MAQS adds capabilities. The QA manual provides details on the items provided in this summary.

Personnel Testing and Training: Personnel testing and training is essential to the production of high quality test results. MAQS training programs include:

- A requirement for all technical personnel to read and understand the test methods performed
- A requirement for all technical personnel to read and understand the MAQS QA manual
- In-house testing and training
- Quality Assurance meetings
- Third party testing where available
- Maintenance of training records.

Equipment Maintenance and Calibration: All laboratory and field equipment used as a part of MAQS emission measurement programs is maintained according to manufacturer's recommendations. A summary of the major equipment maintenance schedules is summarized in Table 1. In addition to routine maintenance, calibrations are performed on all sampling equipment according to the procedures outlined in the applicable test method. The calibration intervals and techniques for major equipment components is summarized in Table 2. The calibration technique may vary to meet regulatory agency requirements.

Knowledge of Current Test Methods: MAQS maintains current copies of EPA, ARB, and SCAQMD Source Test Manuals and Rules and Regulations.

Chain-of-Custody: MAQS maintains chain-of-custody documentation on all data sheets and samples. Samples are stored in a locked area accessible only to MAQS source test personnel. Data sheets are kept in the custody of the originator, program manager, or in locked storage until return to MAQS office. Electronic field data is duplicated for backup on secure storage media. The original data sheets are used for report preparation and any additions are initialed and dated.

QA Reviews: Periodic field, laboratory, and report reviews are performed by the in-house QA coordinator. Periodically, test plans are reviewed to ensure proper test methods are selected and reports are reviewed to ensure that the methods were followed and any deviations from the methods are justified and documented.

ASTM D7036-04 Required Information

Uncertainty Statement

Montrose is qualified to conduct this test program and has established a quality management system that led to accreditation with ASTM Standard D7036-04 (Standard Practice for Competence of Air Emission Testing Bodies). Montrose participates in annual functional assessments for conformance with D7036-04 which are conducted by the American Association for Laboratory Accreditation (A2LA). All testing performed by Montrose is supervised on site by at least one Qualified Individual (QI) as defined in D7036-04 Section 8.3.2. Data quality objectives for estimating measurement uncertainty within the documented limits in the test methods are met by using approved test protocols for each project as defined in D7036-04 Sections 7.2.1 and 12.10. Additional quality assurance information is presented in the report appendices.

Performance Data

Performance data are available for review.

Qualified Personnel

A qualified individual (QI), defined by performance on a third party or internal test on the test methods, will be present on each test event.

Plant Entry and Safety Requirements

Plant Entry

All test personnel are required to check in with the guard at the entrance gate or other designated area. Specific details are provided by the facility and project manager.

Safety Requirements

All personnel shall have the following personal protective equipment (PPE) and wear them where designated:

- Hard Hat
- Safety Glasses
- Steel Toe Boots
- Hearing Protection
- Gloves
- High Temperature Gloves (if required)

The following safety measures will be followed:

- Good housekeeping
- SDS for all on-site hazardous materials
- Confine selves to necessary areas (stack platform, mobile laboratory, CEMS data acquisition system, control room, administrative areas)
- Knowledge of evacuation procedures

Each facility will provide plant specific safety training.

TABLE 1
EQUIPMENT MAINTENANCE SCHEDULE

Equipment	Acceptance Limits	Frequency of Service	Methods of Service
Pumps	1. Absence of leaks 2. Ability to draw manufacturers required vacuum and flow	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Replace parts 4. Leak check
Flow Meters	1. Free mechanical movement	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Calibrate
Sampling Instruments	1. Absence of malfunction 2. Proper response to zero span gas	As recommended by manufacturer	As recommended by manufacturer
Integrated Sampling Tanks	1. Absence of leaks	Depends on nature of use	1. Steam clean 2. Leak check
Mobil Van Sampling System	1. Absence of leaks	Depends on nature of use	1. Change filters 2. Change gas dryer 3. Leak check 4. Check for system contamination
Sampling lines	1. Sample degradation less than 2%	After each test series	1. Blow dry, inert gas through line until dry

TABLE 2
MAJOR SAMPLING EQUIPMENT CALIBRATION REQUIREMENTS

Sampling Equipment	Calibration Frequency	Calibration Procedure	Acceptable Calibration Criteria
Continuous Analyzers	Before and After Each Test Day	3-point calibration error test	< 2% of analyzer range
Continuous Analyzers	Before and After Each Test Run	2-point sample system bias check	< 5% of analyzer range
Continuous Analyzers	After Each Test Run	2-point analyzer drift determination	< 3% of analyzer range
CEMS System	Beginning of Each Day	leak check	< 1 in. Hg decrease in 5 min. at > 20 in. Hg
Continuous Analyzers	Semi-Annually	3-point linearity	< 1% of analyzer range
NO _x Analyzer	Daily	NO ₂ -> NO converter efficiency	> 90%
Differential Pressure Gauges (except for manometers)	Semi-Annually	Correction factor based on 5-point comparison to standard	+/- 5%
Differential Pressure Gauges (except for manometers)	Bi-Monthly	3-point comparison to standard, no correction factor	+/- 5%
Barometer	Semi-Annually	Adjusted to mercury-in-glass or National Weather Service Station	+/- 0.1 inches Hg
Dry Gas Meter	Semi-Annually	Calibration check at 4 flow rates using a NIST traceable standard	+/- 2%
Dry Gas Meter	Bi-Monthly	Calibration check at 2 flow rates using a NIST traceable standard	+/- 2% of semi-annual factor
Dry Gas Meter Orifice	Annually	4-point calibration for $\Delta H@$	--
Temperature Sensors	Semi-Annually	3-point calibration vs. NIST traceable standard	+/- 1.5%

Note: Calibration requirements will be used that meet applicable regulatory agency requirements.

Appendix D.2

SCAQMD and STAC Certifications



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 • www.aqmd.gov

October 30, 2018

Mr. John Peterson
Montrose Air Quality Services, LLC
1631 E. Saint Andrew Place
Santa Ana, CA 92705

Subject: LAP Approval Notice
Reference # 96LA1220

Dear Mr. Peterson:

We have reviewed your renewal letter under the South Coast Air Quality Management District's Laboratory Approval Program (SCAQMD LAP). We are pleased to inform you that your firm is approved for the period beginning October 30, 2018, and ending September 30, 2019 for the following methods, subject to the requirements in the LAP Conditions For Approval Agreement and conditions listed in the attachment to this letter:

SCAQMD Methods 1-4	SCAQMD Methods 5.1, 5.2, 5.3, 6.1
SCAQMD Methods 10.1 and 100.1	SCAQMD Methods 25.1 and 25.3 (Sampling)
USEPA CTM-030 and ASTM D6522-00	SCAQMD Rule 1121/ 1146.2 Protocol
SCAQMD Rule 1420/1420.1/1420.2 – (Lead) Source and Ambient Sampling	

Your LAP approval to perform nitrogen oxide emissions compliance testing for SCAQMD Rule 1121/ 1146.2 Protocols includes satellite facilities located at:

McKenna Boiler
1510 North Spring Street
Los Angeles, CA 90012

Noritz America Corp.
11160 Grace Avenue
Fountain Valley, CA 92708

Ajax Boiler, Inc.
2701 S. Harbor Blvd.
Santa Ana, CA 92704

Thank you for participating in the SCAQMD LAP. Your cooperation helps us to achieve the goal of the LAP: to maintain high standards of quality in the sampling and analysis of source emissions. You may direct any questions or information to LAP Coordinator, Glenn Kasai. He may be reached by telephone at (909) 396-2271, or via e-mail at gkasai@aqmd.gov.

Sincerely,

A handwritten signature in black ink, appearing to read 'D. Sarkar'.

Dipankar Sarkar
Program Supervisor
Source Test Engineering

DS:GK/gk

Attachment

181030 LapRenewalRev.doc

Cleaning the air that we breathe...



American Association for Laboratory Accreditation

Accredited Air Emission Testing Body

A2LA has accredited

MONTROSE AIR QUALITY SERVICES

In recognition of the successful completion of the joint A2LA and Stack Testing Accreditation Council (STAC) evaluation process, this laboratory is accredited to perform testing activities in compliance with ASTM D7036:2004 - Standard Practice for Competence of Air Emission Testing Bodies.

Presented this 5th day of March 2018.



President and CEO
For the Accreditation Council
Certificate Number 3925.01
Valid to February 29, 2020

This accreditation program is not included under the A2LA ILAC Mutual Recognition Arrangement.

Appendix D.3

Individual QI Certificate

CERTIFICATE OF COMPLETION

Sean Donovan

This document certifies that this individual has passed a comprehensive examination and is now a Qualified Individual (QI) as defined in Section 8.3 of ASTM D7036-04 for the following method(s):

SCAQMD Method 207.1

Certificate Number: 002-2016-06

Tate Strickler

DATE OF ISSUE: 11/30/16

Tate Strickler, Accreditation Director

DATE OF
EXPIRATION: 11/30/21



APPENDIX E

APPLICABLE PERMIT SECTIONS



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions * And Requirements	Conditions
Process 1: POWER GENERATION					
GAS TURBINE, NO. 1, NATURAL GAS, GENERAL ELECTRIC, MODEL LM6000PC SPRINT, SIMPLE CYCLE, 479 MMBTU/HR AT 46 DEG F, WITH INLET CHILLING, WITH WATER INJECTION WITH A/N: 555828	D1	C3	NOX: MAJOR SOURCE**	CO: 4 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]; CO: 2000 PPMV NATURAL GAS (5) [RULE 407, 4-2-1982]; NOX: 2.5 PPMV NATURAL GAS (4) [RULE 2005, 6-3-2011]; NOX: 25 PPMV NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; PM10: 0.01 GRAINS/SCF NATURAL GAS (5A) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; PM10: 0.1 GRAINS/SCF NATURAL GAS (5) [RULE 409, 8-7-1981]; PM10: 1.67 LBS/HR NATURAL GAS (5C) [RULE 1303(b)(2)-Offset, 5-10-1996; RULE 1303(b)(2)-Offset, 12-6-2002]; PM10: 11 LBS/HR NATURAL GAS (5B) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; SO2: (9) [40CFR 72 - Acid Rain Provisions, 11-24-1997]; SOX: 0.06 LBS/MMBTU NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; VOC: 2 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A63.1, A99.1, A99.2, A99.3, A195.1, A195.2, A195.3, A327.1, B61.1, D12.1, D29.2, D29.3, D82.1, D82.2, E193.1, H23.1, I298.1, K40.1
GENERATOR, 50.95 MW					

- * (1) (1A) (1B) Denotes RECLAIM emission factor (2) (2A) (2B) Denotes RECLAIM emission rate
(3) Denotes RECLAIM concentration limit (4) Denotes BACT emission limit
(5) (5A) (5B) Denotes command and control emission limit (6) Denotes air toxic control rule limit
(7) Denotes NSR applicability limit (8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(9) See App B for Emission Limits (10) See section J for NESHAP/MACT requirements

** Refer to 40 CFR 60.401 to determine the monitoring, maintenance and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions* And Requirements	Conditions
Process I: POWER GENERATION					
CO OXIDATION CATALYST, NO. 1, BASF, 110 CUBIC FEET OF TOTAL CATALYST VOLUME A/N: 476654	C3	D1 C4			
SELECTIVE CATALYTIC REDUCTION, NO. 1, CORMETECH CMHT-21, 1012 CU.FT.; WIDTH: 2 FT 6 IN; HEIGHT: 25 FT 9 IN; LENGTH: 18 FT WITH A/N: 476654	C4	C3 S6		NH3: 5 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1) -BACT, 12-6-2002]	A195.4, D12.2, D12.3, D12.4, E179.1, E179.2, E193.1
AMMONIA INJECTION					
STACK, TURBINE NO. 1, HEIGHT: 86 FT ; DIAMETER: 11 FT 8 IN A/N: 555828	S6	C4			

- * (1) (1A) (1B) Denotes RECLAIM emission factor
(3) Denotes RECLAIM concentration limit
(5) (5A) (5B) Denotes command and control emission limit
(7) Denotes NSR applicability limit
(9) See App B for Emission Limits

- (2) (2A) (2B) Denotes RECLAIM emission rate
(4) Denotes BACT emission limit
(6) Denotes air toxic control rule limit
(8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(10) See section J for NESHAP/MACT requirements

** Refer to section F and G of this permit to determine the monitoring, recordkeeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

[Devices subject to this condition : C4, C10, C16, C22]

D12.5 The operator shall install and maintain a(n) non-resettable elapsed time meter to accurately indicate the elapsed operating time of the engine.

[RULE 1110.2, 2-1-2008; RULE 1110.2, 9-7-2012; RULE 1303(b)(2)-Offset, 5-10-1996;
RULE 1303(b)(2)-Offset, 12-6-2002; RULE 1401, 9-10-2010; RULE 1470, 5-4-2012;
RULE 2012, 5-6-2005; 40CFR 60 Subpart III, 1-30-2013]

[Devices subject to this condition : D25]

D29.2 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Averaging Time	Test Location
NH3 emissions	District method 207.1 and 5.3 or EPA method 17	1 hour	Outlet of the SCR serving this equipment



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

The test(s) shall be conducted at least quarterly during the first twelve months of operation and at least annually thereafter. The AQMD shall be notified of the date and time of the test at least 10 days prior to the test.

If the turbine is not in operation during one calendar year, then no testing is required during that calendar year.

The NO_x concentration, as determined by the CEMS, shall be simultaneously recorded during the ammonia slip test. If the CEMS is inoperable, a test shall be conducted to determine the NO_x emissions using District Method 100.1 measured over a 60 minute averaging time period.

The test shall be conducted and the results submitted to the District within 60 days after the test date.

The test shall be conducted to demonstrate compliance with the Rule 1303 concentration limit.

[RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]

[Devices subject to this condition : D1, D7, D13, D19]

D29.3 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Sampling Time	Test Location
SOX emissions	AQMD Laboratory Method 307-91	Not Applicable	Fuel sample
VOC emissions	District Method 25.3	1 hour	Outlet of the SCR serving this equipment
PM emissions	District method 5.1	4 hours	Outlet of the SCR serving this equipment

THIS IS THE LAST PAGE OF THIS DOCUMENT

If you have any questions, please contact one of the following individuals by email or phone.

Name: Mr. Sean Donovan
Title: Client Project Manager
Region: West
E-Mail: SDonovan@montrose-env.com
Phone: (714) 279-6777

Name: Mr. Matt McCune
Title: Regional Vice President
Region: West
E-Mail: MMccune@montrose-env.com
Phone: (714) 279-6777

**TEST REPORT FOR
AMMONIA SLIP TEST
AT CANYON POWER PLANT UNIT 2
FACILITY ID: 153992, DEVICE ID: D7**

Prepared For:

Canyon Power Plant
3071 E. Mira Loma Avenue
Anaheim, California 92806

For Submittal To:

South Coast Air Quality Management District
21865 Copley Drive
Diamond Bar, California 91765-4178

Prepared By:

Montrose Air Quality Services, LLC
1631 E. St. Andrew Pl.
Santa Ana, California 92705
(714) 282-8240

Sean Donovan

Test Date: **July 25, 2019**
Production Date: **August 22, 2019**
Report Number: **W002AS-543378-RT-222**



CONFIDENTIALITY STATEMENT

Except as otherwise required by law or regulation, this information contained in this communication is intended exclusively for the individual or entity to which it is addressed. This communication may contain information that is proprietary, privileged or confidential or otherwise legally exempt from disclosure. If you are not the named addressee, you are not authorized to read, print, retain, copy, or disseminate this message or any part of it.

REVIEW AND CERTIFICATION

All work, calculations, and other activities and tasks performed and presented in this document were carried out by me or under my direction and supervision. I hereby certify that, to the best of my knowledge, Montrose operated in conformance with the requirements of the Montrose Quality Management System and ASTM D7036-04 during this test project.

Signature: Sean Donovan Date: 8/22/2019

Name: Sean Donovan Title: Client Project Manager

I have reviewed, technically and editorially, details, calculations, results, conclusions, and other appropriate written materials contained herein. I hereby certify that, to the best of my knowledge, the presented material is authentic, accurate, and conforms to the requirements of the Montrose Quality Management System and ASTM D7036-04.

Signature: Michael Chowsanitphon Date: 8/22/2019

Name: Michael Chowsanitphon Title: Reporting Manager

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1.0 INTRODUCTION AND SUMMARY

Montrose Air Quality Services, LLC (MAQS) was contracted by the Canyon Power Plant to perform an ammonia slip test at Unit 2 as required by the facility Permit (Facility ID 153992) Condition Number D29.2. This report documents the results of the ammonia slip tests performed on July 25, 2019. The test was performed by Sean Donovan, Henry Lee, and Robert Howard. Sean Donovan was the on-site qualified individual for MAQS. Bertha Hernandez coordinated the test for Canyon Power Plant.

The test consisted of duplicate ammonia tests performed at 50 MW. The test program followed the procedures described in the initial compliance test protocol (MAQS document R038842). The results of the test are summarized in Table 1-1. The table shows that the ammonia slip from this unit was less than the permitted limit of 5 ppm corrected to 15% O₂.

**TABLE 1-1
AMMONIA SLIP TEST RESULTS SUMMARY
CANYON POWER PLANT UNIT 2
JULY 25, 2019**

Parameter	Units	Result ⁽¹⁾	Limit
NH ₃	ppm	2.1	--
NH ₃	ppmc	2.0	5

(1) Maximum of duplicate runs, as required by SCAQMD Method 207.1

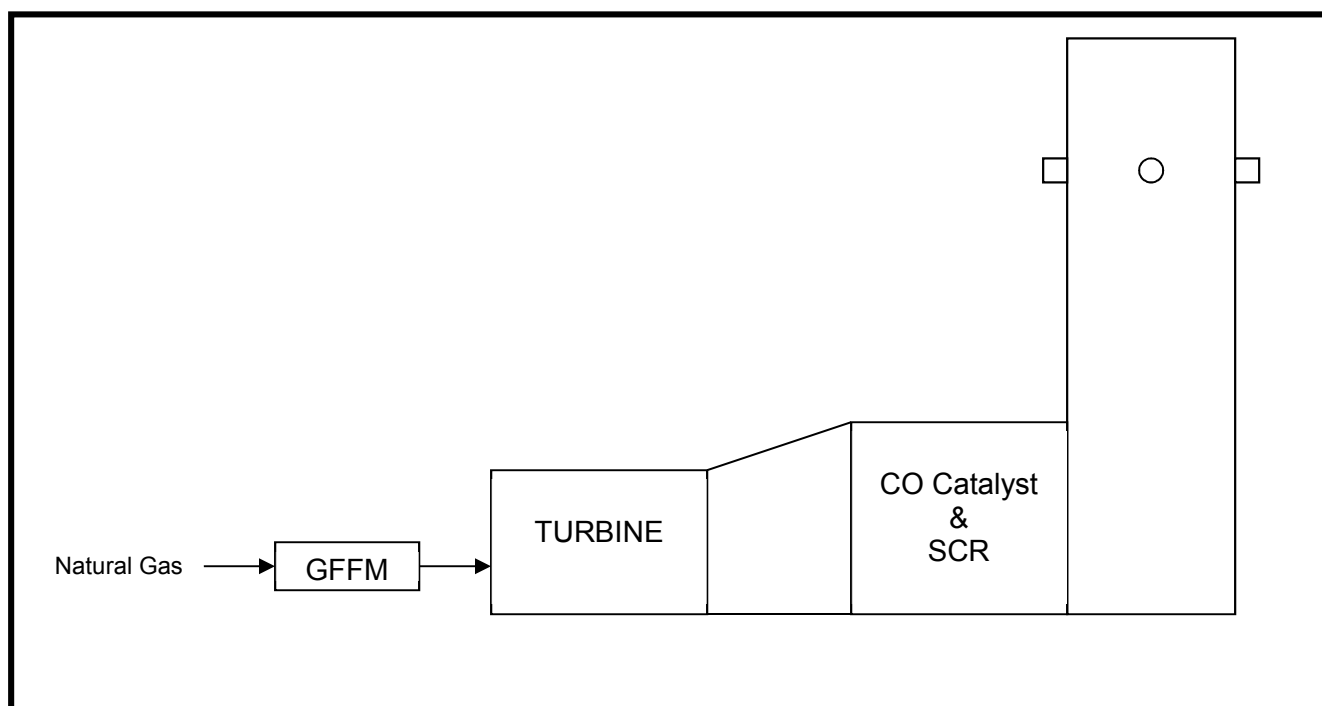
Section 2 of this document provides a brief description of the unit, test conditions, sample location, and CEMS. Details of the test procedures are provided in Section 3. Section 4 provides the results of each individual test. All raw data, calculations, quality assurance data, unit operating conditions, and CEMS data are provided in the appendices.

2.0 UNIT AND CEMS DESCRIPTION

2.1 UNIT DESCRIPTION

The City of Anaheim Canyon Power Plant is located at 3071 E. Mira Loma Avenue, Anaheim, California 92806. The facility consists of four identical generating units. Each unit consists of a natural gas fired, GE Model LM6000PC Sprint simple cycle, gas turbine. The units are natural gas fired with a rated heat input of 479 MMBtu per hour at 46 degrees Fahrenheit, with water injection. The units are equipped with a CO catalyst and Selective Catalytic Reduction (SCR) system for NO_x control. Figure 2-1 presents a block diagram of the unit.

**FIGURE 2-1
UNIT BLOCK DIAGRAM
CANYON POWER PLANT**



Stack Inside Diameter:	11 feet, 8 inches
Distance from Upstream Disturbance:	23 feet, 4 inches (2.0 Diameters)
Distance from Stack Exit:	16 feet, 6 inches (1.4 Diameters)

2.2 TEST CONDITIONS

The tests were performed with the unit operating at an average load of 50 MW. Tests were performed while the unit was firing natural gas and operating under normal conditions. Unit operation was established by the Canyon Power Plant operators.

2.3 SAMPLE LOCATION

The measurements were made from sample ports located on the exhaust stack. There are four sample ports equally spaced at this location. The stack inside diameter at the sample plane is 11 feet, 8 inches. The sample ports are located 23 feet, 4 inches (2.0 diameters) downstream of the nearest flow disturbance and 16 feet, 6 inches (1.4 diameters) from the stack exit.

3.0 TEST DESCRIPTION

Flue gas samples were collected non-isokinetically using a SCAQMD Method 207.1 sample train. The samples were collected using a 12-point traverse at the exhaust stack location. Each test was performed over a 60 minute interval. The sample gas was drawn through a glass probe, Teflon sample line, two impingers each containing 100 ml of 0.1N H₂SO₄, an empty impinger, an impinger containing silica gel, and a dry gas meter. The optional nozzle and filter were not used since the source is natural gas fired. The contents of the sample line and the first three impingers were recovered and analyzed by SCAQMD Method 207.1 for ammonia concentration by Ion Specific Electrode analysis.

Stack O₂ and NO_x concentrations and stack volumetric flow rate data were recorded from the Continuous Emission Monitoring System (CEMS) which is installed on the unit. These data were used to correct the ammonia concentration to 15% O₂.

4.0 TEST RESULTS AND OVERVIEW

4.1 TEST RESULTS

The results of the test are summarized in Table 4-1. The results show that the ammonia slip was 2.0 ppm @ 15% O₂ which is less than the permitted limit of 5 ppm @ 15% O₂.

**TABLE 4-1
AMMONIA SLIP TEST RESULTS
CANYON POWER PLANT UNIT 2
JULY 25, 2019**

Parameter	Units	Run 1	Run 2	Average	Maximum ⁽¹⁾	Limit
Test		1-NH ₃ -U2	2-NH ₃ -U2			--
Date		7/25/2019	7/25/2019			--
Time		0746/0852	1140/1246			--
O ₂ ⁽²⁾	%	14.66	14.63	14.65	--	--
Stack Flow ⁽²⁾	dscfm @ T _{ref}	231,538	232,227	231,883	--	--
NO _x ⁽²⁾	ppmc	2.3	2.4	2.3	--	2.5
NH ₃	ppm	2.1	1.8	2.0	2.1	--
NH ₃	ppmc	2.0	1.7	1.9	2.0	5
NH ₃	lb/hr	1.3	1.1	1.2	1.3	--
NH ₃	lb/MMBtu	0.003	0.002	0.003	0.003	--
NH ₃	lb/MMSCF	2.8	2.5	2.7	2.8	--

(1) Maximum of duplicate test runs, as required by SCAQMD Method 207.1

(2) From facility CEMS

APPENDIX A RAW DATA

Appendix A.1 Sample Data Sheets

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA - Canyon

LOCATION: Unit 2

DATE: 7/25/19

RUN NO: 1-245-02

OPERATOR: QH/HL

METER BOX NO: 19-WCS

METER AH@: 1-745

METER Yd: 1-011

STACK AREA, FT²: 106.90

TRAVERSE POINTS, MIN/POINT: 5/12

AH= — X AP: —

Probe Condition, pre/post test: ✓/✓

Silica Gel Expanded, Y/N: N

Filter Condition after Test: —

Check Weight: 499.9 / 500.0

AMBIENT TEMPERATURE: ~80

BAROMETRIC PRESSURE: 29.66

ASSUMED MOISTURE: 12%

PITOT TUBE COEFF. Cp: N/A

PROBE ID NO/MATERIAL: glass

PROBE LENGTH: 6'

NOZZLE ID NO/MATERIAL: N/A

NOZZLE DIAMETER: N/A

FILTER NO/TY: N/A

PRE-TEST LEAK RATE: 40.005 CFM@ 14 in. Hg.

POST-TEST LEAK RATE: 40.005 CFM@ 14 in. Hg.

PITOT LEAK CHECK - PRE: ✓ POST: ✓

CHAIN OF CUSTODY: SAMPLE CUSTODIAN SD

SAMPLER RM

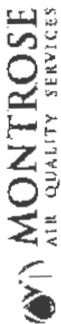
SAMPLE CUSTODIAN SD

Imp. # Contents Post-Test - Pre-Test = Difference

1	H ₂ SO ₄	944.0	729.6
2	H ₂ SO ₄	751.1	747.6
3	MT	656.2	653.4
4	SG	931.8	919.9
LR	H ₂ O	100ml	
Total:			

Point	Time	Meter Volume, ft ³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P, static in. H ₂ O
3	0746	850.000	2.14	2.0	N/A	N/A	N/A	58	72 71	5		N/A
2	0751	844.125		2.0				49	71 71	5		
1	0756	848.065		2.0				47	72 71	5		
PL	0801	901.975		—				—	—	—		
3	0803	901.435		2.0				52	72 71	5		
2	0808	905.870		2.0				48	73 71	5		
1	0813	909.710		2.0				48	73 71	5		
PL	0818	913.652		—				—	—	—		
3	0820	913.682		2.0				55	72 71	5		
2	0825	917.620		2.0				48	71 71	5		
1	0830	921.535		2.0				48	72 72	5		
PL	0835	925.414		—				—	—	—		
3	0837	925.414		2.0				52	72 73	5		
2	0842	929.350		2.0				49	73 71	5		
1	0847	933.256		2.0				49	74 74	5		
END	0852	937.104		—				—	—	—		
Average:												

Comments: _____



WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA - Canyon
LOCATION: 44.1 2
DATE: 7/25/19
RUN NO: 2-NH3-02
OPERATOR: RTH/HL
METER BOX NO: 19-WCS
METER AH@: 1.745
METER Yd: 1.011
STACK AREA, FT²: 106.90
TRAVERSE POINTS, MIN/POINT: 5/12
ΔH= X ΔP:
Probe Condition, pre/post test: ✓/✓
Silica Gel Expanded, Y/N: N
Filter Condition after Test: N/A
Check Weight: 499.61/500.00

AMBIENT TEMPERATURE: 80
BAROMETRIC PRESSURE: 29.66
ASSUMED MOISTURE: 12.0
PITOT TUBE COEFF, Cp: N/A
PROBE ID NO/MATERIAL: glass
PROBE LENGTH: 6.1
NOZZLE ID NO/MATERIAL: N/A
NOZZLE DIAMETER: N/A
FILTER NO/TYPER: N/A
PRE-TEST LEAK RATE: 40.005 CFM@ 11 in. Hg.
POST-TEST LEAK RATE: 40.005 CFM@ 13 in. Hg.
PITOT LEAK CHECK - PRE: N/A POST: N/A
CHAIN OF CUSTODY: SAMPLE CUSTODIAN SD
SAMPLER R-1
SAMPLE CUSTODIAN SD

Imp. # Contents Post-Test - Pre-Test = Difference
1 H₂SO₄ 926.2 741.2
2 H₂SO₄ 774.6 755.2
3 M.I. 667.3 656.2
4 SG 862.5 843.2
CL H₂O 100 ML
Total:

Point	Time	Meter Volume, ft ³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
3	1140	30.700	4.11	2.0	~11	~11	~11	58	83 82	0		
2	1145	34.710		2.0				54	84 83	4		
1	1150	38.665		2.0				51	85 83	4		
9C	1155	42.644										
3	1157	42.644		2.0				57	84 82	4		
2	1202	46.865		2.0				64	84 82	4		
1	1207	50.680		2.0				53	85 82	4		
PC	1212	54.535										
3	1214	54.535		2.0				57	86 82	4		
2	1219	58.475		2.0				55	88 83	4		
1	1224	62.580		2.0				56	88 86	4		
PC	1229	66.485										
3	1231	66.485		2.0				58	87 85	4		
2	1236	70.570		2.0				53	91 87	4		
1	1241	74.385		2.0				56	92 89	4		
END	1246	88.404										
Average:												

Comments:

Appendix A.2 Laboratory Data

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS

Project #: D02AS-543377 District Method: SCAQMD 207.1 Sample Date: 7/25/2019
 Client/Location: SCPPA - Canyon Power Plant Calibration Date: 7/29/2019 Analysis Date: 7/29/2019
 Sample Location: Unit 2 Calibration Curve: $y = -58.2679x + 86.8429$ Analyst's Initials: KC
 Test #s: 1, 2 - NH₃ R²: 1.0000

Sample	Electrode Potential (mV)	TV (ml)	Conc. $\mu\text{g NH}_3 - \text{N / ml}$	Cavg ($\mu\text{g NH}_3 - \text{N / ml}$)	$\mu\text{g NH}_3 / \text{sample}$	Comments/ Temp/pH
Standard Check: 28 $\mu\text{g NH}_3/\text{ml}$	2.4	—	28.133	28.181	—	Percent Recovery: $T=22^\circ\text{C}$ 101% recovery
Repeat 28 $\mu\text{g NH}_3/\text{ml}$	2.3	—	28.245	—	—	$T=22^\circ\text{C}$
1 - NH ₃	63.8	665.3	2.486	2.452	1982.867	$T=22^\circ\text{C}$ pH < 2
Repeat 1 - NH ₃	64.5	—	2.418	—	—	$T=22^\circ\text{C}$
2 - NH ₃	65.1	598.3	2.361	2.347	1707.196	$T=22^\circ\text{C}$ pH < 2
Repeat 2 - NH ₃	65.4	—	2.333	—	—	$T=22^\circ\text{C}$
Spike 2 - NH ₃	8.6	—	22.020	21.933	—	$T=22^\circ\text{C}$
Repeat Spike 2 - NH ₃	8.8	—	21.846	—	—	$T=22^\circ\text{C}$ 101% recovery
28 $\mu\text{g NH}_3/\text{ml}$	2.3	—	28.245	28.300	—	$T=22^\circ\text{C}$
Repeat 28 $\mu\text{g NH}_3/\text{ml}$	2.2	—	28.356	—	—	$T=22^\circ\text{C}$
0.1N H ₂ SO ₄ Reagent blank	178.0	—	0.027	0.027	—	$T=22^\circ\text{C}$
Repeat 0.1N H ₂ SO ₄ Reagent blank	178.5	—	0.027	—	—	$T=22^\circ\text{C}$
Field blank	171.0	—	0.036	0.036	—	$T=22^\circ\text{C}$
Repeat Field blank	171.4	—	0.035	—	—	$T=22^\circ\text{C}$
DI H ₂ O blank	176.3	—	0.029	0.029	—	$T=22^\circ\text{C}$
Repeat DI H ₂ O blank	176.8	—	0.029	—	—	$T=22^\circ\text{C}$
28 $\mu\text{g NH}_3/\text{ml}$	2.3	—	28.245	28.245	—	$T=22^\circ\text{C}$ 101% recovery
Repeat 28 $\mu\text{g NH}_3/\text{ml}$	2.3	—	28.245	—	—	$T=22^\circ\text{C}$

Notes: Total volume of samples and standards used: 100 ml
 Volume of pH adjusting ISA used in ml: 2 ml
 Absorbing solution: 0.1N H₂SO₄

Calculations: Conc. ($\mu\text{g NH}_3 - \text{N / ml}$) = $10^{(P-B)/M}$
 P = electrode potential, B = y-intercept and M = slope
 Cavg = average result of duplicate analyses ($\mu\text{g NH}_3 - \text{N / ml}$) = $(C1+C2)/2$
 $\mu\text{g NH}_3 / \text{sample} = \text{Cavg} \times 17.03 / 14.01 \times \text{TV}$
 $\text{mg / sample} = \mu\text{g / sample} + 1000$
 $\text{ppm NH}_3 = \text{mg NH}_3/\text{sample} \times 1/\text{mstd} \times 1/454000 \times \text{SV}/17 \times 10^3$

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS CALCULATION

Project Number: 002AS-543377
 Client/ Location: SCPPA-Canyon Power Plant
 Sample Location: Unit 2
 District Method: SCAQMD 207.1
 Sample Date: 7/25/2019
 Analysis Date: 7/29/2019
 Analyst's Initials: KC
 Calibration Curve Slope -58.2679
 Y-intercept 86.8429
 R² 1.0000
 probe 9

Sample	P mV	Conc. µg NH ₃ /ml as N	C avg as N	TV (ml)	C avg as NH ₃	µg NH ₃ / sample
28 ug NH ₃ / ml as N	2.4	28.133				
Repeat 28 ug NH ₃ /ml as N	2.3	28.245	28.189	NA	34.265	NA
1-NH ₃	63.8	2.486				
Repeat 2- NH ₃	64.5	2.418	2.452	665.3	2.980	1982.869
2-NH ₃	65.1	2.361				
Repeat 2- NH ₃	65.4	2.333	2.347	598.3	2.853	1707.196
spike 2-NH ₃	8.6	22.020				
Repeat 2-NH ₃ spike	8.8	21.846	21.933	NA	26.661	NA
28 NH ₃ /ml as N	2.3	28.245				
Repeat 28 ug NH ₃ /ml as N	2.2	28.356	28.300	NA	34.401	NA
Reagent Blank	178.0	0.027				
Repeat Reagent Blank	178.5	0.027	0.027	NA	0.033	NA
Field Blank	171.0	0.036				
Repeat Field Blank	171.4	0.035	0.036	NA	0.043	NA
DI H ₂ O Blank	176.3	0.029				
Repeat DI H ₂ O Blank	176.8	0.029	0.029	NA	0.035	NA
28 NH ₃ /ml as N	2.3	28.245				
Repeat 28 ug NH ₃ /ml as N	2.3	28.245	28.245	NA	34.333	NA

Notes:

Measured Concentration of Ammonia (C) in µg NH₃ / ml as N

$$C=10^{(P-B)/M}$$

P = electrode potential (mV), M=slope and B=intercept

Average Measured Ammonia Concentration (Cavg) = (C1 + C2)/2

where C1, C2 results from duplicate analyses (µg NH₃/ml as N)

Cavg (µg NH₃/ml as NH₃) = Cavg (µg NH₃/ ml as N) * 17.03/ 14.01

µg NH₃ / sample = Cavg (µg NH₃/ml as NH₃) * TV

Used 100 ml of samples and standards with 2 ml ISA and constant stirring rate.

All solutions turned blue and remained blue with ISA unless otherwise indicated.

Sample PH and Temperatures can be found on the laboratory datasheet.

Maximum samples (including blanks) between 28 ug/ml check standard is 5 samples analyzed in duplicate.

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS QUALITY CONTROL

Project Number: 002AS-543377
 Client/ Location: SCPPA-Canyon Power Plant
 Sample Location: Unit 2
 District Method: SCAQMD 207.1
 Sample Date: 7/25/2019
 Analysis Date: 7/29/2019
 Analyst's Initials: KC

Sample	% recovery	RPD %	RPA %
28 ug NH3 / ml as N			
Repeat 28 ug NH3/ml as N	NA	-0.40	0.674
1-NH3			
Repeat 2- NH3	NA	2.77	NA
2-NH3			
Repeat 2- NH3	NA	1.19	NA
spike 2-NH3			
Repeat 2-NH3 spike	102.08	0.79	NA
28 NH3/ml as N			
Repeat 28 ug NH3/ml as N	NA	-0.40	1.073
Reagent Blank			
Repeat Reagent Blank	NA	1.98	NA
Field Blank			
Repeat Field Blank	NA	1.58	NA
DI H2O Blank			
Repeat DI H2O Blank	NA	1.98	NA
28 NH3/ml as N			
Repeat 28 ug NH3/ml as N	NA	0.00	0.873

Notes:

spike: 100 ml sample + 2 ml (1000 µg NH₃ / ml as N)

Matrix Spike Percent Recovery (%R)

%R = (C spike*0.104 - Csample*0.102)/2 *100

Cspike = average result of matrix spike (µg NH₃/ ml as N)

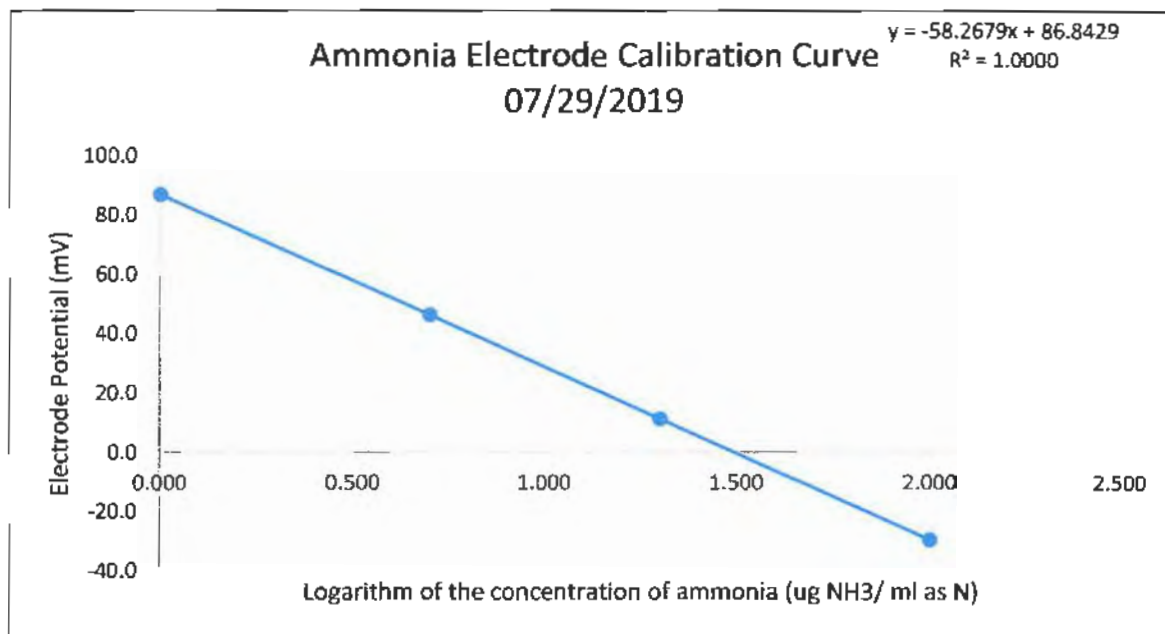
Relative Percent Difference (RPD) = (C1-C2)/ Cavg *100 (must be 5% or less)

Relative Percent Accuracy (RPA) (must be 10% or less)

RPA = (Cavg-theoretical value of standard)/ theoretical value of standard * 100

AMMONIA ELECTRODE CALIBRATION CURVE

NH ₃ concentration (µg NH ₃ / ml as N)	log NH ₃ concentration	Electrode potential (mV)	Sample Temperature (C)	Room Temperature (C)
1	0.000	86.8	22.1	22
5	0.699	46.2	22	22
20	1.301	11.0	22.7	22
100	2.000	-29.7	22.8	22



probe 9
slope -58.2679
y-intercept 86.8429

Concentration (µg NH ₃ / ml as N)	Value LR line	Difference	% Difference
1	1.0017	0.0017	0.1698
5	4.9833	-0.0167	-0.3338
20	20.0274	0.0274	0.1368
100	100.0279	0.0279	0.0279

Calculation:

Regression Line: $P = M \cdot \log(\mu\text{g of NH}_3 / \text{ml as N}) + B$

Measured Concentration of Ammonia (C) in µg / ml NH₃ as N: $C = 10^{(P-B)/M}$

where P = electrode potential, M = slope (must be -57 ± 3) and B = intercept

All standards were prepared in 0.04N H₂SO₄ and allowed to equilibrate to room temperature.

