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Vertical Plume Velocity Assessment

# NorthTown Backup Generating Facility

San Jose, California

Submitted to  
California Energy Commission

Submitted by



Prepared by  
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ATMOSPHERIC DYNAMICS, INC  
Meteorological & Air Quality Modeling

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## Introduction

This report presents the evaluation of the Northtown Backup Generating Facility (NTBGF) source generated plumes from the routine testing of the 42 Caterpillar diesel engines and 36 rooftop closed loop cooling towers on the effects on airport/aircraft operations. The Normal Y. Mineta San Jose International Airport is located approximately 0.7 kilometers miles east west-southwest of the NTBGF. This report is based upon an analysis prepared by Atmospheric Dynamics, Inc. in accordance with the California Energy Commission (CEC) application requirements for a Small Power Plant Exemption (SPPE) pursuant to the power plant siting regulations. This analysis is but one part of a larger analysis, which seeks an SPPE Decision from the CEC.

Based on the stack parameter data, an analysis of the potential plume characteristics from the routine operation the diesel engines and rooftop cooling towers on vertical winds was prepared and compared to the California Energy Commission (CEC) significance criteria of 5.3 meters per second (m/s) for the average vertical plume velocities as described below.

Atmospheric Dynamics, Inc. (ADI) prepared a screening level plume vertical velocity assessment which are based on the calm wind Spillane methodology outlined in the *“Aviation Safety and Buoyant Plumes”* paper (Peter Best, et. al., presented at the Clean Air Conference, Newcastle, New South Wales, Australia, 2003). This methodology is also recognized as a screening tool for aviation safety set out by the Australian Civil Aviation Safety Authority (CASA) and presented in *“AC 139-5(1) Plume Rise Assessments (CASA, 2012)”*.

The aim of this screening assessment is to conservatively determine the potential for turbulence generated by the diesel engines and rooftop cooling tower waste heat exhaust plumes. Part 139.370 of the Australian Civil Aviation Safety Regulations (1998, 2004) provides that CASA may determine that plume velocities in excess of 4.3 m/s is or will be a potential hazard to aircraft operations. The *Manual of Aviation Meteorology* (Australian Bureau of Meteorology 2003) defines severe turbulence as a vertical wind gust velocity in excess of 10.6 m/s. The assumed critical vertical velocity used as a CEC significance threshold is 5.3 meters per second\* (m/s) but it should be noted that the basis of the original CASA derived threshold of 4.3 m/s has been lost in antiquity and that CASA no longer relies on the 1998 and 2004 regulations that established this critical threshold other than to note that a more rigorous analysis, which includes site specific meteorology, should be used if the 4.3 m/s and 10.6 m/s screening thresholds are exceeded. The screening method uses absolute worst-case assumptions of calm winds and neutral atmospheric conditions for the entire vertical extent of the plume to determine these worst-case impacts. It should be noted that these results are extremely conservative in that these worst-case conditions typically only occur during a few hours each year.

The Spillane methodology is generally applied to a limited number of plume source geometry's (turbines, power plant boilers, etc.) with the stacks arranged linearly (in a single straight-line) and separated by distances that typically exceed the individual stack diameters. For the diesel engines, this assumption was maintained. Only one engine stack was modeled consistent with the normal operational testing schedule of the emergency generator engines. For the rooftop closed circuit cooling towers, a conservative assumption was made in order to use the Spillane methodology on an atypical cooling tower plume configuration, which is made up of 18 three (3) cell towers on each building arranged in two (2) parallel rows. Here, the methodology, as described below, assumed that all three (3) cells for each side by side cooling tower were merged into a single stack with an effective diameter based on the combined area of all six (6) cooling

\*For the Puente Power Project (Docket#15-AFC-01, TN#213674, 9/15/2016), “CEC staff ... concluded that an average velocity of 5.3 m/s is the appropriate velocity ... [for a plume velocity threshold].” The CEC staff “Plume Background Threshold” attached to the docketed document concludes with “...[CEC] staff will use 10.6 m/s peak vertical plume velocity as the new threshold. The altitude at which a plume would have a peak vertical velocity of 10.6 m/s would be the same altitude at which a plume would have an average vertical velocity of half that, 5.3 m/s.”



tower cells. In other words, a single stack was assumed to initially describe the release parameters of the combined cooling tower cells in each of the 18 individual cooling towers. The effective plume diameter is appropriate for each individual cooling tower based on the close proximity and arrangement of the six (6) individual cells.

### **Screening Methodology and Vertical Plume Velocity Calculations**

The Spillane methodology is based on worst-case calm wind neutral stability conditions to assess the average plume vertical velocity as a function of height. The methodology is based on well-verified laboratory and theoretical treatments of the rise and spread of a buoyant jet, both into a still ambient environment and into a light crosswind. This treatment covers in detail the initial dynamics of the plume as it exits the stack and the entrainment of ambient air into the plume as it rises directly above the stack. In addition to providing clarifications and algebraic solutions to the Spillane methodology, the 2003 Peter Best paper provides additional methodologies that also consider the enhancement of vertical velocities that may occur if the plumes from multiple identical stacks merge and form a higher buoyancy combined plume (referred to here as the enhanced Spillane methodology).

The vertical plume assessment will involve several stages of development. For individual plumes, the stages are:

- (a) In the first stage very close to the stack exit, the high plume momentum will result in a short section in which the conditions at the center of the plume are relatively unaffected by ambient and plume buoyancy conditions. This jet phase extends from the stack exit to approximately a distance of 6.25 D above the stack (where D is the stack diameter) in calm conditions. At the end of this stage, the plume-averaged vertical velocity has decreased to half of the stack exit velocity, with a corresponding increase, or doubling, in effective plume diameter.
- (b) In the second stage, the plume responds to differences between ambient and plume buoyancy conditions, with much cooler and less turbulent ambient air being entrained into the plume from the outside regions of the plume towards the plume centerline. The momentum and buoyancy of the plume significantly influences plume rise and subsequently the dilution of the stack exhaust to decrease plume vertical velocities. This dilution is very sensitive to ambient wind speed, so the calm wind conditions considered here are extremely conservative.
- (c) In the third stage of plume development, plume rise is due entirely to the buoyancy of the plume and continues from some distance until there is an equalization of turbulence conditions within and outside the plume. This final rise is often only achieved at considerable heights/distances from the stack where the effective average vertical velocity is then close to zero. Since there is very little turbulence and near-zero vertical velocities, this stage of plume development is usually not considered for this type of analysis.

In the second stage of development, the analytical solution of the governing equations under these conditions is given by:

$$a = 0.16(z - z_v)$$



$$V = \{(Va)o^3 + 0.12Fo [(z - zv)^2 - (6.25D - zv)^2]\}^{1/3} / a$$

Where the subscript 'o' refers to values of the parameters at the stack outlet and the variables are:

$a$	plume radius (m)
$V$	average vertical velocity (m/s)
$z$	height above stack top (m)
$z_v$	virtual source height (m)
$D$	stack diameter (m)
$F_o$	buoyancy flux evaluated at the stack outlet ( $m^4s^{-3}$ )

These are the two primary equations governing the growth of a single plume in the second stage of development under neutral calm wind conditions. Additional equations governing the first stage of single plume development as well as the interaction of multiple plumes in the second stage of development are discussed in detail in the Best paper.

For multiple stacks in the enhanced Spillane methodology, the equations governing the second stage are calculated from the point when the plumes begin to merge until they are fully merged. The plume merging begins at the height where the plume diameters equal the stack separations and the plumes are fully merged at the height where the plume diameters are equal to  $2d(N-1)/2$  for three or more stacks or  $2d$  for two stacks. At the fully merged height, the merged plume diameter and velocity is enhanced by the fourth root of the number of stacks. Above the fully merged plume height, the enhanced plume diameter and plume velocities follow the regular equations given for the second stage. Below the fully merged plume height for the merging phase, plume velocities are linearly interpolated by height from the single plume velocity at the height where the plumes begin to merge to the enhanced plume velocity at the fully merged plume height.