Appendix A.3

QA/QC Data

SEMI-ANNUAL DRY GAS METER/ORIFICE CALIBRATION

Office Method - Triplicate Runs/Four Calibration Points
 English Meter Box Units, English K Factor
 Filename: M:\Santa Ana\Equipment\Test Equipment\Calibrations\Dry Gas Meters\19-wcs2019\semi annual cal 19wcs 2-1-19.xls\WCS
 File Modified From: APEX 522 Series Meter box Calibration
 Revised: 4/6/2005

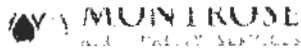
ID #: c-52000
 Date: 19-wcs
 Bar. Pressure: 29.98 (in. Hg)
 Performed By: R. Howard
 Meter Serial #: 371720019

CRITICAL ORIFICE READINGS									
DRY GAS METER READINGS									
dH (in H ₂ O)	Time (min)	Volume Initial (cu ft)	Volume Final (cu ft)	Volume Corrected (liters)	Volume Nominal (cu ft)	Volume Corrected (cu ft)	Volume Nominal (cu ft)	Initial Temp. (deg F)	Final Temp. (deg F)
0.13	26.00	704.500	709.600	5.100	5.100	5.100	5.100	56.0	56.0
0.13	26.00	709.600	714.977	5.377	5.377	5.377	5.377	56.0	56.0
0.13	26.00	714.877	720.063	5.186	5.186	5.186	5.186	56.0	56.0
0.61	12.00	748.000	751.275	3.275	3.275	3.275	3.275	58.0	58.0
0.61	12.00	751.275	756.551	5.276	5.276	5.276	5.276	58.0	58.0
0.61	12.00	756.551	761.825	5.274	5.274	5.274	5.274	58.0	58.0
1.90	7.00	762.200	767.505	5.305	5.305	5.305	5.305	57.0	57.0
1.90	7.00	767.505	772.827	5.322	5.322	5.322	5.322	57.0	57.0
1.90	7.00	772.827	778.139	5.312	5.312	5.312	5.312	57.0	57.0
3.50	5.00	723.500	734.696	11.196	11.196	11.196	11.196	56.0	56.0
3.50	5.00	734.696	739.891	5.195	5.195	5.195	5.195	56.0	56.0
3.50	5.00	739.891	745.091	5.200	5.200	5.200	5.200	56.0	56.0

DRY GAS METER									
ORIFICE									
VOLUME CORRECTED Vm(std) (cu ft)	VOLUME CORRECTED Vm(std) (liters)	VOLUME CORRECTED Vm(std) (cu ft)	VOLUME CORRECTED Vm(std) (liters)	VOLUME NOMINAL Vm (cu ft)	VOLUME NOMINAL Vm (liters)	Y Value (number)	dh@ Value (in H ₂ O)	Individual Run	Individual Office
5.381	152.4	5.477	155.1	5.365	154.9	1.001	1.783	Pass	Pass
5.376	152.3	5.477	155.1	5.365	154.9	1.001	1.783	Pass	Pass
5.372	152.1	5.477	155.1	5.365	154.9	1.001	1.783	Pass	Pass
Average						1.003	1.780	Pass	Pass
5.405	153.1	5.434	153.9	5.313	153.3	1.005	1.800	Pass	Pass
5.412	153.3	5.434	153.9	5.313	153.3	1.004	1.804	Pass	Pass
5.399	152.9	5.434	153.9	5.313	153.3	1.007	1.802	Pass	Pass
Average						1.005	1.804	Pass	Pass
5.337	151.2	5.412	153.3	5.281	152.1	1.014	1.718	Pass	Pass
5.324	150.8	5.412	153.3	5.281	152.1	1.017	1.716	Pass	Pass
5.321	150.7	5.412	153.3	5.281	152.1	1.017	1.716	Pass	Pass
Average						1.016	1.717	Pass	Pass
Average Yd:	1.011	dh@:	1.745						
				Q @ dh = 1:	0.568				

SIGNED: Signature on File

Date: 2/1/2019



DIGITAL TEMPERATURE READOUT CALIBRATION

Digital Temperature Readout ID: 19-WCS
 Readout Description: Control Box
 Date: 7/2/2019
 Performed By: JG/DA/RH/JS

Calibrated Thermocouple ID: TC-CAL
 T1 Reference Thermometer ID: 242196
 T2 Reference Thermometer ID: 242196
 T3 Reference Thermometer ID: 242167

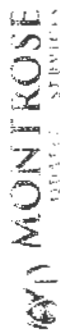
T/C I.D.	Readout I.D.	T/C - Readout °F				Reference Thermometer °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
TC-CAL												
T3 (OIL)	19-WCS	350	350	350	350	358	358	358	358	8.0	1.0%	Pass
T2 (Boiling H ₂ O)	19-WCS	210	210	210	210	212	212	212	212	2.0	0.3%	Pass
T1 (Ice/Water)	19-WCS	36	36	36	36	32	32	32	32	4.0	0.8%	Pass

- 1) Difference % (°R) = Difference (°F) / (Average Tref + 460)
 2) Pass if all Differences are less than 1.5% (°R)

Thermocouple Source Readings

T/C Source S/N		T/C - Readout °F				T/C Source °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
T4 (~650 F)	S/N 106970	657	657	657	657	650	650	650	650	7.0	0.6%	Pass
T3 (~370 F)	S/N 106970	369	369	369	369	370	370	370	370	1.0	0.1%	Pass
T2 (~212 F)	S/N 106970	210	210	210	210	212	212	212	212	2.0	0.3%	Pass
T1 (~32 F)	S/N 106970	29	29	29	29	32	32	32	32	3.0	0.8%	Pass

- 1) Difference % (°R) = Difference (°F) / (Average Tref + 460)
 2) Pass if all Differences are less than 1.5% (°R)



WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET -- STANDARD

CLIENT: SCPPA - Canyon
LOCATION: Unit 1
DATE: 7/23/17
RUN NO: FB-NH3
OPERATOR: RH
METER BOX NO: 19-WCS
METER ΔH@: 1.745
METER Yd: 1.011
STACK AREA, FT²: 106.90
TRAVERSE POINTS, MIN/POINT: --
ΔH= -- X ΔP:
Probe Condition, pre/post test: ✓/✓
Silica Gel Expanded, Y/N: N
Filter Condition after Test: N/A
Check Weight: 499.9 / 500.0


AMBIENT TEMPERATURE:	~ 70°
BAROMETRIC PRESSURE:	29.65
ASSUMED MOISTURE:	12°/10
PITOT TUBE COEFF. Cp:	N/A
PROBE ID NO/MATERIAL:	glass
PROBE LENGTH:	6'
NOZZLE ID NO/MATERIAL:	N/A
NOZZLE DIAMETER:	N/A
FILTER NO/TYPE:	N/A
PRE-TEST LEAK RATE:	40.005 CFM @ 12 in. Hg.
POST-TEST LEAK RATE:	40.004 CFM @ 13 in. Hg.
PITOT LEAK CHECK - PRE:	N/A POST: N/A
CHAIN OF CUSTODY:	SAMPLE CUSTODIAN SD
	SAMPLER PH
	SAMPLE CUSTODIAN SD

Imp. #	Contents	Post-Test	Pre-Test	Difference
1	H ₂ SO ₄	853.0	751.6	
2	H ₂ SO ₄	778.0	777.7	
3	MT	683.9	683.9	
4	SV	906.9	906.9	
UR	H ₂ O		106	
	Total:			

[illegible]

Comments:

CLIENT: SCPPA - Canyon Power Plant	PROJECT #: W002AS-543377	TEST DATE(S): 7/25/2019
LOCATION: U2		SAMPLER(S): RH/HL
SAMPLE LOCATION: Stack		PROJECT MANAGER: SD
TEST METHOD(S): SCAQMD 207.1		DATE DUE: 8/1/2019
OUTSIDE LAB REQUIRED?: No		COMPLIANCE TEST?: Yes

RELEASED BY	DATE/TIME	RECEIVED BY	DATE/TIME
Robert Howard / LAB	7-25-19 / 1440		7/26/19 8:40 am

<p>MONTROSE ALIC</p>	<p>Date of Last Revision 9/1/2017</p>	<p>Chain of Custody - DS834001 - Excel Master Document Storage\Forms\Datasheets\Lab Forms</p>
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APPENDIX B FACILITY CEMS DATA

1-NH3-U2

Average Values Report

Generated: 7/25/2019 09:12

Company: City Of Anaheim
Plant: 3071 Miraloma Ave.,
City/St: Anaheim, CA, 92806
Source: unit2

Period Start: 7/25/2019 07:47
Period End: 7/25/2019 08:52
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

Period Start:	Average 2_O2 %	Average 2_NOXPPM ppm	Average 2_NOX_CORR ppm	Average 2_NOX_LBHR #/hr	Average 2_NOX_LBMM #/MMBTU	Average 2_GasFlow kscf/hr	Average 2_LOAD MW	Average 2_STACKFLOW kscfm	Average 2_CO2PPM ppm	Average 2_CO_CORR ppm	Average 2_CO_LBHR #/hr
07/25/2019 07:47	14.64	2.50	2.36	4.37	0.009	462.5	49.70	235.4	3.65	3.44	3.74
07/25/2019 07:48	14.65	2.50	2.36	4.36	0.009	461.7	49.96	235.3	3.71	3.50	3.83
07/25/2019 07:49	14.64	2.48	2.34	4.37	0.009	462.6	49.82	235.4	3.71	3.50	3.78
07/25/2019 07:50	14.65	2.47	2.33	4.37	0.009	462.1	49.95	235.5	3.66	3.46	3.78
07/25/2019 07:51	14.65	2.47	2.33	4.36	0.009	461.4	49.50	235.2	3.67	3.46	3.78
07/25/2019 07:52	14.65	2.48	2.34	4.36	0.009	461.2	50.00	235.1	3.67	3.46	3.78
07/25/2019 07:53	14.65	2.49	2.35	4.36	0.009	461.4	49.70	235.2	3.79	3.58	3.88
07/25/2019 07:54	14.65	2.51	2.37	4.36	0.009	461.7	49.88	235.3	4.00	3.78	4.12
07/25/2019 07:55	14.65	2.54	2.40	4.36	0.009	461.1	49.90	235.0	4.13	3.90	4.21
07/25/2019 07:56	14.65	2.67	2.52	4.36	0.009	461.4	49.72	235.2	4.00	3.78	4.12
07/25/2019 07:57	14.66	2.85	2.69	4.85	0.010	461.9	49.79	235.8	3.66	3.46	3.78
07/25/2019 07:58	14.64	2.91	2.74	4.84	0.010	461.2	49.86	234.7	3.38	3.19	3.44
07/25/2019 07:59	14.66	3.59	3.39	6.30	0.013	461.3	49.79	235.5	3.26	3.08	3.34
07/25/2019 08:00	14.64	4.10	3.86	6.79	0.014	461.6	49.73	234.9	3.36	3.17	3.44
07/25/2019 08:01	14.66	3.04	2.87	5.33	0.011	461.6	49.81	235.7	3.47	3.28	3.59
07/25/2019 08:02	14.65	1.28	1.21	1.94	0.004	461.5	49.74	235.2	3.63	3.43	3.73
07/25/2019 08:03	14.66	1.18	1.12	1.94	0.004	460.8	49.89	235.2	3.78	3.57	3.87
07/25/2019 08:04	14.66	1.58	1.49	2.90	0.006	460.8	49.68	235.2	3.85	3.64	3.97
07/25/2019 08:05	14.65	2.48	2.34	4.36	0.009	461.3	49.77	235.1	3.83	3.62	3.92
07/25/2019 08:06	14.66	2.58	2.44	4.36	0.009	461.4	49.83	235.6	3.84	3.63	3.92
07/25/2019 08:07	14.66	2.57	2.43	4.35	0.009	460.4	49.95	235.0	3.92	3.71	4.01
07/25/2019 08:08	14.66	2.51	2.37	4.35	0.009	460.8	49.78	235.2	3.98	3.76	4.06
07/25/2019 08:09	14.65	2.38	2.25	3.88	0.008	461.6	49.65	235.3	4.07	3.84	4.17
07/25/2019 08:10	14.65	2.25	2.12	3.87	0.008	461.1	49.91	235.0	4.08	3.85	4.16
07/25/2019 08:11	14.66	2.24	2.12	3.88	0.008	461.3	49.81	235.5	3.92	3.71	4.02
07/25/2019 08:12	14.67	2.23	2.11	3.87	0.008	460.9	49.55	235.7	3.85	3.65	3.97
07/25/2019 08:13	14.65	2.24	2.11	3.87	0.008	460.7	49.83	234.8	4.02	3.79	4.11
07/25/2019 08:14	14.65	2.25	2.12	3.87	0.008	460.3	49.67	234.6	4.05	3.82	4.16
07/25/2019 08:15	14.65	2.27	2.14	3.86	0.008	459.1	49.74	234.0	3.98	3.76	4.05
07/25/2019 08:16	14.66	2.31	2.18	3.86	0.008	459.0	49.71	234.4	3.93	3.72	4.00
07/25/2019 08:17	14.66	2.35	2.22	3.85	0.008	458.9	49.66	234.3	3.91	3.70	4.00
07/25/2019 08:18	14.67	2.36	2.23	3.86	0.008	459.0	49.98	234.7	3.74	3.54	3.81
07/25/2019 08:19	14.66	2.38	2.25	3.85	0.008	458.4	49.58	234.0	3.53	3.34	3.61
07/25/2019 08:20	14.67	2.40	2.27	3.85	0.008	458.8	49.68	234.6	3.53	3.34	3.61
07/25/2019 08:21	14.67	2.39	2.26	3.86	0.008	459.1	49.73	234.8	3.55	3.36	3.62
07/25/2019 08:22	14.66	2.37	2.24	3.86	0.008	459.2	49.74	234.5	3.56	3.37	3.66
07/25/2019 08:23	14.66	2.33	2.20	3.86	0.008	459.6	49.70	234.6	3.49	3.30	3.57
07/25/2019 08:24	14.65	2.31	2.18	3.86	0.008	459.4	49.77	234.2	3.47	3.28	3.52
07/25/2019 08:25	14.66	2.31	2.18	3.86	0.008	459.8	49.81	234.7	3.47	3.28	3.57
07/25/2019 08:26	14.66	2.30	2.17	3.86	0.008	459.9	49.80	234.8	3.46	3.27	3.53
07/25/2019 08:27	14.66	2.29	2.17	3.86	0.008	459.7	49.64	234.7	3.42	3.23	3.52
07/25/2019 08:28	14.65	2.28	2.15	3.86	0.008	459.6	49.77	234.3	3.39	3.20	3.47
07/25/2019 08:29	14.66	2.29	2.17	3.86	0.008	459.8	49.76	234.7	3.53	3.34	3.62
07/25/2019 08:30	14.65	2.30	2.17	3.86	0.008	459.9	49.96	234.4	3.59	3.39	3.67
07/25/2019 08:31	14.65	2.30	2.17	3.86	0.008	460.0	49.67	234.5	3.47	3.28	3.53
07/25/2019 08:32	14.65	2.30	2.17	3.86	0.008	459.9	49.86	234.4	3.32	3.13	3.38
07/25/2019 08:33	14.67	2.29	2.17	3.86	0.008	459.9	49.59	235.2	3.32	3.14	3.43
07/25/2019 08:34	14.67	2.28	2.16	3.87	0.008	460.2	49.89	235.3	3.32	3.14	3.43
07/25/2019 08:35	14.66	2.27	2.15	3.86	0.008	460.1	49.74	234.9	3.31	3.13	3.38

1-NH3-42

Period Start:	Average 2_O2 %	Average 2_NOXPPM ppm	Average 2_NOX_COBR ppm	Average 2_NOX_LBHR #/hr	Average 2_NOX_LBMM #/MMBTU	Average 2_GasFlow kscfh	Average 2_LOAD MW	Average 2_STACKFIM kscfm	Average 2_COPPM ppm	Average 2_CO_CORR ppm	Average 2_CO_LBHR #/hr
07/25/2019 08:36	14.66	2.25	2.13	3.87	0.008	460.7	50.11	235.2	3.34	3.16	3.43
07/25/2019 08:37	14.66	2.24	2.12	3.87	0.008	460.6	49.66	235.1	3.39	3.21	3.48
07/25/2019 08:38	14.65	2.24	2.11	3.87	0.008	460.8	49.76	234.9	3.39	3.20	3.48
07/25/2019 08:39	14.67	2.25	2.13	3.87	0.008	460.9	49.49	235.7	3.37	3.19	3.48
07/25/2019 08:40	14.67	2.25	2.13	3.87	0.008	460.5	49.78	235.5	3.37	3.19	3.48
07/25/2019 08:41	14.67	2.28	2.16	3.87	0.008	460.7	49.72	235.6	3.39	3.21	3.48
07/25/2019 08:42	14.66	2.36	2.23	3.87	0.008	460.3	49.42	235.0	3.43	3.24	3.53
07/25/2019 08:43	14.67	2.43	2.30	3.87	0.008	460.8	49.79	235.6	3.42	3.24	3.53
07/25/2019 08:44	14.66	2.44	2.31	4.36	0.009	461.1	49.65	235.4	3.44	3.25	3.53
07/25/2019 08:45	14.65	2.44	2.30	3.87	0.008	460.9	49.78	234.9	3.47	3.28	3.53
07/25/2019 08:46	14.66	2.46	2.33	4.35	0.009	460.6	49.64	235.1	3.50	3.31	3.58
07/25/2019 08:47	14.67	2.44	2.31	4.35	0.009	460.8	49.76	235.6	3.48	3.30	3.53
07/25/2019 08:48	14.67	2.42	2.29	3.87	0.008	461.0	49.82	235.8	3.45	3.27	3.58
07/25/2019 08:49	14.67	2.41	2.28	3.87	0.008	461.0	49.78	235.8	3.47	3.29	3.58
07/25/2019 08:50	14.67	2.42	2.29	3.87	0.008	460.8	49.80	235.6	3.52	3.33	3.63
07/25/2019 08:51	14.67	2.43	2.30	3.87	0.008	460.8	49.71	235.6	3.70	3.50	3.82
07/25/2019 08:52	14.66	2.43	2.30	3.88	0.008	461.8	49.76	235.8	3.89	3.68	4.02
Daily Average*	14.66	2.40	2.27	4.05	0.008	460.6	49.76	235.1	3.63	3.43	3.72
Maximum*	14.67	4.10	3.86	6.79	0.014	462.6	50.11	235.8	4.13	3.90	4.21
07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019
Minimum*	14.64	1.18	1.12	1.94	0.004	458.4	49.42	234.0	3.26	3.08	3.34
07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019
8:00	8:00	8:03	8:03	8:03	8:03	8:19	8:42	8:19	7:59	7:59	7:59

* Does not include Invalid Averaging Periods ("N/A")

Average Values Report

Generated: 7/25/2019 13:11

Company: City Of Anaheim
Plant: 3071 Miraloma Ave.,
City/St: Anaheim, CA, 92806
Source: unit2

Period Start: 7/25/2019 11:41
Period End: 7/25/2019 12:46
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

W002AS-543378-RT-222

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Period Start:	Average 2_O2 %	Average 2_NOXPPM ppm	Average 2_NOX_CORR ppm	Average 2_NOX_LBHR #/hr	Average 2_NOX_LBMM #/MBO	Average 2_GasFlow kscfm	Average 2_LOAD MW	Average 2_STACKFLOW kscfm	Average 2_COPPM ppm	Average 2_CO_CORR ppm	Average 2_CO_LBHR #/hr
07/25/2019 11:41	14.64	2.20	2.07	3.88	0.008	462.5	49.88	235.4	3.73	3.57	3.88
07/25/2019 11:42	14.63	2.18	2.05	3.89	0.008	462.9	49.63	235.2	3.71	3.49	3.79
07/25/2019 11:43	14.64	2.18	2.05	3.89	0.008	462.8	49.81	235.5	3.72	3.41	3.74
07/25/2019 11:44	14.64	2.22	2.09	3.89	0.008	463.2	49.65	235.7	3.76	3.37	3.70
07/25/2019 11:45	14.64	2.30	2.17	3.89	0.008	462.9	49.93	235.5	3.84	3.43	3.74
07/25/2019 11:46	14.64	2.32	2.19	3.88	0.008	462.4	49.60	235.3	3.80	3.68	3.98
07/25/2019 11:47	14.65	2.33	2.20	3.88	0.008	462.3	49.45	235.6	3.77	3.89	4.22
07/25/2019 11:48	14.65	2.33	2.20	3.89	0.008	462.8	49.65	235.9	3.76	4.01	4.37
07/25/2019 11:49	14.64	2.33	2.20	3.89	0.008	463.1	49.63	235.7	3.80	3.86	4.23
07/25/2019 11:50	14.65	2.36	2.23	3.89	0.008	462.9	49.71	235.9	3.74	3.57	3.89
07/25/2019 11:51	14.64	2.45	2.31	4.38	0.009	463.2	49.93	235.7	3.77	3.17	3.45
07/25/2019 11:52	14.64	2.50	2.36	4.38	0.009	463.1	49.73	235.7	3.77	2.97	3.26
07/25/2019 11:53	14.65	2.51	2.37	4.38	0.009	463.3	49.79	236.2	3.74	2.91	3.16
07/25/2019 11:54	14.65	2.50	2.36	4.37	0.009	462.5	49.69	235.7	3.84	2.91	3.16
07/25/2019 11:55	14.64	2.50	2.36	4.37	0.009	462.6	49.68	235.4	3.77	2.92	3.21
07/25/2019 11:56	14.64	2.50	2.36	4.37	0.009	462.3	50.00	235.3	3.77	2.95	3.20
07/25/2019 11:57	14.65	2.50	2.36	4.37	0.009	462.7	49.96	235.8	3.77	3.03	3.30
07/25/2019 11:58	14.65	2.48	2.34	4.37	0.009	462.9	49.93	235.9	3.76	3.08	3.35
07/25/2019 11:59	14.64	2.48	2.34	4.37	0.009	462.6	49.63	235.4	3.77	3.03	3.30
07/25/2019 12:00	14.64	2.50	2.36	4.37	0.009	462.2	49.91	235.2	3.74	3.00	3.25
07/25/2019 12:01	14.64	2.50	2.36	4.37	0.009	462.9	49.61	235.2	3.77	3.07	3.35
07/25/2019 12:02	14.64	2.49	2.35	4.37	0.009	462.1	49.61	235.2	3.77	3.10	3.40
07/25/2019 12:03	14.64	2.50	2.36	4.37	0.009	462.3	49.83	235.3	3.77	3.16	3.45
07/25/2019 12:04	14.64	2.52	2.38	4.37	0.009	462.8	49.57	235.5	3.67	3.39	3.69
07/25/2019 12:05	14.64	2.50	2.36	4.37	0.009	462.8	49.74	235.5	3.74	3.52	3.84
07/25/2019 12:06	14.64	2.49	2.35	4.37	0.009	462.9	49.73	235.5	3.74	3.52	3.84
07/25/2019 12:07	14.64	2.47	2.33	4.38	0.009	463.7	50.01	236.0	3.74	3.52	3.85
07/25/2019 12:08	14.63	2.46	2.31	4.38	0.009	464.0	49.77	235.8	3.74	3.71	4.04
07/25/2019 12:09	14.62	2.47	2.32	4.39	0.009	464.5	49.79	235.6	3.75	3.62	3.95
07/25/2019 12:10	14.63	2.49	2.34	4.38	0.009	463.8	49.76	235.7	3.74	3.33	3.65
07/25/2019 12:11	14.63	2.55	2.40	4.38	0.009	463.5	49.69	235.5	3.74	3.07	3.36
07/25/2019 12:12	14.63	2.58	2.43	4.38	0.009	464.0	49.70	235.8	3.77	2.98	3.26
07/25/2019 12:13	14.64	2.60	2.45	4.39	0.009	464.2	49.90	236.2	3.09	2.90	3.17
07/25/2019 12:14	14.64	2.62	2.47	4.39	0.009	464.2	49.64	236.2	3.09	2.83	3.07
07/25/2019 12:15	14.64	2.60	2.45	4.38	0.009	463.9	49.91	236.1	3.09	2.83	3.07
07/25/2019 12:16	14.64	2.60	2.45	4.38	0.009	464.0	49.78	236.1	3.09	2.85	3.12
07/25/2019 12:17	14.64	2.57	2.42	4.39	0.009	464.2	49.68	236.2	3.07	2.89	3.17
07/25/2019 12:18	14.63	2.55	2.40	4.39	0.009	464.4	49.64	236.3	3.07	2.92	3.17
07/25/2019 12:19	14.64	2.55	2.40	4.39	0.009	464.9	49.98	236.2	3.07	2.97	3.27
07/25/2019 12:20	14.63	2.55	2.40	4.40	0.009	465.3	49.91	236.8	3.07	2.97	3.27
07/25/2019 12:21	14.64	2.54	2.39	4.39	0.009	464.7	49.72	236.1	3.07	2.90	3.17
07/25/2019 12:22	14.63	2.54	2.39	4.39	0.009	464.1	49.68	235.4	3.08	2.89	3.17
07/25/2019 12:23	14.62	2.56	2.41	4.39	0.009	464.3	49.80	235.5	3.08	2.89	3.17
07/25/2019 12:24	14.62	2.61	2.45	4.39	0.009	464.8	49.74	236.1	3.11	3.11	3.41
07/25/2019 12:25	14.63	2.71	2.55	4.39	0.010	464.9	49.74	236.2	3.10	3.10	3.37
07/25/2019 12:26	14.63	2.84	2.67	4.88	0.010	464.9	49.74	236.2	3.10	3.10	3.37
07/25/2019 12:27	14.63	2.82	2.65	4.88	0.010	464.7	49.86	236.1	2.75	2.75	3.02
07/25/2019 12:28	14.63	2.78	2.62	4.88	0.010	465.1	49.98	236.3	2.75	2.63	2.88
07/25/2019 12:29	14.62	2.80	2.63	4.88	0.010	465.1	49.83	236.0	2.75	2.66	2.93

2-NH3-42

Period Start:	Average 2_O2 %	Average 2_NOXPTM ppm	Average 2_NOX_CORR ppm	Average 2_NOX_LBHR #/hr	Average 2_NOX_LBMT #/MBTU	Average 2_GasFlow kscfh	Average 2_LOAD MW	Average 2_STACKFLW kscfm	Average 2_COPPM ppm	Average 2_CO_CORR ppm	Average 2_CO_LBHR #/hr
07/25/2019 12:30	14.63	2.76	2.60	4.89	0.010	465.3	49.87	236.4	2.84	2.67	2.93
07/25/2019 12:31	14.61	2.82	2.65	4.88	0.010	464.6	49.95	235.3	2.85	2.67	2.93
07/25/2019 12:32	14.62	2.82	2.65	4.87	0.010	464.2	49.90	235.5	2.90	2.72	2.97
07/25/2019 12:33	14.63	2.82	2.65	4.89	0.010	465.2	49.73	236.4	2.98	2.80	3.08
07/25/2019 12:34	14.62	2.83	2.66	4.88	0.010	464.6	49.71	235.7	3.05	2.87	3.12
07/25/2019 12:35	14.63	2.77	2.61	4.88	0.010	464.4	49.63	235.9	3.03	2.85	3.12
07/25/2019 12:36	14.62	2.86	2.69	4.88	0.010	465.1	49.76	236.0	3.06	2.87	3.13
07/25/2019 12:37	14.63	2.87	2.70	4.87	0.010	463.8	49.87	235.7	3.03	2.85	3.12
07/25/2019 12:38	14.63	2.78	2.62	4.88	0.010	464.3	49.87	235.9	3.05	2.87	3.12
07/25/2019 12:39	14.63	2.83	2.66	4.88	0.010	464.6	49.67	236.0	3.15	2.96	3.22
07/25/2019 12:40	14.63	2.81	2.64	4.88	0.010	464.5	49.91	236.0	3.41	3.21	3.51
07/25/2019 12:41	14.63	2.78	2.62	4.88	0.010	465.1	49.69	236.3	3.34	3.14	3.47
07/25/2019 12:42	14.63	2.82	2.65	4.88	0.010	464.9	49.93	236.2	3.13	2.95	3.22
07/25/2019 12:43	14.63	2.66	2.50	4.39	0.009	464.7	49.88	236.1	3.00	2.82	3.07
07/25/2019 12:44	14.62	2.40	2.25	3.91	0.008	465.2	49.71	236.0	3.30	3.10	3.42
07/25/2019 12:45	14.62	2.07	1.94	3.42	0.007	464.9	49.73	235.8	3.52	3.31	3.61
07/25/2019 12:46	14.62	1.95	1.83	3.42	0.007	465.3	49.84	236.1	3.51	3.30	3.62
Daily Average*	14.63	2.55	2.40	4.40	0.009	463.8	49.78	235.8	3.31	3.12	3.40
Maximum*	14.65	2.87	2.70	4.89	0.010	465.3	50.01	236.8	4.25	4.01	4.37
	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019
Minimum*	11.58	12:37	12:37	12:33	12:42	12:46	12:07	12:21	11:48	11:48	11:48
	14.61	1.95	1.83	3.42	0.007	462.1	49.45	235.2	2.79	2.63	2.88
	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019	07/25/2019
	12:31	12:46	12:46	12:46	12:46	12:02	11:47	12:02	12:28	12:28	12:28

* Does not include Invalid Averaging Periods ("N/A")

APPENDIX C CALCULATIONS

Appendix C.1

General Emissions Calculations

GENERAL EMISSION CALCULATIONS

I. Stack Gas Velocity

A. Stack gas molecular weight, lb/lb-mole

$$MW_{dry} = 0.44 * \%CO_2 + 0.32 * \%O_2 + 0.28 * \%N_2$$

$$MW_{wet} = MW_{dry} * (1 - B_{wo}) + 18 * B_{wo}$$

B. Absolute stack pressure, iwg

$$P_s = P_{bar} + \frac{P_{sg}}{13.6}$$

C. Stack gas velocity, ft/sec

$$V_s = 2.9 * C_p * \sqrt{\Delta P} * \sqrt{T_s} * \sqrt{\frac{29.92 * 28.95}{P_s * MW_{wet}}}$$

II. Moisture

A. Sample gas volume, dscf

$$V_{mstd} = 0.03342 * V_m * (P_{bar} + \frac{\Delta H}{13.6}) * \frac{T_{ref}}{T_m} * Y_d$$

B. Water vapor volume, scf

$$V_{wstd} = 0.0472 * V_{lc} * \frac{T_{ref}}{528 ^\circ R}$$

C. Moisture content, dimensionless

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

III. Stack gas volumetric flow rate

A. Actual stack gas volumetric flow rate, wacfm

$$Q = V_s * A_s * 60$$

B. Standard stack gas flow rate, dscfm

$$Q_{sd} = Q * (1 - B_{wo}) * \frac{T_{ref}}{T_s} * \frac{P_s}{29.92}$$

IV. Gaseous Mass Emission Rates, lb/hr

$$M = \frac{\text{ppm} * MW_i * Q_{sd} * 60}{SV * 10^6}$$

V. Emission Rates, lb/MMBtu

$$\frac{\text{lb}}{\text{MMBtu}} = \frac{\text{ppm} * MW_i * F}{SV * 10^6} * \frac{20.9}{20.9 - \%O_2}$$

VI. Percent Isokinetic

$$I = \frac{17.32 * T_s (V_{mstd})}{(1-Bwo) * 0 * V_s * P_s * Dn2} * \frac{520^{\circ}R}{T_{ref}}$$

VII. Particulate emissions

(a) Grain loading, gr/dscf
 $C = 0.01543 (M_n/V_{mstd})$

(b) Grain loading at 12% CO₂, gr/dscf
 $C_{12\% CO_2} = C (12/\% CO_2)$

(c) Mass emissions, lb/hr
 $M = C * Q_{sd} * (60 \text{ min/hr}) / (7000 \text{ gr/lb})$

(d) Particulate emission factor
 $\text{lb}/10^6 \text{ Btu} = C * \frac{1 \text{ lb}}{7000 \text{ gr}} * F * \frac{20.9}{20.9 - \% O_2}$

Nomenclature:

A_s	= stack area, ft ²
B_{wo}	= flue gas moisture content, dimensionless
$C_{12\%CO_2}$	= particulate grain loading, gr/dscf corrected to 12% CO ₂
C	= particulate grain loading, gr/dscf
C_p	= pitot calibration factor, dimensionless
D_n	= nozzle diameter, in.
F	= fuel F-Factor, dscf/MMBtu @ 0% O ₂
H	= orifice differential pressure, iwg
I	= % isokinetics
M_n	= mass of collected particulate, mg
M_i	= mass emission rate of specie i, lb/hr
MW	= molecular weight of flue gas, lb/lb-mole
M_{wi}	= molecular weight of specie i:
	SO ₂ : 64
	NO _x : 46
	CO: 28
	HC: 16
t	= sample time, min.
ΔP	= average velocity head, iwg = $(\sqrt{\Delta P})^2$
P_{bar}	= barometric pressure, inches Hg
P_s	= stack absolute pressure, inches Hg
P_{sg}	= stack static pressure, iwb
Q	= wet stack flow rate at actual conditions, wacfm
Q_{sd}	= dry standard stack flow rate, dscfm
SV	= specific molar volume of an ideal gas at standard conditions, ft ³ /lb-mole
T_m	= meter temperature, °R
T_{ref}	= reference temperature, °R
T_s	= stack temperature, °R
V_s	= stack gas velocity, ft/sec
V_{lc}	= volume of liquid collected in impingers, ml
V_m	= uncorrected dry meter volume, dcf
V_{mstd}	= dry meter volume at standard conditions, dscf
V_{wstd}	= volume of water vapor at standard conditions, scf
Y_d	= meter calibration coefficient

Appendix C.2

Spreadsheet Summaries

SCAQMD 207.1 EXAMPLE CALCULATION

TEST NUMBER: 1-NH3-U2

Identifier	Description	Units	Equation	Value
A	Reference Temperature	F	--	60
B	Reference Temperature	R	$A + 460$	520
C	Meter Calibration Factor (Yd)	--	--	1.011
D	Barometric Pressure	" Hg	--	29.66
E	Meter Volume	acf	--	47.104
F	Meter Temperature	F	--	72.9
G	Meter Temperature	R	$F + 460$	532.9
H	Delta H	" H ₂ O	--	2.0
I	Meter Volume (standard)	dscf	$0.03342 * E * (D + H/13.6) * B/G * C$	46.291
J	Liquid Collected	grams	--	135.9
K	Water vapor volume	scf	$0.0472 * J * B/528$	6.317
L	Moisture Content	--	$K/(K + I)$	0.120
M	Gas Constant	ft-lbf/lb-mole-R	--	1545.33
N	Specific Molar Volume	SCF/lb-mole	$385.3 * B / 528$	379.5
O	F-Factor	dscf/MMBtu	--	8,710
P	HHV	Btu/SCF	--	1,050
Q	Mass Conversion Factor	lb/ug	--	2.2046E-09
R	O ₂ Correction Factor	--	--	15
S	Stack Flow Rate @ 68 F	dscfm	--	235,100
T	Stack Flow Rate @ Tref	dscfm	$S * B/528$	231,538
U	Mass NH ₃	ug	--	1,983
V	Mass NH ₃	lb	$U * Q$	4.37E-06
W	MW of NH ₃	lb/lb-mole	--	17.03
X	NH ₃	ppm	$(V * N * 10^9)/(I * W)$	2.1
Y	Flue Gas O ₂	%	--	14.66
Z	NH ₃	ppmc	$X * (20.9 - R)/(20.9 - Y)$	2.0
AA	NH ₃	lb/hr	$X * T * W * 60/(N * 10^9)$	1.3
AB	NH ₃	lb/MMBtu	$(X * W * O)/(385.3 * 10^9) * 20.9/(20.9 - Y)$	0.003
AC	NH ₃	lb/MMSCF	$AB * P$	2.8

Note:

(1) Some values may be slightly different from those shown on the run sheets due to round off errors. This page is intended to show the calculation methodology only.

SCAQMD METHOD 207.1 DATA WORKSHEET AND SUMMARY

Facility.....	Canyon		Parameter.....		NH₃
Unit.....	U2		Fuel.....		Natural gas
Sample Location.....	Stack		Data By.....		SD
Test Number.....	1-NH3-U2	2-NH3-U2	Average	Maximum	Limit
Reference Temperature (°F).....	60	60			
Test Date.....	7/25/2019	7/25/2019			
Test Method.....	SCAQMD 207.1	SCAQMD 207.1			
Sample Train.....	19-WCS	19-WCS			
Meter Calibration Factor.....	1.011	1.011			
Stack Area (ft ²).....	106.90	106.90			
Sample Time (Minutes).....	60	60			
Barometric Pressure ("Hg).....	29.66	29.66			
Start/Stop Time	0746/0852	1140/1246			
Meter Volume (acf).....	47.104	47.704			
Meter Temperature (°F).....	72.9	85.1			
Meter Pressure (iwg).....	2.0	2.0			
Liquid Volume (ml).....	135.9	134.8			
Stack O ₂ (%).....	14.66	14.63	14.65	(from facility CEMS)	
Unit Load (MW).....	50	50	49.8		
Standard Sample Volume (SCF).....	46.291	45.831			
Moisture Fraction.....	0.120	0.120			
Stack Flow Rate (dscfm, 68 °F).....	235,100	235,800	235,450	(from facility CEMS)	
Stack Flow Rate (@ Tref).....	231,538	232,227	231,883		
Gas Constant (ft-lbf/lb-mole-R).....	1545.33	1545.33			
Molecular Weight NH ₃ (lb/lb-mole).....	17.03	17.03			
Specific Molar Volume (ft ³ /lb-mole)....	379.5	379.5			
F-Factor (dscf/MMBtu).....	8,710	8,710			
HHV(Btu/SCF).....	1,050	1,050			
Mass Conversion (lb/ug).....	2.2046E-09	2.2046E-09			
O ₂ Correction Factor (%).....	15	15			
Mass NH ₃ (ug).....	1,983	1,707			
Mass NH ₃ (lb).....	4.37E-06	3.76E-06			
NH ₃ (ppmv, flue gas).....	2.1	1.8	2.0	2.1	
NH ₃ (ppmv @ O ₂ Correction Factor)...	2.0	1.7	1.9	2.0	5
NH ₃ (lb/hr).....	1.3	1.1	1.2	1.3	
NH ₃ (lb/MMBtu).....	0.003	0.002	0.003	0.003	
NH ₃ (lb/MMSCF).....	2.8	2.5	2.7	2.8	

Note: SCAQMD Method 207.1 requires the higher of the duplicate runs be reported as the test result.

APPENDIX D QUALITY ASSURANCE

Appendix D.1

Quality Assurance Program Summary

QUALITY ASSURANCE PROGRAM SUMMARY

As part of Montrose Air Quality Services, LLC (MAQS) ASTM D7036-04 certification, MAQS is committed to providing emission related data which is complete, precise, accurate, representative, and comparable. MAQS quality assurance program and procedures are designed to ensure that the data meet or exceed the requirements of each test method for each of these items. The quality assurance program consists of the following items:

- Assignment of an Internal QA Officer
- Development and use of an internal QA Manual
- Personnel training
- Equipment maintenance and calibration
- Knowledge of current test methods
- Chain-of-custody
- QA reviews of test programs

Assignment of an Internal QA Officer: MAQS has assigned an internal QA Officer who is responsible for administering all aspects of the QA program.

Internal Quality Assurance Manual: MAQS has prepared a QA Manual according to the requirements of ASTM D7036-04 and guidelines issued by EPA. The manual documents and formalizes all of MAQS QA efforts. The manual is revised upon periodic review and as MAQS adds capabilities. The QA manual provides details on the items provided in this summary.

Personnel Testing and Training: Personnel testing and training is essential to the production of high quality test results. MAQS training programs include:

- A requirement for all technical personnel to read and understand the test methods performed
- A requirement for all technical personnel to read and understand the MAQS QA manual
- In-house testing and training
- Quality Assurance meetings
- Third party testing where available
- Maintenance of training records.

Equipment Maintenance and Calibration: All laboratory and field equipment used as a part of MAQS emission measurement programs is maintained according to manufacturer's recommendations. A summary of the major equipment maintenance schedules is summarized in Table 1. In addition to routine maintenance, calibrations are performed on all sampling equipment according to the procedures outlined in the applicable test method. The calibration intervals and techniques for major equipment components is summarized in Table 2. The calibration technique may vary to meet regulatory agency requirements.

Knowledge of Current Test Methods: MAQS maintains current copies of EPA, ARB, and SCAQMD Source Test Manuals and Rules and Regulations.

Chain-of-Custody: MAQS maintains chain-of-custody documentation on all data sheets and samples. Samples are stored in a locked area accessible only to MAQS source test personnel. Data sheets are kept in the custody of the originator, program manager, or in locked storage until return to MAQS office. Electronic field data is duplicated for backup on secure storage media. The original data sheets are used for report preparation and any additions are initialed and dated.

QA Reviews: Periodic field, laboratory, and report reviews are performed by the in-house QA coordinator. Periodically, test plans are reviewed to ensure proper test methods are selected and reports are reviewed to ensure that the methods were followed and any deviations from the methods are justified and documented.

ASTM D7036-04 Required Information

Uncertainty Statement

Montrose is qualified to conduct this test program and has established a quality management system that led to accreditation with ASTM Standard D7036-04 (Standard Practice for Competence of Air Emission Testing Bodies). Montrose participates in annual functional assessments for conformance with D7036-04 which are conducted by the American Association for Laboratory Accreditation (A2LA). All testing performed by Montrose is supervised on site by at least one Qualified Individual (QI) as defined in D7036-04 Section 8.3.2. Data quality objectives for estimating measurement uncertainty within the documented limits in the test methods are met by using approved test protocols for each project as defined in D7036-04 Sections 7.2.1 and 12.10. Additional quality assurance information is presented in the report appendices.

Performance Data

Performance data are available for review.

Qualified Personnel

A qualified individual (QI), defined by performance on a third party or internal test on the test methods, will be present on each test event.

Plant Entry and Safety Requirements

Plant Entry

All test personnel are required to check in with the guard at the entrance gate or other designated area. Specific details are provided by the facility and project manager.

Safety Requirements

All personnel shall have the following personal protective equipment (PPE) and wear them where designated:

- Hard Hat
- Safety Glasses
- Steel Toe Boots
- Hearing Protection
- Gloves
- High Temperature Gloves (if required)

The following safety measures will be followed:

- Good housekeeping
- SDS for all on-site hazardous materials
- Confine selves to necessary areas (stack platform, mobile laboratory, CEMS data acquisition system, control room, administrative areas)
- Knowledge of evacuation procedures

Each facility will provide plant specific safety training.

TABLE 1
EQUIPMENT MAINTENANCE SCHEDULE

Equipment	Acceptance Limits	Frequency of Service	Methods of Service
Pumps	1. Absence of leaks 2. Ability to draw manufacturers required vacuum and flow	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Replace parts 4. Leak check
Flow Meters	1. Free mechanical movement	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Calibrate
Sampling Instruments	1. Absence of malfunction 2. Proper response to zero span gas	As recommended by manufacturer	As recommended by manufacturer
Integrated Sampling Tanks	1. Absence of leaks	Depends on nature of use	1. Steam clean 2. Leak check
Mobil Van Sampling System	1. Absence of leaks	Depends on nature of use	1. Change filters 2. Change gas dryer 3. Leak check 4. Check for system contamination
Sampling lines	1. Sample degradation less than 2%	After each test series	1. Blow dry, inert gas through line until dry

TABLE 2
MAJOR SAMPLING EQUIPMENT CALIBRATION REQUIREMENTS

Sampling Equipment	Calibration Frequency	Calibration Procedure	Acceptable Calibration Criteria
Continuous Analyzers	Before and After Each Test Day	3-point calibration error test	< 2% of analyzer range
Continuous Analyzers	Before and After Each Test Run	2-point sample system bias check	< 5% of analyzer range
Continuous Analyzers	After Each Test Run	2-point analyzer drift determination	< 3% of analyzer range
CEMS System	Beginning of Each Day	leak check	< 1 in. Hg decrease in 5 min. at > 20 in. Hg
Continuous Analyzers	Semi-Annually	3-point linearity	< 1% of analyzer range
NO _x Analyzer	Daily	NO ₂ -> NO converter efficiency	> 90%
Differential Pressure Gauges (except for manometers)	Semi-Annually	Correction factor based on 5-point comparison to standard	+/- 5%
Differential Pressure Gauges (except for manometers)	Bi-Monthly	3-point comparison to standard, no correction factor	+/- 5%
Barometer	Semi-Annually	Adjusted to mercury-in-glass or National Weather Service Station	+/- 0.1 inches Hg
Dry Gas Meter	Semi-Annually	Calibration check at 4 flow rates using a NIST traceable standard	+/- 2%
Dry Gas Meter	Bi-Monthly	Calibration check at 2 flow rates using a NIST traceable standard	+/- 2% of semi-annual factor
Dry Gas Meter Orifice	Annually	4-point calibration for $\Delta H@$	--
Temperature Sensors	Semi-Annually	3-point calibration vs. NIST traceable standard	+/- 1.5%

Note: Calibration requirements will be used that meet applicable regulatory agency requirements.

Appendix D.2

SCAQMD and STAC Certifications



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 • www.aqmd.gov

October 30, 2018

Mr. John Peterson
Montrose Air Quality Services, LLC
1631 E. Saint Andrew Place
Santa Ana, CA 92705

Subject: LAP Approval Notice
Reference # 96LA1220

Dear Mr. Peterson:

We have reviewed your renewal letter under the South Coast Air Quality Management District's Laboratory Approval Program (SCAQMD LAP). We are pleased to inform you that your firm is approved for the period beginning October 30, 2018, and ending September 30, 2019 for the following methods, subject to the requirements in the LAP Conditions For Approval Agreement and conditions listed in the attachment to this letter:

SCAQMD Methods 1-4	SCAQMD Methods 5.1, 5.2, 5.3, 6.1
SCAQMD Methods 10.1 and 100.1	SCAQMD Methods 25.1 and 25.3 (Sampling)
USEPA CTM-030 and ASTM D6522-00	SCAQMD Rule 1121/ 1146.2 Protocol
SCAQMD Rule 1420/1420.1/1420.2 – (Lead) Source and Ambient Sampling	

Your LAP approval to perform nitrogen oxide emissions compliance testing for SCAQMD Rule 1121/ 1146.2 Protocols includes satellite facilities located at:

McKenna Boiler
1510 North Spring Street
Los Angeles, CA 90012

Noritz America Corp.
11160 Grace Avenue
Fountain Valley, CA 92708

Ajax Boiler, Inc.
2701 S. Harbor Blvd.
Santa Ana, CA 92704

Thank you for participating in the SCAQMD LAP. Your cooperation helps us to achieve the goal of the LAP: to maintain high standards of quality in the sampling and analysis of source emissions. You may direct any questions or information to LAP Coordinator, Glenn Kasai. He may be reached by telephone at (909) 396-2271, or via e-mail at gkasai@aqmd.gov.

Sincerely,

A handwritten signature in black ink that reads "D. Sarkar".

Dipankar Sarkar
Program Supervisor
Source Test Engineering

DS:GK/gk

Attachment

181030 LapRenewalRev.doc

Cleaning the air that we breathe...™



American Association for Laboratory Accreditation

Accredited Air Emission Testing Body

A2LA has accredited

MONTROSE AIR QUALITY SERVICES

In recognition of the successful completion of the joint A2LA and Stack Testing Accreditation Council (STAC) evaluation process, this laboratory is accredited to perform testing activities in compliance with ASTM D7036:2004 - Standard Practice for Competence of Air Emission Testing Bodies.

Presented this 5th day of March 2018.



President and CEO
For the Accreditation Council
Certificate Number 3925.01
Valid to February 29, 2020

This accreditation program is not included under the A2LA ILAC Mutual Recognition Arrangement.

Appendix D.3

Individual QI Certificate

CERTIFICATE OF COMPLETION

Sean Donovan

This document certifies that this individual has passed a comprehensive examination and is now a Qualified Individual (QI) as defined in Section 8.3 of ASTM D7036-04 for the following method(s):

SCAQMD Method 207.1

Certificate Number: 002-2016-06

Tate Strickler

DATE OF ISSUE: 11/30/16

Tate Strickler, Accreditation Director

DATE OF
EXPIRATION: 11/30/21



APPENDIX E

APPLICABLE PERMIT SECTIONS



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions* And Requirements	Conditions
Process 1: POWER GENERATION					
GAS TURBINE, NO. 2, NATURAL GAS, GENERAL ELECTRIC, MODEL LM6000PC SPRINT, SIMPLE CYCLE, 479 MMBTU/HR AT 46 DEG F, WITH INLET CHILLING, WITH WATER INJECTION WITH A/N: 555829	D7	C9	NOX: MAJOR SOURCE**	CO: 4 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]; CO: 2000 PPMV NATURAL GAS (5) [RULE 407, 4-2-1982]; NOX: 2.5 PPMV NATURAL GAS (4) [RULE 2005, 6-3-2011]; NOX: 25 PPMV NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; PM10: 0.01 GRAINS/SCF NATURAL GAS (5A) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; PM10: 0.1 GRAINS/SCF NATURAL GAS (5) [RULE 409, 8-7-1981]; PM10: 1.67 LBS/HR NATURAL GAS (5C) [RULE 1303(b)(2)-Offset, 5-10-1996; RULE 1303(b)(2)-Offset, 12-6-2002]; PM10: 11 LBS/HR NATURAL GAS (5B) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; SO2: (9) [40CFR 72 - Acid Rain Provisions, 11-24-1997]; SOX: 0.06 LBS/MMBTU NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; VOC: 2 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A63.1, A99.1, A99.2, A99.3, A195.1, A195.2, A195.3, A327.1, B61.1, D12.1, D29.2, D29.3, D82.1, D82.2, E193.1, H23.1, I298.2, K40.1
GENERATOR, 50.95 MW					

- * (1) (1A) (1B) Denotes RECLAIM emission factor (2) (2A) (2B) Denotes RECLAIM emission rate
(3) Denotes RECLAIM concentration limit (4) Denotes BACT emission limit
(5) (5A) (5B) Denotes command and control emission limit (6) Denotes air toxic control rule limit
(7) Denotes NSR applicability limit (8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(9) See App B for Emission Limits (10) See section J for NESHAP/MACT requirements

** Refer to 40 CFR 60.473(b)(7) to determine the monitoring, record keeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions * And Requirements	Conditions
Process 1: POWER GENERATION					
CO OXIDATION CATALYST, NO. 2, BASF, 110 CUBIC FEET OF TOTAL CATALYST VOLUME A/N: 476657	C9	D7 C10			
SELECTIVE CATALYTIC REDUCTION, NO. 2, CORMETECH CMHT-21, 1012 CU.FT.; WIDTH: 2 FT 6 IN; HEIGHT: 25 FT 9 IN; LENGTH: 18 FT WITH A/N: 476657 AMMONIA INJECTION	C10	C9 S12		NH3: 5 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1) -BACT, 12-6-2002]	A195.5, D12.2, D12.3, D12.4, E179.1, E179.2, E193.1
STACK, TURBINE NO. 2, HEIGHT: 86 FT ; DIAMETER: 11 FT 8 IN A/N: 555829	S12	C10			

- * (1) (1A) (1B) Denotes RECLAIM emission factor
(3) Denotes RECLAIM concentration limit
(5) (5A) (5B) Denotes command and control emission limit
(7) Denotes NSR applicability limit
(9) See App B for Emission Limits

- (2) (2A) (2B) Denotes RECLAIM emission rate
(4) Denotes BACT emission limit
(6) Denotes air toxic control rule limit
(8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(10) See section J for NESHAP/MACT requirements

** Refer to section F and G of this permit to determine the monitoring, recordkeeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

[Devices subject to this condition : C4, C10, C16, C22]

- D12.5 The operator shall install and maintain a(n) non-resettable elapsed time meter to accurately indicate the elapsed operating time of the engine.

[**RULE 1110.2, 2-1-2008; RULE 1110.2, 9-7-2012; RULE 1303(b)(2)-Offset, 5-10-1996;**
RULE 1303(b)(2)-Offset, 12-6-2002; RULE 1401, 9-10-2010; RULE 1470, 5-4-2012;
RULE 2012, 5-6-2005; 40CFR 60 Subpart III, 1-30-2013]

[Devices subject to this condition : D25]

- D29.2 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Averaging Time	Test Location
NH3 emissions	District method 207.1 and 5.3 or EPA method 17	1 hour	Outlet of the SCR serving this equipment



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

The test(s) shall be conducted at least quarterly during the first twelve months of operation and at least annually thereafter. The AQMD shall be notified of the date and time of the test at least 10 days prior to the test.

If the turbine is not in operation during one calendar year, then no testing is required during that calendar year.

The NO_x concentration, as determined by the CEMS, shall be simultaneously recorded during the ammonia slip test. If the CEMS is inoperable, a test shall be conducted to determine the NO_x emissions using District Method 100.1 measured over a 60 minute averaging time period.

The test shall be conducted and the results submitted to the District within 60 days after the test date.

The test shall be conducted to demonstrate compliance with the Rule 1303 concentration limit.

[RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]

[Devices subject to this condition : D1, D7, D13, D19]

D29.3 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Sampling Time	Test Location
SOX emissions	AQMD Laboratory Method 307-91	Not Applicable	Fuel sample
VOC emissions	District Method 25.3	1 hour	Outlet of the SCR serving this equipment
PM emissions	District method 5.1	4 hours	Outlet of the SCR serving this equipment

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If you have any questions, please contact one of the following individuals by email or phone.

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**TEST REPORT FOR
AMMONIA SLIP TEST
AT CANYON POWER PLANT UNIT 3
FACILITY ID: 153992, DEVICE ID: D13**

Prepared For:

Canyon Power Plant
3071 E. Mira Loma Avenue
Anaheim, California 92806

For Submittal To:

South Coast Air Quality Management District
21865 Copley Drive
Diamond Bar, California 91765-4178

Prepared By:

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Sean Donovan

Test Date: **October 15, 2019**
Production Date: **October 30, 2019**
Report Number: **W002AS-543385-RT-501**



CONFIDENTIALITY STATEMENT

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REVIEW AND CERTIFICATION

All work, calculations, and other activities and tasks performed and presented in this document were carried out by me or under my direction and supervision. I hereby certify that, to the best of my knowledge, Montrose operated in conformance with the requirements of the Montrose Quality Management System and ASTM D7036-04 during this test project.

Signature: Sean Donovan Date: 10/30/2019

Name: Sean Donovan Title: Client Project Manager

I have reviewed, technically and editorially, details, calculations, results, conclusions, and other appropriate written materials contained herein. I hereby certify that, to the best of my knowledge, the presented material is authentic, accurate, and conforms to the requirements of the Montrose Quality Management System and ASTM D7036-04.

Signature: Michael Chowsanitphon Date: 10/30/2019

Name: Michael Chowsanitphon Title: Reporting Manager

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1.0 INTRODUCTION AND SUMMARY

Montrose Air Quality Services, LLC (MAQS) was contracted the Canyon Power Plant to perform an ammonia slip test at Unit 3 as required by the facility Permit (Facility ID 153992) Condition Number D29.2. This report documents the results of the ammonia slip tests performed on October 15, 2019. The test was performed by Sean Donovan, Allen Dusky, and Henry Lee. Sean Donovan was the on-site Qualified Individual for MAQS. Ms. Bertha Hernandez coordinated the test for Canyon Power Plant.

The test consisted of duplicate ammonia tests performed at 50 MW. The test program followed the procedures described in the initial compliance test protocol (MAQS document R038842). The results of the test are summarized in Table 1-1. The table shows that the ammonia slip from this unit was less than the permitted limit of 5 ppm corrected to 15% O₂.

**TABLE 1-1
AMMONIA SLIP TEST RESULTS SUMMARY
CANYON POWER PLANT UNIT 3
OCTOBER 15, 2019**

Parameter	Units	Result ⁽¹⁾	Limit
NH ₃	ppm	1.4	--
NH ₃	ppmc	1.3	5

(1) Maximum of duplicate runs, as required by SCAQMD Method 207.1

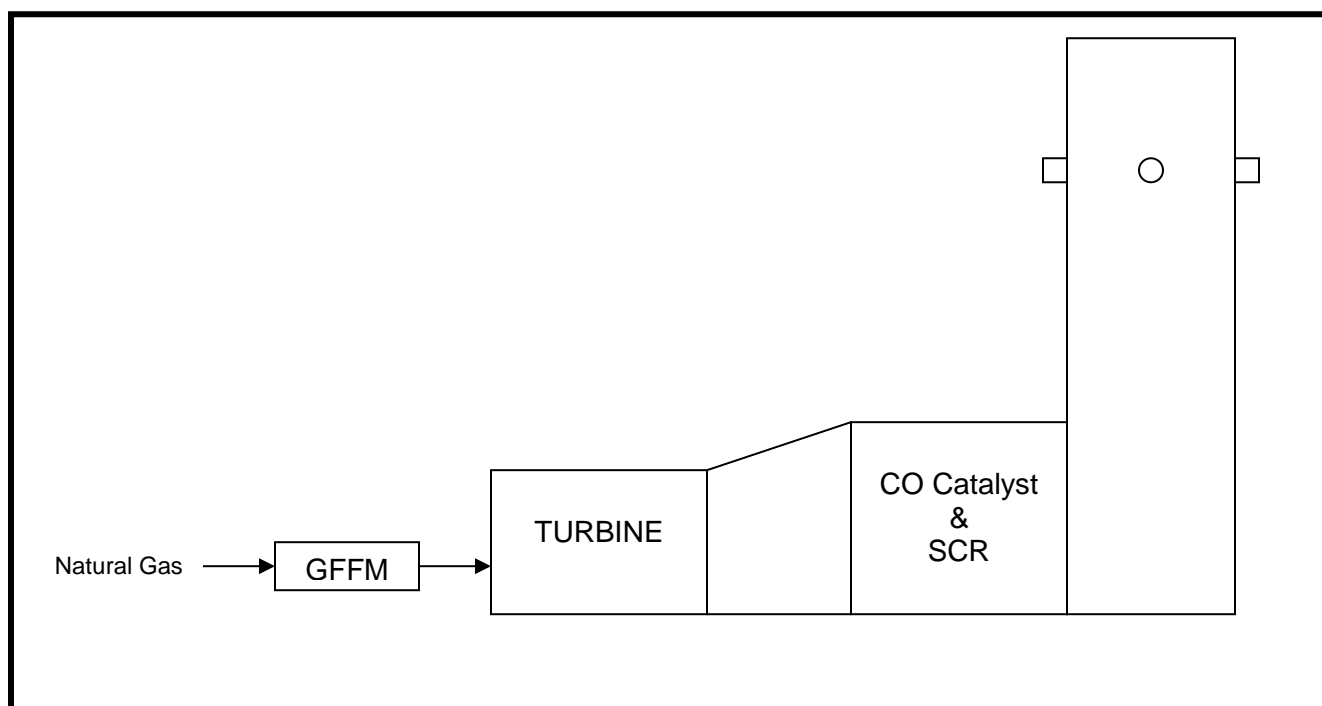
Section 2 of this document provides a brief description of the unit, test conditions, sample location, and CEMS. Details of the test procedures are provided in Section 3. Section 4 provides the results of each individual test. All raw data, calculations, quality assurance data, unit operating conditions, and CEMS data are provided in the appendices.

2.0 UNIT AND CEMS DESCRIPTION

2.1 UNIT DESCRIPTION

The City of Anaheim Canyon Power Plant is located at 3071 E. Mira Loma Avenue, Anaheim, California 92806. The facility consists of four identical generating units. Each unit consists of a natural gas fired, GE Model LM6000PC Sprint simple cycle, gas turbine. The units are natural gas fired with a rated heat input of 479 MMBtu per hour at 46°F, with water injection. The units are equipped with a CO catalyst and Selective Catalytic Reduction (SCR) system for NO_x control. Figure 2-1 presents a block diagram of the unit.

**FIGURE 2-1
UNIT BLOCK DIAGRAM
CANYON POWER PLANT**



Stack Inside Diameter:	11 feet, 8 inches
Distance from Upstream Disturbance:	23 feet, 4 inches (2.0 Diameters)
Distance from Stack Exit:	16 feet, 6 inches (1.4 Diameters)

2.2 TEST CONDITIONS

The tests were performed with the unit operating at an average load of 50 MW. Tests were performed while the unit was firing natural gas and operating under normal conditions. Unit operation was established by the Canyon Power Plant operators.

2.3 SAMPLE LOCATION

The measurements were made from sample ports located on the exhaust stack. There are four sample ports equally spaced at this location. The stack inside diameter at the sample plane is 11 feet, 8 inches. The sample ports are located 23 feet, 4 inches (2.0 diameters) downstream of the nearest flow disturbance and 16 feet, 6 inches (1.4 diameters) from the stack exit.

3.0 TEST DESCRIPTION

Flue gas samples were collected non-isokinetically using a SCAQMD Method 207.1 sample train. The samples were collected using a 12-point traverse at the exhaust stack location. Each test was performed over a 60 minute interval. The sample gas was drawn through a glass probe, Teflon sample line, two impingers each containing 100 ml of 0.1N H₂SO₄, an empty impinger, an impinger containing silica gel, and a dry gas meter. The optional nozzle and filter were not used since the source is natural gas fired. The contents of the sample line and the first three impingers were recovered and analyzed by SCAQMD Method 207.1 for ammonia concentration by Ion Specific Electrode analysis.

Stack NO_x and O₂ concentrations and stack volumetric flow rate data were recorded from the Continuous Emission Monitoring System (CEMS) which is installed on the unit. These data were used to correct the ammonia concentration to 15% O₂.

4.0 TEST RESULTS

The results of the test are summarized in Table 4-1. The results show that the maximum ammonia slip was 1.4 ppm @ 15% O₂ which is less than the permitted limit of 5 ppm @ 15% O₂.

**TABLE 4-1
AMMONIA SLIP TEST RESULTS
CANYON POWER PLANT UNIT 3
OCTOBER 15, 2019**

Parameter	Units	Run 1	Run 2	Average	Maximum ⁽¹⁾	Limit
Test		1-NH ₃ -U3	2-NH ₃ -U3			--
Date		10/15/2019	10/15/2019			--
Time		1518/1624	1652/1758			--
O ₂ ⁽²⁾	%	14.55	14.56	14.56	--	--
Stack Flow ⁽²⁾	dscfm @ T _{ref}	230,061	230,455	230,258	--	--
NO _x ⁽²⁾	ppmc	2.3	2.3	2.3	--	2.5
NH ₃	ppm	1.4	1.3	1.4	1.4	--
NH ₃	ppmc	1.3	1.2	1.3	1.3	5
NH ₃	lb/hr	0.9	0.8	0.8	0.9	--
NH ₃	lb/MMBtu	0.002	0.002	0.002	0.002	--
NH ₃	lb/MMSCF	1.9	1.7	1.8	1.9	--

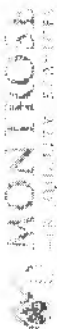
(1) Maximum of duplicate test runs, as required by SCAQMD Method 207.1

(2) From facility CEMS

APPENDIX A RAW DATA

Appendix A.1

Sample Data Sheets



WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA
LOCATION: Canyon / Unit 3
DATE: 10/15/19
RUN NO.: N/A
OPERATOR: CR/AD
METER BOX NO.: 38-425
METER ΔH@: 1.642
METER Yd: 0.994
STACK AREA, FT²: 1015/4
TRAVERSE POINTS, MIN/POINT: 5/12
ΔH= 1.5 X ΔP: N/A
Probe Condition, pre/post test: N/A
Silica Gel Expanded, Y/N: N
Filter Condition after Test: N/A
Check Weight: 500.0/500.0

AMBIENT TEMPERATURE: 78°
BAROMETRIC PRESSURE: 29.80
ASSUMED MOISTURE: 12%
PITOT TUBE COEFF, Cp: NA
PROBE ID NO/MATERIAL: NA/C1-33
PROBE LENGTH: 7
NOZZLE ID NO/MATERIAL: NA
NOZZLE DIAMETER: NA
FILTER NO/TYPE: NA
PRE-TEST LEAK RATE: <0.005 CFM@ 12 in. Hg.
POST-TEST LEAK RATE: <0.005 CFM@ 10 in. Hg.
PITOT LEAK CHECK - PRE: NA POST: NA
CHAIN OF CUSTODY: SAMPLE CUSTODIAN HC
SAMPLER AD
SAMPLE CUSTODIAN HC

Imp. # Contents Post-Test - Pre-Test = Difference
1 H₂O 879.7 687.5
2 H₂O 735.1 732.1
3 M7 623.7 622.2
4 SG 951.2 936.9
CR H₂O 100
Total:

Point	Time	Meter Volume, ft ³	ΔP In. H ₂ O	ΔH In. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum In. Hg.	O ₂ %	P. static in. H ₂ O
3	1518	910.320	X	1.5	X	X	X	58	93 90	5		X
2	1523											
1	1528	921.560										
E	1533	920.860										
3	1535	921.560		1.5				56	94 91	3		
2	1540											
1	1545											
E	1550	932.700										
3	1552	932.700		1.5				55	93 91	3		
2	1557											
1	1602											
E	1607	943.784										
3	1609	943.784		1.5				55	93 91	3		
2	1614											
1	1619											
E	1624	954.798										
Average:												①

Comments: AD 10-15-19



MONTROSE
AIR QUALITY SERVICES

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: SCPPA
LOCATION: Canyon / Unit 3
DATE: 10/15/19
RUN NO: 2 - NH3-03
OPERATOR: HL/AD
METER BOX NO: 3B-WCS
METER ΔH@: 0.994
METER Yd: 0.994
STACK AREA, FT²: 5.12
TRAVERSE POINTS, MIN/POINT: 5/12
ΔH = 1.5 X ΔP:
Probe Condition, pre/post test: N/A
Silica Gel Expanded, Y/N: N
Filter Condition after Test: N/A
Check Weight: 500.0 / 500.0

AMBIENT TEMPERATURE: 76°
BAROMETRIC PRESSURE: 29.80
ASSUMED MOISTURE: 12%
PITOT TUBE COEFF. Cp: NA
PROBE ID NO/MATERIAL: NA/Glass
PROBE LENGTH: 7'
NOZZLE ID NO/MATERIAL: NA
NOZZLE DIAMETER: NA
FILTER NO/TYPE: NA
PRE-TEST LEAK RATE: 50.005 CFM@ 1/3 in. Hg.
POST-TEST LEAK RATE: 40.005 CFM@ 1/2 in. Hg.
PHOT-LEAK CHECK - PRE: NA POST: NA
CHAIN OF CUSTODY: SAMPLE CUSTODIAN HC
SAMPLER AD
SAMPLE CUSTODIAN HC

Imp. # Contents Post-Test - Pre-Test = Difference
1 H2SO4 891.2 648.6
2 H2SO4 713.4 711.0
3 MT 599.3 598.6
4 SG 977.6 967.6
LR H2O 100
Total:

Point	Time	Meter Volume, ft³	ΔP in. H2O	ΔH in. H2O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O2 %	P. static in. H2O
3	1652	956.500	X	1.5	X	X	X	58	87 86	5		X
2	1657											
1	1703											
E	1707	967.215										
3	1709	967.215		1.5				56	84 83	5		
2	1714											
1	1719											
E	1724	978.161										
3	1726	978.161		1.5				55	83 81	5		
2	1731											
1	1736											
E	1741	989.017										
3	1743	989.017		1.5				54	82 80	5		
2	1748											
1	1753											
E	1758	999.811										
Average:												

Comments: * = AD 10-15-19

Appendix A.2 Laboratory Data

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS

Project #: 002AS-543385 District Method: SCAQMD 207.1 Sample Date: 10/15/2019
 Client/Location: SCPPA Calibration Date: 10/17/2019 Analysis Date: 10/17/2019
 Sample Location: U3 Calibration Curve: $y = -58.2497x + 93.4997$ Analyst's Initials: HS
 Test #'s: NH₃-U3 R²: 1.0000

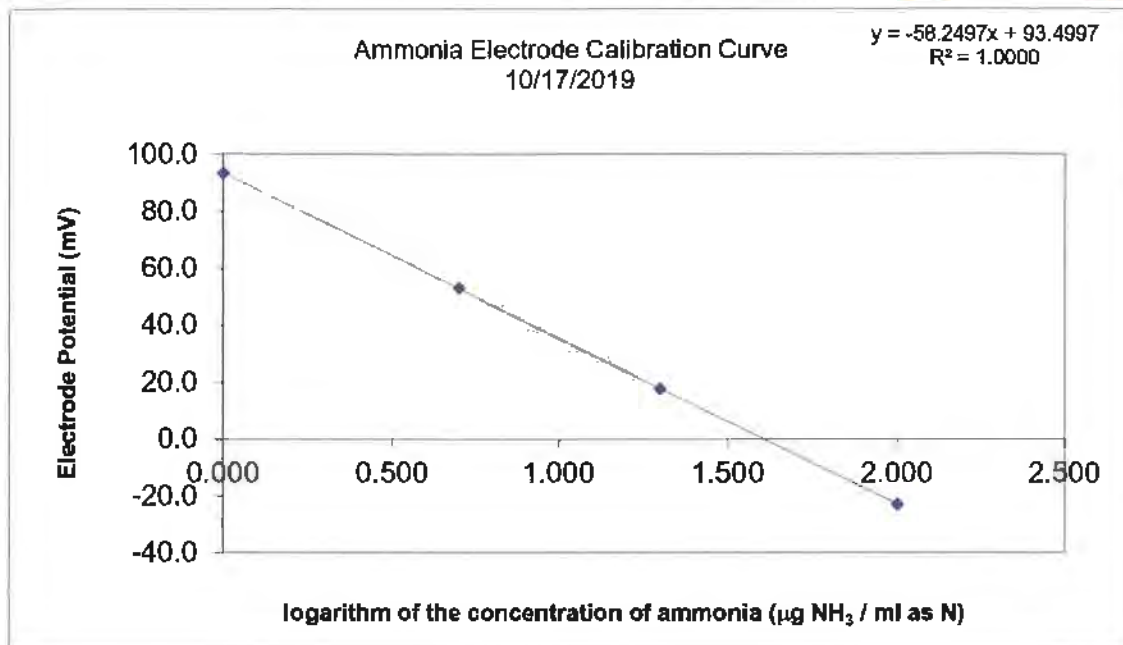
Sample	Electrode Potential (mV)	TV (ml)	Conc. $\mu\text{g NH}_3 - \text{N} / \text{ml}$	Cavg ($\mu\text{g NH}_3 - \text{N} / \text{ml}$)	$\mu\text{g NH}_3 / \text{sample}$	Comments/ Temp/pH
Standard Check: 28 $\mu\text{g NH}_3/\text{ml}$	93	—	27.893	—	—	Percent Recovery:
Repeat 28 $\mu\text{g NH}_3/\text{ml}$	92	—	28.004	27.948	—	100%
1-NH ₃ -U3	77.7	—	1.867	—	—	
1-NH ₃ -U3	78.0	541.7	1.845	1.850	1222.387	pH < 2 23°C
2-NH ₃ -U3	81.5	—	1.607	—	—	
2-NH ₃ -U3	81.6	557.6	1.601	1.604	1087.042	pH < 2 23°C
Spike 2-NH ₃ -U3	10.7	—	20.819	—	—	
Spike 2-NH ₃ -U3	17.0	—	20.573	20.690	—	99%
28 ppm NH ₃	10.2	—	20.918	—	—	
28 ppm NH ₃	10.2	—	20.918	20.918	—	96%
Field Blank	199.9	—	0.015	—	—	
Field Blank	200.0	—	0.015	0.0149	—	
Reagent Blank	199.6	—	0.015	—	—	
Reagent Blank	199.2	—	0.015	0.0152	—	
D1 H ₂ O Blank	207.3	—	0.015	0.011	—	
D1 H ₂ O Blank	207.3	—	0.011	0.0111	—	
28 ppm NH ₃	10.0	—	27.132	—	—	
28 ppm NH ₃	10.0	—	27.132	27.132	—	97%

Notes: Total volume of samples and standards used: 100 ml
 Volume of pH adjusting ISA used in ml: 2 ml
 Absorbing solution: 0.1N H₂SO₄

Calculations: Conc. ($\mu\text{g NH}_3 - \text{N} / \text{ml}$) = $10^{(P-B)/M}$
 P = electrode potential, B = y-intercept and M = slope
 Cavg = average result of duplicate analyses ($\mu\text{g NH}_3 - \text{N} / \text{ml}$) = $(C1+C2)/2$
 $\mu\text{g NH}_3 / \text{sample} = \text{Cavg} * 17.03 / 14.01 * \text{TV}$
 $\text{mg} / \text{sample} = \mu\text{g} / \text{sample} + 1000$
 $\text{ppm NH}_3 = \text{mg NH}_3 / \text{sample} * 1 / \text{Vstd} * 1 / 454000 * \text{SV} / 17 * 10^6$

AMMONIA ELECTRODE CALIBRATION CURVE

NH ₃ concentration (µg NH ₃ / ml as N)	log NH ₃ concentration	Electrode potential (mV)	Sample Temperature (C)	Room Temperature (C)
1	0.000	93.4	23	21
5	0.699	53.0	23	21
20	1.301	17.6	23	21
100	2.000	-23.0	23	21



slope -58.2497
y-intercept 93.4997

Concentration (µg NH ₃ / ml as N)	Value LR line	Difference	% Difference
1	1.0039	0.0039	0.3949
5	4.9577	-0.0423	-0.8467
20	20.0912	0.0912	0.4560
100	100.0012	0.0012	0.0012

Calculation:

Regression Line: $P = M \cdot \log(\mu\text{g of NH}_3 / \text{ml as N}) + B$

Measured Concentration of Ammonia (C) in µg / ml NH₃ as N: $C = 10^{(P-B)/M}$

where P = electrode potential, M= slope (must be -57 ± 3) and B= intercept

All standards were prepared in 0.04N H₂SO₄ and allowed to equilibrate to room temperature.