### Vertical Plume Velocity Calculations for the Diesel Engines

The NTBGF is comprised of 40 individual large and two (2) small diesel emergency generator stacks. The small diesel emergency generator was not assessed as it would have smaller plume vertical velocities. Generator stack parameter data (plume exit velocity, plume exit temperature and stack exit diameter) were provided by Caterpillar. Only one (1) engine will be tested during any one hour. While the engines will be tested at minimum loads, the 100 percent load case was utilized for the worst-case plume analysis. For the engine analysis, two ambient conditions were considered: 41.0°F, the minimum monthly mean of daily minimum temperatures, and 84.3°F, the maximum monthly mean of daily maximum temperatures for the San Jose Airport (*"Climatology of the United States No. 81 – Monthly Station Normals of Temperature, Precipitation, and Heating and Cooling Degree Days 1971-2000 – California"*, February 2002, and *"Climatology of the United States No 20 – Monthly Station Climate Summaries, 1971-2000 – California"*, February 2004). These data is summarized in Table 1.



Table 1 Caterpillar Diesel Stack Characteristics for Vertical Plume Velocity Analysis			
Case #	1	2	
Ambient Temperature (°F)*	41.0	41.0	
Stack Diameter (m)	0.7112	0.7112	
Exhaust Velocity (m/s)*	30.44	30.44	
Exhaust Temperature (K)*	733.15	733.15	
Stack Release Height (m)	7.72	7.72	
Stack Buoyancy Flux (m <sup>4</sup> /s <sup>3</sup> )	22.195	23.439	
*Stack data provided by Caterpillar at 100% load			

Screening level vertical plume velocity assessments were made for two ambient temperatures with calm winds and neutral atmospheric conditions for the cases presented in Table 1 which are based on 100 percent load. The results based on the two ambient conditions are presented in Table 2 and the output from the calculation spreadsheet provided in Attachment A.

The initial jet phase extends to a height of about 39.9 feet above grade level (ft-agl) for both cases. After the jet phase, plume temperature buoyancy characteristics modeled in the Spillane methodology cause a uniform decrease in plume-averaged vertical velocities, with the critical plume-averaged vertical velocity of 5.3 m/s occurring at about 62.3 ft-agl for both cases

Table 2 Diesel Engine Vertical Plume Velocity Analysis Results for Reference Height			
Case #	1	2	
Ambient Temperature (°F)	41.0	84.3	
Single Plume Results:			
Plume-Averaged Vertical Velocity at 200 feet-agl (m/s)	2.40	2.36	
Height of 5.3 m/s Plume-Averaged Vertical Velocity (feet-agl)	62.3	62.6	

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the diesel engine always remain in the light turbulence category and below the significance level of 5.3 m/s at all heights above about 63 ft-agl. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities, so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.

### Vertical Plume Velocity Calculations for the Rooftop Cooling Towers

Each data center has 18 rooftop cooling towers, each of which are each comprised of three (3) individual cells, with a cell fan diameter of 66 inches. The 18 cooling towers are arranged in a 9 x 2 configuration along the longer building length (averaging 4 feet between adjacent towers). Based on the groupings of cooling towers, the single and merged plumes were based on the



combined effective stack of six (6) individual cells (each tower is made up of three cells) by merging plumes along the center in between the two cooling towers (1 merged stack for each cooling tower and 9 merged stacks for the combined plume assessment). Cooling tower stack parameter data (exit velocity and temperature) were provided by the applicant. An effective stack diameter for all six (6) cells was utilized for each merged cooling tower. To utilize conservative modeling methods, all towers/cells were assumed to be operating at full load. These data are summarized in Table 3 for the same ambient temperatures used for the engine analysis.

<b>Table 3</b>			
<b>Chiller Stack Characteristics for Vertical Plume Velocity Analysis</b>			
	<b>Case #</b>	<b>1</b>	<b>2</b>
Ambient Temperature (°F)*		41.0	84.3
Effective Stack Diameter (m)**		4.11	4.11
Exhaust Velocity (m/s)*		13.11	13.11
Exhaust Temperature (K)*		313.32	313.32
Stack Release Height (m)		24.54	24.54
Stack Buoyancy Flux (m <sup>4</sup> /s <sup>3</sup> )		20.85	19.25
*Chiller stack data provided by the applicant			
** Calculated value based on the cell diameter of 66 inches multiplied by the square of the number of operating cells, or $D_{\text{eff}} = 66 \cdot \sqrt{6}$			

The Spillane methodology was originally developed to treat multiple individual stacks that are arranged along a linear x or y direction, but not both directions at once, with stack separations much greater than the stack diameters, typical of boilers/turbines at large power plants. As noted above, the 18 cooling towers are generally arranged in a 9 x 2 pattern. Therefore, the enhanced Spillane methodology was based on calculating the total merging height for the largest linear direction of tower placements (which is nine cooling tower cells spaced 11.7 feet apart (based on the distance between the calculated equivalent diameter cells) along the longer length of the building). The grouping of 9 (3x18) towers were considered in the calculation of vertical velocity plume enhancement (both at and above the totally merged height, and for the interpolation down to the plume touching height). The effective single stack diameter of each merged tower was based on the merged six (6) cell diameter.

Screening level vertical plume velocity assessments were made for the same ambient temperatures with calm winds and neutral atmospheric conditions as was done for the emergency generator engines. These cases represent worst-case conditions of calm winds at all levels of a neutral atmosphere. The results are presented in Table 4 and the output from the calculation spreadsheets are provided in Attachment A.

The initial jet phase extends to a height of about 164.7 ft-agl for both cases. The critical plume-averaged vertical velocity of 5.3 m/s occurs at the end of the jet phase at about 186 ft-agl for both cases. The plumes touch (begin to merge) at about 118.7 ft-agl and are fully merged at about 374.9 ft-agl for both cases. Under the enhanced Spillane methodology, the merged plume-averaged vertical velocities approach 5.3 m/s at 343.9 ft-agl.



Table 4 Chiller Vertical Plume Velocity Analysis Results for Reference Height		
Case #	1	2
Ambient Temperature (°F)	41.0	84.3
<b>Single Plume Results:</b>		
Height of 5.3 m/s Plume-Averaged Vertical Velocity (Within the Jet Phase, feet-agl)	186.0	185.9
<b>Merged Plume Results:</b>		
Height of 5.3 m/s Plume-Averaged Vertical Velocity (Within the Merging Phase, feet-agl)	343.9	342.8
Plume-Averaged Vertical Velocity at 500 feet-agl (m/s)	3.75	3.70

These screening results indicate that mechanical and thermal turbulence levels due to the flow from the cooling towers always remain in the light turbulence category and below the significance level of 5.3 m/s at all heights above about 344 ft-agl. Even light wind speeds can dramatically decrease the predicted plume-averaged vertical velocities so the above results are very conservative indications of adverse conditions. The important factor for a given location is the appropriateness of available information for estimating true wind and temperature profiles throughout a typical year. Theoretical calculations, as shown in the tables above, are likely to overestimate the expected vertical velocities, for the following reasons:

- The wind profile is assumed constant with height with no occurrence of wind-shear when realistically, there is a considerable variation with height, especially in light winds;
- Worst-case scenarios are based on very light-wind, near-neutral atmospheric conditions with maximum loading.