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS CALCULATION

Client/ Location: SCPPA
Sample Location: Unit 3
District Method: SCAQMD 207.1
Sample Date: 10/15/2019
Analysis Date: 10/17/2019
Analyst's Initials: HS
Calibration Curve Slope -58.2497
Y-intercept 93.4997
R²

Sample	P mV	Conc. µg NH ₃ /ml as N	C avg as N	TV (ml)	C avg as NH ₃	µg NH ₃ / sample
28 ug NH ₃ / ml as N	9.3	27.893				
repeat 28 ug NH ₃ /ml as N	9.2	28.004	27.948	NA	33.973	NA
1-NH ₃	77.7	1.867				
repeat 1- NH ₃	78.0	1.845	1.856	541.7	2.257	1222.387
2-NH ₃	81.5	1.607				
repeat 2- NH ₃	81.6	1.601	1.604	557.6	1.950	1087.042
spike 2-NH ₃	16.7	20.819				
repeat spike	17.0	20.573	20.696	NA	25.157	NA
28 NH ₃ /ml as N	10.2	26.918				
repeat 28 ug NH ₃ /ml as N	10.2	26.918	26.918	NA	32.721	NA
Field Blank	199.9	0.015				
repeat Field Blank	200.0	0.015	0.0149	NA	0.018	NA
Reagent Blank	199.6	0.015				
repeat Reagent Blank	199.2	0.015	0.0152	NA	0.018	NA
DI H ₂ O Blank	207.3	0.011				
Repeat DI H ₂ O Blank	207.3	0.011	0.0111	NA	0.014	NA
28 NH ₃ /ml as N	10.0	27.132				
repeat 28 ug NH ₃ /ml as N	10.0	27.132	27.132	NA	32.980	NA

Notes:

Measured Concentration of Ammonia (C) in µg NH₃ / ml as N

$$C=10^{(P-B)/M}$$

P = electrode potential (mV), M=slope and B=intercept

Average Measured Ammonia Concentration (Cavg) = (C1 + C2)/2

where C1, C2 results from duplicate analyses (µg NH₃/ml as N)

Cavg (µg NH₃/ml as NH₃) = Cavg (µg NH₃/ ml as N) * 17.03/ 14.01

µg NH₃ / sample = Cavg (µg NH₃/ml as NH₃) * TV

Used 100 ml of samples and standards with 2 ml ISA and constant stirring rate.

All solutions turned blue and remained blue with ISA unless otherwise indicated.

Sample PH and Temperatures can be found on the laboratory datasheet.

Maximum samples (including blanks) between 28 ug/ml check standard is 5 samples analyzed in duplicate.

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS QUALITY CONTROL

Client/ Location: SCPPA
Sample Location: Unit 3
District Method: SCAQMD 207.1
Sample Date: 10/15/2019
Analysis Date: 10/17/2019
Analyst's Initials: HS

Sample	% recovery	RPD %	RPA %
28 ug NH ₃ / ml as N repeat 28 ug NH ₃ /ml as N	NA	-0.40	-0.185
1-NH ₃ repeat 1- NH ₃	NA	1.19	NA
2-NH ₃ repeat 2- NH ₃	NA	0.40	NA
spike 2-NH ₃ repeat spike	99.44	1.19	NA
28 NH ₃ /ml as N repeat 28 ug NH ₃ /ml as N	NA	0.00	-3.864
Field Blank repeat Field Blank	NA	0.40	NA
Reagent Blank repeat Reagent Blank	NA	-1.58	NA
DI H ₂ O Blank Repeat DI H ₂ O Blank	NA	0.00	NA
28 NH ₃ /ml as N repeat 28 ug NH ₃ /ml as N	NA	0.00	-3.101

Notes:

spike: 100 ml sample + 2 ml (1000 µg NH₃ / ml as N)

Matrix Spike Percent Recovery (%R)

%R = (C spike*0.104 - Csample*0.102)/2 *100

Cspike = average result of matrix spike (µg NH₃/ ml as N)

Relative Percent Difference (RPD) = (C1-C2)/ Cavg *100 (must be 5% or less)

Relative Percent Accuracy (RPA) (must be 10% or less)

RPA = (Cavg-theoretical value of standard)/ theoretical value of standard * 100

Appendix A.3

QA/QC Data

SEMI-ANNUAL DRY GAS METER/ORIFICE CALIBRATION

Orifice Method - Triplicate Runs/Four Calibration Points
English Meter Box Units, English K Factor
Filename: M:\Santia AnalEquipment\Test Equipment\Calibrations\Dry Gas Meters\38-wcs-2019\semi annual cal 38wcs 9-7-19.xlsx\WC
File Modified From: APEX 522 Series Meter box Calibration
Revised: 4/8/2005

ID #: 38-wcs
Date: 9/7/2019
Bar. Pressure: 29.96 (in. Hg)
Performed By: R. Howard
Meter Serial #: c-5000

DRY GAS METER READINGS										CRITICAL ORIFICE READINGS			
dH (in H ₂ O)	Time (min)	Volume Initial (cu ft)	Volume Final (cu ft)	Volume Total (cu ft)	Initial Temps. Inlet (deg F)	Initial Temps. Outlet (deg F)	Final Temps. Inlet (deg F)	Final Temps. Outlet (deg F)	Orifice Serial# (number)	K Orifice Coefficient (see above)	Actual Vacuum (in. Hg)	Ambient Temperature Initial (deg F)	Ambient Temperature Final (deg F)
0.13	26.00	590.100	595.474	5.374	89.0	83.0	87.0	83.0	33	0.1551	18.0	80.0	80.0
0.13	26.00	595.474	600.851	5.377	87.0	83.0	87.0	84.0	33	0.1551	18.0	80.0	80.0
0.13	26.00	600.851	606.221	5.370	87.0	84.0	87.0	83.0	33	0.1551	18.0	80.0	80.0
0.51	12.00	538.700	544.047	5.347	83.0	80.0	84.0	80.0	48	0.3345	16.0	80.0	80.0
0.51	12.00	544.047	549.390	5.343	84.0	80.0	85.0	82.0	48	0.3345	16.0	80.0	80.0
0.51	12.00	549.390	554.742	5.352	85.0	82.0	86.0	83.0	48	0.3345	16.0	80.0	80.0
1.70	7.00	555.400	560.936	5.536	85.0	81.0	87.0	81.0	63	0.5915	15.0	80.0	80.0
1.70	7.00	560.936	566.470	5.534	87.0	81.0	88.0	82.0	63	0.5915	15.0	80.0	80.0
1.70	7.00	566.470	572.006	5.538	88.0	82.0	89.0	82.0	63	0.5915	15.0	80.0	80.0
3.00	5.00	572.900	577.987	5.087	88.0	81.0	90.0	82.0	73	0.7678	12.0	80.0	80.0
3.00	5.00	577.987	583.091	5.094	90.0	82.0	91.0	84.0	73	0.7678	12.0	80.0	80.0
3.00	5.00	583.091	588.191	5.100	91.0	84.0	90.0	83.0	73	0.7678	12.0	80.0	80.0

DRY GAS METER										DRY GAS METER CALIBRATION FACTOR			
ORIFICE					CALIBRATION FACTOR					ORIFICE			
VOLUME CORRECTED V _m (std) (cu ft)	VOLUME CORRECTED V _m (std) (liters)	VOLUME CORRECTED V _m (std) (cu ft)	VOLUME CORRECTED V _m (std) (liters)	VOLUME NOMINAL V _n (cu ft)	Y Value (number)	dH@ Value (in H ₂ O)	Individual Run	Individual Orifice	Y _{max} - Y _{min} < 0.010?	Orifice Average	Y _{max} - Y _{min} < 1.02?	Orifice Average	dH@ - dH@ av < 0.155?
5.208	147.5	5.201	147.3	5.314	0.999	1.779	Pass		0.95 < Y				
5.213	147.6	5.201	147.3	5.314	0.998	1.778	Pass		< 1.05?				
5.207	147.5	5.201	147.3	5.314	0.999	1.778	Pass		Pass				
					Average	1.778			Pass				Pass
5.223	147.9	5.175	146.5	5.287	0.991	1.511	Pass						
5.209	147.5	5.175	146.5	5.287	0.993	1.508	Pass						
5.208	147.5	5.175	146.5	5.287	0.994	1.504	Pass						
					Average	1.507			Pass				Pass
5.406	153.1	5.338	151.2	5.455	0.988	1.607	Pass						
5.394	152.8	5.338	151.2	5.455	0.990	1.605	Pass						
5.393	152.7	5.338	151.2	5.455	0.990	1.604	Pass						
					Average	1.605			Pass				Pass
4.977	140.9	4.950	140.2	5.058	0.995	1.681	Pass						
4.960	140.5	4.950	140.2	5.058	0.998	1.677	Pass						
4.964	140.6	4.950	140.2	5.058	0.997	1.675	Pass						
					Average	1.678			Pass				Pass
					Average Yd:	0.994							
					dH@:	1.642							
					Q @ dH = 1:	0.585							

SIGNED: Signature on File

Date: 9/7/2019



DIGITAL TEMPERATURE READOUT CALIBRATION

Digital Temperature Readout ID: 38-WCS
 Readout Description: Control Box
 Date: 7/2/2019
 Performed By: JG/DA/RH/JS

Calibrated Thermocouple ID: TC-CAL
 T1 Reference Thermometer ID: 242196
 T2 Reference Thermometer ID: 242196
 T3 Reference Thermometer ID: 242167

T/C I.D.	Readout I.D.	T/C - Readout °F				Reference Thermometer °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
TC-CAL												
T3 (OIL)	38-WCS	358	358	358	358	358	358	358	358	0.0	0.0%	Pass
T2 (Boiling H ₂ O)	38-WCS	211	211	211	211	212	212	212	212	1.0	0.1%	Pass
T1 (Ice/Water)	38-WCS	32	32	32	32	32	32	32	32	0.0	0.0%	Pass

- 1) Difference % (°R) = Difference (°F) / (Average Tref + 460)
 2) Pass if all Differences are less than 1.5% (°R)

Thermocouple Source Readings

T/C Source S/N	T/C - Readout °F				T/C Source °F				Difference		
	Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
T4 (~650 F)	S/N 106970	653	653	653	653	650	650	650	3.0	0.3%	Pass
T3 (~370 F)	S/N 106970	378	378	378	378	370	370	370	8.0	1.0%	Pass
T2 (~212 F)	S/N 106970	214	214	214	214	212	212	212	2.0	0.3%	Pass
T1 (~32 F)	S/N 106970	33	33	33	33	32	32	32	1.0	0.2%	Pass

- 1) Difference % (°R) = Difference (°F) / (Average Tref + 460)
 2) Pass if all Differences are less than 1.5% (°R)



WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET – STANDARD

CLIENT: <u>SCPPA</u>		Imp. # Contents		Post-Test = Difference	
LOCATION: <u>canyon / Unit 3</u>		1	H2SO4	821.1	719.6
DATE: <u>10/15/19</u>		2	H2SO4	701.0	700.9
RUN NO: <u>FB-NH3</u>		3	MT	609.9	609.3
OPERATOR: <u>HL</u>		4	SG	859.3	859.1
METER BOX NO: <u>38-WCS</u>		UR			
METER ΔH@:					
METER Yd: <u>0.994</u>					
STACK AREA, FT²: <u>106.90</u>					
TRAVERSE POINTS, MIN/POINT: <u>N/A</u>					
ΔH= <u>N/A</u> X ΔP:					
Probe Condition, pre/post test: <u>N/A</u>					
Silica Gel Expanded, Y/N: <u>N</u>					
Filter Condition after Test: <u>N/A</u>					
Check Weight: <u>500.0 / 500.0</u>					
		Total:			

[illegible]

Comments:

CLIENT: SCPPA	PROJECT #: W002AS-543385	TEST DATE(S): 10/15/2019
LOCATION: U3	SAMPLER(S): HL/AD	
SAMPLE LOCATION: Stack	PROJECT MANAGER: SD	
TEST METHOD(S): SCAQMD 207.1	DATE DUE: 10/22/2019	
OUTSIDE LAB REQUIRED?: No	COMPLIANCE TEST?: Yes	

[illegible][illegible]ANALYSIS REQUIRED: NH_3 by SCAQMD 207.1 (ISE)

APPENDIX B FACILITY CEMS DATA

1-NH₃-U3

Company: City Of Anaheim
Plant: 3071 Miraloma Ave.,
City/ST: Anaheim, CA, 92806
Source: unit3

Average Values Report
Generated: 10/15/2019 17:16

Period Start: 10/15/2019 15:19
 Period End: 10/15/2019 16:24
 Validation Type: 1/1 min
 Averaging Period: 1 min
 Type: Block Avg

[illegible]

* Does not include Invalid Averaging Periods ("N/A")

Period Start: 10/15/2019 16:53
 Period End: 10/15/2019 17:58
 Validation type: 1/1 min
 Averaging Period: 1 min
 Type: Block Avg

Average Values Report
Generated: 10/15/2019 18:24

[illegible]

* Does not include Invalid Averaging Periods ("N/A")

APPENDIX C CALCULATIONS

Appendix C.1

General Emissions Calculations

GENERAL EMISSION CALCULATIONS

I. Stack Gas Velocity

A. Stack gas molecular weight, lb/lb-mole

$$MW_{dry} = 0.44 * \%CO_2 + 0.32 * \%O_2 + 0.28 * \%N_2$$

$$MW_{wet} = MW_{dry} * (1 - B_{wo}) + 18 * B_{wo}$$

B. Absolute stack pressure, iwg

$$P_s = P_{bar} + \frac{P_{sg}}{13.6}$$

C. Stack gas velocity, ft/sec

$$V_s = 2.9 * C_p * \sqrt{\Delta P} * \sqrt{T_s} * \sqrt{\frac{29.92 * 28.95}{P_s * MW_{wet}}}$$

II. Moisture

A. Sample gas volume, dscf

$$V_{mstd} = 0.03342 * V_m * (P_{bar} + \frac{\Delta H}{13.6}) * \frac{T_{ref}}{T_m} * Y_d$$

B. Water vapor volume, scf

$$V_{wstd} = 0.0472 * V_{lc} * \frac{T_{ref}}{528 ^\circ R}$$

C. Moisture content, dimensionless

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

III. Stack gas volumetric flow rate

A. Actual stack gas volumetric flow rate, wacfm

$$Q = V_s * A_s * 60$$

B. Standard stack gas flow rate, dscfm

$$Q_{sd} = Q * (1 - B_{wo}) * \frac{T_{ref}}{T_s} * \frac{P_s}{29.92}$$

IV. Gaseous Mass Emission Rates, lb/hr

$$M = \frac{\text{ppm} * MW_i * Q_{sd} * 60}{SV * 10^6}$$

V. Emission Rates, lb/MMBtu

$$\frac{\text{lb}}{\text{MMBtu}} = \frac{\text{ppm} * MW_i * F}{SV * 10^6} * \frac{20.9}{20.9 - \%O_2}$$

VI. Percent Isokinetic

$$I = \frac{17.32 * T_s (V_{mstd})}{(1-Bwo) * 0 * V_s * P_s * Dn2} * \frac{520^{\circ}R}{T_{ref}}$$

VII. Particulate emissions

(a) Grain loading, gr/dscf
 $C = 0.01543 (M_n/V_{mstd})$

(b) Grain loading at 12% CO₂, gr/dscf
 $C_{12\% CO_2} = C (12/\% CO_2)$

(c) Mass emissions, lb/hr
 $M = C * Q_{sd} * (60 \text{ min/hr}) / (7000 \text{ gr/lb})$

(d) Particulate emission factor
 $\text{lb}/10^6 \text{ Btu} = C * \frac{1 \text{ lb}}{7000 \text{ gr}} * F * \frac{20.9}{20.9 - \% O_2}$

Nomenclature:

A_s	= stack area, ft ²
B_{wo}	= flue gas moisture content, dimensionless
$C_{12\%CO_2}$	= particulate grain loading, gr/dscf corrected to 12% CO ₂
C	= particulate grain loading, gr/dscf
C_p	= pitot calibration factor, dimensionless
D_n	= nozzle diameter, in.
F	= fuel F-Factor, dscf/MMBtu @ 0% O ₂
H	= orifice differential pressure, iwg
I	= % isokinetics
M_n	= mass of collected particulate, mg
M_i	= mass emission rate of specie i, lb/hr
MW	= molecular weight of flue gas, lb/lb-mole
M_{wi}	= molecular weight of specie i: SO ₂ : 64 NO _x : 46 CO: 28 HC: 16
t	= sample time, min.
ΔP	= average velocity head, iwg = $(\sqrt{\Delta P})^2$
P_{bar}	= barometric pressure, inches Hg
P_s	= stack absolute pressure, inches Hg
P_{sg}	= stack static pressure, iwb
Q	= wet stack flow rate at actual conditions, wacfm
Q_{sd}	= dry standard stack flow rate, dscfm
SV	= specific molar volume of an ideal gas at standard conditions, ft ³ /lb-mole
T_m	= meter temperature, °R
T_{ref}	= reference temperature, °R
T_s	= stack temperature, °R
V_s	= stack gas velocity, ft/sec
V_{lc}	= volume of liquid collected in impingers, ml
V_m	= uncorrected dry meter volume, dcf
V_{mstd}	= dry meter volume at standard conditions, dscf
V_{wstd}	= volume of water vapor at standard conditions, scf
Y_d	= meter calibration coefficient

Appendix C.2

Spreadsheet Summaries

SCAQMD 207.1 EXAMPLE CALCULATION

TEST NUMBER: 1-NH3-U3

Identifier	Description	Units	Equation	Value
A	Reference Temperature	F	--	60
B	Reference Temperature	R	$A + 460$	520
C	Meter Calibration Factor (Yd)	--	--	0.994
D	Barometric Pressure	" Hg	--	29.80
E	Meter Volume	acf	--	44.478
F	Meter Temperature	F	--	92.0
G	Meter Temperature	R	$F + 460$	552.0
H	Delta H	" H ₂ O	--	1.5
I	Meter Volume (standard)	dscf	$0.03342 * E * (D + H/13.6) * B/G * C$	41.632
J	Liquid Collected	grams	--	111.0
K	Water vapor volume	scf	$0.0472 * J * B/528$	5.160
L	Moisture Content	--	$K/(K + I)$	0.110
M	Gas Constant	ft-lbf/lb-mole-R	--	1545.33
N	Specific Molar Volume	SCF/lb-mole	$385.3 * B / 528$	379.5
O	F-Factor	dscf/MMBtu	--	8,710
P	HHV	Btu/SCF	--	1,050
Q	Mass Conversion Factor	lb/ug	--	2.2046E-09
R	O ₂ Correction Factor	--	--	15
S	Stack Flow Rate @ 68 F	dscfm	--	233,600
T	Stack Flow Rate @ Tref	dscfm	$S * B/528$	230,061
U	Mass NH ₃	ug	--	1,222
V	Mass NH ₃	lb	$U * Q$	2.69E-06
W	MW of NH ₃	lb/lb-mole	--	17.03
X	NH ₃	ppm	$(V * N * 10^6)/(I * W)$	1.4
Y	Flue Gas O ₂	%	--	14.55
Z	NH ₃	ppmc	$X * (20.9 - R)/(20.9 - Y)$	1.3
AA	NH ₃	lb/hr	$X * T * W * 60/(N * 10^6)$	0.9
AB	NH ₃	lb/MMBtu	$(X * W * O)/(385.3 * 10^6) * 20.9/(20.9 - Y)$	0.002
AC	NH ₃	lb/MMSCF	$AB * P$	1.9

Note:

(1) Some values may be slightly different from those shown on the run sheets due to round off errors. This page is intended to show the calculation methodology only.

SCAQMD METHOD 207.1 DATA WORKSHEET AND SUMMARY

Facility.....	Canyon		Parameter.....		NH₃
Unit.....	U3		Fuel.....		Natural gas
Sample Location.....	Stack		Data By.....		SD
Test Number.....	1-NH3-U3	2-NH3-U3	Average	Maximum	Limit
Reference Temperature (°F).....	60	60			
Test Date.....	10/15/2019	10/15/2019			
Test Method.....	SCAQMD 207.1	SCAQMD 207.1			
Sample Train.....	38-WCS	38-WCS			
Meter Calibration Factor.....	0.994	0.994			
Stack Area (ft ²).....	106.90	106.90			
Sample Time (Minutes).....	60	60			
Barometric Pressure ("Hg).....	29.80	29.80			
Start/Stop Time	1518/1624	1652/1758			
Meter Volume (acf).....	44.478	43.311			
Meter Temperature (°F).....	92.0	83.3			
Meter Pressure (iwg).....	1.5	1.5			
Liquid Volume (ml).....	111.0	105.7			
Stack O ₂ (%).....	14.55	14.56	14.56	(from facility CEMS)	
Unit Load (MW).....	50	50	49.9		
Standard Sample Volume (SCF).....	41.632	41.188			
Moisture Fraction.....	0.110	0.107			
Stack Flow Rate (dscfm, 68 °F).....	233,600	234,000	233,800	(from facility CEMS)	
Stack Flow Rate (@ Tref).....	230,061	230,455	230,258		
Gas Constant (ft-lbf/lb-mole-R).....	1545.33	1545.33			
Molecular Weight NH ₃ (lb/lb-mole).....	17.03	17.03			
Specific Molar Volume (ft ³ /lb-mole).....	379.5	379.5			
F-Factor (dscf/MMBtu).....	8,710	8,710			
HHV(Btu/SCF).....	1,050	1,050			
Mass Conversion (lb/ug).....	2.2046E-09	2.2046E-09			
O ₂ Correction Factor (%).....	15	15			
Mass NH ₃ (ug).....	1,222	1,087			
Mass NH ₃ (lb).....	2.69E-06	2.40E-06			
NH ₃ (ppmv, flue gas).....	1.4	1.3	1.4	1.4	
NH ₃ (ppmv @ O ₂ Correction Factor).....	1.3	1.2	1.3	1.3	5
NH ₃ (lb/hr).....	0.9	0.8	0.8	0.9	
NH ₃ (lb/MMBtu).....	0.002	0.002	0.002	0.002	
NH ₃ (lb/MMSCF).....	1.9	1.7	1.8	1.9	

Note: SCAQMD Method 207.1 requires the higher of the duplicate runs be reported as the test result.

APPENDIX D QUALITY ASSURANCE

Appendix D.1

Quality Assurance Program Summary

QUALITY ASSURANCE PROGRAM SUMMARY

As part of Montrose Air Quality Services, LLC (MAQS) ASTM D7036-04 certification, MAQS is committed to providing emission related data which is complete, precise, accurate, representative, and comparable. MAQS quality assurance program and procedures are designed to ensure that the data meet or exceed the requirements of each test method for each of these items. The quality assurance program consists of the following items:

- Assignment of an Internal QA Officer
- Development and use of an internal QA Manual
- Personnel training
- Equipment maintenance and calibration
- Knowledge of current test methods
- Chain-of-custody
- QA reviews of test programs

Assignment of an Internal QA Officer: MAQS has assigned an internal QA Officer who is responsible for administering all aspects of the QA program.

Internal Quality Assurance Manual: MAQS has prepared a QA Manual according to the requirements of ASTM D7036-04 and guidelines issued by EPA. The manual documents and formalizes all of MAQS QA efforts. The manual is revised upon periodic review and as MAQS adds capabilities. The QA manual provides details on the items provided in this summary.

Personnel Testing and Training: Personnel testing and training is essential to the production of high quality test results. MAQS training programs include:

- A requirement for all technical personnel to read and understand the test methods performed
- A requirement for all technical personnel to read and understand the MAQS QA manual
- In-house testing and training
- Quality Assurance meetings
- Third party testing where available
- Maintenance of training records.

Equipment Maintenance and Calibration: All laboratory and field equipment used as a part of MAQS emission measurement programs is maintained according to manufacturer's recommendations. A summary of the major equipment maintenance schedules is summarized in Table 1. In addition to routine maintenance, calibrations are performed on all sampling equipment according to the procedures outlined in the applicable test method. The calibration intervals and techniques for major equipment components is summarized in Table 2. The calibration technique may vary to meet regulatory agency requirements.

Knowledge of Current Test Methods: MAQS maintains current copies of EPA, ARB, and SCAQMD Source Test Manuals and Rules and Regulations.

Chain-of-Custody: MAQS maintains chain-of-custody documentation on all data sheets and samples. Samples are stored in a locked area accessible only to MAQS source test personnel. Data sheets are kept in the custody of the originator, program manager, or in locked storage until return to MAQS office. Electronic field data is duplicated for backup on secure storage media. The original data sheets are used for report preparation and any additions are initialed and dated.

QA Reviews: Periodic field, laboratory, and report reviews are performed by the in-house QA coordinator. Periodically, test plans are reviewed to ensure proper test methods are selected and reports are reviewed to ensure that the methods were followed and any deviations from the methods are justified and documented.

ASTM D7036-04 Required Information

Uncertainty Statement

Montrose is qualified to conduct this test program and has established a quality management system that led to accreditation with ASTM Standard D7036-04 (Standard Practice for Competence of Air Emission Testing Bodies). Montrose participates in annual functional assessments for conformance with D7036-04 which are conducted by the American Association for Laboratory Accreditation (A2LA). All testing performed by Montrose is supervised on site by at least one Qualified Individual (QI) as defined in D7036-04 Section 8.3.2. Data quality objectives for estimating measurement uncertainty within the documented limits in the test methods are met by using approved test protocols for each project as defined in D7036-04 Sections 7.2.1 and 12.10. Additional quality assurance information is presented in the report appendices.

Performance Data

Performance data are available for review.

Qualified Personnel

A qualified individual (QI), defined by performance on a third party or internal test on the test methods, will be present on each test event.

Plant Entry and Safety Requirements

Plant Entry

All test personnel are required to check in with the guard at the entrance gate or other designated area. Specific details are provided by the facility and project manager.

Safety Requirements

All personnel shall have the following personal protective equipment (PPE) and wear them where designated:

- Hard Hat
- Safety Glasses
- Steel Toe Boots
- Hearing Protection
- Gloves
- High Temperature Gloves (if required)

The following safety measures will be followed:

- Good housekeeping
- SDS for all on-site hazardous materials
- Confine selves to necessary areas (stack platform, mobile laboratory, CEMS data acquisition system, control room, administrative areas)
- Knowledge of evacuation procedures

Each facility will provide plant specific safety training.

TABLE 1
EQUIPMENT MAINTENANCE SCHEDULE

Equipment	Acceptance Limits	Frequency of Service	Methods of Service
Pumps	1. Absence of leaks 2. Ability to draw manufacturers required vacuum and flow	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Replace parts 4. Leak check
Flow Meters	1. Free mechanical movement	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Calibrate
Sampling Instruments	1. Absence of malfunction 2. Proper response to zero span gas	As recommended by manufacturer	As recommended by manufacturer
Integrated Sampling Tanks	1. Absence of leaks	Depends on nature of use	1. Steam clean 2. Leak check
Mobil Van Sampling System	1. Absence of leaks	Depends on nature of use	1. Change filters 2. Change gas dryer 3. Leak check 4. Check for system contamination
Sampling lines	1. Sample degradation less than 2%	After each test series	1. Blow dry, inert gas through line until dry

TABLE 2
MAJOR SAMPLING EQUIPMENT CALIBRATION REQUIREMENTS

Sampling Equipment	Calibration Frequency	Calibration Procedure	Acceptable Calibration Criteria
Continuous Analyzers	Before and After Each Test Day	3-point calibration error test	< 2% of analyzer range
Continuous Analyzers	Before and After Each Test Run	2-point sample system bias check	< 5% of analyzer range
Continuous Analyzers	After Each Test Run	2-point analyzer drift determination	< 3% of analyzer range
CEMS System	Beginning of Each Day	leak check	< 1 in. Hg decrease in 5 min. at > 20 in. Hg
Continuous Analyzers	Semi-Annually	3-point linearity	< 1% of analyzer range
NO _x Analyzer	Daily	NO ₂ -> NO converter efficiency	> 90%
Differential Pressure Gauges (except for manometers)	Semi-Annually	Correction factor based on 5-point comparison to standard	+/- 5%
Differential Pressure Gauges (except for manometers)	Bi-Monthly	3-point comparison to standard, no correction factor	+/- 5%
Barometer	Semi-Annually	Adjusted to mercury-in-glass or National Weather Service Station	+/- 0.1 inches Hg
Dry Gas Meter	Semi-Annually	Calibration check at 4 flow rates using a NIST traceable standard	+/- 2%
Dry Gas Meter	Bi-Monthly	Calibration check at 2 flow rates using a NIST traceable standard	+/- 2% of semi-annual factor
Dry Gas Meter Orifice	Annually	4-point calibration for $\Delta H@$	--
Temperature Sensors	Semi-Annually	3-point calibration vs. NIST traceable standard	+/- 1.5%

Note: Calibration requirements will be used that meet applicable regulatory agency requirements.

Appendix D.2

SCAQMD and STAC Certifications



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 • www.aqmd.gov

September 6, 2019

Mr. John Peterson
Montrose Air Quality Services, LLC
1631 E. Saint Andrew Place
Santa Ana, CA 92705

Subject: LAP Approval Notice
Reference # 96LA1220

Dear Mr. Peterson:

We have reviewed your renewal letter under the South Coast Air Quality Management District's Laboratory Approval Program (LAP). We are pleased to inform you that your firm is approved for the period beginning September 30, 2019, and ending September 30, 2020 for the following methods, subject to the requirements in the LAP Conditions For Approval Agreement and conditions listed in the attachment to this letter:

Methods 1-4	Methods 5.1, 5.2, 5.3, 6.1
Methods 10.1 and 100.1	Methods 25.1 and 25.3 (Sampling)
USEPA CTM-030 and ASTM D6522-00	Rule 1121/ 1146.2 Protocol
Rule 1420/1420.1/1420.2 – (Lead) Source and Ambient Sampling	

Your LAP approval to perform nitrogen oxide emissions compliance testing for Rule 1121/ 1146.2 Protocols includes satellite facilities located at:

McKenna Boiler 1510 North Spring Street Los Angeles, CA 90012	Noritz America Corp. 11160 Grace Avenue Fountain Valley, CA 92708	Ajax Boiler, Inc. 2701 S. Harbor Blvd. Santa Ana, CA 92704
---	---	--

Laundry Building of VA Greater Los Angeles Healthcare System
508 Constitution Avenue
Los Angeles, CA 90049

Thank you for participating in the LAP. Your cooperation helps us to achieve the goal of the LAP: to maintain high standards of quality in the sampling and analysis of source emissions. You may direct any questions or information to LAP Coordinator, Glenn Kasai. He may be reached by telephone at (909) 396-2271, or via e-mail at gkasai@aqmd.gov.

Sincerely,

A handwritten signature in black ink that reads 'D. Sarkar'.

Dipankar Sarkar
Program Supervisor
Source Test Engineering

DS:GK/gk
Attachment

190906 LapRenewalRev.doc

Learning the air that we breathe...



American Association for Laboratory Accreditation

Accredited Air Emission Testing Body

A2LA has accredited

MONTROSE AIR QUALITY SERVICES

In recognition of the successful completion of the joint A2LA and Stack Testing Accreditation Council (STAC) evaluation process, this laboratory is accredited to perform testing activities in compliance with ASTM D7036:2004 - Standard Practice for Competence of Air Emission Testing Bodies.

Presented this 5th day of March 2018.



President and CEO
For the Accreditation Council
Certificate Number 3925.01
Valid to February 29, 2020

This accreditation program is not included under the A2LA ILAC Mutual Recognition Arrangement.

Appendix D.3

Individual QI Certificate

CERTIFICATE OF COMPLETION

Sean Donovan

This document certifies that this individual has passed a comprehensive examination and is now a Qualified Individual (QI) as defined in Section 8.3 of ASTM D7036-04 for the following method(s):

SCAQMD Method 207.1

Certificate Number: 002-2016-06

Tate Strickler

DATE OF ISSUE: 11/30/16

Tate Strickler, Accreditation Director

DATE OF
EXPIRATION: 11/30/21



APPENDIX E

APPLICABLE PERMIT SECTIONS



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions * And Requirements	Conditions
Process 1: POWER GENERATION					
GAS TURBINE, NO. 3, NATURAL GAS, GENERAL ELECTRIC, MODEL LM6000PC SPRINT, SIMPLE CYCLE, 479 MMBTU/HR AT 46 DEG F, WITH INLET CHILLING, WITH WATER INJECTION WITH A/N: 555830	D13	C15	NOX: MAJOR SOURCE**	CO: 4 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]; CO: 2000 PPMV NATURAL GAS (5) [RULE 407, 4-2-1982]; NOX: 2.5 PPMV NATURAL GAS (4) [RULE 2005, 6-3-2011]; NOX: 25 PPMV NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; PM10: 0.01 GRAINS/SCF NATURAL GAS (5A) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; PM10: 0.1 GRAINS/SCF NATURAL GAS (5) [RULE 409, 8-7-1981]; PM10: 1.67 LBS/HR NATURAL GAS (5C) [RULE 1303(b)(2)-Offset, 5-10-1996; RULE 1303(b)(2)-Offset, 12-6-2002]; PM10: 11 LBS/HR NATURAL GAS (5B) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; SO2: (9) [40CFR 72 - Acid Rain Provisions, 11-24-1997]; SOX: 0.06 LBS/MMBTU NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; VOC: 2 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A63.1, A99.1, A99.2, A99.3, A195.1, A195.2, A195.3, A327.1, B61.1, D12.1, D29.2, D29.3, D82.1, D82.2, E193.1, H23.1, I298.3, K40.1
GENERATOR, 50.95 MW					

- * (1) (1A) (1B) Denotes RECLAIM emission factor
(3) Denotes RECLAIM concentration limit
(5) (5A) (5B) Denotes command and control emission limit
(7) Denotes NSR applicability limit
(9) See App B for Emission Limits
(2) (2A) (2B) Denotes RECLAIM emission rate
(4) Denotes BACT emission limit
(6) Denotes air toxic control rule limit
(8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(10) See section J for NESHAP/MACT requirements

** Refer to section F and G of this permit to determine the monitoring, recordkeeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions * And Requirements	Conditions
Process F: POWER GENERATION					
CO OXIDATION CATALYST, NO. 3, BASF, 110 CUBIC FEET OF TOTAL CATALYST VOLUME A/N: 476660	C15	D13 C16			
SELECTIVE CATALYTIC REDUCTION, NO. 3, CORMETECH CMHT-21, 1012 CU.FT.; WIDTH: 2 FT 6 IN; HEIGHT: 25 FT 9 IN; LENGTH: 18 FT WITH A/N: 476660 AMMONIA INJECTION	C16	C15 S18		NH3: 5 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A195.6, D12.2, D12.3, D12.4, E179.1, E179.2, E193.1
STACK, TURBINE NO. 3, HEIGHT: 86 FT; DIAMETER: 11 FT 8 IN A/N: 555830	S18	C16			

- * (1) (1A) (1B) Denotes RECLAIM emission factor
(3) Denotes RECLAIM concentration limit
(5) (5A) (5B) Denotes command and control emission limit
(7) Denotes NSR applicability limit
(9) See App B for Emission Limits
(2) (2A) (2B) Denotes RECLAIM emission rate
(4) Denotes BACT emission limit
(6) Denotes air toxic control rule limit
(8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(10) See section J for NESHAP/MACT requirements

** Refer to section F and G of this permit to determine the monitoring, recordkeeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

[Devices subject to this condition : C4, C10, C16, C22]

- D12.5 The operator shall install and maintain a(n) non-resettable elapsed time meter to accurately indicate the elapsed operating time of the engine.

[RULE 1110.2, 2-1-2008; RULE 1110.2, 9-7-2012; RULE 1303(b)(2)-Offset, 5-10-1996;
RULE 1303(b)(2)-Offset, 12-6-2002; RULE 1401, 9-10-2010; RULE 1470, 5-4-2012;
RULE 2012, 5-6-2005; 40CFR 60 Subpart IIII, 1-30-2013]

[Devices subject to this condition : D25]

- D29.2 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Averaging Time	Test Location
NH3 emissions	District method 207.1 and 5.3 or EPA method 17	1 hour	Outlet of the SCR serving this equipment



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

The test(s) shall be conducted at least quarterly during the first twelve months of operation and at least annually thereafter. The AQMD shall be notified of the date and time of the test at least 10 days prior to the test.

If the turbine is not in operation during one calendar year, then no testing is required during that calendar year.

The NO_x concentration, as determined by the CEMS, shall be simultaneously recorded during the ammonia slip test. If the CEMS is inoperable, a test shall be conducted to determine the NO_x emissions using District Method 100.1 measured over a 60 minute averaging time period.

The test shall be conducted and the results submitted to the District within 60 days after the test date.

The test shall be conducted to demonstrate compliance with the Rule 1303 concentration limit.

[RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]

[Devices subject to this condition : D1, D7, D13, D19]

D29.3 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Sampling Time	Test Location
SOX emissions	AQMD Laboratory Method 307-91	Not Applicable	Fuel sample
VOC emissions	District Method 25.3	1 hour	Outlet of the SCR serving this equipment
PM emissions	District method 5.1	4 hours	Outlet of the SCR serving this equipment

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If you have any questions, please contact one of the following individuals by email or phone.

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TEST REPORT FOR AMMONIA SLIP TEST AT CANYON POWER PLANT UNIT 4 FACILITY ID 153992, DEVICE ID D19

Prepared For:

Canyon Power Plant
3071 E. Mira Loma Avenue.
Anaheim, California 92806

For Submittal To:

South Coast Air Quality Management District
21865 Copley Drive
Diamond Bar, California 91765-4178

Prepared By:

Montrose Air Quality Services, LLC
1631 E. St. Andrew Pl.
Santa Ana, California 92705
(714) 279-6777

Sean M. Donovan

Test Date: **June 11, 2019**
Production Date: **July 16, 2019**
Report Number: **W002AS-543226-RT-53**

CONFIDENTIALITY STATEMENT

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REVIEW AND CERTIFICATION

All work, calculations, and other activities and tasks performed and presented in this document were carried out by me or under my direction and supervision. I hereby certify that, to the best of my knowledge, Montrose operated in conformance with the requirements of the Montrose Quality Management System and ASTM D7036-04 during this test project.

Signature: Sean Donovan Date: 7/16/2019

Name: Sean Donovan Title: Client Project Manager

I have reviewed, technically and editorially, details, calculations, results, conclusions, and other appropriate written materials contained herein. I hereby certify that, to the best of my knowledge, the presented material is authentic, accurate, and conforms to the requirements of the Montrose Quality Management System and ASTM D7036-04.

Signature: Matt McCune Date: 7/16/2019

Name: Matt McCune Title: Regional Vice President

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1.0 INTRODUCTION AND SUMMARY

Montrose Air Quality Services, LLC (MAQS) was contracted the Canyon Power Plant to perform an ammonia slip test at Unit 4 as required by the facility Permit (Facility ID 153992) Condition Number D29.2. This report documents the results of the ammonia slip tests performed on June 11, 2019. The test was performed by John Groenenboom, Shannon Scrugham, and Luis Olivares. John Groenenboom was the on-site Qualified Individual for MAQS. Ms. Bertha Hernandez coordinated the test for Canyon Power Plant.

The test consisted of duplicate ammonia tests performed at 50 MW. The test program followed the procedures described in the initial compliance test protocol (MAQS document R038842). The results of the test are summarized in Table 1-1. The table shows that the ammonia slip from this unit was less than the permitted limit of 5 ppm corrected to 15% O₂.

**TABLE 1-1
AMMONIA SLIP TEST RESULTS
CANYON POWER PLANT UNIT 4
JUNE 11, 2019**

Parameter	Units	Result ⁽¹⁾	Limit
NH ₃	ppm	1.8	--
NH ₃	ppmc	1.7	5

(1) Maximum of duplicate runs, as required by SCAQMD Method 207.1

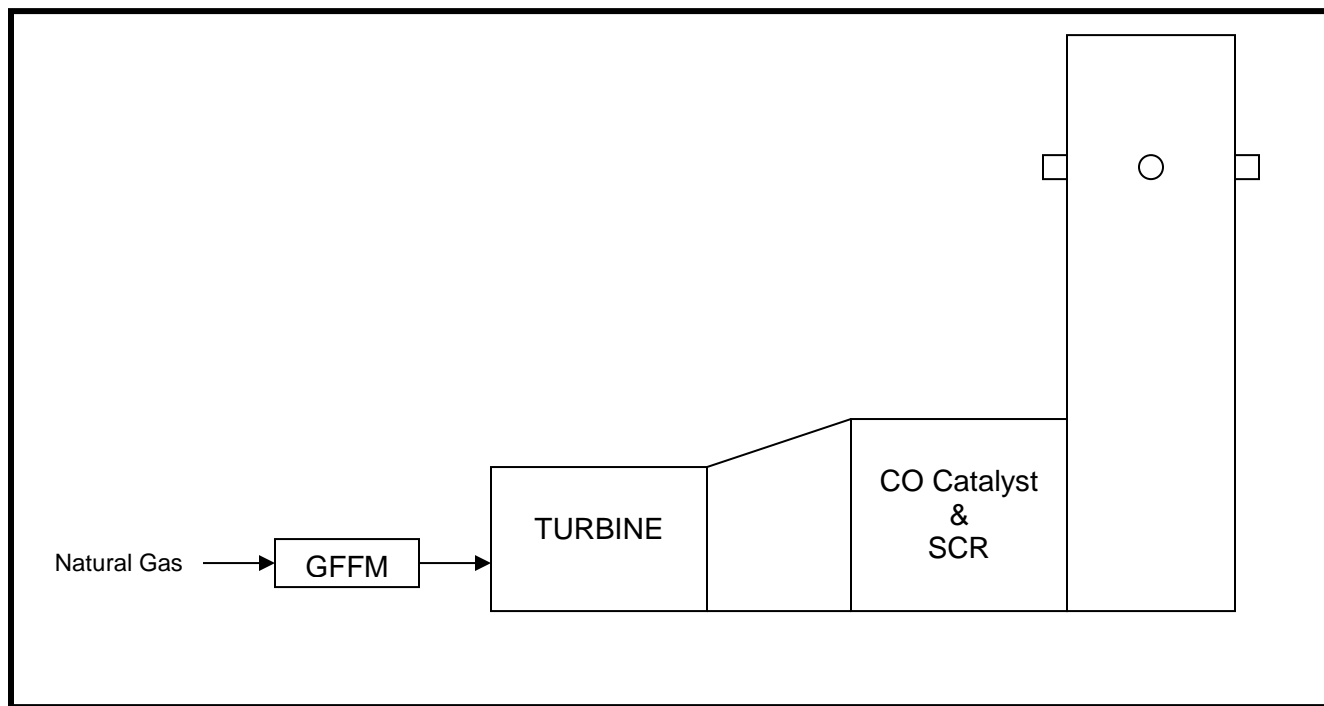
Section 2 of this document provides a brief description of the unit, test conditions, sample location, and CEMS. Details of the test procedures are provided in Section 3. Section 4 provides the results of each individual test. All raw data, calculations, quality assurance data, unit operating conditions, and CEMS data are provided in the appendices.

2.0 UNIT AND CEMS DESCRIPTION

2.1 UNIT DESCRIPTION

The City of Anaheim Canyon Power Plant is located at 3071 E. Mira Loma Avenue, Anaheim, California 92806. The facility consists of four identical generating units. Each unit consists of a natural gas fired, GE Model LM6000PC Sprint simple cycle, gas turbine. The units are natural gas fired with a rated heat input of 479 MMBtu per hour at 46 degrees Fahrenheit, with water injection. The units are equipped with a CO catalyst and Selective Catalytic Reduction (SCR) system for NO_x control. Figure 2-1 presents a block diagram of the unit.

**FIGURE 2-1
UNIT BLOCK DIAGRAM
CANYON POWER PLANT**



Stack Inside Diameter:	11 feet, 8 inches
Distance from Upstream Disturbance:	23 feet, 4 inches (2.0 Diameters)
Distance from Stack Exit:	16 feet, 6 inches (1.4 Diameters)

2.2 TEST CONDITIONS

The tests were performed with the unit operating at an average load of 50 MW. Tests were performed while the unit was firing natural gas and operating under normal conditions. Unit operation was established by the Canyon Power Plant operators.

2.3 SAMPLE LOCATION

The measurements were made from sample ports located on the exhaust stack. There are four sample ports equally spaced at this location. The stack inside diameter at the sample plane is 11 feet, 8 inches. The sample ports are located 23 feet, 4 inches (2.0 diameters) downstream of the nearest flow disturbance and 16 feet, 6 inches (1.4 diameters) from the stack exit.

3.0 TEST DESCRIPTION

Flue gas samples were collected non-isokinetically using a SCAQMD Method 207.1 sample train. The samples were collected using a 12-point traverse at the exhaust stack location. Each test was performed over a 60 minute interval. The sample gas was drawn through a glass probe, Teflon sample line, two impingers each containing 100 ml of 0.1N H₂SO₄, an empty impinger, an impinger containing silica gel, and a dry gas meter. The optional nozzle and filter were not used since the source is natural gas fired. The contents of the sample line and the first three impingers were recovered and analyzed by SCAQMD Method 207.1 for ammonia concentration by Ion Specific Electrode analysis.

Stack O₂ and NO_x concentrations and stack volumetric flow rate data were recorded from the Continuous Emission Monitoring System (CEMS) which is installed on the unit. These data were used to correct the ammonia concentration to 15% O₂.

4.0 TEST RESULTS

The results of the test are summarized in Table 4-1. The results show that the maximum ammonia slip was 1.7 ppm @ 15% O₂ which is less than the permitted limit of 5 ppm @ 15% O₂.

**TABLE 4-1
AMMONIA SLIP TEST RESULTS
CANYON POWER PLANT UNIT 4
JUNE 11, 2019**

Parameter	Units	Run 1	Run 2	Average	Maximum ⁽¹⁾	Limit
Test		1-NH ₃ -U4	2-NH ₃ -U4			--
Date		6/11/2019	6/11/2019			--
Time		1027/1133	1213/1319			--
O ₂ ⁽²⁾	%	14.43	14.39	14.41	--	--
Stack Flow ⁽²⁾	dscfm @ T _{ref}	229,962	227,992	228,977	--	--
NO _x ⁽²⁾	ppmc	2.3	2.1	2.2	--	2.5
NH ₃	ppm	1.8	1.6	1.7	1.8	--
NH ₃	ppmc	1.7	1.4	1.6	1.7	5
NH ₃	lb/hr	1.1	1.0	1.1	1.1	--
NH ₃	lb/MMBtu	0.002	0.002	0.002	0.002	--
NH ₃	lb/MMSCF	2.4	2.1	2.2	2.4	--

(1) Maximum of duplicate test runs, as required by SCAQMD Method 207.1

(2) From facility CEMS

APPENDIX A RAW DATA

Appendix A.1 Sample Data Sheets

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: CANADON
 LOCATION: CANADON 4
 DATE: 6/11/16
 RUN NO: 1-N/A-5-U4
 OPERATOR: SS
 METER BOX NO: 12005
 METER ΔH@: 1.024
 METER Yd: 1.005
 STACK AREA, FT²: 106.90
 TRAVERSE POINTS, MIN/POINT: 5/12
 ΔH = X ΔP:
 Probe Condition, pre/post test: good/good
 Silica Gel Expanded, Y/N: N
 Filter Condition after Test: NA
 Check Weight: 480.9/500.0

AMBIENT TEMPERATURE: 87°
 BAROMETRIC PRESSURE: 29.75
 ASSUMED MOISTURE: NA
 PITOT TUBE COEFF. Cp: NA
 PROBE ID NO/MATERIAL: NA / glass
 PROBE LENGTH: 6'
 NOZZLE ID NO/MATERIAL: NA
 NOZZLE DIAMETER: NA
 FILTER NO/TY: NA
 PRE-TEST LEAK RATE: 0.005 CFM@ 15 in. Hg.
 POST-TEST LEAK RATE: 0.010 CFM@ 15 in. Hg.
 PITOT LEAK CHECK - PRE: NA POST: NA
 CHAIN OF CUSTODY: SAMPLE CUSTODIAN: SS
SAMPLER: SS
SAMPLE CUSTODIAN: SS

Imp. # Contents Post-Test - Pre-Test = Difference
 1 H₂SO₄ 890.6 701.5
 2 H₂SO₄ 731.1 727.0
 3 NA 660.4 659.7
 4 SS 940.2 926.6
LR 100
 Total:

Point	Time	Meter Volume, ft³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
3	1027	184.580	NA	1.5	NA	NA	NA	59	86 87	3.0		NA
2	1032											
1	1037											
508	1042											
N 3	1044	199.875		1.5				56	85 84	3.0		
2	1047											
1	1051											
508	1054											
E 3	1051	210.310		1.5				59	86 86	3.0		
2	1060											
1	1111											
508	1116											
S 3	1116	221.300		1.5				60	88 87	3.0		
2	1123											
1	1128											
END	1133	231.130										
Average:												

Comments:

WET CHEMICAL SAMPLING SYSTEM DATA AND WORKSHEET - STANDARD

CLIENT: CANADIAN AMBIENT TEMPERATURE: 87 Imp. # Contents Post-Test - Pre-Test = Difference

LOCATION: CHRYSLER BAROMETRIC PRESSURE: 29.75 1 H₂SO₄ 873.4678.6

DATE: 6/11/19 ASSUMED MOISTURE: 6.7 2 H₂SO₄ 684.3679.8

RUN NO: 2-2143-214 PITOT TUBE COEFF, Cp: NA 3 mt 644.9640.6

OPERATOR: SS PROBE ID NO/MATERIAL: NA 4 SG 818.7802.3

METER BOX NO: 12005 PROBE LENGTH: 7' 5 100.0 -10.1

METER ΔH@: 1.624 NOZZLE ID NO/MATERIAL: NA

METER Yd: 1.0005 NOZZLE DIAMETER: NA

STACK AREA, FT²: 106.90 FILTER NO/TYPE: NA

TRAVERSE POINTS, MIN/POINT: 5/12 PRE-TEST LEAK RATE: 0.000 CFM@ 1.5 in. Hg.

ΔH= X ΔP: POST-TEST LEAK RATE: 0.009 CFM@ 1.5 in. Hg.

Probe Condition, pre/post test: good/good PITOT LEAK CHECK - PRE: NA POST: NA

Silica Gel Expanded, Y/N: N CHAIN OF CUSTODY: SS

Filter Condition after Test: NA SAMPLER SS

Check Weight: 444.9/500.0 SAMPLE CUSTODIAN SS

Total: SS

Point	1213 Time	Meter Volume, ft ³	ΔP in. H ₂ O	ΔH in. H ₂ O	Stack Temp, °F	Probe Temp, °F	Filter Temp, °F	Imp. Out Temp, °F	Meter Temp, °F In Out	Vacuum in. Hg.	O ₂ %	P. static in. H ₂ O
3	1225	233.300	NA	1.5	NA	NA	NA	60	88 88	3		NA
2	1210											
1	1223											
stop	1225	242.658		1.5				60	87 87	3.0		
3	1230											
2	1235											
1	1240											
stop	1245											
3	1247	253.680		1.5				60	88 87	3.0		
2	1252											
1	1257											
500	1302	264.660		1.5				60	89 88	3.0		
3	1304											
2	1309											
1	1314											
END	1319	275.850										
Average:												

Comments: 536/10/19

Appendix A.2 Laboratory Data

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS

Project #: 002AS-543226 District Method: SCAQMD 207.1 Sample Date: 6/11/19
 Client/Location: SCPFA U4 Calibration Date: 6/18/19 Analysis Date: 6/18/19
 Sample Location: Stack Calibration Curve: $y = -57.6167 + 85.066x$ Analyst's Initials: KC
 Test #s: 1, 2 -NH₃ R²: 0.9999

Sample	Electrode Potential (mV)	TV (ml)	Conc. $\mu\text{g NH}_3 - \text{N / ml}$	Cavg ($\mu\text{g NH}_3 - \text{N / ml}$)	$\mu\text{g NH}_3 / \text{sample}$	Comments/ Temp/pH
Standard Check: 28 $\mu\text{g NH}_3/\text{ml}$	2.2	—	27.431	27.431	—	Percent Recovery: $T = 22^\circ\text{C}$
Repeat 28 $\mu\text{g NH}_3/\text{ml}$	2.2	—	27.431	—	—	$T = 22^\circ\text{C}$
1-NH ₃	65.1	556	2.221	2.170	1480.346	$T = 22^\circ\text{C}$ pH < 2
repeat 1-NH ₃	65.8	—	2.160	—	—	$T = 22^\circ\text{C}$
2-NH ₃	69.9	587	1.833	1.830	1305.518	$T = 22^\circ\text{C}$ pH < 2
repeat 2-NH ₃	70.0	—	1.826	—	—	$T = 22^\circ\text{C}$
Spike 2-NH ₃	8.2	—	21.583	21.713	—	$T = 22^\circ\text{C}$
repeat spike 2-NH ₃	7.9	—	21.843	—	—	$T = 22^\circ\text{C}$
28 $\mu\text{g NH}_3/\text{ml}$	2.5	—	27.104	27.433	—	$T = 22^\circ\text{C}$
repeat 28 $\mu\text{g NH}_3/\text{ml}$	1.9	—	27.762	—	—	$T = 22^\circ\text{C}$
Reagent blank	187.9	—	0.015	0.015	—	$T = 22^\circ\text{C}$
repeat Reagent blank	190.0	—	0.015	—	—	$T = 22^\circ\text{C}$
Field blank	181.0	—	0.022	0.022	—	$T = 22^\circ\text{C}$
repeat Field blank	180.9	—	0.022	—	—	$T = 22^\circ\text{C}$
DI H ₂ O blank	180.0	—	0.023	0.022	—	$T = 22^\circ\text{C}$
repeat DI H ₂ O blank	180.5	—	0.022	—	—	$T = 22^\circ\text{C}$
28 $\mu\text{g NH}_3 / \text{ml}$	2.8	—	26.781	26.888	—	$T = 22^\circ\text{C}$
repeat 28 $\mu\text{g NH}_3/\text{ml}$	2.6	—	26.996	—	—	$T = 22^\circ\text{C}$

Notes: Total volume of samples and standards used: 100 ml * KC 6/18/19
 Volume of pH adjusting ISA used in ml: 2 ml
 Absorbing solution: 0.1N H₂SO₄

Calculations: Conc. ($\mu\text{g NH}_3 - \text{N / ml}$) = $10^{(P-B)/M}$
 P = electrode potential, B = y-intercept and M = slope
 Cavg = average result of duplicate analyses ($\mu\text{g NH}_3 - \text{N / ml}$) = $(C1+C2)/2$
 $\mu\text{g NH}_3 / \text{sample} = \text{Cavg} \times 17.03 / 14.01 \times \text{TV}$
 $\text{mg / sample} = \mu\text{g / sample} + 1000$
 $\text{ppm NH}_3 = \text{mg NH}_3/\text{sample} \times 1/\text{Vstd} \times 1/454000 \times \text{SV}/17 \times 10^6$

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS CALCULATION

Project Number: 002AS-543226
 Client/ Location: SCPPA
 Sample Location: U4
 District Method: SCAQMD 207.1
 Sample Date: 6/11/2019
 Analysis Date: 6/18/2019
 Analyst's Initials: KC
 Calibration Curve Slope -57.6167
 Y-intercept 85.0667
 R² 0.9999
 Probe #9

Sample	P mV	Conc. µg NH ₃ /ml as N	C avg as N	TV (ml)	C avg as NH ₃	µg NH ₃ / sample
28 ug NH ₃ / ml as N	2.2	27.431				
Repeat 28 ug NH ₃ /ml as N	2.2	27.431	27.431	NA	33.344	NA
1-NH ₃	65.1	2.221				
Repeat 1- NH ₃	65.8	2.160	2.190	556	2.662	1480.346
2-NH ₃	69.9	1.833				
Repeat 2- NH ₃	70.0	1.826	1.830	587	2.224	1305.518
spike 2-NH ₃	8.2	21.583				
Repeat 2-NH ₃ spike	7.9	21.843	21.713	NA	26.393	NA
28 NH ₃ /ml as N	2.5	27.104				
Repeat 28 ug NH ₃ /ml as N	1.9	27.762	27.433	NA	33.346	NA
Reagent Blank	189.9	0.015				
Repeat Reagent Blank	190.0	0.015	0.015	NA	0.018	NA
Field Blank	181.0	0.022				
Repeat Field Blank	180.9	0.022	0.022	NA	0.026	NA
DI H ₂ O Blank	180.0	0.023				
Repeat DI H ₂ O Blank	180.5	0.022	0.022	NA	0.027	NA
28 NH ₃ /ml as N	2.8	26.781				
Repeat 28 ug NH ₃ /ml as N	2.6	26.996	26.888	NA	32.685	NA

Notes:

Measured Concentration of Ammonia (C) in µg NH₃ / ml as N

$$C = 10^{(P-B)/M}$$

P = electrode potential (mV), M=slope and B=intercept

Average Measured Ammonia Concentration (Cavg) = (C1 + C2)/2

where C1, C2 results from duplicate analyses (µg NH₃ /ml as N)

Cavg (µg NH₃/ml as NH₃) = Cavg (µg NH₃/ ml as N) * 17.03/ 14.01

µg NH₃ / sample = Cavg (µg NH₃/ml as NH₃) * TV

Used 100 ml of samples and standards with 2 ml ISA and constant stirring rate.

All solutions turned blue and remained blue with ISA unless otherwise indicated.

Sample PH and Temperatures can be found on the laboratory datasheet.

Maximum samples (including blanks) between 28 ug/ml check standard is 5 samples analyzed in duplicate.

AMMONIA BY ION SELECTIVE ELECTRODE ANALYSIS QUALITY CONTROL

Project Number: 002AS-543226
 Client/ Location: SCPPA
 Sample Location: U4
 District Method: SCAQMD 207.1
 Sample Date: 6/11/2019
 Analysis Date: 6/18/2019
 Analyst's Initials: KC

Sample	% recovery	RPD %	RPA %
28 ug NH3 / ml as N Repeat 28 ug NH3/ml as	NA	0.00	-2.032
1-NH3 Repeat 1- NH3	NA	2.80	NA
2-NH3 Repeat 2- NH3	NA	0.40	NA
spike 2-NH3 Repeat 2-NH3 spike	103.58	-1.20	NA
28 NH3/ml as N Repeat 28 ug NH3/ml as	NA	-2.40	-2.025
Reagent Blank Repeat Reagent Blank	NA	0.40	NA
Field Blank Repeat Field Blank	NA	-0.40	NA
DI H2O Blank Repeat DI H2O Blank	NA	2.00	NA
28 NH3/ml as N Repeat 28 ug NH3/ml as	NA	-0.80	-3.970

Notes:

spike: 100 ml sample + 2 ml (1000 µg NH₃ / ml as N)

Matrix Spike Percent Recovery (%R)

%R = (C spike*0.104 - Csample*0.102)/2 *100

Cspike = average result of matrix spike (µg NH₃/ ml as N)

Relative Percent Difference (RPD) = (C1-C2)/ Cavg *100 (must be 5% or less)

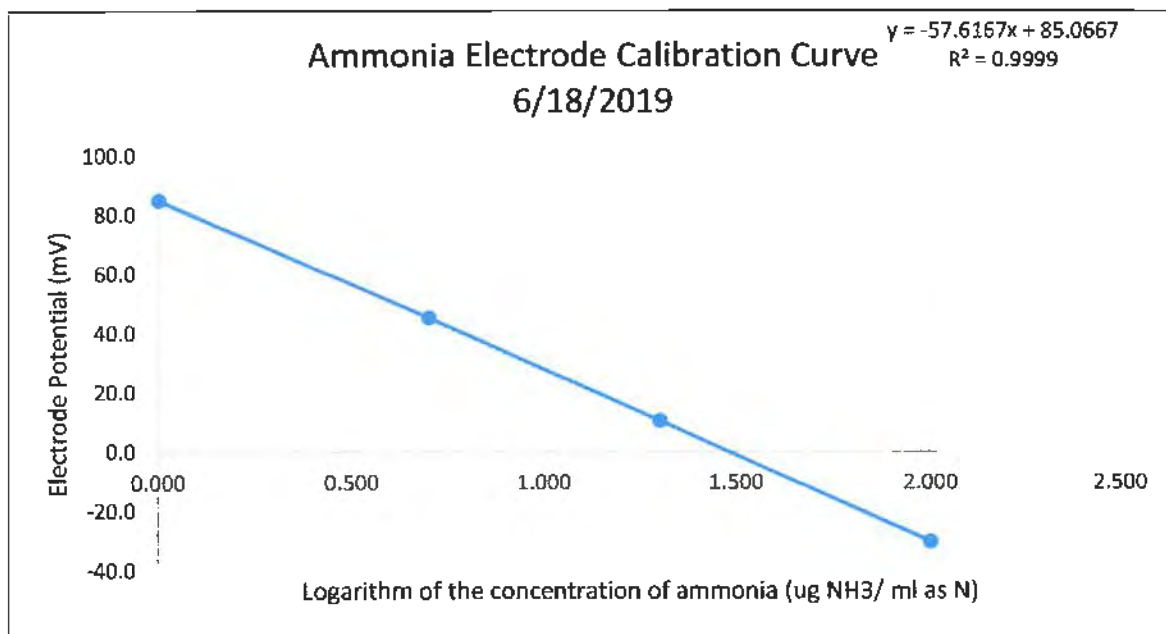
Relative Percent Accuracy (RPA) (must be 10% or less)

RPA = (Cavg-theoretical value of standard)/ theoretical value of standard * 100

AMMONIA ELECTRODE CALIBRATION CURVE

Probe 9

NH ₃ concentration (μg NH ₃ / ml as N)	log NH ₃ concentration	Electrode potential (mV)	Sample Temperature (C)	Room Temperature (C)
1	0.000	84.7	22	22
5	0.699	45.2	22	22
20	1.301	10.4	22	22
100	2.000	-30.5	22	22



```
slope      -57.6167
y-intercept 85.0667
```

Concentration ($\mu\text{g NH}_3$ / ml as N)	Value LR line	Difference	% Difference
1	1.0148	0.0148	1.4765
5	4.9196	-0.0804	-1.6080
20	19.7661	-0.2339	-1.1695
100	101.3407	1.3407	1.3407

Calculation:

Regression Line: $P = M \cdot \log(\mu\text{g of NH}_3 / \text{ml as N}) + B$

Measured Concentration of Ammonia (C) in $\mu\text{g} / \text{ml NH}_3$ as N: $C=10^{(P-B)/M}$

where P = electrode potential, M= slope (must be -57 ± 3) and B= intercept

All standards were prepared in 0.04N H_2SO_4 and allowed to equilibrate to room temperature.

Appendix A.3

QA/QC Data

SCAQMD METHOD 207.1 - AMMONIA DETERMINATION OF SAMPLE TIME

Source: Canyon U4
Date: 6/11/2019
Performed by: JG

Constants:

	1,000	mg/gram
	454	grams/lb
	35.315	SCF/SCM
	379.5	SCF/lb-mole
	1,000,000	parts/million parts
MW _{NH3}	17.03	lb/lb-mole
MW _{N2}	14.01	lb/lb-mole

Variables:

Target concentration	5	ppm @ O ₂ correction factor
O ₂ correction factor	15	% O ₂
Expected Flue Gas O ₂	14.5	% O ₂
F	2	Safety Factor
P	128.5	electrode potential corresponding to minimum value on calibration curve (mV)
B	128.83	y-intercept
M	-58.676	slope
V _r	0.5	Assumed liquid volume of probe rinse and first impinger (L)
Q @ dH = 1	0.55	cfm

Calculated Values:

Target concentration	5.4	ppm - raw
Target concentration	3.90	mg/dscm
C ₁	1.013	Lowest concentration on a calibration curve (mg NH ₃ -N/L)
RL	0.616	analytical mass reporting limit, mg
PSV	0.316	Planned sample volume, cubic meters
PSV	11.144	Planned sample volume, cubic feet
VSR	33.0	achievable volumetric sampling rate (dscf/hr)

PST	20.3	Planned sample time, minutes (minimum)
------------	-------------	---

Notes:

- 1) A minimum of 1 hour sample time is required for any mass per hour limits.
- 2) Facility Permit or Rule may specify sample time

SEMI-ANNUAL DRY GAS METER/ORIFICE CALIBRATION

Orifice Method - Triplicate Runs/Four Calibration Points
English Meter Box Units, English K Factor
Filename: M:\Santa Ana\Equipment\Test Equipment\Calibrations\Dry Gas Meter\12-wcs\2019\2019-19.xls
File Modified From: APEX 522 Series Meter box Calibration
Revised: 4/9/2005

Model #: c5000
ID #: 12 wcs
Date: 2/19/2019
Bar. Pressure: 30.14 (in. Hg)
Performed By: R. Howard

CRITICAL ORIFICE READINGS									
DRY GAS METER READINGS					K Orifice				
dH (in H ₂ O)	Time (min)	Volume Initial (cu ft)	Volume Final (cu ft)	Volume Total (cu ft)	Initial Temp. (deg F)	Outlet Temp. (deg F)	Final Temp. (deg F)	Initial (deg F)	Average (deg F)
0.11	26.00	192.500	197.763	5.263	54.0	53.0	53.0	47.0	47.0
0.11	26.00	197.783	203.063	5.280	54.0	53.0	53.0	48.0	48.0
0.11	26.00	203.063	208.349	5.286	54.0	52.0	54.0	49.0	49.0
0.56	12.00	160.300	165.451	5.151	54.0	52.0	54.0	44.0	44.0
0.56	12.00	165.451	170.606	5.155	54.0	52.0	54.0	45.0	45.0
0.56	12.00	170.606	175.764	5.148	54.0	52.0	54.0	45.0	45.0
1.80	7.00	142.700	147.933	5.233	54.0	50.0	54.0	45.0	45.0
1.80	7.00	147.933	153.160	5.227	54.0	50.0	54.0	45.0	45.0
1.80	7.00	153.160	158.399	5.239	54.0	51.0	54.0	44.0	44.0
3.10	5.00	176.900	181.799	4.899	55.0	52.0	55.0	45.0	45.0
3.10	5.00	181.799	186.690	4.891	55.0	53.0	56.0	46.0	46.0
3.10	5.00	186.690	191.599	4.909	56.0	54.0	57.0	46.0	46.0

DRY GAS METER									
ORIFICE					DRY GAS METER				
CALIBRATION FACTOR					CALIBRATION FACTOR				
VOLUME CORRECTED Vm(std) (cu ft)	VOLUME CORRECTED Vm(std) (liters)	VOLUME CORRECTED Vm(std) (cu ft)	VOLUME CORRECTED Vm(std) (liters)	VOLUME NOMINAL Vm (cu ft)	Y Valve (number)	dH@ Value (in H ₂ O)	Individual Run	Individual Orifice	Orifice Average
5.468	154.8	5.400	152.9	5.149	0.968	1.486	Pass	Ymax - Ymin < 0.010?	dH@ - dH@ av < 0.155?
5.474	155.0	5.394	152.8	5.154	0.996	1.492	Pass		
5.480	155.2	5.389	152.6	5.159	0.963	1.495	Pass		
				Average	0.966	1.481	Pass	Pass	Pass
5.346	151.4	5.386	152.6	5.108	1.008	1.623	Pass		
5.350	151.5	5.393	152.4	5.113	1.006	1.626	Pass		
5.343	151.3	5.383	152.4	5.113	1.008	1.626	Pass		
				Average	1.007	1.626	Pass	Pass	Pass
5.459	154.6	5.553	157.3	5.275	1.017	1.678	Pass		
5.449	154.3	5.553	157.3	5.275	1.019	1.676	Pass		
5.456	154.5	5.559	157.4	5.270	1.019	1.669	Pass		
				Average	1.018	1.674	Pass	Pass	Pass
5.108	144.7	5.149	145.8	4.891	1.008	1.708	Pass		
5.082	144.2	5.144	145.7	4.896	1.010	1.705	Pass		
5.104	144.5	5.144	145.7	4.896	1.008	1.705	Pass		
				Average	1.009	1.706	Pass	Pass	Pass
Average Yd: 1.005					dH@: 1.624				
					Q @ dH = 1: 0.589				

SIGNED: _____

Date: _____

2/19/2019



DIGITAL TEMPERATURE READOUT CALIBRATION

Digital Temperature Readout ID: 12-WCS
 Readout Description: Control Box
 Date: 12/31/2018
 Performed By: JG/DA/RH/JS

Calibrated Thermocouple ID: TC-CAL
 T1 Reference Thermometer ID: 242196
 T2 Reference Thermometer ID: 242196
 T3 Reference Thermometer ID: 242167

T/C I.D. TC-CAL	Readout I.D.	T/C - Readout °F				Reference Thermometer °F				Difference		
		Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
T3 (Oil)	12-WCS	355	355	355	355	358	358	358	358	3.0	0.4%	Pass
T2 (Boiling H ₂ O)	12-WCS	209	209	209	209	212	212	212	212	3.0	0.4%	Pass
T1 (Ice/Water)	12-WCS	29	29	29	29	32	32	32	32	3.0	0.6%	Pass

1) Difference % (°R) = Difference (°F) / (Average Tref + 460)

2) Pass if all Differences are less than 1.5% (°R)

Thermocouple Source Readings

T/C Source S/N	T/C - Readout °F				T/C Source °F				Difference		
	Reading 1	Reading 2	Reading 3	Average	Reading 1	Reading 2	Reading 3	Average	°F	%, (°R)	
T4 (~650 F)	S/N 106970	648	648	648	648	650	650	650	2.0	0.2%	Pass
T3 (~370 F)	S/N 106970	361	361	361	361	365	365	365	4.0	0.5%	Pass
T2 (~212 F)	S/N 106970	209	209	209	209	212	212	212	3.0	0.4%	Pass
T1 (~32 F)	S/N 106970	28	28	28	28	32	32	32	4.0	0.8%	Pass

1) Difference % (°R) = Difference (°F) / (Average Tref + 460)

2) Pass if all Differences are less than 1.5% (°R)

W002AS-543226-RT-53

TEST DATE(S): 6/11/2019

SAMPLER(S): SS/LO

PROJECT MANAGER: JG

DATE DUE: 6/18/2019

COMPLIANCE TEST?: Yes

24 of 53

6/12/19 0500

SAMPLES REQUIRED: NH_3 by SCAQMD 207.1 (ISE)
Samples were stored at 4°C before analysis



Chain of Custody - DS834001 - Excel
Master Document Storage\Forms\Data sheets\Lab Forms

APPENDIX B FACILITY CEMS DATA

Port09

Page 1

Sabco & Wilcox Power Generation Group NetDAHSK
Average Values Report
Version 60.0
Generated: 6/11/2019 13:08

Company: City of Anaheim
Plant: 3071 N. Ralston Ave.,
City/St: Anaheim, CA, 92806
Source: unit4, unit4_inlet

Period Start: 6/11/2019 10:27
Period End: 6/11/2019 11:33
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

Period Start	4_Flame_On 1=ON	4_GasFlow kacfh	4_NH3_Flow #/hr	4_O2 %	4_NOXPPH ppm	4_HCX CORR ppm	4_STACKFLW Kscfm	4T_NOX_COR ppm	4_NH3SLIP ppm	4_LOAD MW	4_NOX_LBHR #/hr
6/11/2019 10:27	1	472.4	81.37	14.44	2.50	2.28	232.9	17.95	9.54	49.98	3.97
6/11/2019 10:28	1	472.9	81.52	14.45	2.50	2.29	233.5	18.05	9.43	50.19	3.97
6/11/2019 10:29	1	472.6	81.40	14.45	2.51	2.30	233.4	18.08	9.38	50.17	3.97
6/11/2019 10:30	1	473.3	81.43	14.44	2.50	2.28	233.4	17.96	9.49	50.21	3.95
6/11/2019 10:31	1	473.2	81.39	14.44	2.50	2.28	233.4	17.96	9.48	50.20	3.95
6/11/2019 10:32	1	473.5	81.44	14.44	2.49	2.27	233.5	18.04	9.35	50.24	3.95
6/11/2019 10:33	1	473.3	81.45	14.44	2.48	2.28	233.4	17.97	9.46	50.11	3.95
6/11/2019 10:34	1	473.3	81.45	14.44	2.42	2.21	233.4	17.91	9.43	50.10	3.95
6/11/2019 10:35	1	473.5	81.51	14.44	2.43	2.20	233.5	17.83	9.56	50.21	3.98
6/11/2019 10:36	1	473.7	81.53	14.44	2.36	2.16	233.7	17.75	9.21	50.45	3.98
6/11/2019 10:37	1	473.9	80.32	14.44	2.36	2.16	233.7	17.75	9.22	50.08	3.98
6/11/2019 10:38	1	474.0	80.36	14.44	2.36	2.16	233.7	17.75	9.22	50.08	3.98
6/11/2019 10:39	1	474.1	80.43	14.45	2.43	2.22	234.2	17.73	9.27	50.17	3.98
6/11/2019 10:40	1	473.8	80.33	14.44	2.47	2.26	233.7	17.63	9.43	50.08	3.98
6/11/2019 10:41	1	474.0	80.32	14.44	2.47	2.26	233.7	17.57	9.49	50.12	3.98
6/11/2019 10:42	1	474.0	80.22	14.44	2.45	2.24	233.7	17.48	9.53	50.16	3.98
6/11/2019 10:43	1	474.3	80.30	14.44	2.44	2.23	233.5	17.42	9.58	50.20	3.98
6/11/2019 10:44	1	474.6	80.27	14.43	2.42	2.21	233.7	17.44	9.55	50.16	3.99
6/11/2019 10:45	1	473.8	80.25	14.43	2.42	2.21	233.3	17.51	9.52	50.17	3.98
6/11/2019 10:46	1	474.3	80.18	14.43	2.44	2.23	233.5	17.44	9.56	50.35	3.98
6/11/2019 10:47	1	474.4	80.33	14.44	2.45	2.24	233.9	17.33	9.69	50.25	3.98
6/11/2019 10:48	1	474.4	80.16	14.43	2.44	2.23	233.6	17.42	9.57	50.15	3.98
6/11/2019 10:49	1	474.3	80.35	14.43	2.43	2.22	233.5	17.40	9.57	50.29	3.98
6/11/2019 10:50	1	474.2	80.28	14.42	2.42	2.20	233.1	17.44	9.60	50.19	3.98
6/11/2019 10:51	1	474.0	80.20	14.43	2.44	2.23	233.4	17.44	9.59	50.19	3.98
6/11/2019 10:52	1	474.2	80.25	14.43	2.44	2.23	233.5	17.37	9.67	50.21	3.98
6/11/2019 10:53	1	474.4	80.35	14.44	2.44	2.23	233.9	17.43	9.58	50.18	3.98
6/11/2019 10:54	1	474.2	80.33	14.43	2.42	2.21	233.5	17.40	9.53	50.13	3.98
6/11/2019 10:55	1	474.3	80.27	14.43	2.41	2.20	233.5	17.44	9.60	50.09	3.98
6/11/2019 10:56	1	474.1	80.24	14.42	2.42	2.20	233.1	17.44	9.60	50.10	3.98
6/11/2019 10:57	1	474.3	80.41	14.43	2.43	2.22	233.5	17.43	9.64	50.10	3.98
6/11/2019 10:58	1	474.3	80.28	14.43	2.43	2.22	233.5	17.38	9.65	50.13	3.98
6/11/2019 10:59	1	474.1	80.29	14.42	2.43	2.21	233.1	17.45	9.61	50.26	3.98
6/11/2019 11:00	1	473.8	80.34	14.43	2.45	2.23	233.8	17.35	9.73	50.10	3.98
6/11/2019 11:01	1	474.2	80.30	14.43	2.47	2.25	233.9	17.19	9.87	50.21	3.98
6/11/2019 11:02	1	474.5	80.26	14.43	2.44	2.23	233.6	17.17	9.85	50.22	3.99
6/11/2019 11:03	1	473.8	80.23	14.42	2.41	2.19	232.9	17.30	9.74	50.23	3.98
6/11/2019 11:04	1	473.8	80.19	14.44	2.42	2.21	233.7	17.38	9.59	50.21	3.98
6/11/2019 11:05	1	473.5	80.10	14.44	2.44	2.23	233.5	17.31	9.67	50.18	3.98
6/11/2019 11:06	1	473.8	80.26	14.44	2.43	2.22	233.7	17.23	9.77	50.11	3.98
6/11/2019 11:07	1	473.9	80.31	14.43	2.43	2.22	233.3	17.17	9.89	50.13	3.98
6/11/2019 11:08	1	473.6	80.33	14.43	2.42	2.21	233.2	17.05	10.01	50.20	3.98
6/11/2019 11:09	1	474.0	80.31	14.44	2.40	2.19	233.7	17.15	9.83	50.05	3.98
6/11/2019 11:10	1	474.5	80.28	14.44	2.35	2.17	234.0	17.30	9.62	50.02	3.95
6/11/2019 11:11	1	474.7	80.40	14.43	2.36	2.18	233.9	17.35	9.64	50.20	3.98
6/11/2019 11:12	1	474.3	80.47	14.44	2.37	2.18	233.9	17.44	9.52	50.25	3.90
6/11/2019 11:13	1	473.9	79.39	14.44	2.39	2.18	233.7	17.44	9.25	50.26	3.98
6/11/2019 11:14	1	474.6	79.21	14.44	2.41	2.20	234.0	17.48	9.14	50.19	3.99
6/11/2019 11:15	1	474.0	79.27	14.42	2.45	2.27	235.0	17.39	9.43	50.16	3.98
6/11/2019 11:16	1	474.4	79.23	14.42	2.54	2.31	233.2	17.45	9.27	50.01	4.48
6/11/2019 11:17	1	474.2	79.20	14.43	2.56	2.33	233.5	17.52	9.28	50.13	4.48
6/11/2019 11:18	1	474.2	79.22	14.42	2.58	2.33	234.1	17.56	9.28	50.05	4.48
6/11/2019 11:19	1	474.3	79.26	14.42	2.57	2.34	234.2	17.61	9.23	50.10	4.48
6/11/2019 11:20	1	474.1	79.22	14.42	2.57	2.34	233.1	17.51	9.35	50.22	4.48
6/11/2019 11:21	1	474.3	79.14	14.42	2.56	2.33	233.2	17.48	9.33	50.22	4.48
6/11/2019 11:22	1	474.5	79.22	14.43	2.56	2.33	233.6	17.60	9.20	50.15	4.48
6/11/2019 11:23	1	474.5	79.14	14.42	2.56	2.33	233.3	17.55	9.25	50.29	4.48
6/11/2019 11:24	1	474.3	79.17	14.43	2.55	2.33	233.5	17.50	9.29	50.18	4.48
6/11/2019 11:25	1	474.3	79.24	14.44	2.55	2.33	233.7	17.62	9.15	50.26	4.48
6/11/2019 11:26	1	474.1	79.16	14.43	2.55	2.33	233.4	17.63	9.15	50.39	4.48
6/11/2019 11:27	1	474.3	79.17	14.43	2.57	2.34	233.2	17.60	9.20	50.16	4.48
6/11/2019 11:28	1	474.2	79.19	14.43	2.58	2.35	233.5	17.57	9.25	50.12	4.48
6/11/2019 11:29	1	474.2	79.22	14.43	2.58	2.35	233.5	17.54	9.29	50.19	4.48
6/11/2019 11:30	1	473.5	79.26	14.42	2.58	2.35	233.0	17.48	9.41	50.17	4.48
6/11/2019 11:31	1	473.9	79.21	14.42	2.58	2.35	233.0	17.44	9.44	50.18	4.48
6/11/2019 11:32	1	473.9	79.14	14.43	2.58	2.35	233.3	17.52	9.30	50.19	4.48
6/11/2019 11:33	1	473.6	79.12	14.42	2.60	2.37	232.8	17.45	9.46	50.17	4.48
Final Average*	1	474.5	80.33	14.43	2.47	2.25	233.6	17.52	9.49	50.18	4.11
Maximum*	1	474.6	81.53	14.45	2.60	2.37	234.2	18.08	10.01	50.45	4.48
Minimum*	1	472.4	79.14	14.42	2.36	2.15	232.8	17.05	9.14	49.98	3.97