**Attachment A**  
**Spillane Method Plume Velocity Calculations**



SINGLE Plume Average Vertical Velocities for Large Emer.Gen Engine, 100% Load, and Maximum Stack Height - Winter Min*					
"Aviation Safety and Buoyant Plumes," Peter Best, et. al.					
"The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane					
<b>Ambient Conditions:</b>		Ambient Potential Temp $\theta_a$		Constants: Assume neutral conditions ( $d\theta/dz=0$ or $\theta_a=\theta_0$ )	
	278.15 Kelvins	41.0 °F		0.3048 meters/foot	
<b>Plume Exit Conditions:</b>		Maximum Stack Height $h_s$		Gravity g	
	7.72 meters	25 4/12 feet-inches		9.81 m/s <sup>2</sup>	
	Stack Diameter D	28 inches		$\lambda$	1.11
	Stack Velocity $V_{exit}$	99.86 ft/sec		$\lambda_{\theta}$	-1.0
	Volumetric Flow	25,620 ACFM		$\pi V_{exit} D^2/4$	Sect.2/¶1
	Stack Potential Temp $\theta_s$	860 °F		$g V_{exit} D^2 (1-\theta_s/\theta_a)/4 = Vol.Flow(g/\pi)(1-\theta_s/\theta_a)$	Sect.2/¶1
	Initial Stack Buoyancy Flux $F_b$	23.4388 m <sup>4</sup> /s <sup>3</sup>		$\lambda^2 g V a^2 (1-\theta_s/\theta_a)$ for a, V, $\theta_s$ at plume height (see below)	
	Plume Buoyancy Flux F	N/A m <sup>4</sup> /s <sup>3</sup>		$\lambda^2 g V a^2 (1-\theta_s/\theta_a)$ for a, V, $\theta_s$ at plume height (see below)	
	No. of Stacks N	1		1.000 Multiple Stack Multiplication Factor ( $N^{0.25}$ )	
<b>Conditions at End (Top) of Jet Phase:</b>					
	Height above Stack $Z_{jet}$	14.6 feet*		$Z_{jet} = 6.25D$ , meters*=meters above stack top	Sect.3/¶1
	Height above Ground $Z_{jet}+h_s$	39.9 feet			"
	Vertical Velocity $V_{jet}$	49.93 ft/sec		$V_{jet} = 0.5V_{exit} = V_{exit}/2$	"
	Plume Top-Hat Diameter $2a_{jet}$	4.7 feet		$2a_{jet} = 2D$	Conservation of momentum
<b>Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase</b>					
Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:					
	Plume Top-Hat Radius a	Solutions in Table Below		0.16(z-z <sub>v</sub> ), or linear increase with height	Sect.2/Eq.6
	Virtual Source Height z <sub>v</sub>	5.6 feet*		$6.25D[1-(\theta_s/\theta_a)]^{1/2}$ , meters*=meters above stack top	Sect.2/Eq.6
	Height above Ground z <sub>v</sub> +h <sub>s</sub>	30.9 feet		where $(\theta_s/\theta_a)^{1/2} = (\theta_s/\theta_a)^{1/2} = 0.6159$	0.6159
	Vertical Velocity V	Solutions in Table Below		$\{(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / a$	Sect.2.1(6)
	Product (Va) <sub>0</sub>	6.666 m <sup>2</sup> /s		$V_{exit} D/2(\theta_s/\theta_a)^{1/2}$	
	Solve for plume-averaged vertical velocity at height	200.0 feet		60.96 meters above ground (z+h <sub>s</sub> )	
	Gives the following Height above Stack z'	53.240 meters*		174.7 feet*	
	Plume Top-Hat Diameter 2a'	54.1 feet		$2a' = 2*0.16(z'-z_v)$	Sect.2/Eq.6
	Vertical Velocity V	7.87 ft/sec		$V = \{(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / (2a'/2)$	Sect.2/Eq.6
	Solve for Height of CASC critical vertical velocity V <sub>crit</sub>	5.30 m/s plume-averaged vertical velocity		Critical VV > Top of Jet (Spillane)	
	Find Height above Stack z <sub>crit</sub>	11.262 meters		36.9 feet	Solve for x=(z-z <sub>v</sub> ) simultaneously in both eqs. (i.e., Va and a)
	Height above Ground z <sub>crit</sub> +h <sub>s</sub>	18.982 meters		62.3 feet	for V=4.3 m/s using the cubic equation ax <sup>3</sup> +bx <sup>2</sup> +cx+d=0, where
	Interpolated Height of critical vertical velocity in Jet Phase:				a=1, c=0, and b=-0.12F <sub>b</sub> /(4.3 <sup>3</sup> 0.16 <sup>3</sup> )=-4.6124
	Find Height above Stack z <sub>crit</sub>	#N/A meters		#N/A feet	and d=[0.12F <sub>b</sub> (6.25D-z <sub>v</sub> ) <sup>2</sup> -(Va) <sub>0</sub> <sup>3</sup> ]/(4.3 <sup>3</sup> 0.16 <sup>3</sup> )=-451.18
	Height above Ground z <sub>crit</sub> +h <sub>s</sub>	#N/A meters		#N/A feet	<a href="http://www.1728.org/cubic.htm">http://www.1728.org/cubic.htm</a>
					gives the real solution x = z-zv = 9.5546
					or z(m/above stack) = 11.262
					z(ft/above ground) = 62.3
<b>Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:</b>					
	Height (feet)	(meters)	Plume Radius(m)	SingleStk VertVel(m/s)	Plume Temp(K)
	above ground	above stack			
	Stack.Rel.Ht = 25.3	0.00	0.356	30.44	
	30.0	1.42	0.470	25.56	Jet Phase Eqs: 5 foot Intervals
	35.0	2.95	0.592	20.34	Linearly interpolated from Stack Rel.Ht to Top of Jet
	Top of jet = 39.9	4.44	0.711	15.22	Spillane Equations:
	40.0	4.47	0.442	15.08	$V_{plume} = \{(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / a$
	50.0	7.52	0.930	7.72	a = 0.16(z-z <sub>v</sub> )
	60.0	10.57	1.418	5.58	10 foot Intervals
	Spillane 5.3 m/s Height = 62.3	11.26	1.529	5.30	$\theta_s = \theta_a (1 + (1 - \theta_s/\theta_a)) (V_{exit} D^2 / (4V_{plume} a^2 \lambda^2))$
	70.0	13.62	1.905	4.60	
	80.0	16.66	2.393	4.04	
	90.0	19.71	2.881	3.68	Max<5.30 m/s
	100.0	22.76	3.368	3.41	
	110.0	25.81	3.856	3.22	
	120.0	28.86	4.344	3.06	
	160.0	41.05	6.294	2.65	40 foot Intervals
	200.0	53.24	8.245	2.40	
	240.0	65.43	10.196	2.23	
	280.0	77.62	12.147	2.10	
	320.0	89.82	14.097	1.99	
	360.0	102.01	16.048	1.90	
	400.0	114.20	17.999	1.83	
	500.0	144.68	22.876	1.69	100 foot Intervals
	600.0	175.16	27.752	1.58	
	700.0	205.64	32.629	1.50	
	800.0	236.12	37.506	1.43	
	900.0	266.60	42.383	1.37	
	1000.0	297.08	47.260	1.33	
	1100.0	327.56	52.136	1.28	
	1200.0	358.04	57.013	1.24	
	1300.0	388.52	61.890	1.21	
	1400.0	419.00	66.767	1.18	
	1500.0	449.48	71.644	1.15	
	1600.0	479.96	76.520	1.13	
	1700.0	510.44	81.397	1.11	
	1800.0	540.92	86.274	1.08	
	1900.0	571.40	91.151	1.06	

\*Winter Min = Monthly Mean of Minimum Daily Temperatures for 1971-2000 (Lowest in December)  
 NOAA Sources: Climatology of the United States No.81 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