*Does not include Invalid Averaging Periods ("N/A")

2-NH₃

Font09

Babcock & Wilcox Power Generation Group Ne-DARE50
Average Values Report
Version 60.0
Generated: 6/11/2019 15:40

Page 1

Company: City Of Anaheim
Plant: 5071 Miraloma Ave.,
City/State: Anaheim, CA 92806
Source: Unit4, unit4_inlet

Period Start: 6/11/2019 12:13
Period End: 6/11/2019 13:19
Validation Type: 1/1 min
Averaging Period: 1 min
Type: Block Avg

Period Start	4_Flame_On 1-on	4_GasFlow kscfh	4_NH3_Flow #/hr	4_O2 %	4_NOXPPM ppm	4_1_NOX ppm	4_STACKFLOW kscfm	4_NOX CORR ppm	4_NH3SLIP ppm	4_LOAD MW	4_NOX_LBRH #/hr
6/11/2019 12:13	1	474.3	80.40	14.35	2.17	19.07	230.7	1.95	9.93	50.27	3.49
6/11/2019 12:14	1	474.5	80.32	14.35	2.23	18.99	230.8	2.01	10.01	50.16	3.49
6/11/2019 12:15	1	474.2	80.23	14.35	2.31	19.05	230.6	2.08	10.02	50.26	3.90
6/11/2019 12:16	1	474.5	80.95	14.35	2.34	19.01	230.8	2.11	10.11	50.36	3.99
6/11/2019 12:17	1	474.0	80.24	14.35	2.34	19.01	230.9	2.11	10.06	50.16	3.99
6/11/2019 12:18	1	473.9	80.20	14.36	2.32	18.87	230.8	2.09	10.14	50.17	3.98
6/11/2019 12:19	1	474.2	80.13	14.30	2.28	18.87	231.7	2.07	9.94	50.26	3.98
6/11/2019 12:20	1	473.5	80.30	14.38	2.23	18.75	231.4	2.02	10.09	50.22	3.48
6/11/2019 12:21	1	473.8	80.29	14.38	2.20	18.76	231.5	1.99	10.03	50.28	3.48
6/11/2019 12:22	1	473.7	79.92	14.38	2.2	18.72	231.5	2.00	9.97	50.23	3.48
6/11/2019 12:23	1	473.6	79.13	14.37	2.23	18.68	231.7	2.01	9.83	50.14	3.48
6/11/2019 12:24	1	474.0	79.19	14.38	2.25	18.69	231.6	2.07	9.84	50.20	3.98
6/11/2019 12:25	1	474.1	79.17	14.38	2.35	18.64	231.6	2.13	9.92	50.15	3.98
6/11/2019 12:26	1	474.0	79.15	14.38	2.34	18.66	231.6	2.12	9.89	50.18	3.98
6/11/2019 12:27	1	473.9	79.11	14.38	2.34	18.56	231.6	2.12	9.96	50.17	3.98
6/11/2019 12:28	1	473.9	79.17	14.39	2.32	18.68	231.9	2.10	9.80	50.19	3.98
6/11/2019 12:29	1	473.8	79.17	14.39	2.31	18.64	231.9	2.09	9.83	50.16	3.98
6/11/2019 12:30	1	473.3	79.20	14.39	2.31	18.70	231.6	2.09	9.81	50.12	3.98
6/11/2019 12:31	1	473.5	79.26	14.39	2.31	18.66	231.7	2.09	9.86	50.13	3.98
6/11/2019 12:32	1	473.1	79.24	14.39	2.31	18.70	231.5	2.09	9.84	50.17	3.97
6/11/2019 12:33	1	473.3	79.34	14.39	2.32	18.76	231.6	2.10	9.82	50.28	3.98
6/11/2019 12:34	1	473.7	79.22	14.38	2.32	18.69	231.5	2.10	9.88	50.25	3.98
6/11/2019 12:35	1	473.1	79.24	14.39	2.34	18.70	231.5	2.12	9.87	50.09	3.97
6/11/2019 12:36	1	473.2	79.24	14.39	2.34	18.77	231.6	2.12	9.80	50.23	3.98
6/11/2019 12:37	1	473.2	79.27	14.39	2.33	18.67	231.6	2.11	9.88	50.07	3.98
6/11/2019 12:38	1	473.4	79.21	14.38	2.31	18.64	231.3	2.09	9.93	50.32	3.98
6/11/2019 12:39	1	473.1	79.23	14.39	2.31	18.75	231.5	2.09	9.79	50.24	3.97
6/11/2019 12:40	1	473.3	79.26	14.39	2.32	18.75	231.6	2.10	9.80	50.11	3.98
6/11/2019 12:41	1	473.2	79.19	14.38	2.35	18.77	231.2	2.11	9.83	50.14	3.98
6/11/2019 12:42	1	473.4	78.48	14.38	2.35	18.75	231.3	2.11	9.98	50.23	3.98
6/11/2019 12:43	1	473.2	78.42	14.38	2.35	18.71	231.2	2.13	9.67	50.14	3.98
6/11/2019 12:44	1	473.2	78.38	14.39	2.41	18.76	231.6	2.18	9.60	50.12	3.98
6/11/2019 12:45	1	473.1	78.31	14.39	2.44	18.76	231.5	2.21	9.62	50.26	3.97
6/11/2019 12:46	1	472.7	78.27	14.39	2.44	18.69	231.3	2.21	9.68	50.10	3.97
6/11/2019 12:47	1	473.2	78.28	14.39	2.43	18.82	231.6	2.20	9.53	50.21	3.98
6/11/2019 12:48	1	473.2	78.29	14.39	2.36	18.73	231.6	2.17	9.58	50.06	3.98
6/11/2019 12:49	1	473.1	78.30	14.39	2.38	18.73	231.3	2.16	9.59	50.12	3.97
6/11/2019 12:50	1	473.3	78.25	14.39	2.38	18.75	231.6	2.16	9.51	50.17	3.98
6/11/2019 12:51	1	473.1	78.30	14.39	2.38	18.74	231.5	2.16	9.58	50.13	3.97
6/11/2019 12:52	1	473.2	78.35	14.39	2.37	18.73	231.6	2.15	9.59	50.34	3.98
6/11/2019 12:53	1	473.1	78.33	14.39	2.37	18.65	231.5	2.15	9.68	50.28	3.97
6/11/2019 12:54	1	473.3	78.31	14.39	2.37	18.67	231.5	2.15	9.64	50.16	3.97
6/11/2019 12:55	1	472.9	78.22	14.40	2.37	18.66	231.7	2.15	9.57	50.22	3.97
6/11/2019 12:56	1	472.9	78.23	14.39	2.40	18.70	231.4	2.15	9.62	50.23	3.97
6/11/2019 12:57	1	473.0	78.25	14.40	2.44	18.84	231.8	2.21	9.47	50.30	3.97
6/11/2019 12:58	1	473.1	78.29	14.39	2.45	18.95	231.5	2.22	9.54	50.21	3.97
6/11/2019 12:59	1	473.1	78.41	14.39	2.45	18.81	231.5	2.22	9.61	50.10	3.97
6/11/2019 13:00	1	473.0	78.35	14.40	2.44	18.80	231.8	2.21	9.55	50.20	3.97
6/11/2019 13:01	1	473.2	78.29	14.39	2.43	18.89	231.6	2.20	9.47	50.28	3.98
6/11/2019 13:02	1	473.1	78.49	14.39	2.43	18.72	231.5	2.20	9.69	50.10	3.97
6/11/2019 13:03	1	473.3	78.40	14.39	2.42	18.70	231.6	2.19	9.66	50.23	3.98
6/11/2019 13:04	1	473.3	78.33	14.39	2.42	18.65	231.6	2.19	9.69	50.23	3.98
6/11/2019 13:05	1	473.3	78.41	14.39	2.42	18.72	231.6	2.19	9.65	50.16	3.98
6/11/2019 13:06	1	473.2	78.32	14.39	2.42	18.81	231.6	2.19	9.54	50.15	3.98
6/11/2019 13:07	1	473.2	78.31	14.39	2.42	18.80	231.6	2.19	9.55	50.25	3.98
6/11/2019 13:08	1	473.1	78.30	14.39	2.41	18.78	231.5	2.18	9.56	50.11	3.97
6/11/2019 13:09	1	473.1	78.40	14.40	2.41	18.73	231.9	2.19	9.60	50.17	3.97
6/11/2019 13:10	1	473.2	78.45	14.40	2.41	18.83	231.9	2.19	9.51	50.23	3.98
6/11/2019 13:11	1	473.5	78.44	14.39	2.41	18.79	231.7	2.18	9.58	50.23	3.98
6/11/2019 13:12	1	473.2	78.49	14.39	2.41	18.79	231.6	2.18	9.60	50.14	3.97
6/11/2019 13:13	1	473.1	78.42	14.39	2.42	18.77	231.5	2.19	9.62	50.08	3.97
6/11/2019 13:14	1	473.2	78.58	14.39	2.43	18.84	231.6	2.20	9.61	50.40	3.98
6/11/2019 13:15	1	473.8	78.59	14.39	2.42	18.77	231.9	2.19	9.63	50.31	3.98
6/11/2019 13:16	1	473.2	78.53	14.39	2.41	18.76	231.6	2.18	9.64	50.10	3.98
6/11/2019 13:17	1	473.0	78.42	14.39	2.41	18.75	231.5	2.18	9.63	50.19	3.97
6/11/2019 13:18	1	473.4	78.45	14.39	2.41	18.75	231.7	2.18	9.62	50.15	3.98
6/11/2019 13:19	1	473.1	78.58	14.39	2.40	18.73	231.5	2.18	9.70	50.21	3.97
Final Average*	1	473.4	78.39	14.39	2.36	18.76	231.5	2.14	9.73	50.19	3.93
Maximum*	1	474.8	80.40	14.40	2.45	19.07	231.9	2.22	10.14	50.40	3.99
Minimum*	1	472.7	78.22	14.35	2.17	18.56	230.6	1.95	9.47	50.06	3.48

*Does not include Invalid Averaging Periods ("N/A")

APPENDIX C CALCULATIONS

Appendix C.1

General Emissions Calculations

GENERAL EMISSION CALCULATIONS

I. Stack Gas Velocity

A. Stack gas molecular weight, lb/lb-mole

$$MW_{dry} = 0.44 * \%CO_2 + 0.32 * \%O_2 + 0.28 * \%N_2$$

$$MW_{wet} = MW_{dry} * (1 - B_{wo}) + 18 * B_{wo}$$

B. Absolute stack pressure, iwg

$$P_s = P_{bar} + \frac{P_{sg}}{13.6}$$

C. Stack gas velocity, ft/sec

$$V_s = 2.9 * C_p * \sqrt{\Delta P} * \sqrt{T_s} * \sqrt{\frac{29.92 * 28.95}{P_s * MW_{wet}}}$$

II. Moisture

A. Sample gas volume, dscf

$$V_{mstd} = 0.03342 * V_m * (P_{bar} + \frac{\Delta H}{13.6}) * \frac{T_{ref}}{T_m} * Y_d$$

B. Water vapor volume, scf

$$V_{wstd} = 0.0472 * V_{lc} * \frac{T_{ref}}{528 ^\circ R}$$

C. Moisture content, dimensionless

$$B_{wo} = \frac{V_{wstd}}{(V_{mstd} + V_{wstd})}$$

III. Stack gas volumetric flow rate

A. Actual stack gas volumetric flow rate, wacfm

$$Q = V_s * A_s * 60$$

B. Standard stack gas flow rate, dscfm

$$Q_{sd} = Q * (1 - B_{wo}) * \frac{T_{ref}}{T_s} * \frac{P_s}{29.92}$$

IV. Gaseous Mass Emission Rates, lb/hr

$$M = \frac{\text{ppm} * MW_i * Q_{sd} * 60}{SV * 10^6}$$

V. Emission Rates, lb/MMBtu

$$\frac{\text{lb}}{\text{MMBtu}} = \frac{\text{ppm} * MW_i * F}{SV * 10^6} * \frac{20.9}{20.9 - \%O_2}$$

VI. Percent Isokinetic

$$I = \frac{17.32 * T_s (V_{mstd})}{(1-Bwo) * 0 * V_s * P_s * Dn2} * \frac{520^{\circ}R}{T_{ref}}$$

VII. Particulate emissions

(a) Grain loading, gr/dscf
 $C = 0.01543 (M_n/V_{mstd})$

(b) Grain loading at 12% CO₂, gr/dscf
 $C_{12\% CO_2} = C (12/\% CO_2)$

(c) Mass emissions, lb/hr
 $M = C * Q_{sd} * (60 \text{ min/hr}) / (7000 \text{ gr/lb})$

(d) Particulate emission factor
 $\text{lb}/10^6 \text{ Btu} = C * \frac{1 \text{ lb}}{7000 \text{ gr}} * F * \frac{20.9}{20.9 - \% O_2}$

Nomenclature:

A_s	= stack area, ft ²
B_{wo}	= flue gas moisture content, dimensionless
$C_{12\%CO_2}$	= particulate grain loading, gr/dscf corrected to 12% CO ₂
C	= particulate grain loading, gr/dscf
C_p	= pitot calibration factor, dimensionless
D_n	= nozzle diameter, in.
F	= fuel F-Factor, dscf/MMBtu @ 0% O ₂
H	= orifice differential pressure, iwg
I	= % isokinetics
M_n	= mass of collected particulate, mg
M_i	= mass emission rate of specie i, lb/hr
MW	= molecular weight of flue gas, lb/lb-mole
M_{wi}	= molecular weight of specie i: SO ₂ : 64 NO _x : 46 CO: 28 HC: 16
t	= sample time, min.
ΔP	= average velocity head, iwg = $(\sqrt{\Delta P})^2$
P_{bar}	= barometric pressure, inches Hg
P_s	= stack absolute pressure, inches Hg
P_{sg}	= stack static pressure, iwb
Q	= wet stack flow rate at actual conditions, wacfm
Q_{sd}	= dry standard stack flow rate, dscfm
SV	= specific molar volume of an ideal gas at standard conditions, ft ³ /lb-mole
T_m	= meter temperature, °R
T_{ref}	= reference temperature, °R
T_s	= stack temperature, °R
V_s	= stack gas velocity, ft/sec
V_{lc}	= volume of liquid collected in impingers, ml
V_m	= uncorrected dry meter volume, dcf
V_{mstd}	= dry meter volume at standard conditions, dscf
V_{wstd}	= volume of water vapor at standard conditions, scf
Y_d	= meter calibration coefficient

Appendix C.2

Spreadsheet Summaries

SCAQMD 207.1 EXAMPLE CALCULATION

TEST NUMBER: 1-NH3-U4

Identifier	Description	Units	Equation	Value
A	Reference Temperature	F	--	60
B	Reference Temperature	R	$A + 460$	520
C	Meter Calibration Factor (Yd)	--	--	1.005
D	Barometric Pressure	" Hg	--	29.69
E	Meter Volume	acf	--	41.550
F	Meter Temperature	F	--	86.1
G	Meter Temperature	R	$F + 460$	546.1
H	Delta H	" H ₂ O	--	1.5
I	Meter Volume (standard)	dscf	$0.03342 * E * (D + H/13.6) * B/G * C$	39.600
J	Liquid Collected	grams	--	107.5
K	Water vapor volume	scf	$0.0472 * J * B/528$	4.997
L	Moisture Content	--	$K/(K + I)$	0.112
M	Gas Constant	ft-lbf/lb-mole-R	--	1545.33
N	Specific Molar Volume	SCF/lb-mole	$385.3 * B / 528$	379.5
O	F-Factor	dscf/MMBtu	--	8,710
P	HHV	Btu/SCF	--	1,050
Q	Mass Conversion Factor	lb/ug	--	2.2046E-09
R	O ₂ Correction Factor	--	--	15
S	Stack Flow Rate @ 68 F	dscfm	--	233,500
T	Stack Flow Rate @ Tref	dscfm	$S * B/528$	229,962
U	Mass NH ₃	ug	--	1,480
V	Mass NH ₃	lb	$U * Q$	3.26E-06
W	MW of NH ₃	lb/lb-mole	--	17.03
X	NH ₃	ppm	$(V * N * 10^6)/(I * W)$	1.8
Y	Flue Gas O ₂	%	--	14.43
Z	NH ₃	ppmc	$X * (20.9 - R)/(20.9 - Y)$	1.7
AA	NH ₃	lb/hr	$X * T * W * 60/(N * 10^6)$	1.1
AB	NH ₃	lb/MMBtu	$(X * W * O)/(385.3 * 10^6) * 20.9/(20.9 - Y)$	0.002
AC	NH ₃	lb/MMSCF	$AB * P$	2.4

Note:

(1) Some values may be slightly different from those shown on the run sheets due to round off errors. This page is intended to show the calculation methodology only.

SCAQMD METHOD 207.1 DATA WORKSHEET AND SUMMARY

Facility.....	Canyon		Parameter.....	NH₃	
Unit.....	U4		Fuel.....	Natural gas	
Sample Location.....	Stack		Data By.....	JG	
Test Number.....	1-NH3-U4	2-NH3-U4	Average	Maximum	Limit
Reference Temperature (°F).....	60	60			
Test Date.....	6/11/2019	6/11/2019			
Test Method.....	SCAQMD 207.1	SCAQMD 207.1			
Sample Train.....	12-WCS	12-WCS			
Meter Calibration Factor.....	1.005	1.005			
Stack Area (ft ²).....	106.90	106.90			
Sample Time (Minutes).....	60	60			
Barometric Pressure ("Hg).....	29.75	29.75			
Start/Stop Time	1027/1133	1213/1319			
Meter Volume (acf).....	41.550	42.550			
Meter Temperature (°F).....	86.1	87.8			
Meter Pressure (iwg).....	1.5	1.5			
Liquid Volume (ml).....	107.5	112.0			
Stack O ₂ (%).....	14.43	14.39	14.41	(from facility CEMS)	
Unit Load (MW).....	50.2	50.2	50.2		
Standard Sample Volume (SCF).....	39.680	40.509			
Moisture Fraction.....	0.112	0.114			
Stack Flow Rate (dscfm, 68 °F).....	233,500	231,500	232,500	(from facility CEMS)	
Stack Flow Rate (@ Tref).....	229,962	227,992	228,977		
Gas Constant (ft-lbf/lb-mole-R).....	1545.33	1545.33			
Molecular Weight NH ₃ (lb/lb-mole).....	17.03	17.03			
Specific Molar Volume (ft ³ /lb-mole).....	379.5	379.5			
F-Factor (dscf/MMBtu).....	8,710	8,710			
HHV(Btu/SCF).....	1,050	1,050			
Mass Conversion (lb/ug).....	2.2046E-09	2.2046E-09			
O ₂ Correction Factor (%).....	15	15			
Mass NH ₃ (ug).....	1,480	1,306			
Mass NH ₃ (lb).....	3.26E-06	2.88E-06			
NH ₃ (ppmv, flue gas).....	1.8	1.6	1.7	1.8	
NH ₃ (ppmv @ O ₂ Correction Factor).....	1.7	1.4	1.6	1.7	5
NH ₃ (lb/hr).....	1.1	1.0	1.1	1.1	
NH ₃ (lb/MMBtu).....	0.002	0.002	0.002	0.002	
NH ₃ (lb/MMSCF).....	2.4	2.1	2.2	2.4	

Note: SCAQMD Method 207.1 requires the higher of the duplicate runs be reported as the test result.

APPENDIX D QUALITY ASSURANCE

Appendix D.1

Quality Assurance Program Summary

QUALITY ASSURANCE PROGRAM SUMMARY

As part of Montrose Air Quality Services, LLC (MAQS) ASTM D7036-04 certification, MAQS is committed to providing emission related data which is complete, precise, accurate, representative, and comparable. MAQS quality assurance program and procedures are designed to ensure that the data meet or exceed the requirements of each test method for each of these items. The quality assurance program consists of the following items:

- Assignment of an Internal QA Officer
- Development and use of an internal QA Manual
- Personnel training
- Equipment maintenance and calibration
- Knowledge of current test methods
- Chain-of-custody
- QA reviews of test programs

Assignment of an Internal QA Officer: MAQS has assigned an internal QA Officer who is responsible for administering all aspects of the QA program.

Internal Quality Assurance Manual: MAQS has prepared a QA Manual according to the requirements of ASTM D7036-04 and guidelines issued by EPA. The manual documents and formalizes all of MAQS QA efforts. The manual is revised upon periodic review and as MAQS adds capabilities. The QA manual provides details on the items provided in this summary.

Personnel Testing and Training: Personnel testing and training is essential to the production of high quality test results. MAQS training programs include:

- A requirement for all technical personnel to read and understand the test methods performed
- A requirement for all technical personnel to read and understand the MAQS QA manual
- In-house testing and training
- Quality Assurance meetings
- Third party testing where available
- Maintenance of training records.

Equipment Maintenance and Calibration: All laboratory and field equipment used as a part of MAQS emission measurement programs is maintained according to manufacturer's recommendations. A summary of the major equipment maintenance schedules is summarized in Table 1. In addition to routine maintenance, calibrations are performed on all sampling equipment according to the procedures outlined in the applicable test method. The calibration intervals and techniques for major equipment components is summarized in Table 2. The calibration technique may vary to meet regulatory agency requirements.

Knowledge of Current Test Methods: MAQS maintains current copies of EPA, ARB, and SCAQMD Source Test Manuals and Rules and Regulations.

Chain-of-Custody: MAQS maintains chain-of-custody documentation on all data sheets and samples. Samples are stored in a locked area accessible only to MAQS source test personnel. Data sheets are kept in the custody of the originator, program manager, or in locked storage until return to MAQS office. Electronic field data is duplicated for backup on secure storage media. The original data sheets are used for report preparation and any additions are initialed and dated.

QA Reviews: Periodic field, laboratory, and report reviews are performed by the in-house QA coordinator. Periodically, test plans are reviewed to ensure proper test methods are selected and reports are reviewed to ensure that the methods were followed and any deviations from the methods are justified and documented.

ASTM D7036-04 Required Information

Uncertainty Statement

Montrose is qualified to conduct this test program and has established a quality management system that led to accreditation with ASTM Standard D7036-04 (Standard Practice for Competence of Air Emission Testing Bodies). Montrose participates in annual functional assessments for conformance with D7036-04 which are conducted by the American Association for Laboratory Accreditation (A2LA). All testing performed by Montrose is supervised on site by at least one Qualified Individual (QI) as defined in D7036-04 Section 8.3.2. Data quality objectives for estimating measurement uncertainty within the documented limits in the test methods are met by using approved test protocols for each project as defined in D7036-04 Sections 7.2.1 and 12.10. Additional quality assurance information is presented in the report appendices.

Performance Data

Performance data are available for review.

Qualified Personnel

A qualified individual (QI), defined by performance on a third party or internal test on the test methods, will be present on each test event.

Plant Entry and Safety Requirements

Plant Entry

All test personnel are required to check in with the guard at the entrance gate or other designated area. Specific details are provided by the facility and project manager.

Safety Requirements

All personnel shall have the following personal protective equipment (PPE) and wear them where designated:

- Hard Hat
- Safety Glasses
- Steel Toe Boots
- Hearing Protection
- Gloves
- High Temperature Gloves (if required)

The following safety measures will be followed:

- Good housekeeping
- SDS for all on-site hazardous materials
- Confine selves to necessary areas (stack platform, mobile laboratory, CEMS data acquisition system, control room, administrative areas)
- Knowledge of evacuation procedures

Each facility will provide plant specific safety training.

TABLE 1
EQUIPMENT MAINTENANCE SCHEDULE

Equipment	Acceptance Limits	Frequency of Service	Methods of Service
Pumps	1. Absence of leaks 2. Ability to draw manufacturers required vacuum and flow	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Replace parts 4. Leak check
Flow Meters	1. Free mechanical movement	As recommended by manufacturer	1. Visual inspection 2. Clean 3. Calibrate
Sampling Instruments	1. Absence of malfunction 2. Proper response to zero span gas	As recommended by manufacturer	As recommended by manufacturer
Integrated Sampling Tanks	1. Absence of leaks	Depends on nature of use	1. Steam clean 2. Leak check
Mobil Van Sampling System	1. Absence of leaks	Depends on nature of use	1. Change filters 2. Change gas dryer 3. Leak check 4. Check for system contamination
Sampling lines	1. Sample degradation less than 2%	After each test series	1. Blow dry, inert gas through line until dry

TABLE 2
MAJOR SAMPLING EQUIPMENT CALIBRATION REQUIREMENTS

Sampling Equipment	Calibration Frequency	Calibration Procedure	Acceptable Calibration Criteria
Continuous Analyzers	Before and After Each Test Day	3-point calibration error test	< 2% of analyzer range
Continuous Analyzers	Before and After Each Test Run	2-point sample system bias check	< 5% of analyzer range
Continuous Analyzers	After Each Test Run	2-point analyzer drift determination	< 3% of analyzer range
CEMS System	Beginning of Each Day	leak check	< 1 in. Hg decrease in 5 min. at > 20 in. Hg
Continuous Analyzers	Semi-Annually	3-point linearity	< 1% of analyzer range
NO _x Analyzer	Daily	NO ₂ -> NO converter efficiency	> 90%
Differential Pressure Gauges (except for manometers)	Semi-Annually	Correction factor based on 5-point comparison to standard	+/- 5%
Differential Pressure Gauges (except for manometers)	Bi-Monthly	3-point comparison to standard, no correction factor	+/- 5%
Barometer	Semi-Annually	Adjusted to mercury-in-glass or National Weather Service Station	+/- 0.1 inches Hg
Dry Gas Meter	Semi-Annually	Calibration check at 4 flow rates using a NIST traceable standard	+/- 2%
Dry Gas Meter	Bi-Monthly	Calibration check at 2 flow rates using a NIST traceable standard	+/- 2% of semi-annual factor
Dry Gas Meter Orifice	Annually	4-point calibration for ΔH@	--
Temperature Sensors	Semi-Annually	3-point calibration vs. NIST traceable standard	+/- 1.5%

Note: Calibration requirements will be used that meet applicable regulatory agency requirements.

Appendix D.2

SCAQMD and STAC Certifications



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 • www.aqmd.gov

October 30, 2018

Mr. John Peterson
Montrose Air Quality Services, LLC
1631 E. Saint Andrew Place
Santa Ana, CA 92705

Subject: LAP Approval Notice
Reference # 96LA1220

Dear Mr. Peterson:

We have reviewed your renewal letter under the South Coast Air Quality Management District's Laboratory Approval Program (SCAQMD LAP). We are pleased to inform you that your firm is approved for the period beginning October 30, 2018, and ending September 30, 2019 for the following methods, subject to the requirements in the LAP Conditions For Approval Agreement and conditions listed in the attachment to this letter:

SCAQMD Methods 1-4	SCAQMD Methods 5.1, 5.2, 5.3, 6.1
SCAQMD Methods 10.1 and 100.1	SCAQMD Methods 25.1 and 25.3 (Sampling)
USEPA CTM-030 and ASTM D6522-00	SCAQMD Rule 1121/ 1146.2 Protocol
SCAQMD Rule 1420/1420.1/1420.2 – (Lead) Source and Ambient Sampling	

Your LAP approval to perform nitrogen oxide emissions compliance testing for SCAQMD Rule 1121/ 1146.2 Protocols includes satellite facilities located at:

McKenna Boiler
1510 North Spring Street
Los Angeles, CA 90012

Noritz America Corp.
11160 Grace Avenue
Fountain Valley, CA 92708

Ajax Boiler, Inc.
2701 S. Harbor Blvd.
Santa Ana, CA 92704

Thank you for participating in the SCAQMD LAP. Your cooperation helps us to achieve the goal of the LAP: to maintain high standards of quality in the sampling and analysis of source emissions. You may direct any questions or information to LAP Coordinator, Glenn Kasai. He may be reached by telephone at (909) 396-2271, or via e-mail at gkasai@aqmd.gov.

Sincerely,

A handwritten signature in black ink that reads 'D. Sarkar'.

Dipankar Sarkar
Program Supervisor
Source Test Engineering

DS:GK/gk

Attachment

181030 LapRenewalRev.doc

Cleaning the air that we breathe...™



American Association for Laboratory Accreditation

Accredited Air Emission Testing Body

A2LA has accredited

MONTROSE AIR QUALITY SERVICES

In recognition of the successful completion of the joint A2LA and Stack Testing Accreditation Council (STAC) evaluation process, this laboratory is accredited to perform testing activities in compliance with ASTM D7036:2004 - Standard Practice for Competence of Air Emission Testing Bodies.

Presented this 5th day of March 2018.



President and CEO
For the Accreditation Council
Certificate Number 3925.01
Valid to February 29, 2020

This accreditation program is not included under the A2LA ILAC Mutual Recognition Arrangement.

Appendix D.3 Individual QI Certificate

CERTIFICATE OF COMPLETION

John Groenenboom

This document certifies that this individual has passed a comprehensive examination and is now a Qualified Individual (QI) as defined in Section 8.3 of ASTM D7036-04 for the following method(s):

SCAQMD Method 207.1

Certificate Number: 002-2017-51

Tate Strickler

Tate Strickler, Accreditation Director

DATE OF ISSUE: 1/17/17

DATE OF
EXPIRATION: 1/17/22



APPENDIX E APPLICABLE PERMIT SECTIONS



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions* And Requirements	Conditions
Process 1: POWER GENERATION					
GAS TURBINE, NO. 4, NATURAL GAS, GENERAL ELECTRIC, MODEL LM6000PC SPRINT, SIMPLE CYCLE, 479 MMBTU/HR AT 46 DEG F, WITH INLET CHILLING, WITH WATER INJECTION WITH A/N: 555831	D19	C21	NOX: MAJOR SOURCE**	CO: 4 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]; CO: 2000 PPMV NATURAL GAS (5) [RULE 407, 4-2-1982]; NOX: 2.5 PPMV NATURAL GAS (4) [RULE 2005, 6-3-2011]; NOX: 25 PPMV NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; PM10: 0.01 GRAINS/SCF NATURAL GAS (5A) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; PM10: 0.1 GRAINS/SCF NATURAL GAS (5) [RULE 409, 8-7-1981]; PM10: 1.67 LBS/HR NATURAL GAS (5C) [RULE 1303(b)(2)-Offset, 5-10-1996; RULE 1303(b)(2)-Offset, 12-6-2002]; PM10: 11 LBS/HR NATURAL GAS (5B) [RULE 475, 10-8-1976; RULE 475, 8-7-1978]; SO2: (9) [40CFR 72 - Acid Rain Provisions, 11-24-1997]; SOX: 0.06 LBS/MMBTU NATURAL GAS (8) [40CFR 60 Subpart KKKK, 7-6-2006]; VOC: 2 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A63.1, A99.1, A99.2, A99.3, A195.1, A195.2, A195.3, A327.1, B61.1, D12.1, D29.2, D29.3, D82.1, D82.2, E193.1, H23.1, I298.4, K40.1
GENERATOR, 50.95 MW					

* (1) (1A) (1B) Denotes RECLAIM emission factor (2) (2A) (2B) Denotes RECLAIM emission rate
(3) Denotes RECLAIM concentration limit (4) Denotes BACT emission limit
(5) (5A) (5B) Denotes command and control emission limit (6) Denotes air toxic control rule limit
(7) Denotes NSR applicability limit (8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(9) See App B for Emission Limits (10) See section J for NESHAP/MACT requirements

** Refer to 40 CFR 60.441 for information to determine the monitoring, testing and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

Equipment	ID No.	Connected To	RECLAIM Source Type/ Monitoring Unit	Emissions* And Requirements	Conditions
Process 1: POWER GENERATION					
CO OXIDATION CATALYST, NO. 4, BASE, 110 CUBIC FEET OF TOTAL CATALYST VOLUME A/N: 476663	C21	D19 C22			
SELECTIVE CATALYTIC REDUCTION, NO. 4, CORMETECH CMHT-21, 1012 CU.FT.; WIDTH: 2 FT 6 IN; HEIGHT: 25 FT 9 IN; LENGTH: 18 FT WITH A/N: 476663	C22	C21 S24		NH3: 5 PPMV NATURAL GAS (4) [RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]	A195.7, D12.2, D12.3, D12.4, E179.1, E179.2, E193.1
AMMONIA INJECTION					
STACK, TURBINE NO. 4, HEIGHT: 86 FT ; DIAMETER: 11 FT 8 IN A/N: 555831	S24	C22			
System 2: INTERNAL COMBUSTION ENGINE					

- * (1) (1A) (1B) Denotes RECLAIM emission factor
(3) Denotes RECLAIM concentration limit
(5) (5A) (5B) Denotes command and control emission limit
(7) Denotes NSR applicability limit
(9) See App B for Emission Limits
- (2) (2A) (2B) Denotes RECLAIM emission rate
(4) Denotes BACT emission limit
(6) Denotes air toxic control rule limit
(8) (8A) (8B) Denotes 40 CFR limit (e.g. NSPS, NESHAPS, etc.)
(10) See section J for NESHAP/MACT requirements

** Refer to section F and G of this permit to determine the monitoring, recordkeeping and reporting requirements for this device.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

[Devices subject to this condition : C4, C10, C16, C22]

D12.5 The operator shall install and maintain a(n) non-resettable elapsed time meter to accurately indicate the elapsed operating time of the engine.

[RULE 1110.2, 2-1-2008; RULE 1110.2, 9-7-2012; RULE 1303(b)(2)-Offset, 5-10-1996;
RULE 1303(b)(2)-Offset, 12-6-2002; RULE 1401, 9-10-2010; RULE 1470, 5-4-2012;
RULE 2012, 5-6-2005; 40CFR 60 Subpart IIII, 1-30-2013]

[Devices subject to this condition : D25]

D29.2 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Averaging Time	Test Location
NH3 emissions	District method 207.1 and 5.3 or EPA method 17	1 hour	Outlet of the SCR serving this equipment



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION D: FACILITY DESCRIPTION AND EQUIPMENT SPECIFIC CONDITIONS

The operator shall comply with the terms and conditions set forth below:

The test(s) shall be conducted at least quarterly during the first twelve months of operation and at least annually thereafter. The AQMD shall be notified of the date and time of the test at least 10 days prior to the test.

If the turbine is not in operation during one calendar year, then no testing is required during that calendar year.

The NO_x concentration, as determined by the CEMS, shall be simultaneously recorded during the ammonia slip test. If the CEMS is inoperable, a test shall be conducted to determine the NO_x emissions using District Method 100.1 measured over a 60 minute averaging time period.

The test shall be conducted and the results submitted to the District within 60 days after the test date.

The test shall be conducted to demonstrate compliance with the Rule 1303 concentration limit.

[RULE 1303(a)(1)-BACT, 5-10-1996; RULE 1303(a)(1)-BACT, 12-6-2002]

[Devices subject to this condition : D1, D7, D13, D19]

D29.3 The operator shall conduct source test(s) for the pollutant(s) identified below.

Pollutant(s) to be tested	Required Test Method(s)	Sampling Time	Test Location
SOX emissions	AQMD Laboratory Method 307-91	Not Applicable	Fuel sample
VOC emissions	District Method 25.3	1 hour	Outlet of the SCR serving this equipment
PM emissions	District method 5.1	4 hours	Outlet of the SCR serving this equipment

THIS IS THE LAST PAGE OF THIS DOCUMENT

If you have any questions, please contact one of the following individuals by email or phone.

Name: Mr. John Groenenboom
Title: Client Project Manager
Region: Western
E-Mail: JGroenenboom@montrose-env.com
Phone: (714) 279-6777

Name: Mr. Matt McCune
Title: Regional Vice President
Region: Western
E-Mail: MMccune@montrose-env.com
Phone: (714) 279-6777

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 17

AQ-14 & AQ-24
RTC INVENTORY



South Coast Air Quality Management District
21865 Copley Drive, Diamond Bar, CA 91765-4178

Title Page
Facility ID: 153992
Revision #: 14
Date: January 01, 2019

FACILITY PERMIT TO OPERATE


**CANYON POWER PLANT
3071 E MIRALOMA AVE
ANAHEIM, CA 92806**

NOTICE

IN ACCORDANCE WITH RULE 206, THIS PERMIT TO OPERATE OR A COPY THEREOF MUST BE KEPT AT THE LOCATION FOR WHICH IT IS ISSUED.

THIS PERMIT DOES NOT AUTHORIZE THE EMISSION OF AIR CONTAMINANTS IN EXCESS OF THOSE ALLOWED BY DIVISION 26 OF THE HEALTH AND SAFETY CODE OF THE STATE OF CALIFORNIA OR THE RULES OF THE SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT. THIS PERMIT SHALL NOT BE CONSTRUED AS PERMISSION TO VIOLATE EXISTING LAWS, ORDINANCES, REGULATIONS OR STATUTES OF ANY OTHER FEDERAL, STATE OR LOCAL GOVERNMENTAL AGENCIES.