SINGLE Plume Average Vertical Velocities for Single Large Emer.Gen Engine, 100% Load, and Maximum Stack Height - Summer Max*					
"Aviation Safety and Buoyant Plumes," Peter Best, et. al.					
"The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane					
<b>Ambient Conditions:</b>		Ambient Potential Temp $\theta_a$		Constants: Assume neutral conditions ( $d\theta/dz=0$ or $\theta_a=\theta_b$ )	
		302.21 Kelvins	84.3 °F		0.3048 meters/feet
<b>Plume Exit Conditions:</b>		Maximum Stack Height $h_s$		Gravity $g$	
		7.72 meters	25 4/12 feet-inches		9.81 m/s <sup>2</sup>
		Stack Diameter $D$	28 inches		$\lambda$ 1.11
		Stack Velocity $V_{exit}$	99.86 ft/sec		$\lambda_o$ -1.0
		Volumetric Flow	25,620 ACFM	$\pi V_{exit} D^2/4$	Sect.2/¶1
		Stack Potential Temp $\theta_s$	860 °F		
		Initial Stack Buoyancy Flux $F_{\theta}$	22,1953 m <sup>4</sup> /s <sup>3</sup>	$g V_{exit} D^2 (1-\theta_s/\theta_a)/4 = Vol.Flow/g(\pi)(1-\theta_s/\theta_a)$	Sect.2/¶1
		Plume Buoyancy Flux $F$	N/A m <sup>4</sup> /s <sup>3</sup>	$\lambda^2 g V a^2 (1-\theta_s/\theta_a)$ for a, V, $\theta_s$ at plume height (see below)	
		No. of Stacks $N$	1	1.000 Multiple Stack Multiplication Factor ( $N^{0.25}$ )	
<b>Conditions at End (Top) of Jet Phase:</b>					
		Height above Stack $z_{jet}$	14.6 feet*	$z_{jet} = 6.25D$ , meters*=meters above stack top	Sect.3/¶1
		Height above Ground $z_{jet}+h_s$	39.9 feet		"
		Vertical Velocity $V_{jet}$	49.93 ft/sec	$V_{jet} = 0.5 V_{exit} = V_{exit}/2$	"
		Plume Top-Hat Diameter $2a_{jet}$	4.7 feet	$2a_{jet} = 2D$	Conservation of momentum
<b>Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase</b>					
Single Plume-averaged Vertical Velocity $V$ given by Analytical Solution in Paper where Product $Va$ given by equations below:					
		Plume Top-Hat Radius $a$	Solutions in Table Below	$0.16(z-z_v)$ , or linear increase with height	Sect.2/Eq.6
		Virtual Source Height $z_v$	5.2 feet*	$6.25D[1-(\theta_s/\theta_a)]^{1/2}$ , meters*=meters above stack top	Sect.2/Eq.6
		Height above Ground $z_v+h_s$	30.5 feet	where $(\theta_s/\theta_a)^{1/2} = (\theta_s/\theta_a)^{1/2} = 0.6420$	
		Vertical Velocity $V$	Solutions in Table Below	$\{(Va)_s^3 + 0.12F_{\theta} [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / a$	Sect.2.1(6)
		Product $(Va)_s$	6.950 m <sup>2</sup> /s	$V_{exit} D/2(\theta_s/\theta_a)^{1/2}$	
		Solve for plume-averaged vertical velocity at height	200.0 feet	60.96 meters above ground ( $z+h_s$ )	
		Gives the following Height above Stack $z'$	53.240 meters*	174.7 feet*	
		Plume Top-Hat Diameter $2a'$	16.528 meters	54.2 feet	$2a' = 2 \cdot 0.16(z'-z_v)$
		Vertical Velocity $V$	2.360 m/s	7.74 ft/sec	$V = \{(Va)_s^3 + 0.12F_{\theta} [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / (2a'/2)$
		Solve for Height of CASC critical vertical velocity $V_{crit}$	5.30 m/s plume-averaged vertical velocity		Critical $VV >$ Top of Jet (Spillane)
		Find Height above Stack $z_{crit}$	11.358 meters	37.3 feet	Solve for $x=(z-z_v)$ simultaneously in both eqs. (i.e., $Va$ and $a$ )
		Height above Ground $z_{crit}+h_s$	19.078 meters	62.6 feet	for $V=4.3$ m/s using the cubic equation $ax^3+bx^2+cx+d=0$ , where
				$a=1$ , $c=0$ , and $b=-0.12F_{\theta}/(4.3^3 \cdot 0.16^3) = -4.3677$	
				and $d=[0.12F_{\theta}(6.25D-z_v)^2 - (Va)_s^3]/(4.3^3 \cdot 0.16^3) = -514.94$	
		Interpolated Height of critical vertical velocity in Jet Phase:			<a href="http://www.1728.org/cubic.htm">http://www.1728.org/cubic.htm</a>
		Find Height above Stack $z_{crit}$	#N/A meters	#N/A feet	gives the real solution $x = z-z_v =$
		Height above Ground $z_{crit}+h_s$	#N/A meters	#N/A feet	or $z$ (m/above stack) = 11.358
					$z$ (ft/above ground) = 62.6
<b>Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:</b>					
	Height (feet)	Height (meters)	Plume Radius(m)	SingleStk VertVel(m/s)	Plume Temp(K)
	above ground	above stack			
	<b>Stack.Rel.Ht = 25.3</b>	<b>0.00</b>	<b>0.356</b>	<b>30.44</b>	
	30.0	1.42	0.470	25.56	
	35.0	2.95	0.592	20.34	
	<b>Top of jet = 39.9</b>	<b>4.44</b>	<b>0.711</b>	<b>15.22</b>	
	40.0	4.47	0.461	15.08	475.37
	50.0	7.52	0.949	7.82	381.11
	60.0	10.57	1.436	5.63	349.99
	<b>Spillane 5.3 m/s Height = 62.6</b>	<b>11.36</b>	<b>1.563</b>	<b>5.30</b>	<b>345.09</b>
	70.0	13.62	1.924	4.61	334.71
	80.0	16.66	2.412	4.03	325.88
	90.0	19.71	2.899	3.65	320.28
	100.0	22.76	3.387	3.39	316.50
	110.0	25.81	3.875	3.18	313.82
	120.0	28.86	4.362	3.02	311.86
	160.0	41.05	6.313	2.61	307.55
	200.0	53.24	8.264	2.36	305.65
	240.0	65.43	10.215	2.19	304.64
	280.0	77.62	12.165	2.06	304.03
	320.0	89.82	14.116	1.96	303.63
	360.0	102.01	16.067	1.87	303.36
	400.0	114.20	18.017	1.80	303.16
	500.0	144.68	22.894	1.66	302.85
	600.0	175.16	27.771	1.56	302.67
	700.0	205.64	32.648	1.47	302.56
	800.0	236.12	37.525	1.41	302.49
	900.0	266.60	42.401	1.35	302.44
	1000.0	297.08	47.278	1.30	302.40
	1100.0	327.56	52.155	1.26	302.37
	1200.0	358.04	57.032	1.22	302.35
	1300.0	388.52	61.909	1.19	302.33
	1400.0	419.00	66.785	1.16	302.32
	1500.0	449.48	71.662	1.13	302.31
	1600.0	479.96	76.539	1.11	302.30
	1700.0	510.44	81.416	1.09	302.29
	1800.0	540.92	86.293	1.06	302.28
	1900.0	571.40	91.169	1.05	302.27

\*Summer Max = Monthly Mean of Maximum Daily Temperatures for 1971-2000 (Highest in July)  
 NOAA Sources: Climatology of the United States No.81 "Monthly Station Normals of Temperatures, Precipitation, and Heating and Cooling Degree Days, 1971-2000 California" and Climatology of the United States No. 20 "Monthly Station Climate Summaries, 1971-2000 California"



SINGLE/Approximated Plume Average Vertical Velocities for Northtown Chillers - Winter Min*				
Based on 9 chillers w/ 6 cells/combined tower. "Aviation Safety and Buoyant Plumes," Peter Best, et. al.				
Calc' eff.diam for each tower with each cell at 66" ID (368,400 ACFM total for each combined tower). "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane				
Ambient Conditions:		Constants: Assume neutral conditions (dθ/dz=0 or θ <sub>a</sub> =θ <sub>0</sub> )		
Ambient Potential Temp θ <sub>a</sub>	278.15 Kelvins	41.0 °F	0.3048 meters/feet	
Plume Exit Conditions:		Gravity g 9.81 m/s <sup>2</sup>		
Stack Height h <sub>s</sub>	24.54 meters	80 6/12 feet-inches	λ 1.11	
Individual Chiller Stack Diameter D	4.1063 meters	161.7 inches	λ <sub>0</sub> ~1.0	
Stack Velocity V <sub>exit</sub>	13.13 m/s	43.07 ft/sec	4V <sub>col</sub> /(80πD <sup>2</sup> )	
Individual Chiller Volumetric Flow	173.87 cu.m/sec	368,400 ACFM	πV <sub>exit</sub> D <sup>2</sup> /4	
Stack Potential Temp θ <sub>s</sub>	289.26 Kelvins	61.0 °F		
Initial Stack Buoyancy Flux F <sub>0</sub>	20.8545 m <sup>4</sup> /s <sup>3</sup>	20.0 ΔT(°F)	gV <sub>exit</sub> D <sup>2</sup> (1-θ <sub>s</sub> /θ <sub>a</sub> )/4 = Vol.Flow(g/π)(1-θ <sub>s</sub> /θ <sub>a</sub> )	
Plume Buoyancy Flux F	N/A m <sup>4</sup> /s <sup>3</sup>		λ <sup>2</sup> gVa <sup>2</sup> (1-θ <sub>s</sub> /θ <sub>a</sub> ) for a.V.θ <sub>s</sub> at plume height (see below)	
Number of Towers n	9		1.732 Multiple Stack Multiplication Factor (n <sup>0.25</sup> )	
Conditions at End (Top) of Jet Phase:				
Height above Stack z <sub>jet</sub>	25.664 meters*	84.2 feet*	z <sub>jet</sub> = 6.25D, meters*=meters above stack top	
Height above Ground z <sub>jet</sub> +h <sub>s</sub>	50.201 meters	164.7 feet		
Vertical Velocity V <sub>jet</sub>	6.564 m/s	21.54 ft/sec	V <sub>jet</sub> = 0.5V <sub>exit</sub> = V <sub>exit</sub> /2	
Plume Top-Hat Diameter 2a <sub>jet</sub>	8.213 meters	26.9 feet	2a <sub>jet</sub> = 2D Conservation of momentum	
Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase				
Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:				
Plume Top-Hat Radius a	Solutions in Table Below		0.16(z-z <sub>v</sub> ), or linear increase with height	
Virtual Source Height z <sub>v</sub>	0.498 meters*	1.6 feet*	6.25D[1-(θ <sub>s</sub> /θ <sub>a</sub> ) <sup>1/2</sup> ], meters*=meters above stack top	
Height above Ground z <sub>v</sub> +h <sub>s</sub>	25.034 meters	82.1 feet	where (θ <sub>s</sub> /θ <sub>a</sub> ) <sup>1/2</sup> = (θ <sub>s</sub> /θ <sub>a</sub> ) <sup>1/2</sup> = 0.9806	
Vertical Velocity V	Solutions in Table Below		{(Va) <sub>0</sub> <sup>3</sup> + 0.12F <sub>0</sub> [(z-z <sub>v</sub> ) <sup>2</sup> - (6.25D-z <sub>v</sub> ) <sup>2</sup> ] <sup>1/3</sup> / a	
Product (Va) <sub>0</sub>	26.432 m <sup>2</sup> /s		V <sub>exit</sub> D/2(θ <sub>s</sub> /θ <sub>a</sub> ) <sup>1/2</sup>	
Single Chiller Results:				
Solve for plume-averaged vertical velocity at height		500.0 feet	152.4 meters above ground (z'+h <sub>s</sub> )	
Gives the following Height above Stack z'		127.864 meters*	419.5 feet*	
Plume Top-Hat Diameter 2a'		40.757 meters	133.7 feet	
Vertical Velocity V		1.894 m/s	6.21 ft/sec	
Solve for Height of CASC critical vertical velocity V <sub>crit</sub>		5.30 m/s plume-averaged vertical velocity	Critical VV > Top of Jet (Spillane)	
Find Height above Stack z <sub>crit</sub>		32.151 meters	105.5 feet	
Height above Ground z <sub>crit</sub> +h <sub>s</sub>		56.687 meters	186.0 feet	
for V=V <sub>crit</sub> using the cubic equation ax <sup>3</sup> +bx <sup>2</sup> +cx+d=0, where				
a=1, c=0, and b=(0.12F <sub>0</sub> )/(V <sub>crit</sub> <sup>3</sup> 0.16 <sup>3</sup> )= -4.10387				
and d=(0.12F <sub>0</sub> (6.25D-z <sub>v</sub> ) <sup>2</sup> -(Va) <sub>0</sub> <sup>3</sup> )/(V <sub>crit</sub> <sup>3</sup> 0.16 <sup>3</sup> )= -27684.01				
Interpolated Height of critical vertical velocity in Jet Phase:				
Find Height above Stack z <sub>crit</sub>		#N/A meters	#N/A feet	
Height above Ground z <sub>crit</sub> +h <sub>s</sub>		#N/A meters	#N/A feet	
gives the real solution x = z-z <sub>v</sub> = 31.6532				
or z(m/above stack) = 32.151				
z(ft/above ground) = 186.0				
Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:				
Height (feet)	(meters)	Plume Radius(m)	SingleStk vertVel(m/s)	Plume Temp(K)
Stack.Rel.Ht = 80.5	0.00	2.053	13.13	
100.0	5.94	2.529	11.61	
120.0	12.04	3.016	10.05	
140.0	18.14	3.504	8.49	
160.0	24.23	3.992	6.93	
160.0	24.23	3.992	6.93	
Top of Single jet = 164.7	25.66	4.106	6.56	
180.0	30.33	4.773	5.60	282.49
200.0	36.42	5.748	4.73	281.91
220.0	42.52	6.723	4.12	281.22
240.0	48.62	7.699	3.68	280.72
260.0	54.71	8.674	3.34	280.35
280.0	60.81	9.650	3.07	280.06
300.0	66.90	10.625	2.86	279.83
350.0	82.14	13.063	2.47	279.64
400.0	97.38	15.502	2.21	279.29
450.0	112.62	17.940	2.03	279.05
500.0	127.86	20.379	1.89	278.88
550.0	143.10	22.817	1.79	278.76
600.0	158.34	25.255	1.70	278.67
650.0	173.58	27.694	1.63	278.59
700.0	188.82	30.132	1.57	278.53
800.0	219.30	35.009	1.47	278.49
900.0	249.78	39.886	1.40	278.42
1000.0	280.26	44.763	1.33	278.37
1100.0	310.74	49.639	1.28	278.33
1200.0	341.22	54.516	1.24	278.30
1300.0	371.70	59.393	1.20	278.28
1400.0	402.18	64.270	1.17	278.26
1500.0	432.66	69.147	1.14	278.25
2000.0	585.06	93.531	1.02	278.24
2500.0	737.46	117.915	0.94	278.20
3000.0	889.86	142.299	0.88	278.19
3500.0	1042.26	166.683	0.84	278.18
4000.0	1194.66	191.067	0.80	278.17
4500.0	1347.06	215.451	0.77	278.17
5000.0	1499.46	239.835	0.74	278.16

\*Winter Min = Monthly Mean of Minimum Daily Temperatures for 1971-2000 (Lowest in December)  
 NOAA Sources: Climatography of the United States