Wayne Nastri
Executive Officer

By  For
Laki Tisopoulos, Ph.D., P.E.
Deputy Executive Officer
Engineering and Permitting



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

TABLE OF CONTENTS

Section	Description	Revision #	Date Issued
A	Facility Information	2	11/06/2015
B	RECLAIM Annual Emission Allocation	11	01/01/2019
C	Facility Plot Plan	TO BE DEVELOPED	
D	Facility Description and Equipment Specific Conditions	3	11/06/2015
E	Administrative Conditions	1	11/06/2015
F	RECLAIM Monitoring and Source Testing Requirements	1	11/06/2015
G	Recordkeeping and Reporting Requirements for RECLAIM Sources	1	11/06/2015
H	Permit To Construct and Temporary Permit to Operate	3	11/06/2015
I	Compliance Plans & Schedules	1	11/06/2015
J	Air Toxics	1	11/06/2015
K	Title V Administration	1	11/06/2015
Appendix			
A	NOx and SOx Emitting Equipment Exempt From Written Permit Pursuant to Rule 219	1	11/06/2015
B	Rule Emission Limits	1	11/06/2015



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION B: RECLAIM ANNUAL EMISSION ALLOCATION

The annual allocation of NOx RECLAIM Trading Credits (RTCs) for this facility is calculated pursuant to Rule 2002. Total NOx emission shall not exceed such annual allocations unless the operator obtains RTCs corresponding to the facility's increased emissions in compliance with Rules 2005 and 2007.

The level of Starting Allocation plus Non-Tradable Credits used to determine compliance with Rule 2005(c)(4) and applicability of Rule 2005(e) - Trading Zone Restrictions is listed on the last page of this Section.

The following table lists the annual allocations that were issued to this facility and the amounts of RTCs held by this facility on the day of printing this Section.

RECLAIM POLLUTANT ANNUAL ALLOCATION (POUNDS)

Year Begin End (month/year)	Zone	NOx RTC Initially Allocated	NOx RTC ¹ Holding as of 01/01/2019 (pounds)	Non-Tradable ² Non-Usable RTCs (pounds)
7/2016 6/2017	Coastal	0	3238	2548
1/2017 12/2017	Coastal	0	6391	0
7/2017 6/2018	Coastal	0	14377	0
1/2018 12/2018	Coastal	0	42179	1648
7/2018 6/2019	Coastal	0	18585	1292
1/2019 12/2019	Coastal	0	40532	1648
7/2019 6/2020	Coastal	0	17292	1292
1/2020 12/2020	Coastal	0	37283	3248
7/2020 6/2021	Coastal	0	14745	2548
1/2021 12/2021	Coastal	0	33988	3295
7/2021 6/2022	Coastal	0	12160	2585
1/2022 12/2022	Coastal	0	27445	6543
7/2022 6/2023	Coastal	0	7027	5133
1/2023 12/2023	Coastal	0	27445	0
7/2023 6/2024	Coastal	0	7027	0
1/2024 12/2024	Coastal	0	27445	0
7/2024 6/2025	Coastal	0	7027	0

Footnotes:

1. This number may change due to pending trades, emissions reported under Quarterly Certification of Emissions Report (QCER) and Annual Permit Emission Program (APEP) Report required pursuant to Rule 2004, or deductions made pursuant to Rule 2010(b). The most recent total RTC information can be obtained from the District's RTC Listing.
2. The use of such credits is subject to restrictions set forth in paragraph (f)(1) of Rule 2002.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION B: RECLAIM ANNUAL EMISSION ALLOCATION

The annual allocation of NO_x RECLAIM Trading Credits (RTCs) for this facility is calculated pursuant to Rule 2002. Total NO_x emission shall not exceed such annual allocations unless the operator obtains RTCs corresponding to the facility's increased emissions in compliance with Rules 2005 and 2007.

The level of Starting Allocation plus Non-Tradable Credits used to determine compliance with Rule 2005(c)(4) and applicability of Rule 2005(e) - Trading Zone Restrictions is listed on the last page of this Section.

The following table lists the annual allocations that were issued to this facility and the amounts of RTCs held by this facility on the day of printing this Section.

RECLAIM POLLUTANT ANNUAL ALLOCATION (POUNDS)

Year Begin End (month/year)	Zone	NO _x RTC Initially Allocated	NO _x RTC ¹ Holding as of 01/01/2019 (pounds)	Non-Tradable ² Non-Usable RTCs (pounds)
1/2025 12/2025	Coastal	0	27445	0
7/2025 6/2026	Coastal	0	7027	0
1/2026 12/2026	Coastal	0	27445	0
7/2026 6/2027	Coastal	0	7027	0
1/2027 12/2027	Coastal	0	27445	0
7/2027 6/2028	Coastal	0	7027	0
1/2028 12/2028	Coastal	0	27445	0
7/2028 6/2029	Coastal	0	7027	0
1/2029 12/2029	Coastal	0	27445	0
7/2029 6/2030	Coastal	0	7027	0
1/2030 12/2030	Coastal	0	27445	0
7/2030 6/2031	Coastal	0	7027	0
1/2031 12/2031	Coastal	0	27445	0
7/2031 6/2032	Coastal	0	7027	0
1/2032 12/2032	Coastal	0	27445	0
7/2032 6/2033	Coastal	0	7027	0
1/2033 12/2033	Coastal	0	27445	0

Footnotes:

1. This number may change due to pending trades, emissions reported under Quarterly Certification of Emissions Report (QCER) and Annual Permit Emission Program (APEP) Report required pursuant to Rule 2004, or deductions made pursuant to Rule 2010(b). The most recent total RTC information can be obtained from the District's RTC Listing.
2. The use of such credits is subject to restrictions set forth in paragraph (f)(1) of Rule 2002.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION B: RECLAIM ANNUAL EMISSION ALLOCATION

The annual allocation of NOx RECLAIM Trading Credits (RTCs) for this facility is calculated pursuant to Rule 2002. Total NOx emission shall not exceed such annual allocations unless the operator obtains RTCs corresponding to the facility's increased emissions in compliance with Rules 2005 and 2007.

The level of Starting Allocation plus Non-Tradable Credits used to determine compliance with Rule 2005(c)(4) and applicability of Rule 2005(e) - Trading Zone Restrictions is listed on the last page of this Section.

The following table lists the annual allocations that were issued to this facility and the amounts of RTCs held by this facility on the day of printing this Section.

RECLAIM POLLUTANT ANNUAL ALLOCATION (POUNDS)

Year Begin End (month/year)	Zone	NOx RTC Initially Allocated	NOx RTC ¹ Holding as of 01/01/2019 (pounds)	Non-Tradable ² Non-Usable RTCs (pounds)
7/2033 6/2034	Coastal	0	7027	0
1/2034 12/2034	Coastal	0	27445	0

Footnotes:

1. This number may change due to pending trades, emissions reported under Quarterly Certification of Emissions Report (QCER) and Annual Permit Emission Program (APEP) Report required pursuant to Rule 2004, or deductions made pursuant to Rule 2010(b). The most recent total RTC information can be obtained from the District's RTC Listing.
2. The use of such credits is subject to restrictions set forth in paragraph (f)(1) of Rule 2002.



FACILITY PERMIT TO OPERATE CANYON POWER PLANT

SECTION B: RECLAIM ANNUAL EMISSION ALLOCATION

The annual allocation of RECLAIM Trading Credits (RTCs) for this facility is calculated pursuant to Rule 2002. If the facility submits a permit application to increase in an annual allocation to a level greater than the facility's starting Allocation plus Non-Tradable credits as listed below, the application will be evaluated for compliance with Rule 2005 (c)(4). Rule 2005 (e) - Trading Zone Restrictions applies if an annual allocation is increased to a level greater than the facility's Starting Allocation plus Non-Tradable Credits:

Year			RTC	
Begin	End	Zone	Starting Allocation	Non-Tradable
(month/year)			(pounds)	Credits(NTC)
				(pounds)

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 18

AQ-17
NH3 FLOW METER ACCURACY REPORTS

HOMER R. DULIN CO.
729 EAST WILLOW STREET
SIGNAL HILL, CALIFORNIA 90755
(562) 424-8533 FAX (562) 426-7707
CERT. NO. 4-198AF-19
CALIBRATION CERTIFICATION

SUBMITTED BY: CITY OF ANAHEIM

FLOWMETER SERIAL NO: MFG. SERIAL NO: 14136005

MANUFACTURER: MICRO MOTION MODEL: CMF025M313NQBUEZZZ

TUBE NO: FLOAT NO:

DATA IS: As Found ; Out of Tolerance, See As Left Data See Remarks ☒
Adjustment Required Calibrated @ customer's facility ☐

REMARKS: METER VERY UNSTABLE & OUT OF TOLERANCE - PROGRAMMING REQUIRED - SEE AS LEFT DATA -

ACCURACY N/A

INDICATED		ACTUAL	
LB/H		LBS/HR	
150.22		152.40	
131.53		133.92	
112.60		114.36	
93.91		96.00	
75.00		76.68	
56.31		57.78	
46.83		48.30	
37.34		38.70	
28.22		28.80	
0.00		0.00	

Flowmeter Certified with HOMER R. DULIN CO.

Equip. No. 11605 Accuracy 0.005% Equip. Cal. Date: 8/29/18 Cal. Due: 8/29/21

NIST Cert. No. TEST# MS 15560 Procedure No: ISA:RP 16.6

Our standards are certified by or are traceable to the National Institute of Standards and Technology and systems comply with MIL-STD 45662A, ANSI/NCSL Z540.3, ISO/IEC 17025, and ISO 10012. The collective uncertainty of the standards used in this calibration does not exceed 25% of the certified accuracy of the instrument under test. This document may not be reproduced, except in full, without prior written approval of the Homer R. Dulin Co. Rev.1 Dated 8/19/14

P.O. No. Shipper No.

4-9-19

N/A

R. MARTINEZ *Rogelio Martinez*

CALIBRATION DATE

RECALIBRATION DUE

CALIBRATION TECHNICIAN

HOMER R. DULIN CO.
729 EAST WILLOW STREET
SIGNAL HILL, CALIFORNIA 90755
(562) 424-8533 FAX (562) 426-7707
CERT. NO. 4-198AL-19
CALIBRATION CERTIFICATION

SUBMITTED BY: CITY OF ANAHEIM

FLOWMETER SERIAL NO: MFG. SERIAL NO: 14136005

MANUFACTURER: MICRO MOTION MODEL: CMF025M313NQBUEZZZ

TUBE NO: FLOAT NO:

DATA IS: As Left ; In Tolerance See Remarks ☒

Calibrated @ customer's facility ☐

REMARKS: METER PROGRAMMED PRIOR TO AS LEFT DATA - DIRECT READING ELECTRONIC INDICATOR
TRANSMITTER S/N: 14136005, CALIBRATED IN LBS/HR H2O @ 75°F. SP.GR. 1.0 FIRST CALIBRATION

ACCURACY \pm 1% RATE

INDICATED		ACTUAL	
LB/H		LBS/HR	
150.20		151.20	
132.60		133.56	
112.90		113.70	
92.50		93.06	
75.10		75.48	
55.50		55.74	
37.78		37.80	
28.30		28.26	
18.85		18.95	
0.00		0.00	

Flowmeter Certified with HOMER R. DULIN CO.

Equip. No. 11605 Accuracy 0.005% Equip. Cal. Date: 8/29/18 Cal. Due: 8/29/21

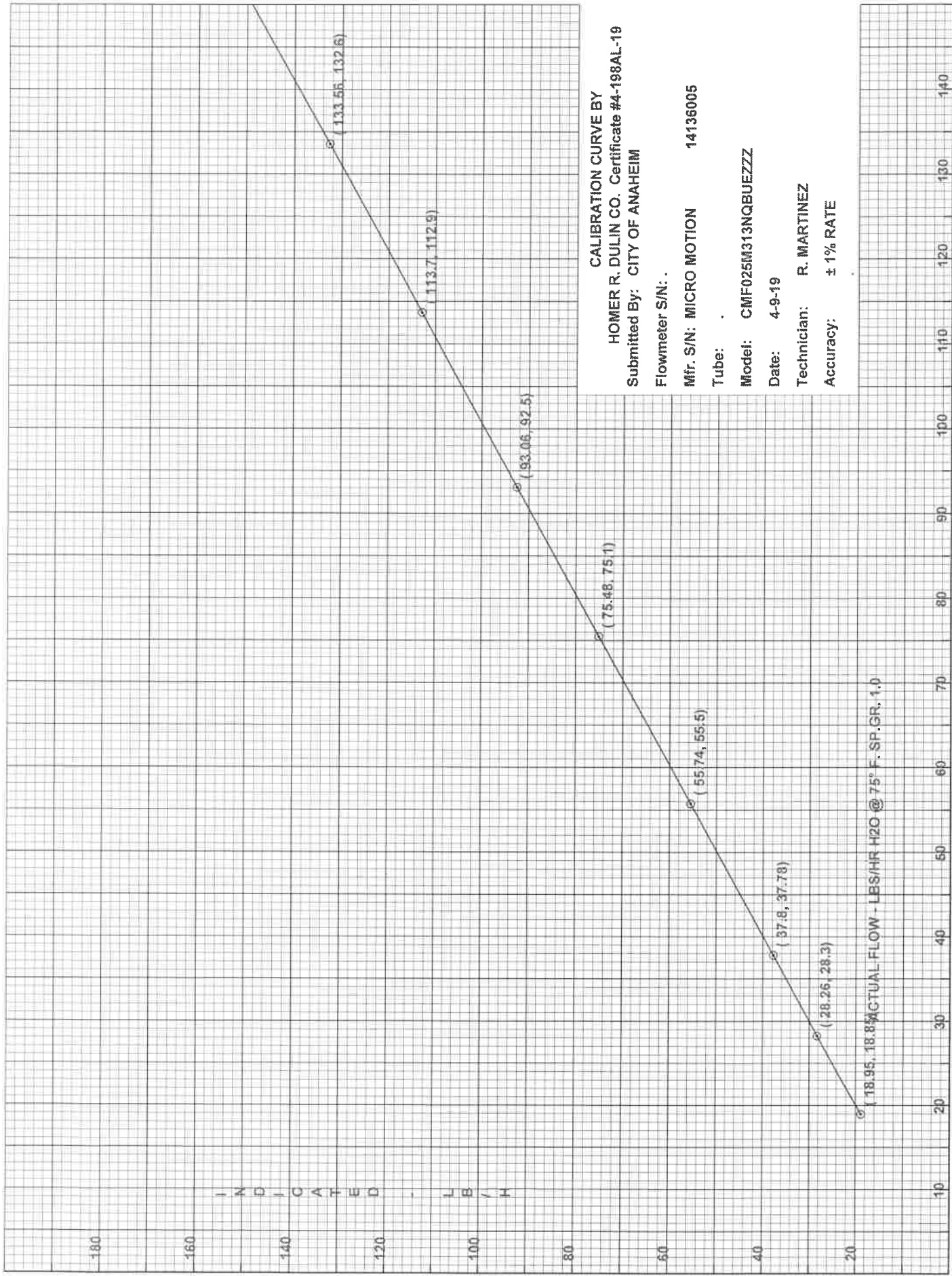
NIST Cert. No. TEST# MS 15560 Procedure No: ISA:RP 16.6

Our standards are certified by or are traceable to the National Institute of Standards and Technology and systems comply with MIL-STD 45662A, ANSI/NCSL Z540.3, ISO/IEC 17025, and ISO 10012. The collective uncertainty of the standards used in this calibration does not exceed 25% of the certified accuracy of the instrument under test. This document may not be reproduced, except in full, without prior written approval of the Homer R. Dulin Co. Rev.1 Dated 8/19/14

P.O. No. Shipper No.

4-9-19 4-9-20 R. MARTINEZ *Rogelio Martinez*

CALIBRATION DATE RECALIBRATION DUE CALIBRATION TECHNICIAN



CALIBRATION CURVE BY
HOMER R. DULIN CO. Certificate #4-198AL-19
Submitted By: CITY OF ANAHEIM
Flowmeter S/N: .
Mfr. S/N: MICRO MOTION 14136005
Tube: .
Model: CMF025M313NQBUEZZZ
Date: 4-9-19
Technician: R. MARTINEZ
Accuracy: ± 1% RATE

HOMER R. DULIN CO.
729 EAST WILLOW STREET
SIGNAL HILL, CALIFORNIA 90755
(562) 424-8533 FAX (562) 426-7707
CERT. NO. 4-134-19
CALIBRATION CERTIFICATION

SUBMITTED BY: CITY OF ANAHEIM

FLOWMETER SERIAL NO: MFG. SERIAL NO: 14236418

MANUFACTURER: MICRO MOTION MODEL: CMF025M313NQBUEZZZ

TUBE NO: FLOAT NO:

DATA IS: As Found/As Left ; In Tolerance

See Remarks ☒

Calibrated @ customer's facility ☐

REMARKS: DIRECT READING ELECTRONIC INDICATOR TRANSMITTER S/N: 14138117, CALIBRATED IN LBS/HR H2O
@ 75°F. SP.GR. 1.0 FIRST CALIBRATION

ACCURACY \pm 1% RATE

INDICATED		ACTUAL	
LB/H		LBS/HR	
148.30		148.56	
132.20		131.88	
112.50		112.20	
94.00		94.08	
75.38		75.30	
56.20		55.98	
37.57		37.38	
27.78		27.60	
18.85		18.78	
0.00		0.00	

Flowmeter Certified with HOMER R. DULIN CO.

Equip. No. 11605 Accuracy 0.005% Equip. Cal. Date: 8/29/18 Cal. Due: 8/29/21

NIST Cert. No. TEST# MS 15560 Procedure No: ISA:RP 16.6

Our standards are certified by or are traceable to the National Institute of Standards and Technology and systems comply with MIL-STD 45662A, ANSI/NCSL Z540.3, ISO/IEC 17025, and ISO 10012. The collective uncertainty of the standards used in this calibration does not exceed 25% of the certified accuracy of the instrument under test. This document may not be reproduced, except in full, without prior written approval of the Homer R. Dulin Co. Rev.1 Dated 8/19/14

P.O. No. Shipper No.

4-5-19

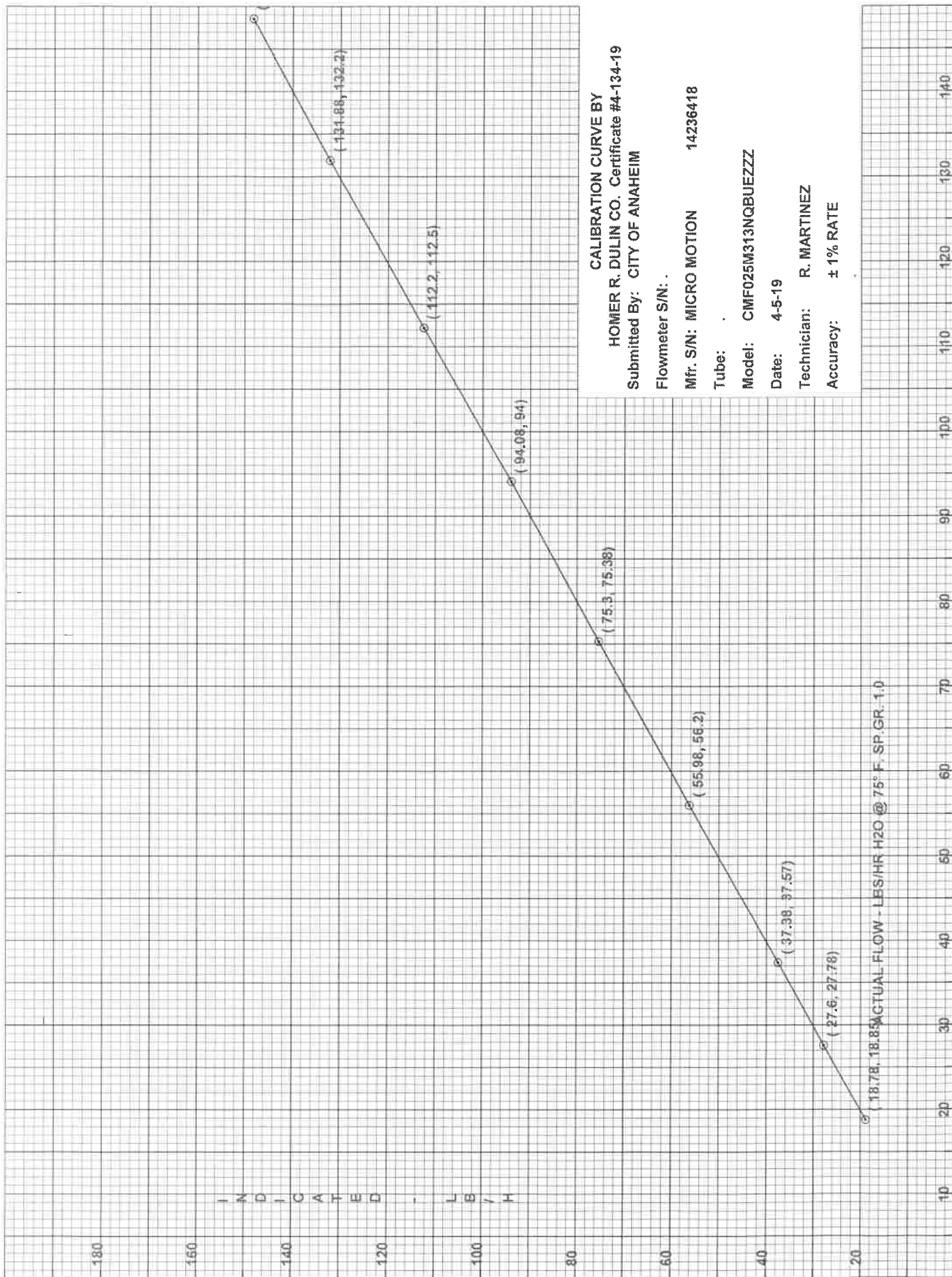
4-5-20

R. MARTINEZ *Rogelio Martinez*

CALIBRATION DATE

RECALIBRATION DUE

CALIBRATION TECHNICIAN



HOMER R. DULIN CO.
729 EAST WILLOW STREET
SIGNAL HILL, CALIFORNIA 90755
(562) 424-8533 FAX (562) 426-7707

CERT. NO. 5-254-19

CALIBRATION CERTIFICATION

SUBMITTED BY: CITY OF ANAHEIM

FLOWMETER SERIAL NO: .

MFG. SERIAL NO: 14139410

MANUFACTURER: MICRO MOTION

MODEL: CMF025M313NQBUEZZZ

TUBE NO: .

FLOAT NO: .

DATA IS: As Left ; In Tolerance

See Remarks ☒

Calibrated @ customer's facility ☐

REMARKS: NO AS FOUND DATA - METER PROGRAMMED PRIOR TO CALIBRATION - DIRECT READING ELECTRONIC
INDICATOR TRANSMITTER S/N: 14139410, CALIBRATED IN LBS/HR H2O @ 75° F. SP.GR. 1.0 FIRST CALIBRATION

ACCURACY \pm 1% RATE

INDICATED		ACTUAL	
LB/HR		LBS/HR	
150.4		149.7	
132.5		132.9	
113.4		113.1	
94.5		94.3	
75.6		75.8	
55.9		55.8	
38.2		38.4	
28.6		28.5	
18.8		18.8	
0.0		0.0	

Flowmeter Certified with HOMER R. DULIN CO.

Equip. No. 11605

Accuracy 0.005%

Equip. Cal. Date: 8/29/18

Cal. Due: 8/29/21

NIST Cert. No. TEST# MS 15560

Procedure No: ISA:RP 16.6

Our standards are certified by or are traceable to the National Institute of Standards and Technology and systems comply with MIL-STD 45662A, ANSI/NCSL Z540.3, ISO/IEC 17025, and ISO 10012. The collective uncertainty of the standards used in this calibration does not exceed 25% of the certified accuracy of the instrument under test. This document may not be reproduced, except in full, without prior written approval of the Homer R. Dulin Co. Rev.1 Dated 8/19/14

P.O. No. .

Shipper No. .

5-8-19

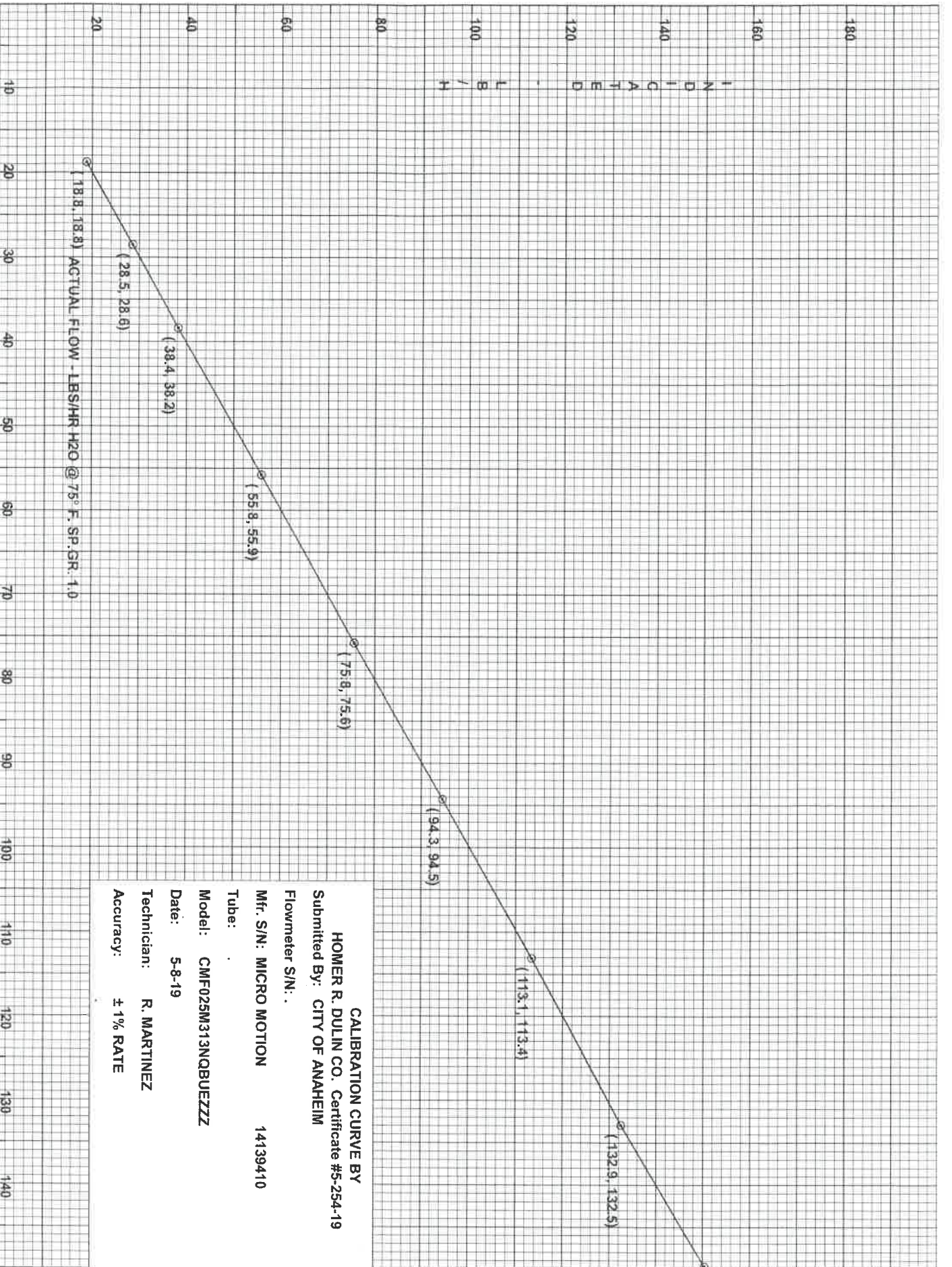
CALIBRATION DATE

5-8-20

RECALIBRATION DUE

R. MARTINEZ

CALIBRATION TECHNICIAN



CALIBRATION CURVE BY

HOMER R. DULIN CO. Certificate #5-254-19

Submitted By: CITY OF ANAHEIM

Flowmeter S/N: .

Mfr. S/N: MICRO MOTION 14139410

Tube: .

Model: CMF025M313NQBUEZZZ

Date: 5-8-19

Technician: R. MARTINEZ

Accuracy: ± 1% RATE

HOMER R. DULIN CO.
729 EAST WILLOW STREET
SIGNAL HILL, CALIFORNIA 90755
(562) 424-8533 FAX (562) 426-7707
CERT. NO. 3-417-19

CALIBRATION CERTIFICATION

SUBMITTED BY: CITY OF ANAHEIM

FLOWMETER SERIAL NO: MFG. SERIAL NO: 14134531

MANUFACTURER: MICRO MOTION MODEL: CMF025M313NQBUEZZZ

TUBE NO: FLOAT NO:

DATA IS: As Found/As Left ; In Tolerance

See Remarks ☒

Calibrated @ customer's facility ☐

REMARKS: DIRECT READING ELECTRONIC INDICATOR TRANSMITTER S/N: 14134531, CALIBRATED IN LBS/HR H2O
@ 75°F. SP.GR. 1.0 METER UNSTABLE BELOW 18.70 LB/HR INDICATED - FIRST CALIBRATION

ACCURACY \pm 1% RATE

INDICATED		ACTUAL	
LB/H		LBS/HR	
149.70		149.46	
131.50		131.46	
112.70		112.80	
94.20		94.08	
75.60		75.54	
56.80		56.82	
37.80		38.02	
27.70		27.93	
18.70		18.85	
0.00		0.00	

Flowmeter Certified with HOMER R. DULIN CO.

Equip. No. 11605 Accuracy 0.005% Equip. Cal. Date: 8/29/18 Cal. Due: 8/29/21

NIST Cert. No. TEST# MS 15560 Procedure No: ISA:RP 16.6

Our standards are certified by or are traceable to the National Institute of Standards and Technology and systems comply with MIL-STD 45662A, ANSI/NCSL Z540.3, ISO/IEC 17025, and ISO 10012. The collective uncertainty of the standards used in this calibration does not exceed 25% of the certified accuracy of the instrument under test. This document may not be reproduced, except in full, without prior written approval of the Homer R. Dulin Co. Rev.1 Dated 8/19/14

P.O. No. Shipper No.

3-28-19

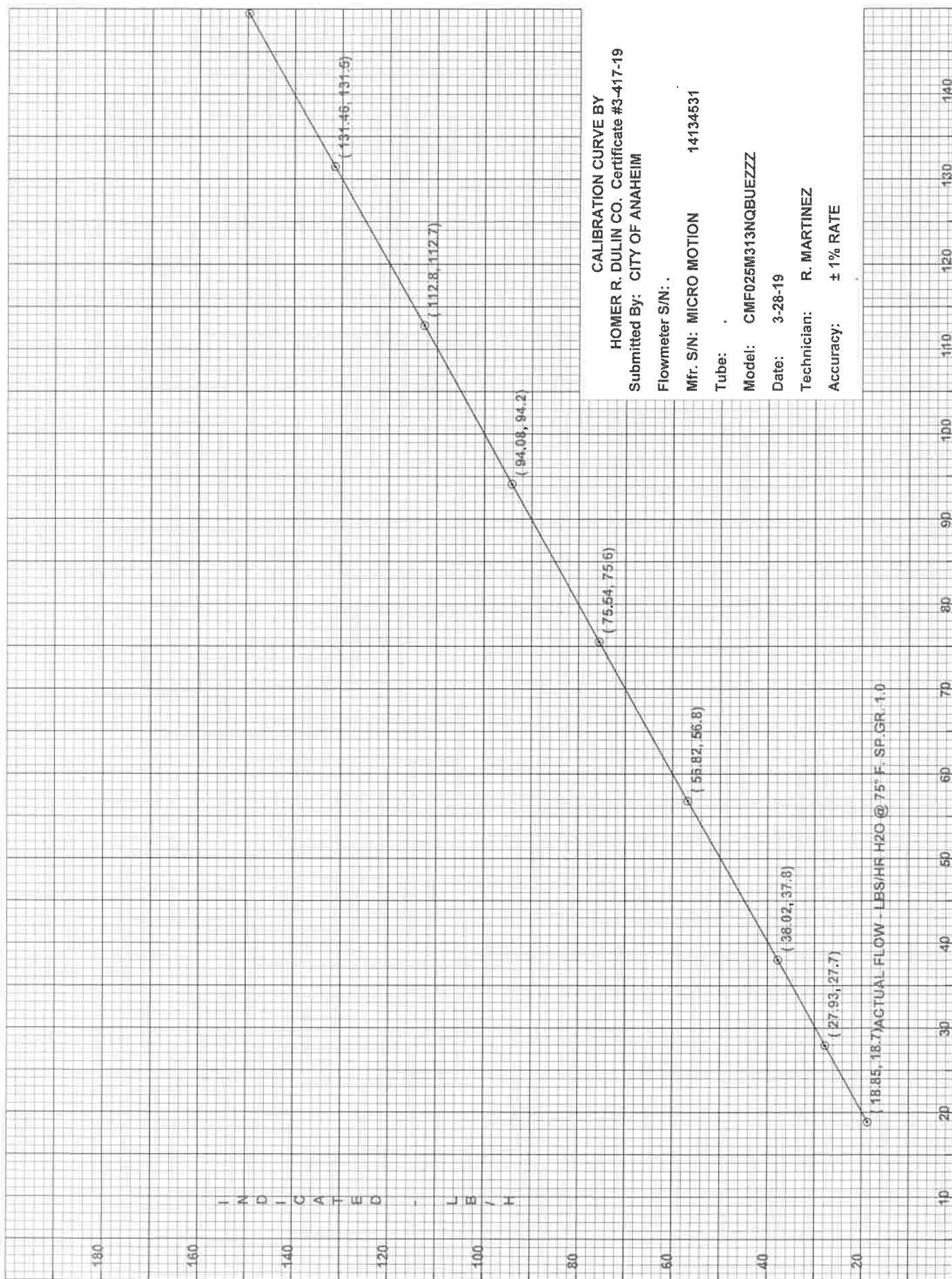
3-28-20

R. MARTINEZ

CALIBRATION DATE

RECALIBRATION DUE

CALIBRATION TECHNICIAN



CALIBRATION CURVE BY
HOMER R. DULIN CO. Certificate #3-417-19
Submitted By: CITY OF ANAHEIM

Flowmeter S/N: .

Mfr. S/N: MICRO MOTION 14134531

Tube: .