MERGED (along length) Plume Average Vertical Velocities for Northtown Chillers - Winter Min*				
*Aviation Safety and Buoyant Plumes," Peter Best, et. al.				
*The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Merged				
Plume from Two Gas-Turbine Power Station at Oakley, Queensland, Australia," Dr. K.T. Spillane				
Ambient Conditions:		Constants: Assume neutral conditions (dB/dz=0 or $\theta_a=\theta_a$ )		
Ambient Potential Temp $\theta_a$	278.15 Kelvins	41.0 °F	0.3048 meters/feet	
Plume Exit Conditions:		Gravity g		
Stack Height $h_s$	24.54 meters	80 6/12 feet-inches	$\lambda$	1.11
Individual Stack Diameter D	4.1063 meters	161.7 inches	$\lambda_c$	-1.0
Stack Velocity $V_{exit}$	13.13 m/s	43.07 ft/sec	$4Vol/(60\pi D^2)$	
Individual Volumetric Flow	173.87 cu.m/sec	368,400 ACFM	$\pi V_{exit} D^2/4$	
Stack Potential Temp $\theta_s$	289.26 Kelvins	61.0 °F	Sect.2/¶1	
Initial Stack Buoyancy Flux $F_b$	20.85 m <sup>4</sup> /s <sup>3</sup>	20.0 ΔT(°F)	$g_{exit} D^2 (1-\theta_s/\theta_a)/4 = Vol.Flow(g/m^3)(1-\theta_s/\theta_a)$	
Plume Buoyancy Flux F	N/A m <sup>4</sup> /s <sup>3</sup>		$\lambda^2 g V a^2 (1-\theta_s/\theta_a)$ for a, V, $\theta_s$ at plume height (see below)	
Total Number of Stacks n	9			
Average Adjacent Stack Separation d	3.57 meters	11.7 feet	Calcs based on multiple plume treatment in Peter Best Paper: plume velocities increased by N <sup>0.25</sup> at the height where plumes fully merged (interp. below ht, single merged stack above ht)	
Number of Stacks along Orientation N	9			
Conditions at End (Top) of Jet Phase:				
Height above Stack $z_{jet}$	25.664 meters*	84.2 feet*	$z_{jet} = 6.25D$ , meters*=meters above stack top	
Height above Ground $z_{jet}+h_s$	50.201 meters	164.7 feet		
Vertical Velocity $V_{jet}$	6.564 m/s	21.54 ft/sec	$V_{jet} = 0.5 V_{exit} = V_{exit}/2$	
Plume Top-Hat Diameter $2a_{jet}$	8.213 meters	26.9 feet	$2a_{jet} = 2D$ Conservation of momentum	
Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet and Merging Phases				
Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:				
Single Plume Values: Plume Top-Hat Radius a		Used in Plume Merging Only		a = 0.16(z-z <sub>v</sub> ), or linear increase with height
Virtual Source Height $z_v$	4.988 meters*	1.6 feet*	$z_v = 6.25D[1-(\theta_s/\theta_a)^{1/2}]$ , meters*=meters above stack top	
Height above Ground $z_v+h_s$	25.034 meters	82.1 feet	where $(\theta_s/\theta_a)^{1/2} = (\theta_s/\theta_a)^{1/2} = 0.9806$	
Single Plume Values: Vertical Velocity V		Used in Plume Merging Only		$[(Va)_s^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$
Product (Va) <sub>s</sub>	26.432 m <sup>2</sup> /s		$V_{exit}(D/2)(\theta_s/\theta_a)^{1/2}$	
Plume Merging - Based on Single Plume Calculations where:				
Begin Merging Plume Top-Hat Diameter $2a_{touch}$		3.570 meters	11.7 feet	$2a_{touch}=d$ , (or $a_{touch}=d/2$ )
Height above Stack $z_{touch}$	11.654 meters*	38.2 feet*	$z_{touch} = z_v + d/(2*0.16)$ , meters*=meters above stack top	
Height above Ground $z_{touch}+h_s$	36.190 meters	118.7 feet		
Vertical Velocity $V_{touch}$	14.459 m/s	47.4 ft/sec	$V_{touch} = \{[(Va)_s^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$	
Total Merging Plume Top-Hat Diameter $2a_{full}$		28.560 meters	93.7 feet	$2a_{full}=2d(N-1)/2$ , (or $a_{full}=d(N-1)/2$ ) FOR 2 STACKS, $2a_{full}=2d$
Height above Stack $z_{full}$	89.748 meters*	294.4 feet*	$z_{full} = z_v + 2d/(2*0.16)$ , meters*=meters above stack top	
Height above Ground $z_{full}+h_s$	114.284 meters	374.9 feet		
Vertical Velocity $V_{full}$	2.330 m/s	7.6 ft/sec	$V_{full} = \{[(Va)_s^3 + 0.12F_b [(z_{full}-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a_{full}$	
Product (V <sup>3</sup> a) <sub>full</sub>	181 m <sup>4</sup> /s <sup>3</sup>			
Conditions at End (Top) of Merging Phase - Define new values for $V_{full}$ and $a_{full}$ in Merged Plume calculations (based on TOTAL number of stacks):				
Merged Plume Values: Plume Diameter $2a$		Solutions in Table Below		$2a = 2x(a_m + 0.16(z-z_{full}))$ , or linear increase with height
Revised Merged Plume Radius $a_m$	24.734 meters	81.1 feet	where $a_m = n^{0.25} a_{full}$ where Total Merging Occurs	
Revised Merged Plume Velocity $V_m$	4.035 m/s	13.24 ft/sec	and $V_m = n^{0.25} V_{full}$ where Total Merging Occurs	
Revised Virtual Source Height $z_{full}$	89.748 meters*	294.4 feet*	Height above stack where Total Merging Occurs (shown above)	
Revised Vertical Velocity V	Solutions in Tables Below		$V = \{n(V^3 a)_{full}/a\}^{1/3}$ for heights above total merging elevation	
Multiple Plume Calculations				
Solve for plume-averaged vertical velocity at height		500.0 feet	152.4 meters above ground (z+h <sub>s</sub> )	
Gives the following Height above Stack z	127.864 meters*	419.5 feet*	REGULAR EQNS	
Plume Top-Hat Radius a	30.832 meters	101.2 feet	$a = a_m + 0.16(z-z_{full})$ if $z > z_{full}$	
Vertical Velocity V	3.749 m/s	12.30 ft/sec	$V = \{n(V^3 a)_{full}/a\}^{1/3}$ if $z > z_{full}$	
$V = V_{touch} + (V_m - V_{touch}) \{ (z - z_{touch}) / (z_{full} - z_{touch}) \}$ if $z_{touch} < z < z_{full}$				
$V =$ single plume values if $z < z_{touch}$				
LESS THAN TOP OF MERGING PHASE-INTERPO				
Find Height above Stack $z_{crit}$	80.271 meters	263.4 feet	$z_{crit} = z_{full} + \{ [n(V^3 a)_{full} (V_{crit})^3] - a_m \} / 0.16$ if $V_{crit} < V_m$	
Height above Ground $z_{crit}+h_s$	104.807 meters	343.9 feet	$z_{crit} = z_{touch} + (z_{full} - z_{touch}) \{ V_{crit} - V_{touch} \} / (V_m - V_{touch})$ if $V_{crit} > V_m$	
Table of MERGED Plume-Averaged Vertical Velocities starting at Touching Height:				
Single Plume Eqns (see Single Plume spreadsheet)				
Height (feet)	(meters)	Plume	Vert.	$V_{full} = \{ [(Va)_s^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$
above ground above stack Radius(m)		Vel(m/s)	$a = 0.16(z-z_v)$	
Begin Merging (touch) = 118.7		11.64	1.785	14.46
125.0	13.56	#N/A	14.20	
150.0	21.18	#N/A	13.19	
175.0	28.80	#N/A	12.17	
200.0	36.42	#N/A	11.15	
225.0	44.04	#N/A	10.14	
250.0	51.66	#N/A	9.12	
275.0	59.28	#N/A	8.10	
300.0	66.90	#N/A	7.08	
325.0	74.52	#N/A	6.07	
350.0	82.14	#N/A	5.05	
End Merging (full/mp) = 374.9		89.73	24.731	4.04
400.0	97.38	25.955	3.97	
450.0	112.62	28.394	3.85	
500.0	127.86	30.832	3.75	
600.0	158.34	35.709	3.57	
700.0	188.82	40.586	3.42	
800.0	219.30	45.463	3.29	
900.0	249.78	50.339	3.18	
1000.0	280.26	55.216	3.09	
1100.0	310.74	60.093	3.00	
1200.0	341.22	64.970	2.92	
1300.0	371.70	69.847	2.85	
1500.0	432.66	79.600	2.73	
2000.0	585.06	103.984	2.50	
2500.0	737.46	128.368	2.33	
3000.0	889.86	152.752	2.20	
3500.0	1042.26	177.136	2.09	
4000.0	1194.66	201.520	2.01	
4500.0	1347.06	225.904	1.93	



**SINGLE/Approximated Plume Average Vertical Velocities for Northtown Chillers - Summer Max\***  
 Based on 9 chillers w/ 6 cells/combined tower. "Aviation Safety and Buoyant Plumes," Peter Best, et. al.  
 Calc' eff. diam for each tower with each cell at 66" ID (368,400 ACFM total for each combined tower). "The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Plume from a Gas-Turbine Power Station at Oakey, Queensland, Australia," Dr. K.T. Spillane

**Ambient Conditions:** Ambient Potential Temp  $\theta_a$  302.21 Kelvins 84.3 °F Gravity g 0.3048 meters/feet  
**Plume Exit Conditions:** Stack Height  $h_s$  24.54 meters 80 6/12 feet-inches  $\lambda$  1.11  
 Individual Chiller Stack Diameter D 4.1063 meters 161.7 inches  $\lambda_o$  ~1.0  
 Stack Velocity  $V_{exit}$  13.13 m/s 43.07 ft/sec  $4Vol/(80\pi D^2)$   
 Individual Chiller Volumetric Flow 173.87 cu.m/sec 368,400 ACFM  $\pi V_{exit} D^2/4$  Sect.2/¶1  
 Stack Potential Temp  $\theta_s$  313.32 Kelvins 104.3 °F  
 Initial Stack Buoyancy Flux  $F_o$  19.2457 m<sup>4</sup>/s<sup>3</sup> 20.0 ΔT(°F)  $gV_{exit} D^2(1-\theta_s/\theta_a)/4 = Vol.Flow(g/\pi)(1-\theta_s/\theta_a)$  Sect.2/¶1  
 Plume Buoyancy Flux F N/A m<sup>4</sup>/s<sup>3</sup>  $\lambda^2 g V a^2 (1-\theta_s/\theta_a)$  for a, V,  $\theta_s$  at plume height (see below)  
 Number of Towers n 9 1.732 Multiple Stack Multiplication Factor ( $n^{0.25}$ )

**Conditions at End (Top) of Jet Phase:**  
 Height above Stack  $z_{jet}$  25.664 meters\* 84.2 feet\*  $z_{jet} = 6.25D$ , meters\*=meters above stack top Sect.3/¶1  
 Height above Ground  $z_{jet}+h_s$  50.201 meters 164.7 feet  
 Vertical Velocity  $V_{jet}$  6.564 m/s 21.54 ft/sec  $V_{jet} = 0.5V_{exit} = V_{exit}/2$   
 Plume Top-Hat Diameter  $2a_{jet}$  8.213 meters 26.9 feet  $2a_{jet} = 2D$  Conservation of momentum

**Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet Phase**  
 Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:  
 Plume Top-Hat Radius a Solutions in Table Below 0.16(z-z<sub>v</sub>), or linear increase with height Sect.2/Eq.6  
 Virtual Source Height z<sub>v</sub> 4.459 meters\* 1.5 feet\*  $6.25D[1-(\theta_s/\theta_a)^{1/2}]$ , meters\*=meters above stack top Sect.2/Eq.6  
 Height above Ground z<sub>v</sub>+h<sub>s</sub> 24.995 meters 82.0 feet where  $(\theta_s/\theta_a)^{1/2} = (\theta_s/\theta_a)^{1/2} = 0.9821$   
 Vertical Velocity V Solutions in Table Below  $\{(Va)_o^3 + 0.12F_o [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / a$  Sect.2.1(6)  
 Product (Va)<sub>o</sub> 26.473 m<sup>2</sup>/s  $V_{exit} D/2(\theta_s/\theta_a)^{1/2}$

**Single Chiller Results:**  
 Solve for plume-averaged vertical velocity at height 500.0 feet 152.4 meters above ground (z'+h<sub>s</sub>)  
 Gives the following Height above Stack z' 127.864 meters\* 419.5 feet\*  
 Plume Top-Hat Diameter 2a' 40.769 meters 133.8 feet  $2a'=2*0.16(z'-z_v)$  Sect.2/Eq.6  
 Vertical Velocity V 1.861 m/s 6.10 ft/sec  $V=\{(Va)_o^3+0.12F_o[(z-z_v)^2-(6.25D-z_v)^2]^{1/3}\}/(2a'/2)$  Sect.2/Eq.6

**Solve for Height of CASC critical vertical velocity V<sub>crit</sub> 5.30 m/s plume-averaged vertical velocity Critical VV > Top of Jet (Spillane)**  
 Find Height above Stack z<sub>crit</sub> 32.116 meters 105.4 feet Solve for x=(z-z<sub>v</sub>) simultaneously in both eqs. (i.e., Va and a)  
 Height above Ground z<sub>crit</sub>+h<sub>s</sub> 56.653 meters 185.9 feet for V=V<sub>crit</sub> using the cubic equation ax<sup>3</sup>+bx<sup>2</sup>+cx+d=0, where  
 a=1, c=0, and b=(0.12F<sub>o</sub>)/(V<sub>crit</sub><sup>3</sup>0.16<sup>3</sup>)=-3.78727  
 and d=[0.12F<sub>o</sub>(6.25D-z<sub>v</sub>)<sup>2</sup>-(Va)<sub>o</sub><sup>3</sup>]/(V<sub>crit</sub><sup>3</sup>0.16<sup>3</sup>)=-28018.28  
<http://www.1728.org/cubic.htm>  
 Interpolated Height of critical vertical velocity in Jet Phase:  
 Find Height above Stack z<sub>crit</sub> #N/A meters #N/A feet  
 Height above Ground z<sub>crit</sub>+h<sub>s</sub> #N/A meters #N/A feet gives the real solution x = z-z<sub>v</sub> = 31.6574  
 or z(m/above stack) = 32.116  
 z(ft/above ground) = 185.9

**Table of Plume Top-Hat Diameters (2a) and Plume-Averaged Vertical Velocities starting at end of jet phase:**

Height (feet)	(meters)	Plume Radius(m)	SingleStk vertVel(m/s)	Plume Temp(K)
Stack Rel.Ht = 80.5	0.00	2.053	13.13	
100.0	5.94	2.529	11.61	
120.0	12.04	3.016	10.05	
140.0	18.14	3.504	8.49	
160.0	24.23	3.992	6.93	
160.0	24.23	3.992	6.93	
Top of Single jet = 164.7	25.66	4.106	6.56	
180.0	30.33	4.779	5.60	306.56
200.0	36.42	5.754	4.72	305.97
220.0	42.52	6.730	4.11	305.29
240.0	48.62	7.705	3.66	304.79
260.0	54.71	8.680	3.32	304.42
280.0	60.81	9.656	3.05	304.13
300.0	66.90	10.631	2.83	303.90
350.0	82.14	13.070	2.44	303.71
400.0	97.38	15.508	2.18	303.36
450.0	112.62	17.946	2.00	303.13
500.0	127.86	20.385	1.86	302.96
550.0	143.10	22.823	1.75	302.83
600.0	158.34	25.262	1.67	302.74
650.0	173.58	27.700	1.60	302.66
700.0	188.82	30.138	1.54	302.60
800.0	219.30	35.015	1.44	302.56
900.0	249.78	39.892	1.36	302.48
1000.0	280.26	44.769	1.30	302.43
1100.0	310.74	49.646	1.25	302.39
1200.0	341.22	54.522	1.21	302.37
1300.0	371.70	59.399	1.17	302.34
1400.0	402.18	64.276	1.14	302.33
1500.0	432.66	69.153	1.11	302.31
2000.0	585.06	93.537	1.00	302.30
2500.0	737.46	117.921	0.92	302.27
3000.0	889.86	142.305	0.86	302.25
3500.0	1042.26	166.689	0.82	302.24
4000.0	1194.66	191.073	0.78	302.23
4500.0	1347.06	215.457	0.75	302.23
5000.0	1499.46	239.841	0.72	302.22

**Jet Phase Eqs: 20 ft Intervals**  
 Linearly interpolated from Stack Rel.Ht to Top of Jet  
**Spillane Equations:**  
 $V_{plume} = \{(Va)_o^3 + 0.12F_o [(z-z_v)^2 - (6.25D-z_v)^2]^{1/3}\} / a$   
 $a = 0.16(z-z_v)$   
 $\theta_p = \theta_a (1 + (1 - (\theta_s/\theta_a)) * (V_{exit} D^2 / (4V_{plume} * a^2 * \lambda^2)))$   
**CEC Staff Equation:**  
 $V_{mp} = n^{0.25} V_{sp}$   
**Brigg's Equation:**  
 $V_{avg} = (2/3) * 1.6^{(0.2)} * F_{mp}^{(1/2)} * x^{(1/2)} * z^{(1/2)}$   
 where  $F_{mp} = nF_{sp}$

**50 ft Intervals**  
 Max<5.3 m/s

**100 ft Intervals**  
**500 ft Intervals**

\*Winter Min = Monthly Mean of Minimum Daily Temperatures for 1971-2000 (Lowest in December)  
 NOAA Sources: Climatography of the United