Model: CMF025M313NQBUEZZZ

Date: 3-28-19

Technician: R. MARTINEZ

Accuracy: ± 1% RATE

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 19

AQ-18
SCR INLET TEMPERATURE SENSOR
CALIBRATION REPORTS

Calibration: SCR Inlet Temperature
Unit 1 TE-403A-403D

Calibration Certificate

Certificate Number:
Position ID: 1-TE-403A

Printed: 2/1/2019 12:31:37 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U1/

Device

Device ID 1-TE-403A
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U1 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

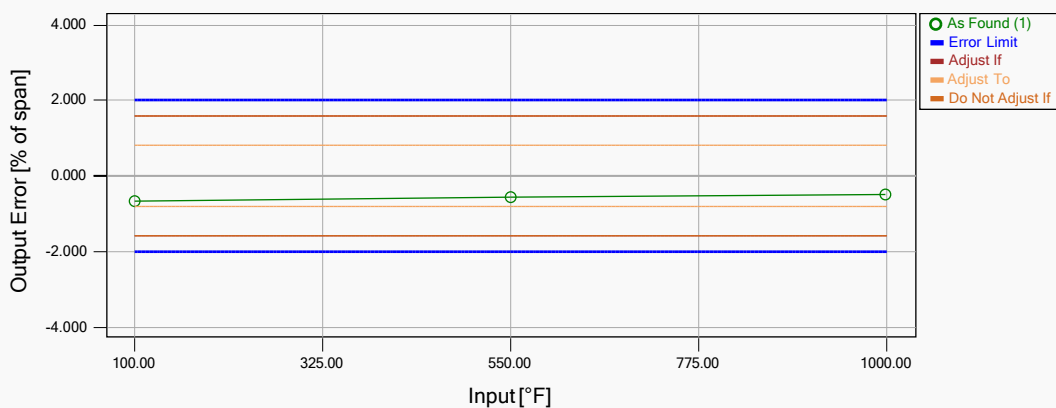
Calibration time 2/1/2019 10:21:23 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.667 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.00	100.0	94.000	-0.667
550.0	550.00	550.0	545.000	-0.556
1000.0	999.99	1000.0	995.500	-0.499

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/1/2019 10:21:23 AM

Calibration Certificate

Certificate Number:
Position ID: 1-TE-403B

Printed: 2/1/2019 12:31:37 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U1/

Device

Device ID 1-TE-403B
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U1 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

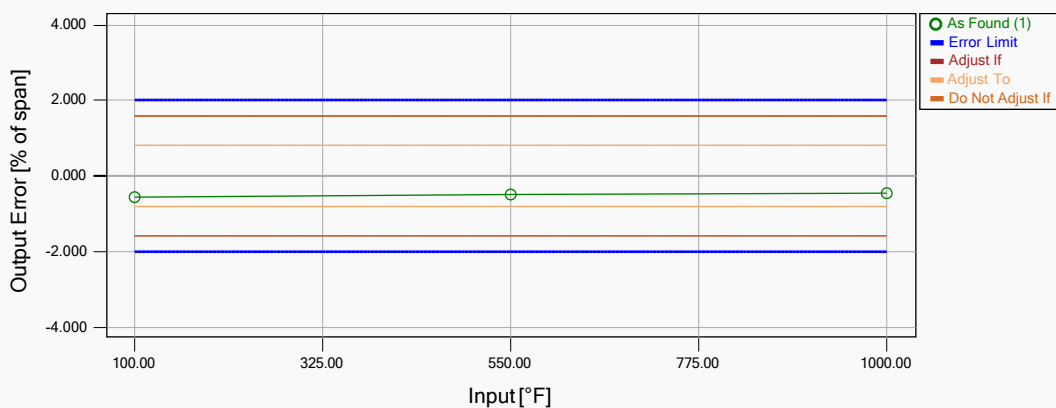
Calibration time 2/1/2019 10:24:47 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.556 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.00	100.0	95.000	-0.556
550.0	550.00	550.0	545.500	-0.500
1000.0	1000.00	1000.0	996.000	-0.444

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/1/2019 10:24:47 AM

Calibration Certificate

Certificate Number:
Position ID: 1-TE-403C

Printed: 2/1/2019 12:31:37 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U1/

Device

Device ID 1-TE-403C
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U1 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

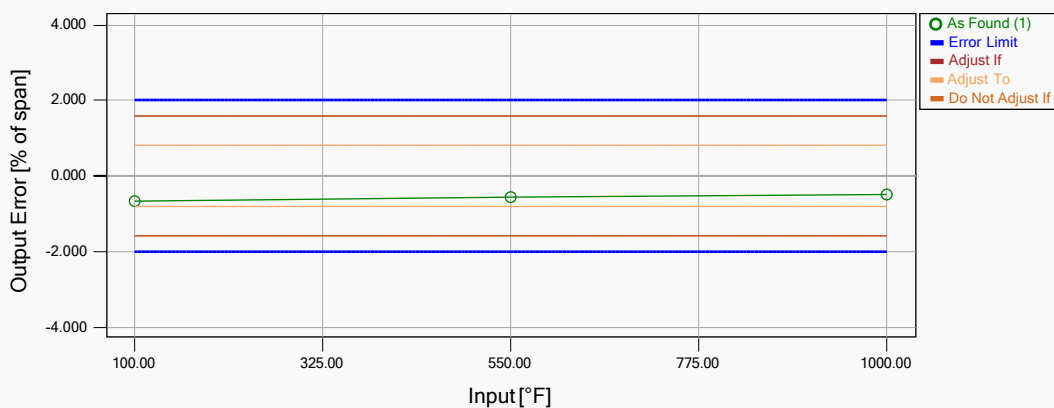
Calibration time 2/1/2019 10:28:38 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.667 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.00	100.0	94.000	-0.667
550.0	550.01	550.0	545.000	-0.557
1000.0	1000.01	1000.0	995.500	-0.501

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/1/2019 10:28:38 AM

Calibration Certificate

Certificate Number:
Position ID: 1-TE-403D

Printed: 2/1/2019 12:31:37 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U1/

Device

Device ID 1-TE-403D
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U1 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

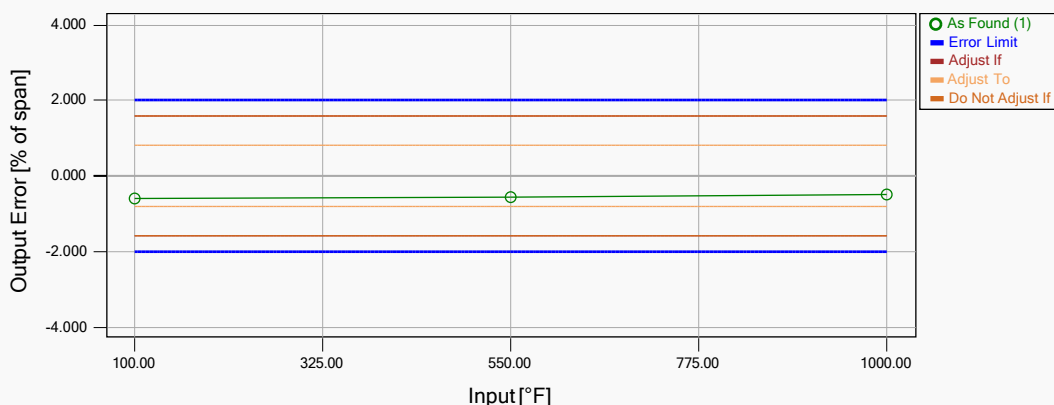
Calibration time 2/1/2019 10:32:11 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.612 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.01	100.0	94.500	-0.612
550.0	550.01	550.0	545.000	-0.557
1000.0	1000.00	1000.0	995.500	-0.500

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/1/2019 10:32:11 AM

Calibration: SCR Inlet Temperature
Unit 2 TE-403A-403D

Calibration Certificate

Certificate Number:
Position ID: 2-TE-403A

Printed: 2/1/2019 12:32:35 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U2/

Device

Device ID 2-TE-403A
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U2 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

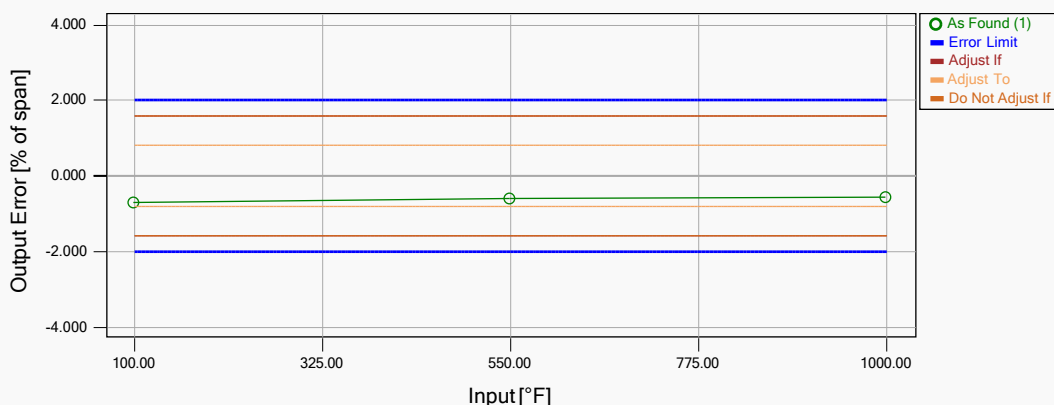
Calibration time 1/31/2019 10:14:33 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.720 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.98~	100.0	93.500	-0.720~
550.0	549.96	550.0	544.500	-0.607
1000.0	999.97	1000.0	995.000	-0.552

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/31/2019 10:14:33 AM

Calibration Certificate

Certificate Number:
Position ID: 2-TE-403B

Printed: 2/1/2019 12:32:35 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U2/

Device

Device ID 2-TE-403B
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U2 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

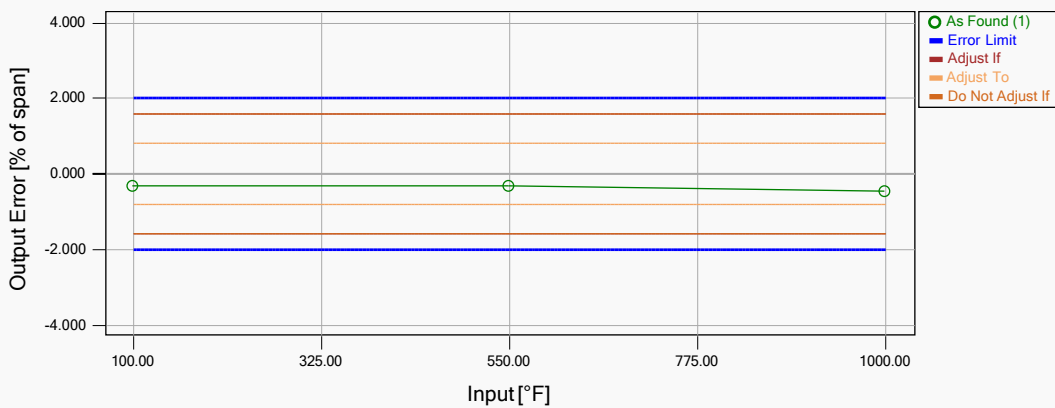
Calibration time 1/31/2019 10:18:28 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.442 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.98	100.0	97.000	-0.331
550.0	549.98	550.0	547.000	-0.331
1000.0	999.98	1000.0	996.000	-0.442

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/31/2019 10:18:28 AM

Calibration Certificate

Certificate Number:
Position ID: 2-TE-403C

Printed: 2/1/2019 12:32:35 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U2/

Device

Device ID 2-TE-403C
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U2 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

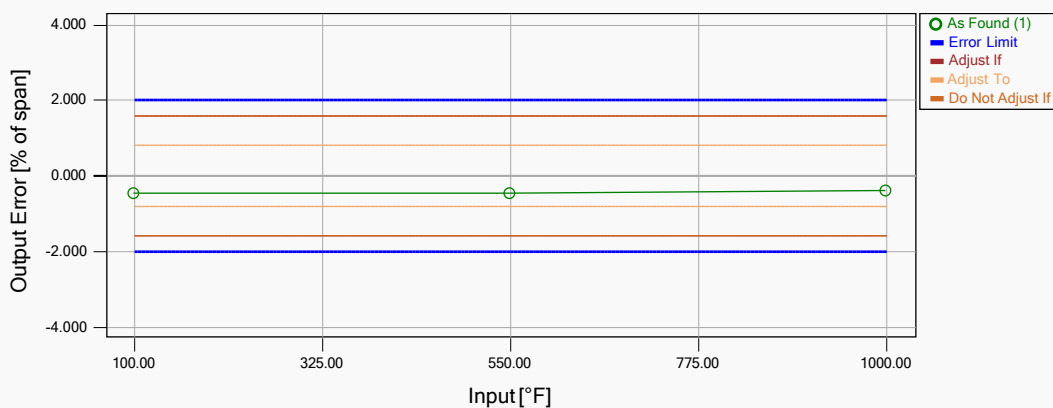
Calibration time 1/31/2019 10:22:35 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.443 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.99	100.0	96.000	-0.443
550.0	549.99	550.0	546.000	-0.443
1000.0	999.99	1000.0	996.500	-0.388

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/31/2019 10:22:35 AM

Calibration Certificate

Certificate Number:
Position ID: 2-TE-403D

Printed: 2/1/2019 12:32:35 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U2/

Device

Device ID 2-TE-403D
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U2 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

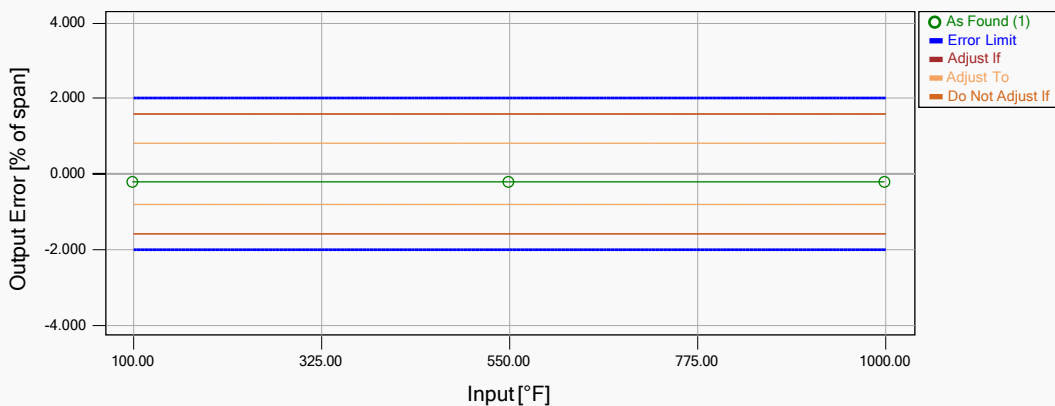
Calibration time 1/31/2019 10:26:02 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.221 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.99	100.0	98.000	-0.221
550.0	549.99	550.0	548.000	-0.221
1000.0	999.99	1000.0	998.000	-0.221

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/31/2019 10:26:02 AM

Calibration: SCR Inlet Temperature
Unit 3 TE-403A-403D

Calibration Certificate

Certificate Number:
Position ID: 3-TE-403A

Printed: 2/1/2019 12:33:24 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U3/

Device

Device ID 3-TE-403A
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U3 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

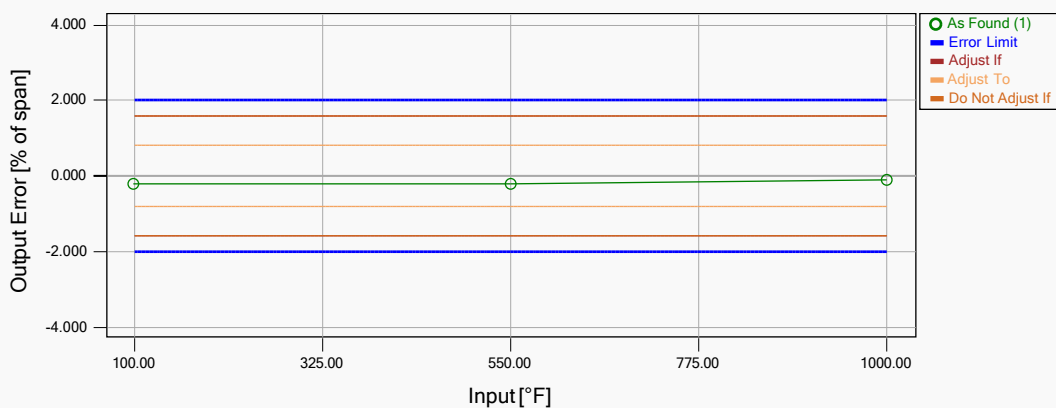
Calibration time 1/30/2019 12:19:42 PM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.223 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.99	100.0	98.000	-0.221
550.0	550.01	550.0	548.000	-0.223
1000.0	1000.01	1000.0	999.000	-0.112

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 12:19:42 PM

Calibration Certificate

Certificate Number:
Position ID: 3-TE-403B

Printed: 2/1/2019 12:33:24 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U3/

Device

Device ID 3-TE-403B
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U3 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

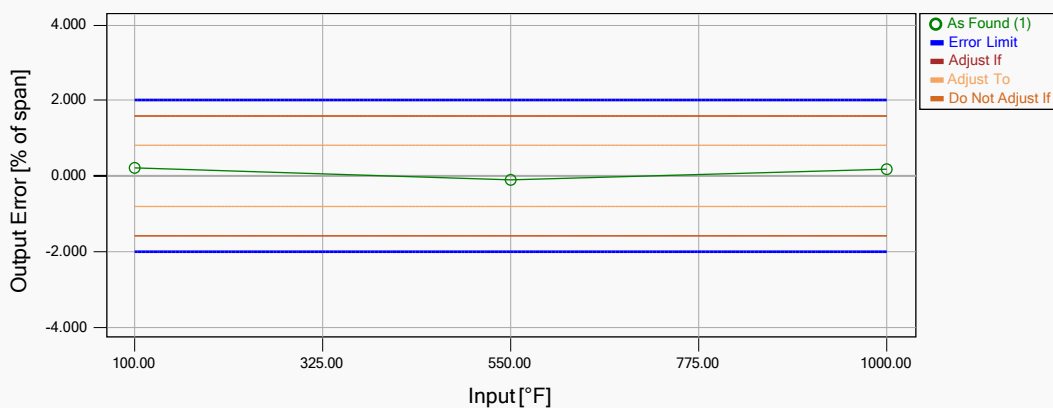
Calibration time 1/30/2019 12:24:20 PM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: 0.221 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.01	100.0	102.000	0.221
550.0	550.01	550.0	549.000	-0.112
1000.0	1000.01	1000.0	1001.500	0.166

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 12:24:20 PM

Calibration Certificate

Certificate Number:
Position ID: 3-TE-403C

Printed: 2/1/2019 12:33:24 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U3/

Device

Device ID 3-TE-403C
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U3 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

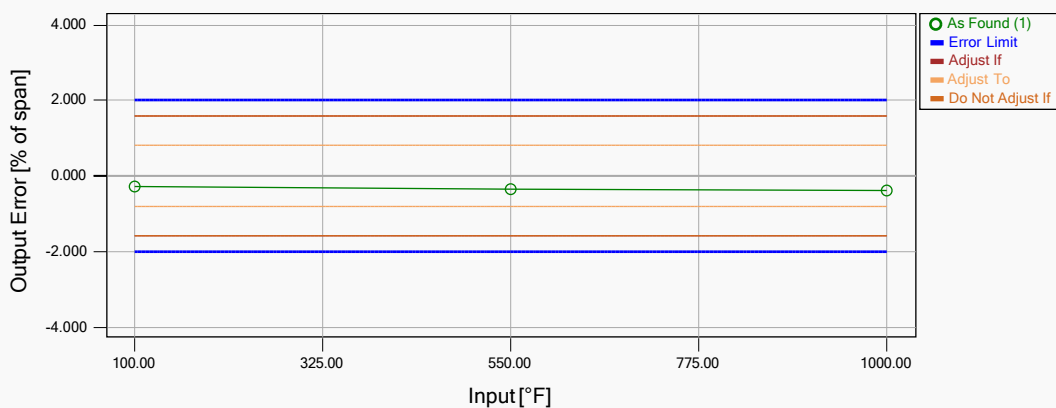
Calibration time 1/30/2019 12:31:44 PM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.391 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.03~	100.0	97.500	-0.281~
550.0	550.05~	550.0	547.000	-0.339~
1000.0	1000.02~	1000.0	996.500	-0.391~

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 12:31:44 PM

Calibration Certificate

Certificate Number:
Position ID: 3-TE-403D

Printed: 2/1/2019 12:33:24 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U3/

Device

Device ID 3-TE-403D
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U3 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

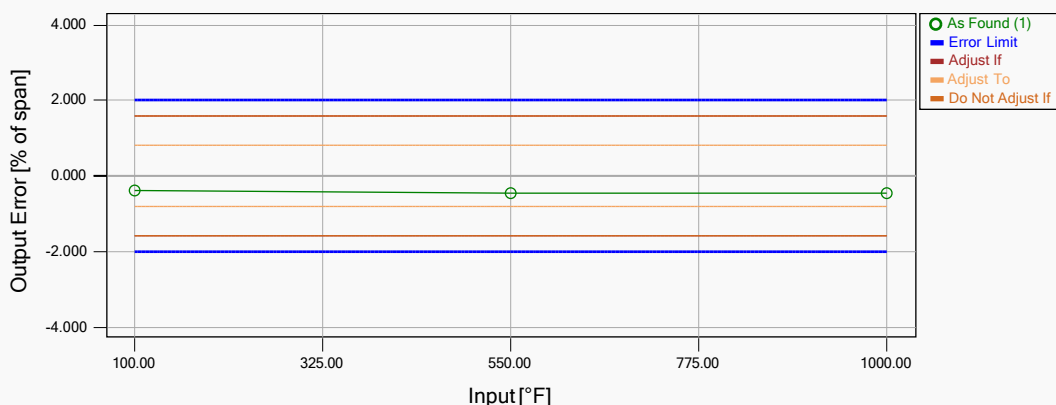
Calibration time 1/30/2019 12:36:09 PM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.450 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.03~	100.0	96.500	-0.392~
550.0	550.05~	550.0	546.000	-0.450~
1000.0	1000.04~	1000.0	996.000	-0.449~

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 12:36:09 PM

Calibration: SCR Inlet Temperature
Unit 4 TE-403A-403D

Calibration Certificate

Certificate Number:
Position ID: 4-TE-403A

Printed: 2/1/2019 12:20:15 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U4/

Device

Device ID 4-TE-403A
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U4 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

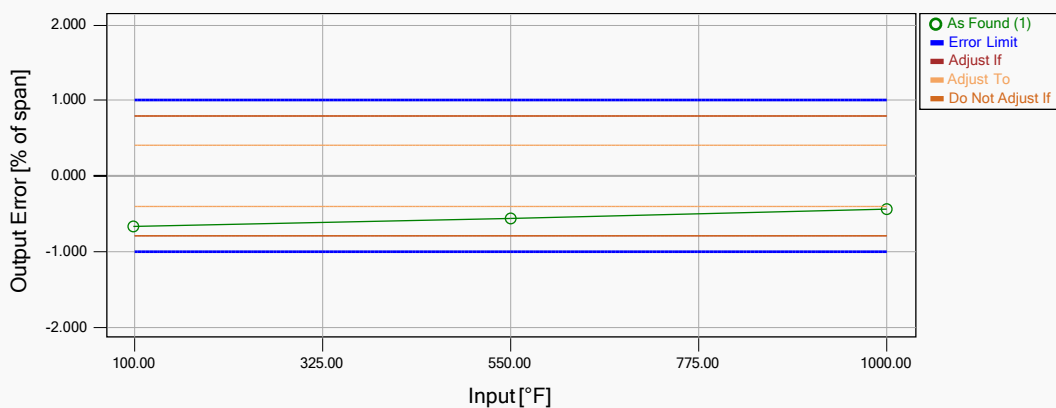
Calibration time 1/29/2019 11:08:05 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.666 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.99	100.0	94.000	-0.666
550.0	550.00	550.0	545.000	-0.556
1000.0	1000.00	1000.0	996.000	-0.444

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/29/2019 11:08:05 AM

Calibration Certificate

Certificate Number:
Position ID: 4-TE-403B

Printed: 2/1/2019 12:20:15 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U4/

Device

Device ID 4-TE-403B
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U4 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

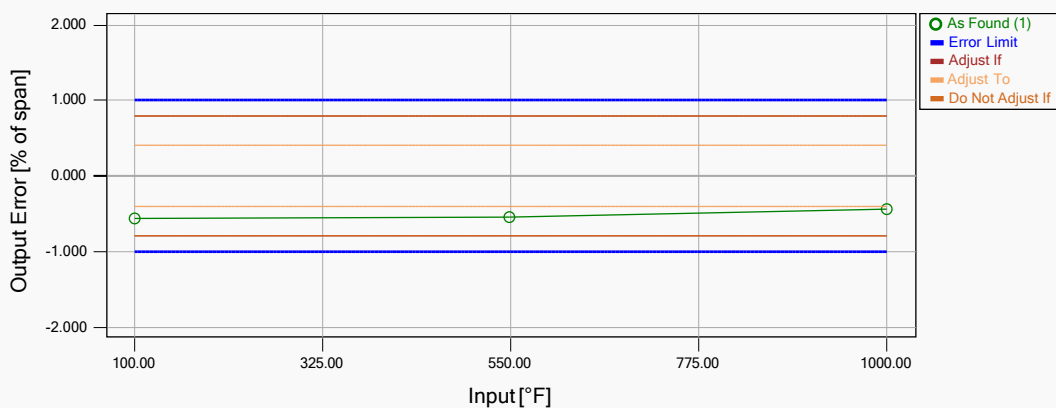
Calibration time 1/29/2019 11:14:28 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -0.556 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.00	100.0	95.000	-0.556
550.0	549.99	550.0	545.000	-0.554
1000.0	1000.00	1000.0	996.000	-0.444

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/29/2019 11:14:28 AM

Calibration Certificate

Certificate Number:
Position ID: 4-TE-403C

Printed: 2/1/2019 12:20:15 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U4/

Device

Device ID 4-TE-403C
Serial Number
Manufacturer
Rangeability
Operating Operating Humidity

Function

Name U4 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

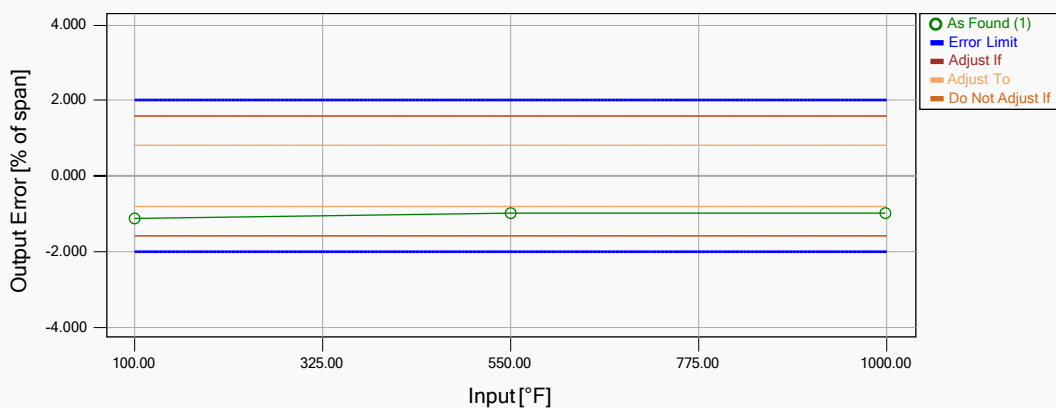
Calibration time 1/30/2019 10:07:32 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -1.111 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	100.00	100.0	90.000	-1.111
550.0	550.00	550.0	541.000	-1.000
1000.0	999.99	1000.0	991.000	-0.999

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 10:07:32 AM

Calibration Certificate

Certificate Number:
Position ID: 4-TE-403D

Printed: 2/1/2019 12:20:15 PM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name SCR INLET TEMP
Work Order Number
Location NH3 INJ SKID
Plant CANYON/ERU/U4/

Device

Device ID 4-TE-403D
Serial Number
Manufacturer
Rangeability
Operating
Operating Humidity

Function

Name U4 SCR INLET TEMP (ud)
Transfer Function Linear
Range 100 ... 1000 °F 100 ... 1000 °F

Calibration Event

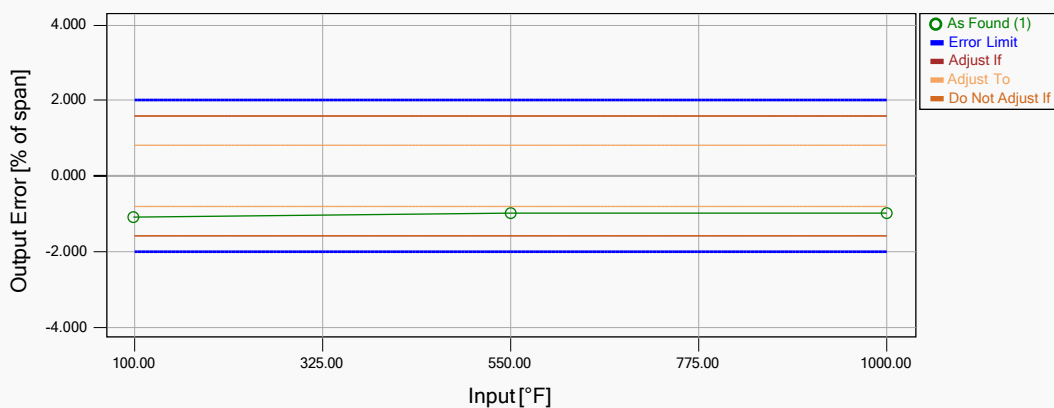
Calibration time 1/30/2019 10:12:04 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 2 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module TC-R-OUT/ TC1 : 65279 Due Date: 4/13/2019
Output Calibrator Due Date:
Output Module Due Date:



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: -1.110 % of span

Nominal Input [°F]	Actual Input [°F]	Nominal Output [°F]	Actual Output [°F]	Found Error [% of span]
100.0	99.99	100.0	90.000	-1.110
550.0	550.00	550.0	541.000	-1.000
1000.0	1000.00	1000.0	991.000	-1.000

Calibration Note:

Calibrated by: VINCENT NGUYEN
1/30/2019 10:12:04 AM

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 20

AQ-19
SCR DIFFERENTIAL PRESSURE SENSOR
CALIBRATION REPORTS

Calibration Certificate

Certificate Number:
Position ID: 1-PDIT-4

Printed: 3/1/2019 11:31:32 AM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name U1 SCR DP
Work Order Number
Location U1 ERU
Plant

Device

Device ID 1-PDIT-4
Serial Number 393478
Manufacturer Rosemount 3051C
Rangeability
Operating Operating Humidity

Function

Name U1 SCR DP (ud)
Transfer Function Linear
Range 0 ... 10 inH2O (G) 4 ... 20 mA

Calibration Event

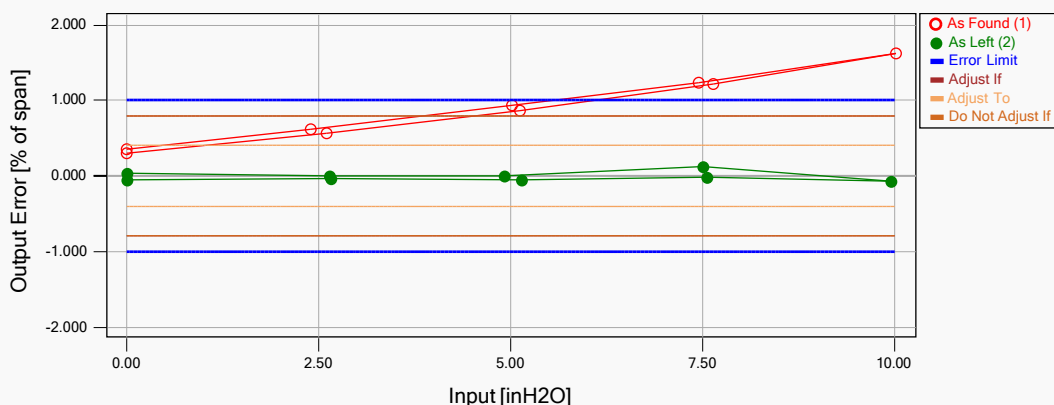
Calibration time 2/7/2019 9:16:37 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module P2C : 69381 Due Date: 4/12/2019
Output Calibrator MC6 : 605835 Due Date: 4/12/2019
Output Module IN : 25613 Due Date: 4/12/2019



1. As Found

FAILED

Maximum Error: 1.626 % of span

Nominal Input [inH2O]	Actual Input [inH2O]	Nominal Output [mA]	Actual Output [mA]	Found Error [% of span]
0.0000	0.01	4.0000	4.0717	0.348
2.500	2.41	8.000	7.9535	0.609
5.000	5.02	12.000	12.1812	0.933
7.500	7.45	16.000	16.1186	1.241
10.000	10.03	20.000	20.3082	1.626
7.500	7.65	16.000	16.4352	1.220
5.000	5.13	12.000	12.3472	0.870
2.500	2.61	8.000	8.2665	0.566
0.0000	0.00	4.0000	4.0468	0.293

2. As Left

PASSED, DO NOT ADJUST

Maximum Error: 0.116 % of span

Nominal Input [inH2O]	Actual Input [inH2O]	Nominal Output [mA]	Actual Output [mA]	Found Error [% of span]
0.0000	0.01	4.0000	4.0219	0.037
2.500	2.65	8.000	8.2408	0.005
5.000	4.93	12.000	11.8892	0.008
7.500	7.50	16.000	16.0186	0.116
10.000	9.95	20.000	19.9087	-0.071
7.500	7.56	16.000	16.0925	-0.022
5.000	5.14	12.000	12.2157	-0.052
2.500	2.67	8.000	8.2669	-0.032
0.0000	0.00	4.0000	3.9920	-0.050

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/7/2019 9:16:37 AM

Calibration Certificate

Certificate Number:
Position ID: 2-PDIT-4

Printed: 3/1/2019 11:36:49 AM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name U2 CO CAT DP
Work Order Number
Location U1 ERU
Plant

Device

Device ID 2-PDIT-4
Serial Number 393483
Manufacturer Rosemount 3051C
Rangeability
Operating Operating Humidity

Function

Name U2 CO CAT DP (ud)
Transfer Function Linear
Range 0 ... 5 inH2O (G) 4 ... 20 mA

Calibration Event

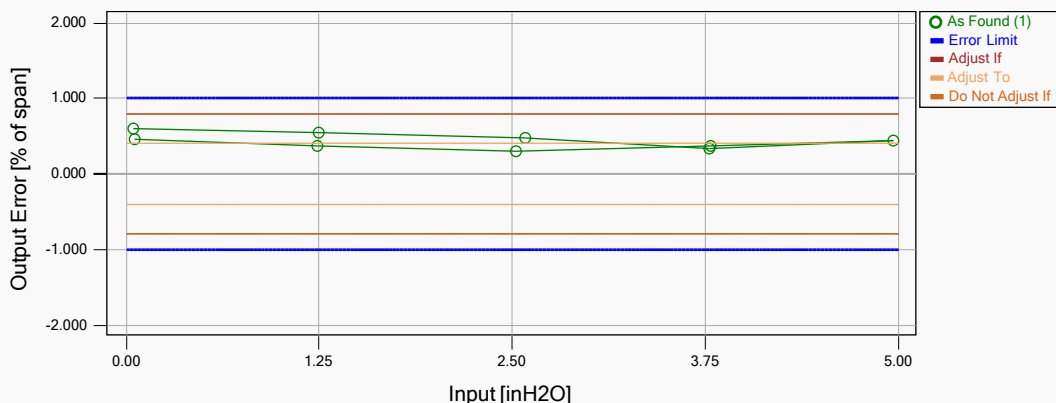
Calibration time 2/6/2019 9:16:23 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module P2C : 69381 Due Date: 4/12/2019
Output Calibrator MC6 : 605835 Due Date: 4/12/2019
Output Module IN : 25613 Due Date: 4/12/2019



1. As Found

PASSED, DO NOT ADJUST

Maximum Error: 0.595 % of span

Nominal Input [inH2O]	Actual Input [inH2O]	Nominal Output [mA]	Actual Output [mA]	Found Error [% of span]
0.0000	0.05	4.0000	4.2552	0.595
1.250	1.25	8.000	8.0883	0.552
2.500	2.59	12.000	12.3641	0.476
3.750	3.78	16.000	16.1500	0.338
5.0000	4.97	20.0000	19.9736	0.435
3.750	3.79	16.000	16.1874	0.371
2.500	2.53	12.000	12.1448	0.305
1.250	1.24	8.000	8.0282	0.376
0.0000	0.06	4.0000	4.2652	0.458

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/6/2019 9:16:23 AM

Calibration Certificate

Certificate Number:
Position ID: 3-PDIT-4

Printed: 3/1/2019 11:39:09 AM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name U3 SCR DP
Work Order Number
Location U3 ERU
Plant

Device

Device ID 3-PDIT-4
Serial Number 393480
Manufacturer Rosemount 3051C
Rangeability
Operating Operating Humidity

Function

Name U3 SCR DP (ud)
Transfer Function Linear
Range 0 ... 10 inH2O (G) 4 ... 20 mA

Calibration Event

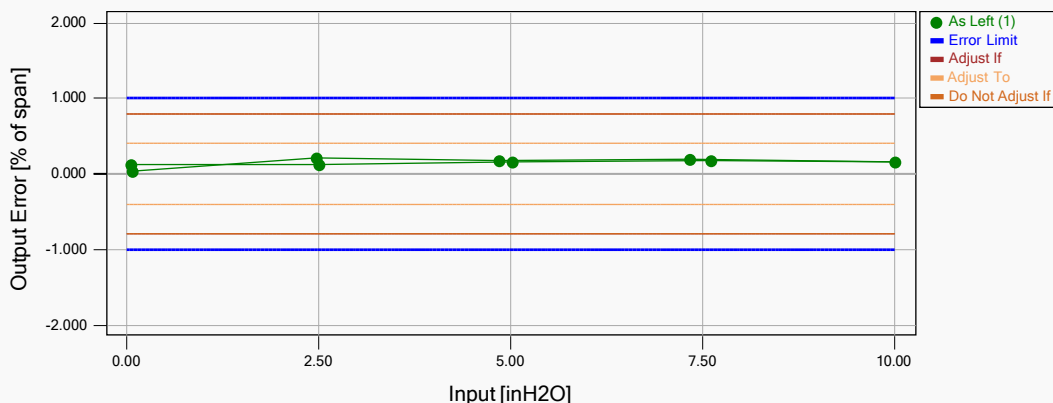
Calibration time 2/6/2019 10:47:44 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module P2C : 69381 Due Date: 4/12/2019
Output Calibrator MC6 : 605835 Due Date: 4/12/2019
Output Module IN : 25613 Due Date: 4/12/2019



1. As Left

PASSED, DO NOT ADJUST

Maximum Error: 0.208 % of span

Nominal Input [inH2O]	Actual Input [inH2O]	Nominal Output [mA]	Actual Output [mA]	Found Error [% of span]
0.0000	0.07	4.0000	4.1178	0.036
2.500	2.47	8.000	7.9853	0.208
5.000	4.85	12.000	11.7892	0.183
7.500	7.34	16.000	15.7752	0.195
10.000	10.01	20.000	20.0406	0.154
7.500	7.61	16.000	16.2054	0.184
5.000	5.03	12.000	12.0740	0.163
2.500	2.51	8.000	8.0362	0.126
0.0000	0.06	4.0000	4.1164	0.128

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/6/2019 10:47:44 AM

Calibration Certificate

Certificate Number:
Position ID: 4-PDIT-403

Printed: 3/1/2019 11:29:59 AM
Printed by: vnguyen
CMX Version: 2.11.214.0 (2.11)

Position

Name U4 SCR DP
Work Order Number
Location U4 ERU
Plant CANYON/ERU/U4/

Device

Device ID 4-PDIT-403
Serial Number 393481
Manufacturer Rosemount 3051C
Rangeability
Operating Operating Humidity

Function

Name U4 SCR DP (ud)
Transfer Function Linear
Range 0 ... 10 inH2O (G) 4 ... 20 mA

Calibration Event

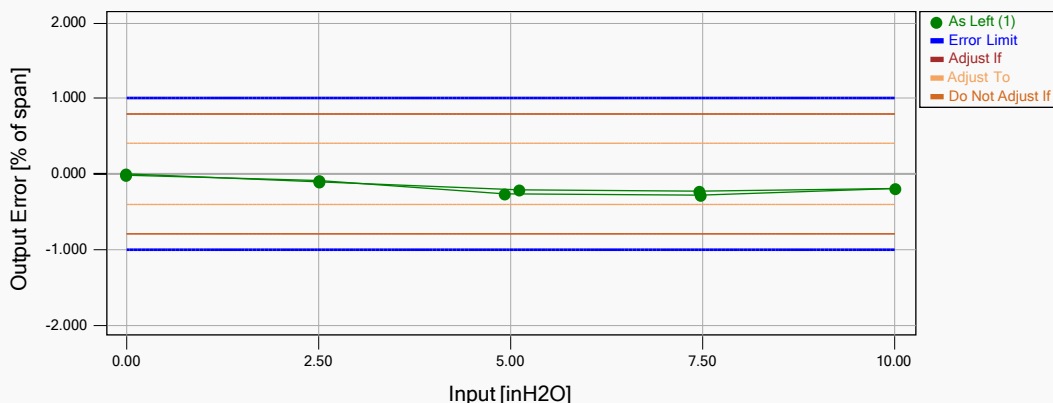
Calibration time 2/28/2019 10:05:25 AM
Next Calibration
Environment Environment

Calibration Procedure

Due Date Interval 0
Reject If Error > 1 % of span
Adjust To Error < 40 % of Reject If Error Classification
Calibration Strategy

Calibrators

Input Calibrator MC6 : 605835 Due Date: 4/12/2019
Input Module P2C : 69381 Due Date: 4/12/2019
Output Calibrator MC6 : 605835 Due Date: 4/12/2019
Output Module IN : 25613 Due Date: 4/12/2019



1. As Left

PASSED, DO NOT ADJUST

Maximum Error: -0.283 % of span

Nominal Input [inH2O]	Actual Input [inH2O]	Nominal Output [mA]	Actual Output [mA]	Found Error [% of span]
0.0000	-0.01	4.0000	3.9804	-0.023
2.500	2.51	8.000	8.0032	-0.080
5.000	4.92	12.000	11.8309	-0.257
7.500	7.47	16.000	15.9068	-0.283
10.000	10.00	20.000	19.9689	-0.194
7.500	7.46	16.000	15.8987	-0.233
5.000	5.11	12.000	12.1425	-0.209
2.500	2.50	8.000	7.9843	-0.098
0.0000	-0.01	4.0000	3.9849	0.006

Calibration Note:

Calibrated by: VINCENT NGUYEN
2/28/2019 10:05:25 AM

CANYON POWER PLANT
ANNUAL COMPLIANCE REPORT

ATTACHMENT 21

WASTE-10
COOLING TOWER SLUDGE TESTING

No Sludge developed for CY 2019