MERGED (along length) Plume Average Vertical Velocities for Northtown Chillers - Summer Max*				
"Aviation Safety and Buoyant Plumes," Peter Best, et. al.				
"The Evaluation of Maximum Updraft Speeds for Calm Conditions at Various Heights in the Merged Plume from Two Gas-Turbine Power Station at Oaky, Queensland, Australia," Dr. K.T. Spillane				
Ambient Conditions: Constants: Assume neutral conditions (dB/dz=0 or $\theta_a=\theta_a$ )				
Ambient Potential Temp $\theta_a$	302.21 Kelvins	84.3 °F		0.3048 meters/feet
Plume Exit Conditions:			Gravity g	9.81 m/s <sup>2</sup>
Stack Height $h_s$	24.54 meters	80 6/12 feet-inches	$\lambda$	1.11
Individual Stack Diameter D	4.10632 meters	161.7 inches	$\lambda_c$	-1.0
Stack Velocity $V_{exit}$	13.13 m/s	43.07 ft/sec	$4Vol/(60\pi D^2)$	
Individual Volumetric Flow	173.87 cu.m/sec	368,400 ACFM	$\pi V_{exit} D^2/4$	Sect.2/¶1
Stack Potential Temp $\theta_s$	313.32 Kelvins	104.3 °F		
Initial Stack Buoyancy Flux $F_b$	19.25 m <sup>4</sup> /s <sup>3</sup>	20.0 ΔT(°F)	$g_{exit} D^2 (1-\theta_s/\theta_a)/4 = Vol.Flow(g/m^3)(1-\theta_s/\theta_a)$	Sect.2/¶1
Plume Buoyancy Flux F	N/A m <sup>4</sup> /s <sup>3</sup>		$\lambda^2 g V_a^2 (1-\theta_p/\theta_a)$ for a, V, $\theta_p$ at plume height (see below)	
Total Number of Stacks n	9			
Average Adjacent Stack Separation d	3.57 meters	11.7 feet	Calcs based on multiple plume treatment in Peter Best Paper: plume velocities increased by N <sup>0.25</sup> at the height where plumes fully merged (interp. below ht, single merged stack above ht)	
Number of Stacks along Orientation n	9			
Conditions at End (Top) of Jet Phase:				
Height above Stack $z_{jet}$	25.664 meters*	84.2 feet*	$z_{jet} = 6.25D$ , meters*=meters above stack top	Sect.3/¶1
Height above Ground $z_{jet}+h_s$	50.201 meters	164.7 feet		"
Vertical Velocity $V_{jet}$	6.564 m/s	21.54 ft/sec	$V_{jet} = 0.5V_{exit} = V_{exit}/2$	"
Plume Top-Hat Diameter $2a_{jet}$	8.213 meters	26.9 feet	$2a_{jet} = 2D$	Conservation of momentum
Spillane Methodology - Analytical Solutions for Calm Conditions for Plume Heights above Jet and Merging Phases				
Single Plume-averaged Vertical Velocity V given by Analytical Solution in Paper where Product Va given by equations below:				
Single Plume Values:	Plume Top-Hat Radius a	Used in Plume Merging Only	$a = 0.16(z-z_v)$ , or linear increase with height	Sect.2/Eq.6
Virtual Source Height $z_v$	0.459 meters*	1.5 feet*	$z_v = 6.25D[1-(\theta_p/\theta_a)^{1/2}]$ , meters*=meters above stack top	Sect.2/Eq.6
Height above Ground $z_v+h_s$	24.995 meters	82.0 feet	where $(\theta_p/\theta_a)^{1/2} = (\theta_p/\theta_a)^{1/2} = 0.9821$	
Single Plume Values:	Vertical Velocity V	Used in Plume Merging Only	$[(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$	Sect.2.1(6)
Product (Va) <sub>0</sub>	26.473 m <sup>2</sup> /s		$V_{exit}(D/2)(\theta_p/\theta_a)^{1/2}$	
Plume Merging - Based on Single Plume Calculations where:				
Begin Merging Plume Top-Hat Diameter $2a_{touch}$	3.570 meters	11.7 feet	$2a_{touch}=d$ , (or $a_{touch}=d/2$ )	Sect.3/¶3
Height above Stack $z_{touch}$	11.615 meters*	38.1 feet*	$z_{touch} = z_v + d/(2*0.16)$ , meters*=meters above stack top	
Height above Ground $z_{touch}+h_s$	36.152 meters	118.6 feet		
Vertical Velocity $V_{touch}$	14.510 m/s	47.6 ft/sec	$V_{touch} = \{[(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$	
Total Merging Plume Top-Hat Diameter $2a_{full}$	28.560 meters	93.7 feet	$2a_{full}=2d(N-1)/2$ , (or $a_{full}=d(N-1)/2$ ) FOR 2 STACKS, $2a_{full}=2d$	
Height above Stack $z_{full}$	89.709 meters*	294.3 feet*	$z_{full} = z_v + 2d/(2*0.16)$ , meters*=meters above stack top	
Height above Ground $z_{full}+h_s$	114.245 meters	374.8 feet		
Vertical Velocity $V_{full}$	2.301 m/s	7.6 ft/sec	$V_{full} = \{[(Va)_0^3 + 0.12F_b [(z_{full}-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a_{full}$	
Product (V <sup>3</sup> a) <sub>full</sub>	174 m <sup>4</sup> /s <sup>3</sup>			
Conditions at End (Top) of Merging Phase - Define new values for $V_{full}$ and $a_{full}$ in Merged Plume calculations (based on TOTAL number of stacks):				
Merged Plume Values:	Plume Diameter $2a$	Solutions in Table Below	$2a = 2x(a_m + 0.16(z-z_{full}))$ , or linear increase with height	
Revised Merged Plume Radius $a_m$	24.734 meters	81.1 feet	where $a_m = n^{0.25} a_{full}$ where Total Merging Occurs	
Revised Merged Plume Velocity $V_m$	3.986 m/s	13.08 ft/sec	and $V_m = n^{0.25} V_{full}$ where Total Merging Occurs	
Revised Virtual Source Height $z_{full}$	89.709 meters*	294.3 feet*	Height above stack where Total Merging Occurs (shown above)	
Revised Vertical Velocity V		Solutions in Tables Below	$V = \{n(V^3 a_{full}/a)^{1/3}$ for heights above total merging elevation	
Multiple Plume Calculations				
Solve for plume-averaged vertical velocity at height	500.0 feet		for heights below total merging elevation	
Gives the following Height above Stack z	127.864 meters*	419.5 feet*	REGULAR EQNS	
Plume Top-Hat Radius a	30.838 meters	101.2 feet	$a = a_m + 0.16(z-z_{full})$ if $z > z_{full}$	
Vertical Velocity V	3.703 m/s	12.15 ft/sec	$V = \{n(V^3 a_{full}/a)^{1/3}$ if $z > z_{full}$	
			$V = V_{touch} + (V_m - V_{touch}) [(z - z_{touch}) / (z_{full} - z_{touch})]$ if $z_{touch} < z < z_{full}$	
			$V =$ single plume values if $z < z_{touch}$	
Solve for Height of CASC critical vertical velocity $V_{crit}$	5.30 m/s		LESS THAN TOP OF MERGING PHASE-INTERPO	
Find Height above Stack $z_{crit}$	79.956 meters	262.3 feet	$z_{crit} = z_{full} + \{[(nV^3 a_{full})(V_{crit})^3 - a_m]\} / 0.16$ if $V_{crit} < V_m$	
Height above Ground $z_{crit}+h_s$	104.492 meters	342.8 feet	$z_{crit} = z_{touch} + (z_{full} - z_{touch}) \{V_{crit} - V_{touch}\} / (V_m - V_{touch})$ if $V_{crit} > V_m$	
Table of MERGED Plume-Averaged Vertical Velocities starting at Touching Height:				
Height (feet)	(meters)	Plume	Vert.	Single Plume Eqns (see Single Plume spreadsheet)
above ground above stack	Radius(m)	Vel(m/s)		$V_{plume} = \{[(Va)_0^3 + 0.12F_b [(z-z_v)^2 - (6.25D-z_v)^2]]^{1/3} / a$
				$a = 0.16(z-z_v)$
Begin Merging (touch) = 118.6	11.61	1.785	14.51	$\theta_p = \theta_a [1 + (1 - (\theta_p/\theta_a)) (V_{exit} D^2 / (4V_{plume} a^2 \lambda^2))]$
125.0	13.56	#N/A	14.25	Interpolated Layer Eqns
150.0	21.18	#N/A	13.22	$V = V_{touch} + (V_m - V_{touch}) [(z - z_{touch}) / (z_{full} - z_{touch})]$
175.0	28.80	#N/A	12.19	
200.0	36.42	#N/A	11.17	
225.0	44.04	#N/A	10.14	
250.0	51.66	#N/A	9.11	
275.0	59.28	#N/A	8.09	
300.0	66.90	#N/A	7.06	
325.0	74.52	#N/A	6.03	$V = \{n(V^3 a_{full}/a)^{1/3}$
350.0	82.14	#N/A	5.01	$a = a_m + 0.16(z - z_{full})$
End Merging (full/mp) = 374.8	89.70	24.733	3.99	
400.0	97.38	25.962	3.92	
450.0	112.62	28.400	3.81	
500.0	127.86	30.838	3.70	
600.0	158.34	35.715	3.53	
700.0	188.82	40.592	3.38	
800.0	219.30	45.469	3.25	
900.0	249.78	50.346	3.14	
1000.0	280.26	55.222	3.05	
1100.0	310.74	60.099	2.96	
1200.0	341.22	64.976	2.89	
1300.0	371.70	69.853	2.82	
1500.0	432.66	79.606	2.70	
2000.0	585.06	103.990	2.47	
2500.0	737.46	128.374	2.30	
3000.0	889.86	152.758	2.17	
3500.0	1042.26	177.142	2.07	
4000.0	1194.66	201.526	1.98	
4500.0	1347.06	225.910	1.91	

